



Mark Dangler  
Vice President, Logistics

IES Downstream, LLC  
91-480 Malakole Street  
Kapolei, HI 96707  
Tel 808 682 2299  
Fax 808 682 2214  
[MDangler@IslandEnergyServices.com](mailto:MDangler@IslandEnergyServices.com)

18 FEB 11 2021

POSTMARK

FEB - 9 2021

February 8, 2021

**CERTIFIED MAIL No. 7015 0640 0002 5911 5886  
RETURN RECEIPT REQUESTED**

Ms. Marianne Rossio  
Manager  
Clean Air Branch  
2827 Waimano Home Road #130  
Pearl City, Hawaii 96782

**IES Downstream, LLC  
CSP 0863-01-C and 0863-02-C  
GHG Emission Reduction Plan Rev 2**

Dear Ms. Rossio:

IES Downstream, LLC (IES) is hereby submitting its updated Greenhouse Gas Emission Reduction Plan (GHGERP) Rev 2 for its equipment located at 91-480 Malakole Street, Kapolei, Hawaii as further described below. This plan is being submitted to meet the requirements of §11-60.1-204(a) and revises the GHGERP that was submitted by Chevron on June 30, 2015.

IES transferred certain Kapolei Refinery operating units to Par Refining Hawaii, Inc. (Par) on December 19, 2018 at 11:59 pm; Par now operates the transferred refining units under CSP Nos. 0088-01-C, 0088-02-C and 0088-03-C. CSP 0088-01-C was amended to separate certain assets retained by IES and these assets' permitting obligations were addressed in a new permit for IES: CSP 0863-01-C. However, CSP 0863-01-C did not include process units that were being retained by IES (FCCU, part of Alky, and Dimersol) and further modification was recently completed to Par's CSP 0088-01-C to remove these IES retained process units that were omitted from the initial CSP 0863-01-C application. The permit CSP 0863-02-C for these process units was issued on December 18, 2020.

The transaction described above required a modification to the IES GHG Emission Reduction Plan. The original plan proposed 2009 as the baseline year and this update splits the baseline GHG emissions between both IES and Par in alignment with equipment ownership relative to CSP 0088-01-C, 0088-02-C, and 0088-03-C for Par and CSP 0863-01-C and 0863-02-C for IES. IES' new baseline will include the emissions for CSP 0863-01-C and CSP 0863-02-C. This update (Rev 2) to the Rev 1 GHG Emission Reduction Plan issued in August 2019 is intended to provide additional clarification to the baseline year calculations and also the equipment split between IES and Par West. It also reflects the most recent change in equipment ownership between IES and Par West related to Par's acquisition of Boilers 1,2, & 3 in January 2021, transferring the baseline emissions from Boilers 1,2,& 3 to Par West's GHG Baseline.

Manager  
HDOH Clean Air Branch  
February 8, 2021

Should you have any questions or require further information, please contact Gail Godenzi, Environmental and Process Engineer, at (808) 682-3113.

I certify as the company official having supervisory responsibility for the persons who prepared this document that this information is true, accurate, and complete to the best of my knowledge, information and belief.

Sincerely,



Mark Dangler

gng

Attachments and CD w/Attachments

FEB 11 2021

POSTMAF

FEB - 9 2021



## Greenhouse Gas Emission Reduction Plan

**IES Downstream, LLC  
91-480 Malakole Street  
Kapolei, HI 96707**

**Covered Source Permit Nos. 0863-01-C  
and  
0863-02-C**

**January 2021**

## Table of Contents

<b>1.0</b>	<b>INTRODUCTION .....</b>	<b>1</b>
<b>2.0</b>	<b>REQUEST FOR ALTERNATE BASELINE ANNUAL EMISSION YEAR.....</b>	<b>1</b>
<b>2.1</b>	<b>PROPOSED ALTERNATE BASELINE YEAR.....</b>	<b>1</b>
<b>2.2</b>	<b>JUSTIFICATION .....</b>	<b>2</b>
2.2.1	Unit Downtime .....	2
2.2.2	Refinery Utilization .....	3
2.2.3	Procedures for Determining Alternative Baseline Year .....	3
2.2.4	Baseline Year Determination Conclusion .....	5
2.2.5	Additional documentation requested.....	6
2.2.6	Conclusion .....	7
<b>2.3</b>	<b>BASELINE EMISSION SPLIT .....</b>	<b>7</b>
<b>3.0</b>	<b>2020 DIRECT GHG EMISSIONS CAP – IES DOWNSTREAM, LLC .....</b>	<b>12</b>
<b>4.0</b>	<b>GHG CONTROL ASSESSMENT.....</b>	<b>12</b>
<b>5.0</b>	<b>PROPOSED CONTROL STRATEGY.....</b>	<b>12</b>
<b>6.0</b>	<b>PARTNERING CSP 0863-01-C AND CSP 0863-02-C.....</b>	<b>13</b>

## TABLES

- 1 – GHG Annual Emission Summary
- 2 – Normal Operation Analyses Summary
- 3 – Baseline Emission Split
- 4 – Split of Permitted Equipment in 2009 Proposed Baseline Year Emissions
- 5 – Post-transfer Split of Permitted Equipment as of January 2021
- 6 – Individual and Combined CO<sub>2</sub>e Baseline and Caps

## APPENDICES

- A – October 28, 2016 Chevron Response in Request for Additional Information
- B – August 31, 2018 IES Response to DOH Email dated July 24, 2018
- C – CAB Letter dated July 22, 2019 – Request clarification to Baseline Yr Calculations
- D – IES Email sent on March 25, 2019 in response to 2/7/2019 Meeting

## **GHG EMISSION REDUCTION PLAN REV 2**

**IES DOWNSTREAM, LLC**

**JANUARY 2021**



### **1.0 Introduction**

---

A Greenhouse Gas ("GHG") Emission Reduction Plan ("the GHG Plan" or "the Plan") was submitted by Chevron on June 30, 2015 for the Hawaii Refinery to comply with requirements of the Hawaii Greenhouse Gas Emissions law<sup>1</sup> (the Act) and implement regulations of the Hawaii Department of Health ("DOH").<sup>2</sup> On November 1, 2016, IES Downstream, LLC ("IES") acquired the Hawaii Refinery and assumed responsibility of the GHG Plan. The GHG rule<sup>3</sup> sets forth the regulatory program for meeting the statutory statewide GHG limit that is equal to or below the 1990 statewide GHG emission levels for each facility that emits more than 100,000 tons per year of GHG emissions. The GHG rule generally requires each regulated source to propose a GHG Plan that would cap the source's direct GHG emissions to 16% of that source's 2010 direct GHG emissions. In meeting the GHG limit, the regulation provides flexibility to the Director of the Department of Health, Clean Air Branch ("Director" or "CAB") to set the facility-wide GHG emissions cap for an individual source by varying from the established regulatory structure in two ways: 1) by granting a request to use an alternate emission baseline; and 2) establishing an alternate GHG emission cap based on a finding that the presumptively required 16% reduction is not attainable.

The GHG rule is premised on an assumption that the GHG covered sources reducing their direct GHG levels by 16% from 2010 emission levels will be adequate to return the State of Hawaii to 1990 GHG levels. Although the ultimate goal of the Act is to reduce statewide GHG emissions to 1990 emission levels, the Kapolei Refinery has actually achieved reductions in GHG emissions to less than its estimated 1990 levels and, as a prudent operator, continues to seek these as part of our business. Unlike other sources of GHGs within the state and the selected industries subject to the current GHG rule that have seen growth, and thus increases in GHG emissions since 1990, the Kapolei Refinery has not experienced sustained increases in capacity and have decreased GHG emissions over this same period of time.

This updated GHG Plan is being submitted by IES to meet the requirements of §11-60.1-204(a). The IES Downstream, LLC – Kapolei Terminal and Kapolei Process Units, formerly known as the IES Kapolei Refinery ("Kapolei Refinery"), and further formerly known as the Chevron Hawaii Refinery, is located within the Campbell Industrial Park at 91-480 Malakole Street, Kapolei, Hawaii. The facility currently operates under two Covered Source Permits (CSP) Nos. 0863-01-C (Terminal), and 0863-02-C (Process Units) issued by the Hawaii Department of Health.

The Kapolei Refinery began operation in 1960 with capacity of processing up to 58,000 barrels of crude oil per day. The Kapolei Refinery did not operate at this rated capacity in recent history but rather set its operations based on market demands. The facility consisted of numerous

---

<sup>1</sup> HRS §§ 342B *et seq.*, enacted by Act 234, 2007 Hawaii Session Laws.

<sup>2</sup> HAR § 11-60.1-204, "Greenhouse gas emission reduction plan." Hereinafter, the "GHG rule."

<sup>3</sup> HAR §11-60.1-201, Purpose.

## **GHG EMISSION REDUCTION PLAN REV 2**

**IES DOWNSTREAM, LLC**

**JANUARY 2021**



operational units, including crude vacuum and distillation units, fluid catalytic cracker, dimersol, hydrogen manufacturing, alkylation, and isomerization units. The Kapolei Refinery operated utilities including boilers, cogeneration units, effluent treatment plant, and tank fields for storage, blending, and shipping capability in support of its operations.

IES transferred certain Kapolei Refinery operating units to Par Refining Hawaii, Inc. (Par) on December 19, 2018 at 11:59 pm; Par ("Par West") now operates the transferred refining units under CSP Nos. 0088-01-C, 0088-02-C and 0088-03-C. CSP 0088-01-C was initially amended to separate certain assets retained by IES and these assets' permitting obligations were addressed in a new permit for IES: CSP 0863-01-C. However, CSP 0863-01-C did not include refining units that were being retained by IES (FCCU, part of Alky, and Dimersol) and further modification was recently completed to amend CSP 0088-01-C to remove these IES retained process units that were omitted from the initial CSP 0863-01-C application. The permit CSP 0863-02-C for these process units was issued on December 18, 2020.

The transaction described above requires a modification to the IES GHG Emission Reduction Plan. The original plan proposed 2009 as the baseline year and this update splits the baseline GHG emissions between both IES and Par West in alignment with equipment/permit ownership, CSP 0088-01-C, 0088-02-C, and 0088-03-C for Par and CSP 0863-01-C and 0863-02-C for IES. IES' new baseline will include the emissions for CSP 0863-01-C and CSP 0863-02-C. This update (Rev 2) to the Rev 1 GHG Emission Reduction Plan issued in August 2019 is intended to provide additional clarification to the baseline year calculations and also the equipment split between IES and Par West. It also reflects the most recent change in equipment ownership between IES and Par West related to Par's acquisition of Boilers 1,2, & 3 in January 2021, transferring the baseline emissions from Boilers 1,2,& 3 to Par West's GHG Baseline.

This plan consists of 6 sections. Section 2 presents the proposed baseline emissions year for the Kapolei Refinery and splits the baseline emissions between Par owned facility (hereinafter referred to as the "Par West") and the IES Terminal and IES Process Units (hereinafter referred to as the "IES Facility"). Section 3, discusses the proposed IES Facility 2020 facility-wide direct GHG Emissions cap. Section 4 discusses the IES Facility GHG Control Assessment, Section 5 discusses the IES Facility Proposed Control Strategy, and Section 6 discusses Partnering the IES Terminal and IES Process Units. Appendices of this plan contain past submittals to DOH CAB with detailed calculations and analysis supporting the baseline selection.

## **2.0 Request for Alternate Baseline Annual Emission Year**

---

Section 11-60.1-204(d)(1) generally requires regulated sources to use 2010 to compute the GHG baseline emissions. This paragraph, however, also allows an owner or operator to propose an alternate GHG emission baseline and includes several potential methodologies to support computation of an acceptable alternative. These alternatives allow an owner or operator to use emissions from the years 2006-2010 in various formulations, if the owner or operator documents that 2010 is "not representative of normal source operations."

### **2.1 PROPOSED ALTERNATE BASELINE YEAR**

Per §11-60.1-204(d)(1)(A)(i), the GHG Plan submitted on June 30, 2015, requested that the Director approve an alternative baseline year of 2009 based on the criteria that it is the most representative year during the five-year period between 2006 and 2010 calendar years. Direct GHG emission estimates for the proposed 2009 baseline year are 577,945 metric tons (tonnes) per year of carbon dioxide equivalent (CO<sub>2</sub>e). Table 1. GHG Annual Emission Summary indicates the direct GHG emissions estimated for the 1990 calendar year as well as the calculated 2009 and 2010 calendar years. The 1990, 2009, and 2010 calendar years were calculated using the methodologies as required by the GHG Reporting Rule in 40 CFR Part 98; however, estimates were used for some operational data that was unavailable for the 1990 calendar year.

**Table 1. GHG Annual Emission Summary**

Calendar Year	Direct emissions reported per year of CO <sub>2</sub> e
1990 (est)	613,900 MT (676,709 T)
2009 (Baseline year)	577,945 MT (637,075 T)
2010	529,651 MT (583,840 T)

To provide context for the Refinery's request to use alternative baseline year, the table above also shows that the refinery had already taken significant measures to reduce energy consumption and CO<sub>2</sub>e emissions well below the levels that had been established back in 1990, which was the stated purpose of both the Act and the GHG regulation.

## **2.2 JUSTIFICATION**

Follow up documentation to support the selection of 2009 as the baseline year was requested by DOH CAB on February 10, 2016 resulting in two response letters submitted by Chevron on October 28, 2016, one with Confidential Business Information (CBI) and the other with non-CBI information. The CBI letter explained the criteria used for determining normal source operations in which process unit shutdown periods and utilization-related data were analyzed to determine the most representative year during the five-year period ending in 2010. They presented three alternatives for consideration to be used as the baseline with 2009 emissions as the most recent representative year. The non-confidential content of the CBI response is summarized in section 2.2.1 through 2.2.4. The non-CBI letter provided additional data and information about GHG emission calculations for the 2006-2010 calendar years and is summarized in section 2.3 and Appendix A.

### **2.2.1 Unit Downtime**

Kapolei Refinery GHG emissions occur from the processing of crude oil to produce high value products that are distributed in commerce for fuels. GHG emissions<sup>2</sup> from normal operations are generated from the following sources:

1. Combustion of fuels supplying heat to the Kapolei Refinery processes (account for approximately 60% of total GHG emissions from the Kapolei Refinery)
2. Coke combustion in the Fluid Catalytic Cracking (FCC) Unit (account for approximately 35% of total GHG emissions from the Kapolei Refinery)
3. Hydrogen Plant
4. Crude Storage
5. Fugitives (piping)
6. (Emissions from) Flaring Events
7. Acid Gas Production (<5% of total GHG emissions from the Kapolei Refinery).

Normal source operations are characterized by crude and process unit throughputs (utilization) and continuous operation that allow the Kapolei Refinery to meet the fuel market demands.

Factors that can impact normal operations include:

1. Unit downtime, whether planned or unplanned, including crude supply interruptions and turnaround years;
2. External factors that reduce utilization, including widespread economic downturns impacting fuel market demands;
3. Periods of malfunction resulting in excess emissions, including force majeure events.

At the Kapolei Refinery, planned maintenance is required for each unit. Short-term shutdowns to service equipment in each process unit occur regularly during the year and typically only last hours. Approximately every five years the units have scheduled long-term shutdowns that can last weeks or months, which all occur in a "turnaround (TA) year". A TA year differs on average

12% of CO<sub>2</sub>e GHG emissions from the year before it and can vary up to 19%. TA years are not considered representative of normal operation due to this impact.

## **2.2.2 Refinery Utilization**

A second quantitative marker of “normal source operations” is refinery utilization. Utilization can be described in several ways including crude throughput, process unit feed rates, product output, and Complexity Weighted Barrels (CWB) throughput.

Throughput is typically measured in barrels or barrels per day. For benchmarking comparison of multiple facilities in the refining industry, California Air Resources Board has standardized on Complexity Weighted Barrels, CWB, as a refinery’s throughput measurement in their Regulation for the Mandatory Reporting of Greenhouse Emissions.<sup>4</sup>

In determining the CWB throughput, the actual crude and individual process unit throughputs, in barrels, are weighted by factors that equalize the number and complexity differences in process units found at different facilities. For the same crude throughput, a refinery with more processing will have a higher CWB.

CWB is correlated with GHG emissions, because more processing generally leads to higher GHG emissions. Thus, CWB is a throughput measurement normalized for the complexity of the Kapolei Refinery that is a reasonable metric for discussing GHG emissions.

## **2.2.3 Procedures for Determining Alternative Baseline Year**

### **2.2.3.1 HAR §11-60.1-204 (d)(1)(A)(i)**

HAR §11-60.1-204 (d)(1)(A)(i) allows a facility to determine alternative facility-wide GHG emissions (less biogenic CO<sub>2</sub>) based on the most recent representative year during the five-year period ending 2010. The Kapolei Refinery considers representative operation to be periods with (1) no significant process unit shutdowns and (2) a CWB throughput that reflects normal fuel markets and falls within the normal operating window.

No significant process unit shutdowns are a measure of normal operation because during extended periods of shutdown or shutdowns of the large process units such as the Crude Unit or the Fluid Catalytic Cracker, the emissions are low to zero, and do not represent emissions when the units are operating. Refinery CWB throughput is determined by the fuel markets that the Kapolei Refinery supplies and relates to Actual GHG emissions because firing rates of Kapolei Refinery heaters and boilers are determined by the feed to the process units.

#### 2009

The 2009 calendar year meets the criteria of normal operation, as no significant shutdowns occurred and Kapolei Refinery CWB throughput was within the normal range.

---

<sup>4</sup> Title 17, California Code of Regulations, Section 95100 et seq., (MRR)

**GHG EMISSION REDUCTION PLAN REV 2****IES DOWNSTREAM, LLC****JANUARY 2021****2008**

2008 was a turnaround year, in which the Kapolei Refinery executed a planned refinery-wide shutdown that lasted 31 days (8% of the year) at the Crude Unit and 41 days (11% of the year) for the FCCU. The CWB throughput for the year was significantly impacted by this downtime. The combined influence of these two criteria makes the 2008 calendar year non-representative of normal operation.

**2007**

The 2007 calendar year meets the criteria of normal operation, as no significant shutdowns occurred and Kapolei Refinery CWB throughput was within the normal range.

**2006**

In calendar year 2006, two external events occurred that resulted in significant unit downtime and had impact on the Kapolei Refinery CWB throughput. On February 21, 2006, a refinery-wide shutdown unexpectedly occurred as a result of an island-wide power outage. The FCC downtime was extended in order to internally inspect equipment. On October 15, 2006, a second refinery-wide shutdown occurred as a result of an island-wide power outage following an earthquake off the island of Hawaii. These two events resulted in 30 days of FCC downtime, or 8% of the year. It also resulted in a 1% overall downtime for the Crude Unit. This significant downtime also lowered the Kapolei Refinery CWB. The combined influence of these two events makes the 2006 calendar year non-representative of normal operation.

Table 2. below summarizes the evaluation of the 2006-2010 calendar years.

**Table 2. Normal Operation Analyses Summary**

Year	Direct Actual GHG Emissions	Kapolei Refinery Operation Impacted by Shutdowns	Kapolei Refinery Throughput	Representative Year?
2010	529,651 MT (583,840 T)	Kapolei Refinery Actual GHG emissions reduced due to an unplanned FCC shutdown	Kapolei Refinery Actual GHG emissions reduced due to lower refinery throughput	No
2009	577,945 MT (637,075 T)	No impact	No impact	Yes
2008	522,593 MT (576,060 T)	Planned Kapolei Refinery turnaround (TA)	Not estimated due to impact from TA	No
2007	569,048 MT (627,268 T)	No impact	No impact	Yes
2006	536,124 MT (590,976 T)	Kapolei Refinery Actual GHG	No impact	No

## **GHG EMISSION REDUCTION PLAN REV 2**

**IES DOWNSTREAM, LLC**

**JANUARY 2021**



		emissions reduced due to an unplanned refinery-wide shutdown		
--	--	--	--	--

### **2.2.3.2 HAR §11-60.1-204 (d)(1)(A)(ii)**

The next method allowed by HAR §11-60.1-204 (d)(1)(A)(ii) is to average facility-wide Actual GHG emissions (less biogenic CO<sub>2</sub>) over any consecutive two-year period during the five-year period ending in 2010. As described in the previous section, there are no representative consecutive two-year periods; therefore, this method is not feasible.

However, averaging the two years with Actual GHG emissions representative of normal operation, 2009 and 2007, does reflect emissions that could be considered representative. The average Actual GHG emissions for 2007 and 2009 are 573,496 tonnes CO<sub>2</sub>e.

### **2.2.3.3 HAR §11-60.1-204 (d)(1)(A)(iii)**

The third method allowed by HAR §11-60.1-204 (d)(1)(A)(iii) is to average facility-wide GHG emissions (less biogenic CO<sub>2</sub>) for the five-year period ending in 2010. As described in the previous section, the five-year period ending in 2010 includes three years that are not representative of normal operation for GHG emissions; therefore, this method is not feasible.

### **2.2.3.4 HAR §11-60.1-204 (d)(1)(A)(iv)**

The fourth method allowed by HAR §11-60.1-204 (d)(1)(A)(iv) is to utilize comparable methods as approved by the director. As noted in the regulation, the director will not consider the use of periods greater than five years from 2010, except for extreme cases such as where an affected source may not have been fully operational for an extended period of time.

A comparable method for determining an alternative baseline year, is to adjust the actual emissions of a non-representative year to reflect expected emissions from restored operation. Chevron adjusted the 2010 calendar year emissions to include the GHG emissions for the FCC shutdown days and unrealized refinery throughput (adjusted to mean CWB value). Data showed that 2010 GHG CO<sub>2</sub>e emissions would have been at most 2.5% greater than years 2007 and 2009 emissions and 2010 CWB varied from 2% and 4% of years 2007 and 2009 throughput which had throughput within normal the range.

## **2.2.4 Baseline Year Determination Conclusion**

Following HAR §11-60.1-204 (d)(1)(A)(i-iv), the procedures set forth to evaluate alternative baseline year emissions, the Kapolei Refinery has determined the following:

## **GHG EMISSION REDUCTION PLAN REV 2**

**IES DOWNSTREAM, LLC**

**JANUARY 2021**



1. Calendar year 2009 Actual GHG emissions are the most recent representative of normal operations. These emissions are 577,945 tonnes CO<sub>2</sub>e per year.
2. The average of Actual GHG emissions for calendar years 2009 and 2007 is the second most representative baseline emissions. These emissions are 573,497 tonnes CO<sub>2</sub>e per year.
3. The adjusted 2010 calendar year Actual GHG emissions estimated to remove the impacts of downtime and lost CWB throughput could be considered feasible and is the third most representative baseline emissions. These emissions are ~0.3% greater than 2009 emissions.

### **2.2.5 Additional documentation requested**

In meetings with DOH, Chevron shared that calculations of GHG emissions had been performed in 3 different tools from 2006-2015. SANGEA (2006-2009); CGERS (2010-2014); ESS (2015). In the non-CBI letter submitted on October 28, 2016, Chevron reviewed the different calculation methodologies used for Kapolei Refinery GHG emissions from 2006 to 2010. They also used the input data from those years and recalculated emissions using current GHG calculation methods in a demonstration workbook. Emissions differed from between 1% to 7-10% due to differences in averaging and summing data, changes in GWP conversion factors for CO<sub>2</sub>e, changes in emission factors for fuel combustion, and a difference in FCC Unit coke combustion methodology in 2006-2007. Appendix A contains a copy of the non-CBI letter with details on the methodology and calculations in the demonstration workbook.

A follow up email from DOH was sent to IES on April 4, 2018, in response to the non-CBI letter from Chevron. The email identified items of interest related to the calculation of the proposed GHG Plan baseline and SLEIS reporting, where DOH used SLEIS data to validate the GHG emissions calculations provided by Chevron for calendar years 2006 to 2010. Of interest to HDOH were calculation differences between the FCC CO<sub>2</sub> emission calculations and differences between fuel throughputs, higher heating values (HHV) and annual heats associated with fuel oil, fuel gas, and whole straight run combustion for the proposed 2009 baseline year. IES concluded that these differences were attributed to differences in averaging and summing data, data gathering methods, and the use of the default Natural Gas HHV for fuel gas calculations. IES provided a written emailed response along with a copy their 2016 and 2017 GHG calculation worksheets and fuel oil, fuel gas, and whole straight run analysis worksheets in an email to DOH on August 31, 2018. The emailed response sent to DOH is included in Appendix B.

After careful review of all the data, the January 2021 Rev 2 GHG Emission Reduction Plan proposes to use the most conservative approach to the numbers for the baseline year request.

## 2.2.6 Conclusion

Based on detailed reviews of historical operation, 2006-2010 GHG input data, and computational comparisons with SLEIS data done in cooperation with DOH CAB, 2009 is the most recent representative year for the Kapolei Refinery facility-wide baseline annual emission rate during the five-year period ending 2010 with emissions of 577,945 tonnes of CO<sub>2</sub>e per year.

## 2.3 BASELINE EMISSION SPLIT

IES proposes to split the Kapolei Refinery 2009 baseline emissions, which contain equipment transferred to Par in CSP 0088-01-C, in alignment with IES Terminal (CSP 0863-01-C) and IES Terminal (CSP 0863-02-C). The breakdown of emissions is listed in Table 3.

**Table 3. Baseline Emission Split**

Permit Number	Baseline Year	Jan-21		Jan-21	
		Par West Refinery	IES Terminal + Process Units	IES Terminal	IES Process Units
		0088-01-C	0863-01-C and 0863-02-C	0863-01-C	0863-02-C
Subpart C	Fuel Oil Combustion	193,346			
	Fuel Gas Combustion	100,767	3,223		3,223
	WSR Combustion	44,986			
	Total Subpart C	339,099	3,223		3,223
Subpart P	Hydrogen Mfg	7,247	-		-
Subpart Y	FCC Coke Combustion	-	226,349		226,349
	Flare P1	1,017	-		-
	Flare P2 (Crude/Sweet)	117	-		-
	Acid Plant	485	-		-
	Fugitive Venting (Columns)	308	55		55
	Loading Vent (Crude Receipts)	-	45	45	
	Total Subpart Y	1,927	226,449	45	226,404
Totals		348,273	229,672	45	229,627
		<b>577,945</b>		<b>229,672</b>	

The permitted equipment in the 2009 Baseline Emission between Par West Refinery and IES Terminal & IES Process Units as shown in Table 4.

**Table 4. Split of Permitted Equipment in 2009 Proposed Baseline Year Emissions**

<b>2009</b>		
<b>CSP 0088-01-C (unless noted)</b>		
<b>Subpart C</b>	<b>Refinery</b>	<b>Terminal</b>
	<b>Fuel Oil Combustion</b>	<b>Fuel Oil Combustion</b>
	F-5103 - Crude Atm Furnace	
	F-5153 - Crude Vac Furnace	
	F-5201 - Boiler	
	F-5202 - Boiler	
	F-5203 - Boiler	
	<b>Fuel Gas Combustion</b>	<b>Fuel Gas Combustion</b>
	F-5103 - Crude Atm Furnace	F-5300 - FCC Furnace
	F-5153 - Crude Vac Furnace	F-5310 - FCC Startup Air Heater
	F-5700 - Hydrogen Furnace	
	F-5930 - Isomerization Furnace	
	F-5950 - Isomerization Furnace	
	F-5600 - Hydrogenation Furnace	
	F-6200 - Acid Plant Combustion Chamber	
	F-6260 - Acid Plant Pre-heater	
	F-6701 - Cogen	
	F-6702 - Cogen	
	F-6703 - Cogen	
	F-6704 - Cogen (CSP 0088-02-C)	
	F-5201 - Boiler	
	F-5202 - Boiler	
	F-5203 - Boiler	
	<b>WSR Combustion</b>	<b>WSR Combustion</b>

**GHG EMISSION REDUCTION PLAN REV 2**

IES DOWNSTREAM, LLC

JANUARY 2021



	TG-6701 - Cogen	
	TG-6702 - Cogen	
	TG-6703 - Cogen	
	TG-6704 - Cogen (CSP 0088-02-C)	
<b>Subpart P</b>	Hydrogen Mfg Plant	
<b>Subpart Y</b>		FCC Coke Combustion
	Flare P1	
	Flare P2 (Crude/Sweet)	
	Acid Plant	
	<b>Fugitive Venting (Columns)</b>	<b>Fugitive Venting (Columns)</b>
	C-5100 - Crude Unit	C-6660 - Dimersol Unit
	C-5150 - Crude Unit	C-5850 - Alkylation Unit
	C-5170 - Crude Unit	C-5860 - Alkylation Unit
	C-5830 - Alkylation Unit	C-5330 - FCC Unit
	C-5840 - Alkylation Unit	C-5340 - FCC Unit
	C-5940 - Isomerization Unit	C-5350 - FCC Unit
	C-6101 - Amine/Acid Unit	C-5405 - FCC Unit
		C-5400 - FCC Unit
		C-5410 - FCC Unit
		C-5420 - FCC Unit
		C-5450 - FCC Unit
		Loading Vent (Crude Receipts)

**GHG EMISSION REDUCTION PLAN REV 2**  
**IES DOWNSTREAM, LLC**  
**JANUARY 2021**



The post-transfer split of currently permitted equipment in Par Refinery CSP Nos. 0088-01-C, and IES Terminal CSP No. 0863-01-C and CSP No. 0863-02-C are shown in Table 5.

**Table 5. Post-transfer Split of Permitted Equipment as of January 2021**

<b>2021</b>			
	<b>CSP 0088-01-C (unless noted)</b>	<b>CSP 0863-01-C</b>	<b>CSP 0863-02-C</b>
<b>Subpart C</b>	<b>Par West Refinery</b>	<b>IES Terminal</b>	<b>IES Process Units</b>
	Fuel Oil Combustion	Fuel Oil Combustion	Fuel Oil Combustion
	F-5103 - Crude Atm Furnace		
	F-5153 - Crude Vac Furnace		
	F-5201 - Boiler		
	F-5202 - Boiler		
	F-5203 - Boiler		
	<b>Fuel Gas Combustion</b>	<b>Fuel Gas Combustion</b>	<b>Fuel Gas Combustion</b>
	F-5103 - Crude Atm Furnace		F-5300 - FCC Furnace
	F-5153 - Crude Vac Furnace		F-5310 - FCC Startup Air Heater
	F-5700 - Hydrogen Furnace		
	F-5930 - Isomerization Furnace		
	F-5950 - Isomerization Furnace		
	F-5600 - Hydrogenation Furnace		
	F-6200 - Acid Plant CC		
	F-6260 - Acid Plant Pre-heater		
	F-6701 - Cogen		
	F-6702 - Cogen		
	F-6703 - Cogen		
	F-6704 - Cogen (CSP 0088-02-C)		
	F-5201 - Boiler		
	F-5202 - Boiler		
	F-5203 - Boiler		
	<b>WSR Combustion</b>	<b>WSR Combustion</b>	<b>WSR Combustion</b>
	TG-6701 - Cogen		
	TG-6702 - Cogen		
	TG-6703 - Cogen		

**GHG EMISSION REDUCTION PLAN REV 2**
**IES DOWNSTREAM, LLC**
**JANUARY 2021**


	TG-6704 - Cogen (CSP 0088-02-C)		
	<b>Diesel</b>		
	F-5205 – Boiler (CSP 0088-02-C)		
	F-5206 – Boiler (CSP 0088-02-C)		
	Black Start Generator (CSP 0088-03-C)		
	RICE-110 (CSP 0088-03-C)		
	Rice-1233 (CSP 0088-03-C)		
	RICE-1522 (CSP 0088-03-C)		
	<b>CatOx</b>		
	Catalytic Oxidizer		
<b>Subpart P</b>	Hydrogen Mfg Plant		
<b>Subpart Y</b>			FCC Coke Combustion
	Flare P1		
	Flare P2 (Crude/Sweet)		
	Acid Plant		
	Fugitive Venting (Columns)		Fugitive Venting (Columns)
	C-5100 - Crude Unit		C-6660 - Dimersol Unit
	C-5150 - Crude Unit		C-5850 - Alkylation Unit
	C-5170 - Crude Unit		C-5860 - Alkylation Unit
	C-5830 - Alkylation Unit		C-5330 - FCC Unit
	C-5840 - Alkylation Unit		C-5340 - FCC Unit
	C-5940 - Isomerization Unit		C-5350 - FCC Unit
	C-6101 - Amine/Acid Unit		C-5405 - FCC Unit
			C-5400 - FCC Unit
			C-5410 - FCC Unit
			C-5420 - FCC Unit
			C-5450 - FCC Unit
		Loading Vent (Crude Receipts)	

### **3.0 2020 Direct GHG Emissions Cap – IES Downstream, LLC**

---

Per §11-60.1-204(d)(2), the regulation requires a 16% reduction from the proposed IES Terminal and Process units 2009 baseline year emission split of 229,672 tonnes per year CO<sub>2</sub>e. This equates to a reduction of 36,748 total tonnes per year of CO<sub>2</sub>e and a combined emissions cap of 192,924 tonnes per year CO<sub>2</sub>e.

IES proposes a cap of **192,924 tonnes (212,660 T)** per year CO<sub>2</sub>e for its combined operations under CSP 0863-01-C and 0863-02-C operating permits to meet the State's 16% emission reduction requirement. IES is requesting to partner the two facilities into one combine facility-wide GHG emission caps. See section 6.0.

### **4.0 GHG Control Assessment**

---

Per §11-60.1-204(d)(2), the GHG rule requires each affected source to conduct a GHG control assessment. IES has reviewed the available control measures identified in §11-60.1-204(d)(3), and developed a control strategy based on the available control measures but, have not included it in the updated GHG plan because IES can attain a 16% reduction in emissions.

### **5.0 Proposed Control Strategy**

---

Per §11-60.1-204(d), the regulation requires each affected source to propose a control strategy to include a listing of identified control measures that can be implemented in order to meet the required or proposed alternate 2020 facility-wide GHG emissions cap. IES has conducted a GHG control assessment of these control measures. IES control strategy is as follows:

#### **§11-60.1-204(d)(3)**

(E) Restrictive Operation: Process Unit Turndown: Reduce output from certain process units

The above Control strategy of Unit Turndown of the Process units (CSP 0863-02-C) will allow for a 16% reduction from the proposed combined facility 2009 baseline year and has been deemed technically feasible. This equates to a reduction of **36,748 tonnes per year CO<sub>2</sub>e** and an emissions cap of **192,924 tonnes per year CO<sub>2</sub>e**.

## 6.0 Partnering of CSP 0863-01-C and CSP 0863-02-C

---

Pursuant to the provisions of the GHG Rule §11-60.1-204(d)(6)(A), the regulation allows facilities to propose to combine their facility-wide GHG emission caps to leverage emission reductions among partnering facilities in meeting the combined GHG emission caps. IES plans to partner the IES Terminal facilities and IES Process Units to achieve the State's GHG emission reduction target. The combined emissions cap will be made part of the permit for each partnering facility in accordance with HAR §11-60.1-204(d)(6)(C).

Table 6. Reflects the individual facility and combined partnering baseline and annual GHG emissions limits.

**Table 6. Individual and Combined CO<sub>2</sub>e Baseline and Caps**

	IES Terminal	IES Process Units
	0863-01-C	0863-02-C
	<b>2009</b>	<b>2009</b>
<b>Subpart C</b>		
Fuel Oil Combustion		
Fuel Gas Combustion		3,223
WSR Combustion		
<b>Total Subpart C</b>		<b>3,223</b>
<b>Subpart P</b>		
Hydrogen Mfg		-
<b>Subpart Y</b>		
FCC Coke Combustion		226,349
Flare P1		-
Flare P2 (Crude/Sweet)		-
Acid Plant		-
Fugitive Venting (Columns)		55
Loading Vent (Crude Receipts)	45	
<b>Total Subpart Y</b>	<b>45</b>	<b>226,404</b>

<b>Individual Baselines, CO<sub>2</sub>e Tonnes</b>	<b>45</b>	<b>229,627</b>
<b>Total Baseline, Tonnes</b>	<b>229,672</b>	
<b>Proposed Cap - 84%, Tonnes</b>	38	192,924
<b>CO<sub>2</sub>e Reduction, Metric Tonnes</b>	7	36,748

## **Appendix A**

### **October 28, 2016 Chevron Response in Request for Additional Information**



Jon Mauer  
Refinery Manager

**Chevron Products Company**  
Hawaii Refinery  
91-480 Malakole Street  
Kapolei HI 96707-1807  
Tel 808-682-5711  
Fax 808-682-2324  
[JonMauer@chevron.com](mailto:JonMauer@chevron.com)

October 28, 2016

**CERTIFIED MAIL No. 7016 0750 0001 1527 8811  
RETURN RECEIPT REQUESTED**

Ms. Catherine Lopez  
Acting Manager, Clean Air Branch  
Environmental Management Division  
919 Ala Moana Boulevard  
Honolulu, Hawaii 96814

**Chevron Hawaii Refinery  
Response to Item 2(d) in Request for Additional Information  
GHG Emission Reduction Plan**

Dear Ms. Lopez:

The Chevron Products Company is hereby submitting additional information as requested by the Clean Air Branch (CAB) staff for evaluation of the Refinery's Greenhouse Gas Emission Reduction Plan (GHGERP), submitted June 30, 2015. This submittal provides the information requested in item 2(d) from the CAB letter dated February 10, 2016. This information is submitted to meet the requirements of §11-60.1-204(a).

The following attachments are provided in this submittal:

- Attachment I      Refinery GHGERP submitted June 30, 2015
- Attachment II      CAB letter Requesting Additional Information, dated February 10, 2016
- Attachment III      Refinery Preliminary Recommendation Plan, dated June 30, 2016
- Attachment IV      Compact Disc (CD) containing GHG Calculations 2006-2010.xlsx
- Attachment V      Printout of Excel File on CD

If you should have questions or require further information, please contact Anna Chung at (808) 682-3366.

I certify, as the company official having supervisory responsibility for the persons who acting under my direct instructions made the verification, that this knowledge is true, and accurate, and complete to the best of their knowledge, information, and belief.

Sincerely,

asc  
Attachments

**Chevron Hawaii Refinery**  
**GHG Emissions for Calendar Years 2006-2010**  
**October 31, 2016**

## **1.0 Introduction**

The Chevron Hawaii Refinery (referred to here as the Refinery) submitted the GHG Emission Reduction Plan, as required by HAR §11-60.1-204(a), on June 30, 2015 (Attachment I). The Department of Health (DOH) Clean Air Branch (CAB) requested additional information in the February 10, 2016 letter (Attachment II), and over the next several months, the Refinery provided information and communicated with CAB staff to clarify the information requested. The Refinery provided a preliminary recommendation to provide the remaining information in a letter dated June 30, 2016 (Attachment III).

The additional information on GHG emission calculations for the 2006-2010 calendar years, requested in item 2(d) in CAB's February letter, is provided in this submittal. The summary of the calculation methodologies is included below. A compact disk (CD) is included as Attachment IV which contains the detailed calculations. Attachment V contains a printout of the detailed calculations.

## **2.0 GHG Emissions**

### **2.1 Calculation Methodology**

Refinery GHG emissions occur from the processing of crude oil to produce high value products that are distributed in commerce for fuels. Greenhouse gases generated at the refinery include carbon dioxide (CO<sub>2</sub>), nitrous oxide (N<sub>2</sub>O), and methane (CH<sub>4</sub>). These emissions are reported as both mass emission rates and the CO<sub>2</sub> equivalent (CO<sub>2</sub>e) emission rates. CO<sub>2</sub>e emissions are computed by multiplying the mass amount of emissions (tpy) for each of the greenhouse gases by each of the gases' associated global warming potential values published at 40 CFR Part 98, Subpart A, Table A-1, and summing the resultant values of each gas to compute a tpy CO<sub>2</sub> equivalent (CO<sub>2</sub>e).

Three greenhouse gases included in the HAR §11-60.1-1 definition are not generated (hydrofluorocarbons, perfluorocarbons, and sulfur hexafluoride), and therefore are not included in the further GHG discussion and calculations. In addition, there are no biogenic CO<sub>2</sub> emissions at the refinery, or indirect GHG emissions (GHG emissions generated by a different facility), in accordance with HAR §11-60.1-202 definition of the facility-wide GHG emissions cap.

Refinery GHG emissions can be categorized by the type of emissions source:

1. Combustion of liquid and gaseous fuels in stationary sources including process heaters, boilers, cogeneration units
2. Coke combustion in the Fluid Catalytic Cracking Unit
3. Remaining sources, including:
  - a. Hydrogen Manufacturing
  - b. Crude Storage
  - c. Fugitives
  - d. Flaring
  - e. Acid Gas Processing

**Chevron Hawaii Refinery**

**GHG Emissions Item 2(d) in CAB February 10, 2016 Letter**

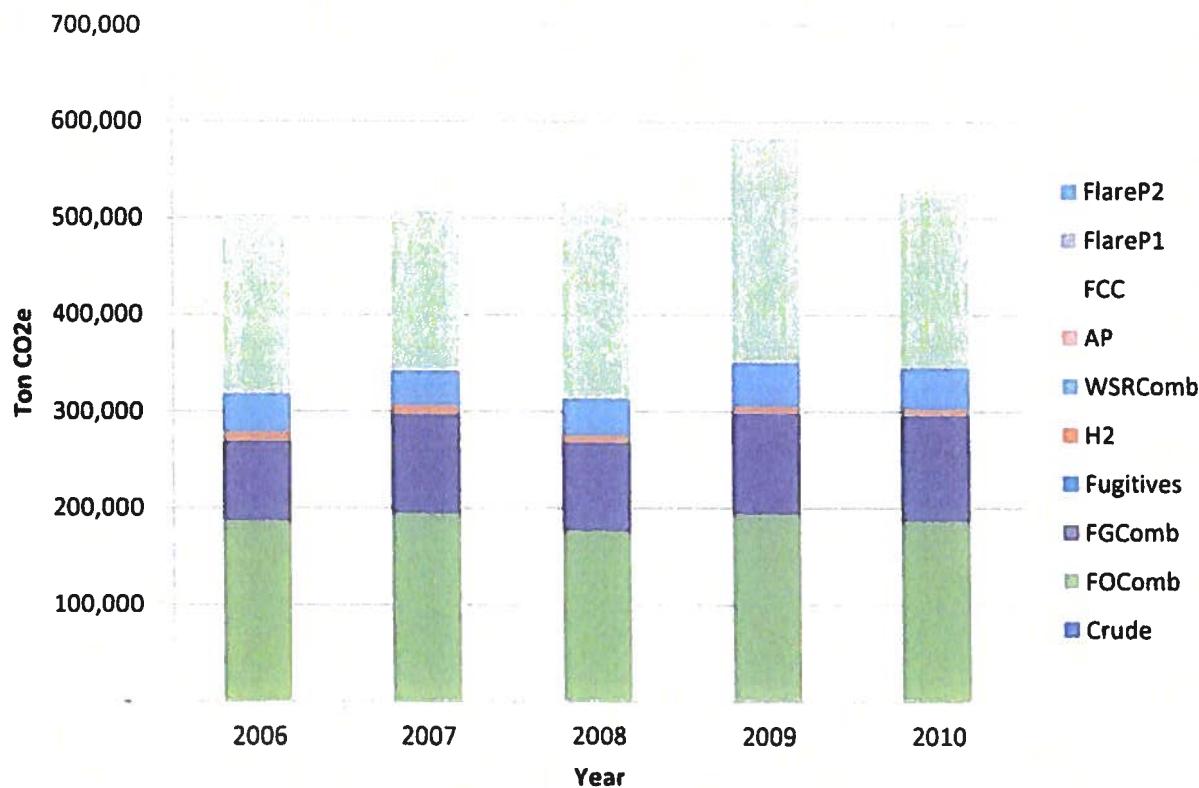
**GHG Emissions for Calendar Years 2006-2010**

**October 31, 2016**

As shown in Figure 1, the Refinery's GHG Emissions are primarily a result of fuels combustion and the FCC Unit coke combustion. Fuels combustion includes combustion of Fuel Oil (FO), Fuel Gas (FG), and Whole Straight Run (WSR).

**Figure 1. GHG Emissions Breakdown**

### Hawaii Refinery CO<sub>2</sub>e Emissions



Combustion Emissions from Fuel Oil, Fuel Gas and Whole Straight Run Fuels: FOComb, FGComb, and WSRComb

Coke Combustion Emissions from Fluid Catalytic Cracking (FCC) Unit: FCC

Hydrogen Manufacturing Vent Emissions: H2

Crude Storage Emissions: Crude

Fugitive Emissions from Process Piping: Fugitives

Flaring Emissions: Flare P2 and Flare P1

Acid Gas Processing Emissions: AP

**Chevron Hawaii Refinery**

**GHGERP Additional Information, Item 2(d) in CAB February 10, 2016 Letter**

**GHG Emissions for Calendar Years 2006-2010**

**October 31, 2016**

The GHG emission calculation methodologies in the attached Excel workbook (Attachment IV) follow the methods prescribed in the following 40 CFR 98 sections:

- Subpart A – General Provisions
- Subpart C – General Stationary Fuel Combustion Sources
- Subpart P – Hydrogen Production
- Subpart Y – Petroleum Refineries

These calculation methodologies are the basis for current regulatory compliance for estimating and reporting GHG emissions, and are summarized in Table 1 below.

The GHG emissions results from the workbook for the years 2008 through 2010 are a demonstration of current GHG calculation methods. The demonstration workbook introduces minor differences (approximately 1%) from the actual GHG emissions due to differences in averaging and summing data, changes in GWP conversion factors for CO<sub>2</sub>e, and changes in emission factors for fuel combustion. The demonstration workbook utilizes current (2015) emission factors and GWP factors, and sums and averages on a monthly basis.

For the reporting years 2006-2007, the demonstration workbook GHG emissions are 7-10% different from the actual emissions calculated at the time utilizing standardized emissions methodologies<sup>1</sup>. These differences are due to the same issues described above, and also due to a different methodology for FCC Unit coke combustion emissions. For 2006 and 2007, the emissions for the FCC Unit are calculated by a different methodology from later years due to the lack of reliable CO<sub>2</sub> analyzer data for those periods. This methodology calculates GHG emissions from emission factors and average coke burn rate.

---

<sup>1</sup> American Petroleum Institute, Compendium of Greenhouse Gas Emissions Methodologies for the Oil and Natural Gas Industry, Releases 2001, 2004, 2009.

**Chevron Hawaii Refinery**  
**GHGERP Additional Information, Item 2(d) in CAB February 10, 2016 Letter**  
**GHG Emissions for Calendar Years 2006-2010**  
**October 31, 2016**

**Table 1. Refinery GHG Emission Calculation Methodologies**

<b>GHG Emissions Source</b>	<b>CO<sub>2</sub></b>	<b>CH<sub>4</sub></b>	<b>N<sub>2</sub>O</b>	<b>Methodology</b>	<b>Equations</b>	<b>Input Data</b>
Liquid Fuel Combustion (FO Comb and WSR Comb) <sup>2</sup>	X	X	X	Subpart C Tier 2	Equations: C-2a C-2b C-9a	Fuel Volume HHV
Gaseous Fuel Combustion (FGComb) <sup>2</sup>	X	X	X	Subpart C Tier 3	Equations: C-5 C-8	Carbon Content Molecular Wt Fuel Flow Rate
FCC Coke Combustion (FCC) <sup>2</sup>	X	X	X	Subpart Y Tier 4	Equations: Y-6 Y-7a Y-7b Y-9 Y-10	Analyzer data Inlet Air Carbon Fraction in Coke Burned
Hydrogen Production (H <sub>2</sub> ) <sup>2</sup>	X			Subpart P	Equations: P-1	Carbon Content Molecular Wt Fuel Flow Rate
Flaring (Flare P1 and Flare P2) <sup>2</sup>	X	X	X	Subpart Y	Equations: Y-3 Y-4 Y-5	Molecular Fraction of Carbon HHV Manual Samples
Acid Gas Processing (AP) <sup>2</sup>	X			Subpart Y	Equations: Y-12	Volumetric Flow rate
Fugitives (Fugitives) <sup>2</sup>		X		Subpart Y	Equations: Y-21	Equipment type Number of units
Crude Storage (Crude) <sup>2</sup>		X		Subpart Y	Equations: Y-22	Crude Received

<sup>2</sup>( ) refer to naming conventions in Figure 1.

**Chevron Hawaii Refinery**  
**GHGERP Additional Information, Item 2(d) in CAB February 10, 2016 Letter**  
**GHG Emissions for Calendar Years 2006-2010**  
**October 31, 2016**

## 2.2 Results

GHG emissions for the 2006-2010 calendar years are shown in Table 2, below, for the 2006-2010 calendar years.

**Table 2. Refinery GHG Emissions<sup>3</sup>**

Year	Demonstration Workbook Calculated Emissions				Actual Emissions
	Fuel Combustion (tonnes/yr)	FCC Emissions (tonnes/yr)	All Other Emissions (tonnes/yr)	Total Emissions (tonnes/yr)	
2006	308,406	162,976	11,148	482,530	536,124
2007	331,667	184,301	11,486	527,454	569,048
2008	305,447	203,649	8,321	517,418	522,593
2009	342,322	230,138	9,274	577,945	581,734
2010	337,371	184,372	7,907	523,117	529,651

<sup>3</sup> Actual GHG emissions were calculated by methods and data available at the time and reported for EPA MRR and internal compliance. Demonstration Workbook Calculated Emissions are results from utilizing current methodologies and input data.

As mentioned previously, GHG emissions and detailed calculations, mathematical equations, input data, and emission factors for the 2006-2010 calendar years are provided in Attachment IV and in hardcopy format as Attachment V.

**Attachment I**  
**Chevron Hawaii GHG Emission Reduction Plan**  
**Dated June 30, 2015**



**Jon Mauer**  
Refinery Manager

**Chevron Products Company**  
Hawaii Refinery  
91-480 Malakole Street  
Kapolei HI 96707-1807  
Tel 808-682-5711  
Fax 808-682-2324  
JonMauer@chevron.com

June 30, 2015

**CERTIFIED MAIL No. 7014 1820 0000 0357 1755**  
**RETURN RECEIPT REQUESTED**

Mr. Nolan Hirai  
Manager, Clean Air Branch  
Environmental Management Division  
919 Ala Moana Boulevard  
Honolulu, Hawaii 96814

**Chevron Hawaii Refinery**  
**GHG Emission Reduction Plan**

Dear Mr. Hirai:

The Chevron Products Company is hereby submitting its Greenhouse Gas Emission Reduction Plan for the Chevron Hawaii Refinery. This plan is being submitted to meet the requirements of §11-60.1-204(a).

If you should have questions or require further information, please contact Kristi Mitchum at (808) 682-3145.

I certify, as the company official having supervisory responsibility for the persons who act under my direct instructions made the verification, that this knowledge is true, and accurate, and complete to the best of their knowledge, information, and belief.

Sincerely,



A handwritten signature in black ink, appearing to read "Jon Mauer". Below the signature is a small oval containing the initials "kam".

Enclosures

**Chevron Hawaii Refinery  
GHG Emission Reduction Plan  
§11-60.1-204  
June 30, 2015**

## **Introduction**

This plan is being submitted in order to meet the requirements of §11-60.1-204(a). The Chevron Hawaii Refinery (Chevron or the Refinery) is located within the Campbell Industrial Park at 91-480 Malakole Street, Kapolei, Hawaii. The facility operates under a Covered Source Permit No. 0088-01-C issued by the Hawaii Department of Health. The Refinery began operation in 1960 with capacity of processing up to 58,000 barrels of crude oil per day. The Refinery has not operated at this rated capacity in recent history but rather sets operations based on market demands. The facility consists of numerous operational units, including crude vacuum and distillation units, fluid catalytic cracker, dimersol, hydrogen manufacturing, alkylation, and isomerization units. The refinery operates utilities including boilers, cogeneration units, effluent treatment plant, and tank fields for storage, blending, and shipping capability in support of its operations.

Chevron has prepared this Greenhouse Gas (GHG) Emission Reduction Plan (the GHG Plan or the Plan) to comply with requirements of the Hawaii Greenhouse Gas Emissions law<sup>1</sup> (the Act) and implementing regulations of the Hawaii Department of Health ("DOH").<sup>2</sup> The GHG rule<sup>3</sup> sets forth the regulatory program for meeting the statutory statewide GHG limit that is equal to or below the 1990 statewide GHG emission levels. The GHG rule generally requires each regulated source to propose a GHG Plan that would cap the source's direct GHG emissions to 16% of that source's 2010 direct GHG emissions. In meeting the GHG limit, the regulation provides flexibility to the Director of the Department of Health, Clean Air Branch (Director or CAB) to set the facility-wide GHG emissions cap for an individual source by varying from the established regulatory structure in two ways: 1) by granting a request to use an alternate emission baseline; and 2) establishing an alternate GHG emission cap based on a finding that the presumptively required 16% reduction is not attainable.

The GHG rule is premised on an assumption that the GHG covered sources reducing their direct GHG levels by 16% from 2010 emission levels will be adequate to return the State of Hawaii to 1990 GHG levels. Although the ultimate goal of the Act is to reduce statewide GHG emissions to 1990 emission levels, the Refinery has actually achieved reductions in GHG emissions to less than its estimated 1990 levels and, as a prudent operator, continues to seek these as part of our business. Unlike other sources of GHGs within the state and the selected industries subject to the current GHG rule that have seen growth, and thus increases in GHG emissions since 1990, the Refinery has not experienced sustained increases in capacity and therefore, increased GHG emissions over this same period of time.

---

<sup>1</sup> HRS §§ 342B *et seq.*, enacted by Act 234, 2007 Hawaii Session Laws.

<sup>2</sup> HAR § 11-60.1-204, "Greenhouse gas emission reduction plan." Hereinafter, the "GHG rule."

<sup>3</sup> HAR §11-60.1-201, Purpose.

### **Request for Alternate Baseline Annual Emission Year**

Section 11-60.1-204(d)(1) generally requires regulated sources to use 2010 to compute the GHG baseline emissions. This paragraph, however, also allows an owner or operator to propose an alternate GHG emission baseline, and includes several potential methodologies to support computation of an acceptable alternative. These alternatives allow an owner or operator to use emissions from the years 2005-2010 in various formulations, if the owner or operator documents that 2010 is "not representative of normal source operations."

Per §11-60.1-204(d)(1)(A)(i), Chevron requests that the Director approve an alternative baseline year of 2009 based on the most representative year during the five-year period ending 2010. Considering the criteria in paragraph (d)(1)(A), 2009 is an appropriate baseline year. Emissions reported for the 2010 reporting year do not accurately reflect normal operation which resulted in less GHG emissions.

An analysis of the Refinery operations during the 5-year period ending in 2010 demonstrate that the 2009 reporting year is more representative of current operations and anticipated future operations than the 2010 reporting year. In 2010, the Refinery conducted a major plant turnaround of its Fluid Catalytic Cracker (FCC) unit. The result of this maintenance event significantly reduced the GHG emissions for the 2010 calendar year making the use of the 2010 calendar year as a baseline not representative of normal and continuous operation. In 2009, Refinery operations were continuous. Chevron has been estimating GHG emissions internally for several years prior to the GHG Reporting Rule requirement. The 2009 emission calculations are representative and comparable to the 2010 reporting year calculation methodology.

Direct GHG emission estimates for the proposed 2009 baseline year are 581,734 metric tons per year (tpy) of carbon dioxide equivalent (CO<sub>2</sub>e). Table 1. GHG Annual Emission Summary indicates the direct GHG emissions estimated for the 1990 calendar year as well as the calculated 2009 and 2010 calendar years. The 1990, 2009, and 2010 calendar years were calculated using the methodologies as required by the GHG Reporting Rule in 40 CFR Part 98; however, estimates were used some operational data that was unavailable for the 1990 calendar year

**Table 1. GHG Annual Emission Summary**

Calendar Year	Direct emissions reported in metric tons per year of CO <sub>2</sub> e
1990	613,900 (estimated)
2009 (baseline year)	581,734
2010	529,651

## **2020 Facility-Wide Direct GHG Emissions Cap**

Per §11-60.1-204(d)(2), the regulation requires a 16% reduction from the proposed 2009 baseline year which would equate to a reduction of 93,077 metric tpy CO<sub>2</sub>e and an emissions cap of 488,657 metric tpy CO<sub>2</sub>e. For this facility, a reduction of this size is not attainable for long term sustainability of the Refinery.

The Refinery proposes a direct GHG emissions cap of 569,000 tons CO<sub>2</sub>e. This is equivalent to a 7.3% reduction in direct GHG emissions since 1990 (or 44,900 tpy of CO<sub>2</sub>e) or a 2.2% (or 12,734 tpy of CO<sub>2</sub>e) reduction from the baseline year of 2009. Since 2009, the Refinery implemented several energy efficiency measures, and consequently, reduced GHG emissions below this proposed cap. However, these GHG emission reductions were incidental to the intended benefits of the various projects. Those GHG reductions were never intended to be considered an enforceable GHG limit in the refinery Covered Source Permit and are not necessarily permanent.

Minimal decreases, as discussed below, may be attainable but anything greater would not survive the economic impact analysis that the rule requires in §11-60.1-204(d)(5).

## **GHG Control Assessment**

Per §11-60.1-204(d)(2), the GHG rule requires each affected source to conduct a GHG control assessment. The Refinery has reviewed the available control measures identified §11-60.1-204(d)(3), as well as other sources including available EPA guidelines for GHG Best Available Control Technology. These included "Available and Emerging Technologies for Reducing Greenhouse Gas Emissions from the Petroleum Refining Industry", EPA Office of Air and Radiation, October 2010 and "Available and Emerging Technologies for Reducing Greenhouse Gas Emissions from Industrial, Commercial, and Institutional Boilers", EPA Office of Air and Radiation, October 2010.

Chevron has conducted a GHG control assessment of these control measures and has included the technical feasibility, control effectiveness, and cost evaluation of each measure. A summary of this information is provided in Table 2. GHG Control Assessment. Please note that the refinery already has a many of these measures in place and has noted this where applicable.

## **Proposed Control Strategy**

Per §11-60.1-204(d)(6), the regulation requires each affected source to propose a control strategy to include a listing of identified control measures that can be implemented in order to meet the required or proposed alternate 2020 facility-wide GHG emissions cap.

From 1990 to present, Chevron Hawaii Refinery has completed many control measures that have attributed to the reduction of direct GHG emissions.

- Economizers were installed on the 2 crude furnaces in 1993,
- In 1999, the boiler feed water preparation system (hot lime water) was replaced with reverse osmosis which treats wastewater from the City and County of Honolulu's Honouliuli wastewater treatment plant,
- Control and operational improvements were realized with the new FCC reactor which was replaced in 2003 which also included flare reductions,
- In 2005, the cooling tower motorization was completed,
- In 2006, a flare gas recovery system was installed to recover waste gases being routed to the flare for destruction which is now used for energy recovery; and,
- As part of the Energy Project which began in the early 2000's, Chevron built a new cogeneration unit (Cogen #4) which allows the refinery to optimize its energy use and steam generation. This project included motorization of the Alky plant compressor in April 2013 which enabled full utilization of 4 cogen units. The project also included replacement of three existing boilers with two more energy efficient boilers. A revision of the permit limits for the boilers is pending and the ultimate shutdown of the original three boilers will achieve further reductions in direct GHG emissions.

Since 1990, the Refinery has not expanded nor increased its rated production capacity, nor has the Refinery operated at its maximum permitted rate in the allowable baseline years (2006 through 2010). In fact, Chevron has made significant progress by continuing to evaluate and integrate energy efficiency projects as well as operational best practices which have resulted in lowering GHG emissions for the refinery and the state of Hawaii.

These reductions and other optimization projects have reduced the refinery's Direct GHG emissions by 7.3% since 1990.

Chevron continues to evaluate energy efficiency measures to streamline its cost of operation as well as reducing emissions of GHG. However, cost efficient measures resulting in large reductions in energy consumption and subsequent direct GHG emissions have already been utilized by the Refinery. Additional control measures have been evaluated utilizing a cost per ton methodology similar to Best Achievable Control Technology (BACT). Similar BACT exercises for GHG have been performed within the US resulting in a \$20 per ton (CO<sub>2</sub>e basis) threshold for refineries. Reference: US EPA Region 8 Response to Comments for Sinclair Wyoming Refinery's PSD permit March 21, 2013; PSD permit for Flint Hills Corpus Christi West Refinery April 2014]. In addition, recent regulations like the Heater and Boiler MACT have energy assessment criteria that would only include projects that have payback within 2 year or less.

Utilizing this information, Chevron's GHG control assessment does not yield any additional future projects that result in significant direct GHG emissions reductions given the practical and technical feasibility and cost effectiveness considerations. A waterfall diagram depicting Chevron's GHG emission history including historical projects and the impact of current planned reductions is shown in Chart 1. Waterfall Diagram of GHG Control Assessment. Projects will continue to be evaluated for future emission reductions and future business needs.

Table 2. GHG Control Assessment

Chevron Hawaii Refinery  
June 30, 2015

		Control Effectiveness and Cost Evaluation						
		(A) Control	(B) Expected emission rate (tons per year CO2e, pounds CO2e/kilowatt-hour)	(C) Expected emission reduction (tons per year CO2e)	(D) Energy impacts (BTU, kilowatt-hour)	(E) Environmental impacts (other media and the emissions of other regulated air pollutants)	(F) Any secondary impacts resulting from the production or acquisition of the control measure	(G) Economic impact (cost effectiveness: annualized control cost, \$/megawatt-hr, \$/ton CO2e removed, and incremental cost effectiveness between the control and status quo)
GHG Control Measure	Applicable Source Type	Technically Feasible Measures (eliminated all technically infeasible options based on physical, chemical, or engineering principles)						
(A) GHG Capture and Control		Technically infeasible						
Carbon dioxide capture and storage (CCS)	Large combustion sources; large CO2 vents (e.g., hydrogen plant)	Physical: CO2 storage in local geologic formations (volcanic formations) is not feasible.						
		Engineering: Techno-economic studies indicate that CCS is not likely to be economically feasible below about 1,000,000 tonnes per year of capture, particularly if the carbon dioxide cannot be used for enhanced oil recovery	N/A	N/A	N/A	N/A	N/A	
(B) Fuel Switching or Co-firing		Technically feasible						
Co-firing	Fuel-fired sources (including boilers, furnaces)	Actual: Boiler F-5201 is currently operated on a combination of fuel oil and refinery fuel gas.	2%	118,831	1,853	1	Reduction in criteria pollutant emissions	Additional emissions for storage of secondary fuel
Fuel Switching	Fuel-fired sources (including boilers, furnaces, and cogens)	Technically feasible Not Considered: Fuel switching is not cost effective.	19.5% reduction in CO2	26,425	6,398	No Change	Reduction in criteria pollutant emissions	Additional emissions for storage of secondary fuel
(C) Energy efficiency upgrades								

Table 2. GHG Control Assessment

Chevron Hawaii Refinery  
June 30, 2015

§11-60-1-204(d)(3)		§11-60-1-204(d)(4)		Control Effectiveness and Cost Evaluation §11-60-1-204(d)(5)(A through G)				
GHG Control Measure	Applicable Source Type	(A) Control Effectives (eliminate all technically infeasible options based on physical, chemical, or engineering principles)	(B) Expected emission rate (tons per year CO2e, pounds CO2e/kilowatt-hour)	(C) Expected emission reduction (tons per year CO2e)	(D) Energy impacts (BTU, kilowatt-hour)	(E) Environmental Impacts (other media and the emissions of other regulated air pollutants)	(F) Any secondary impacts resulting from the production or acquisition of the control measure	(G) Economic impact (cost effectiveness: annualized control cost, \$/megawatt-hour, \$/ton CO2e removed, and incremental cost effectiveness between the control and status quo)
Replace equipment	Boilers	Technically feasible.  Current Plan: Boilers F-5201, F-5202, and F-5203 will be replaced with Boilers F-5205 & F-5206 in 2016.	9.80%	45,437	4,940	100	None	Boiler construction is complete. Permit is pending.
Replace/ upgrade burners	Furnaces	Technically feasible  Not Considered: Replacing or upgrading burners is not cost effective.	0.60%	144,520	903	4	Reduction in criteria pollutant emissions	\$554
Cogeneration	Actual: Cogens 1, 2, and 3 are installed and operational. Cogen 4 was installed and operational as of 2010.	Technically feasible						
Instrumentation and controls (improve process monitoring and control systems)	Furnaces, boilers, cogens	Actual: Refinery furnaces, boilers, and cogens are currently equipped with instrumentation and controls to improve process monitoring.  Not Considered: Additional instrumentation and controls are not cost effective.	0.20%	237,022	451	2	None	\$1,109  Additional LDAR regulated components
Economizer	Actual: Boilers (F-5201, F-5202, F-5203, F-5205, and F-5206) have economizers. Crude furnaces (F-5150 and F-5153) were equipped with economizers in 1993.	Technically feasible						

Table 2. GHG Control Assessment

Chevron Hawaii Refinery  
June 30, 2015

§111-60.1-204(d)(3)		§111-60.1-204(d)(4)	Control Effectiveness and Cost Evaluation						
			(A) Control Effectiveness	(B) Expected emission rate (tons per year CO <sub>2</sub> e, pounds CO <sub>2</sub> e/kilowatt-hour)	(C) Expected emission reduction (tons per year CO <sub>2</sub> e)	(D) Energy impacts (BTU, kilowatt-hour)	(E) Environmental impacts (other media and the emissions of other regulated air pollutants)	(F) Any secondary impacts resulting from the production or acquisition of the control measure	(G) Economic impact (cost effectiveness: annualized control cost, \$/megawatt-hour, \$/ton CO <sub>2</sub> e removed, and incremental cost effectiveness between the control and status quo)
GHG Control Measure	Applicable Source Type	Technically Feasible Measures (eliminate all technically infeasible options based on physical, chemical, or engineering principles)							
Heat Recovery: Air Preheater	Furnaces, boilers, cogens	Actual: Crude furnaces (F-5150 and F-5153) and boilers (F-5201, F-5202, F-5203, F-5205, and F-5206) have air preheat.	0.60%	85,257	500	20	None	May increase NO <sub>x</sub> emissions (2)	\$10,000
Power/ waste heat recovery		Actual: Furnaces have waste heat recovery.							
Create turbulent flow within fire tubes		Not applicable. The refinery does not operate fire tubes.							
Capture energy from boiler blowdown		Actual: Boiler blowdown system exchanges heat with RO water	Technically feasible						
		Actual: Condensate return system in place and operational!							

Table 2. GHG Control Assessment

Chevron Hawaii Refinery  
June 30, 2015

		§11-60-1-204(d)(3)						§11-60-1-204(d)(4)						§11-60-1-204(d)(5)(A through G)					
		Control Effectiveness and Cost Evaluation																	
GHG Control Measure	Applicable Source Type	(A) Control Effectives	(B) Expected emission rate (tons per year CO2e, pounds CO2e/kilowatt-hour)	(C) Expected emission reduction (tons per year CO2e)	(D) Energy impacts (BTU, kilowatt-hour)	(E) Environmental Impacts (other media and the emissions of other regulated air pollutants)	(F) Any secondary emissions or impacts resulting from the production or acquisition of the control measure	(G) Economic impact (cost effectiveness: annualized control cost, \$/megawatt-hr, \$/ton CO2e removed, and incremental cost effectiveness between the control and status quo)											
Condensate return system	Technically Feasible Measures (eliminate all technically infeasible options based on physical, chemical, or engineering principles)																		
	Under Evaluation: Improvements to condensate recovery are under evaluation but are not cost effective at this time.	2.20%	58,416	1,338	13	None	None	\$374											
Motorization projects (use high efficiency motors; use variable speed drives)	Technically feasible																		
	Actual: Completed motorization of Alky Compressor in 2013 and Cooling Tower in 2005.	9.50%	212,467	25,006	70	Reduction in criteria pollutant emissions	Increase emissions for HE CO	Complete											
Optimize compressed air systems	Optimization of existing air compressors	Technically feasible																	
	Not Considered: Optimization of existing air compressors is not cost effective.	0.01%	237,457	16	1	None	None	\$31,250											
Power/ waste heat recovery	Actual: Already in place for furnaces.																		
(D) Combustion and operational improvements	Technically feasible																		

Table 2. GHG Control Assessment

Chevron Hawaii Refinery  
June 30, 2015

§11-60.1-204(d)(3)		§11-60.1-204(d)(4)		Control Effectiveness and Cost Evaluation						
§11-60.1-204(d)(5)(A through G)				(A) Control	(B) Expected emission rate (tons per year CO <sub>2</sub> e, pounds CO <sub>2</sub> e/kilowatt-hour)	(C) Expected emission reduction (tons per year CO <sub>2</sub> e, pounds CO <sub>2</sub> e/kilowatt-hour)	(D) Energy impacts (BTU, kilowatt-hour)	(E) Environmental impacts (other media and the emissions of other regulated air pollutants)	(F) Any secondary emissions or impacts resulting from the production or acquisition of the control measure	(G) Economic impact (cost effectiveness: annualized control cost, \$/megawatt-hour, \$/ton CO <sub>2</sub> e removed, and incremental cost effectiveness between the control and status quo)
GHG Control Measure	Applicable Source Type	Technically Feasible Measures (eliminate all technically infeasible options based on physical, chemical, or engineering principles)								
Tuning (optimizing excess oxygen)	Furnaces, boilers, cogens	Under Evaluation: Furnace tuning is under evaluation but is not cost effective at this time.	0.80%	235,667	1,806	12	Reduction in NO <sub>x</sub> emissions	\$277	Low excess air may lead to increased CO emissions	
Optimization	Furnaces, boilers, cogens	Covered under Instrumentation and Controls - Energy Efficiency - as well as Tuning above								
Reduce air leakages	Furnaces, boilers	Technically feasible								
		Under Evaluation: Reducing air leakages is under evaluation but is not cost effective at this time.	0.66%	235,890	1,583	5	Reduction in criteria pollutant emissions	\$190	None	
Reduce steam trap leaks	All	Technically feasible								
		Actual: Program in place at refinery to reduce steam trap leaks.	0.14%	237,140	333	3	Reduction in criteria pollutant emissions	\$150	None	
Insulation/insulating jackets	for surface temperatures above 120 degrees F (1)	Technically feasible								
		Under Evaluation: Insulation improvements are under evaluation.	0.50%	236,286	1,187	10	Reduction in criteria pollutant emissions	\$126	None	

Table 2. GHG Control Assessment

Chevron Hawaii Refinery  
June 30, 2015

§11-60-1-204(d)(3)		§11-60-1-204(d)(4)		§11-60-1-204(d)(5)(A through G)					
		Control Effectiveness and Cost Evaluation							
GHG Control Measure	Applicable Source Type	(A) Control Effectives (eliminate all technically Infeasible options based on physical, chemical, or engineering principles)	(B) Expected emission rate (tons per year CO2e, pounds CO2e/kilowatt-hour)	(C) Expected emission reduction (tons per year CO2e)	(D) Energy Impacts (BTU, kilowatt-hour)	(E) Environmental Impacts (other media and the emissions of other regulated air pollutants)	(F) Any secondary impacts resulting from the production or acquisition of the control measure	(G) Economic impact (cost effectiveness: annualized control cost, \$/megawatt-hr, \$/ton CO2e removed, and incremental cost effectiveness between the control and status quo)	
Reduce slagging and Fouling of heat transfer surfaces (furnace tube coatings)	Furnaces, boilers	Not Considered: The addition of furnace tube coatings is not cost effective.	0.02%	63,366	10	0.12	Reduction in criteria pollutant emissions	\$10,000	
Furnace cleaning during turnarounds	Actual: Furnace cleaning is performed during turnarounds.						None		
FCC surface condenser ejector cleaning	Actual: FCC surface condenser ejector cleaning is performed.								
Manage steam letdown	Actual: Refinery manages steam letdown.								
Implement lighting system efficiency improvements	Technically feasible  Not Considered: Implementing lighting system efficiency improvements is not cost effective.		0.01%	237462	11	0.1	None	\$909	

Table 2. GHG Control Assessment

Chevron Hawaii Refinery  
June 30, 2015

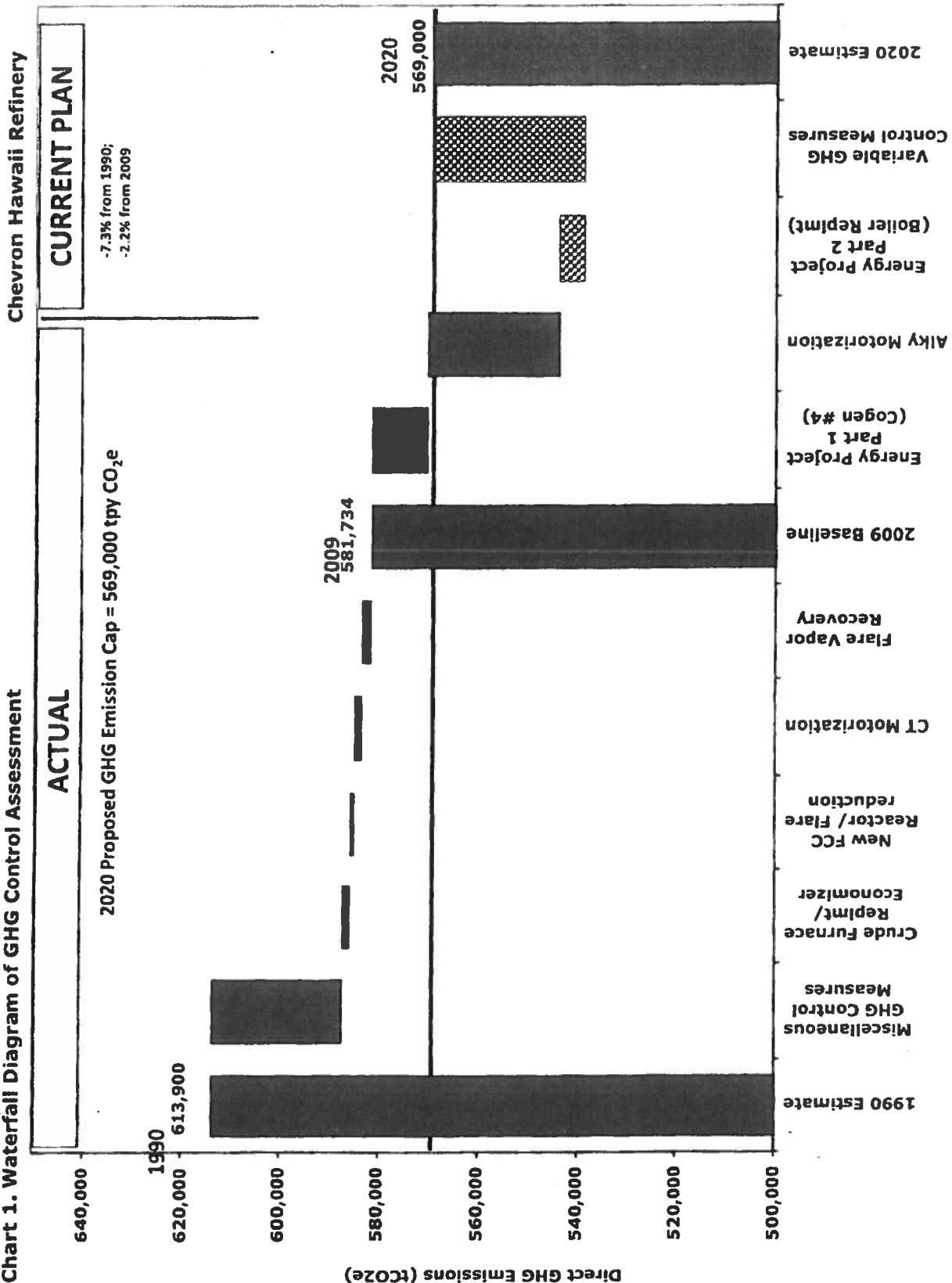
		Control Effectiveness and Cost Evaluation						
		§11-60-1-204(d)(5)(A through G)						
GHG Control Measure	Applicable Source Type	(A) Control Effectives (eliminate all technically infeasible options based on physical, chemical, or engineering principles)	(B) Expected emission rate (tons per year CO2e, pounds CO2e/kilowatt-hour)	(C) Expected emission reduction (tons per year CO2e)	(D) Energy impacts (BTU, kilowatt-hour)	(E) Environmental impacts (other media and the emissions of other regulated air pollutants)	(F) Any secondary emissions or impacts resulting from the production or acquisition of the control measure	(G) Economic impact (cost effectiveness: annualized control cost, \$/megawatt-hr, \$/ton CO2e removed, and incremental cost effectiveness between the control and status quo)
Online Furnace Cleaning	Furnaces	Under Evaluation: Programs to incorporate online furnace cleaning are under evaluation but are not cost effective at this time.	0.14%	237,140	333	2	None	\$180
(E) Restrictive operation	Minimize use of import electricity	Actual: Refinery optimizes use of cogens and boilers for energy efficiency to minimize use of import electricity	Technically feasible	25%	300	100	1	Reduction in criteria pollutants
Optimize FCC preheat furnace	FCC Preheat Furnace	Under Evaluation: Optimization of FCC preheat furnace operation is under evaluation.	Technically feasible	13%	207473	30,000	None	\$100
Refinery turndown	Refinery-wide	Not Considered: Refinery turndown is not cost effective.	Technically feasible	0.31%	236,733	740	5	Reduction in criteria pollutants
Reduce steam vents on reboilers		Under Evaluation: Reboiler vent reduction efforts are under evaluation but not cost effective at this time.					None	> \$1,000
(F) Planned upgrades, overhaul or retirement of equipment								

Table 2. GHG Control Assessment

Chevron Hawaii Refinery  
June 30, 2015

§11-60-1-204(d)(3)		§11-60-1-204(g)(4)		Control Effectiveness and Cost Evaluation				§11-60-1-204(d)(5)(A through G)	
GHG Control Measure	Applicable Source Type	(A) Control Effectives	(B) Expected emission rate (tons per year CO2e, pounds CO2e/kilowatt-hour)	(C) Expected emission reduction (tons per year CO2e, pounds CO2e/kilowatt-hour)	(D) Energy Impacts (BTU, kilowatt-hour)	(E) Environmental impacts (other media and the emissions of other regulated air pollutants)	(F) Any secondary impacts resulting from the production or acquisition of the control measure	(G) Economic Impact (cost effectiveness: annualized control cost, \$/megawatt-hr, \$/ton CO2e removed, and incremental cost effectiveness between the control and status quo)	
<b>Included in line items above and below.</b>									
<b>(G) Outstanding regulatory mandates, emission standards and binding agreements</b>									
Heater and Boiler MACT									
NSPS 1a									
Furnaces, Boilers									
Energy assessments for applicable sources are required to be completed by January 31, 2016. Impacts of this regulation are included in line items above.									
Flare monitoring equipment and flare monitoring plan are required to be completed by November 11, 2015. Impacts of this regulation are included in line items above.									
<b>(H) Other GHG reduction initiatives that may affect the facility's GHG emissions</b>									
Leak detection and repair	Actual:	Refinery complies with existing leak detection and repair regulatory requirements.							
Flare gas recovery	Actual:	Refinery installed flare gas recovery in 2006.							

**Chart 1. Waterfall Diagram of GHG Control Assessment**



**Attachment II**  
**DOH Letter Requesting Additional Information**  
**Dated February 10, 2016**

DAVID Y. IGE  
GOVERNOR OF HAWAII



VIRGINIA PRESSLER, M.D.  
DIRECTOR OF HEALTH

STATE OF HAWAII  
DEPARTMENT OF HEALTH  
P.O Box 3378  
HONOLULU, HAWAII 96801-3378

In reply please refer to  
File:

16-071E CAB  
File No. 0088

February 10, 2016

Ms. Kristi Mitchum  
HES Manager  
Chevron Products Company  
Hawaii Refinery  
91-480 Malakole Street  
Kapolei, Hawaii 96707-1807

Dear Ms. Mitchum:

**SUBJECT:** Greenhouse Gas (GHG) Emissions Reduction Plan  
Covered Source Permit (CSP) Nos. 0088-01-C, 0088-02-C, and 0088-03-C  
Chevron Products Company  
Hawaii Refinery  
Located At: 91-480 Malakole Street, Kapolei, Oahu

The Department of Health, Clean Air Branch (CAB), completed an initial review of your GHG Emissions Reduction Plan and determined that additional information is needed for the plan. Please refer to the enclosed attachment and Compact Disk (CD) for the requested information.

Pursuant to the Hawaii Administrative Rules §11-60.1-204(e), the CAB requests that the additional information be provided by April 8, 2016.

If you have any questions, please contact Mr. Keith McFall of my staff at (808) 586-4200.

Sincerely,

A handwritten signature in black ink, appearing to read "Nolan S. Hirai".

NOLAN S. HIRAI, P.E.  
Manager, Clean Air Branch

KM:mah

Enclosures

Chevron Products Company  
Greenhouse Gas Emissions Reduction Plan (GHGERP)  
Hawaii Refinery  
CSP Nos. 0088-01-C, 0088-02-C, and 0088-03-C  
February 10, 2016

**ATTACHMENT**

Please provide the following information and/or clarifications:

- 1) Table 1 of your GHGERP presents GHG emissions from the Chevron Products Company, Hawaii Refinery for calendar years 2009 and 2010 to provide information on an appropriate baseline level for the GHG emissions cap. These results were compared with GHG emissions based on fuel consumption data from annual emission reports submitted to the CAB for calendar years 2009 and 2010. The results show emissions based on Chevron's fuel burning data account for about half of the total GHG emissions in Table 1 of your GHGERP. Thus, the detailed GHG emissions information provided in the GHGERP appears crucial to accurately estimating GHG emissions. The CAB requests confirmation on whether or not fuel burning data alone is sufficient to determine GHG emissions.
- 2) Pursuant to Hawaii Administrative Rules §11-60.1-204(d)(1)(A), the owner or operator shall clearly document why calendar year 2010 is not representative of normal operations and why the proposed alternate year or period is more suitable based on trends, existing equipment and controls, scheduled maintenance, operational practices, and any other relevant information.

The "Request for Alternate Baseline Annual Emission Year" section of your GHGERP discusses a proposed 2009 alternative baseline year and presents Chevron's associated justification and rationale and states:

**Statement #1:** "Considering the criteria in paragraph (d)(1)(A), 2009 is an appropriate baseline year. Emissions reported for the 2010 reporting year do not accurately reflect normal operation which resulted in less GHG emissions. An analysis of the Refinery operations during the 5-year period ending in 2010 demonstrate that the 2009 reporting year is more representative of current operations and anticipated future operations than the 2010 reporting year. In 2010, the Refinery conducted a major plant turnaround of its Fluid Catalytic Cracker (FCC) unit. The result of this maintenance event significantly reduced the GHG emissions for the 2010 calendar year making the use of the 2010 calendar year as a baseline not representative of normal and continuous operation. In 2009, Refinery operations were continuous. Chevron has been estimating GHG emissions internally for several years prior to the GHG Reporting Rule requirement. The 2009 emission calculations are representative and comparable to the 2010 reporting year calculation methodology."

**Statement #2:** "Direct GHG emission estimates for the proposed 2009 baseline year are 581,734 metric tons per year (tpy) of carbon dioxide equivalent (CO<sub>2</sub>e). Table 1. GHG Annual Emission Summary indicates the direct GHG emissions estimated for the 1990 calendar year as well as the calculated 2009 and 2010 calendar years."

The CAB examined the information provided in your GHGERP and identified the following items:

- a) Statement#1 indicates that facility GHG emissions for calendar year 2010 are not representative of normal operations due to operations associated with the FCC unit, and that facility emissions associated with calendar year 2009 are "more representative of current operations and anticipated future operations than the 2010 reporting year." The GHGERP did not include the "analysis of Refinery operations" associated with your calendar year 2006 through 2010 GHG emissions. It did not quantify the significance of the "major plant turnaround" of the FCC unit relative to other changes in operations that occurred during the 2006 to 2010 period. The CAB examined annual fuel burning data associated with the Chevron Refinery, including calendar years 2006 through 2010, and calculated the annual heat content associated with the FCC Furnace (Unit F5300) for this period. Please see Table A-1 below. Presuming these results are correct, there does not appear to be a significant difference between the values for 2009 and 2010. However, as shown in Table A-1, relative to the 5-year mean value of 96,011 MMBTU, there is significant reduction in energy use for the FCC between the 2006 to 2007 years (~ 142% of the mean) and the 2009 to 2010 years (~ 61% of the mean).

Table A-1. FCC Furnace (Unit F5300) Heat Content

	2006 (MMBTU)	2007 (MMBTU)	2008 (MMBTU)	2009 (MMBTU)	2010 (MMBTU)
FCC Unit No. F5300	136,305	136,553	89,606	59,897.4	57,694
% of 5-year mean <sup>a</sup>	142.0%	142.2%	93.3%	62.4%	60.1%

a. Percentage of the average 96,011 MMBtu energy use between 2006 and 2010.

Total MMBtu per year energy use associated with all annual fuel consumption was also calculated. Please see Table A-2 below. Presuming these results are correct, there does not appear to be a significant difference in energy use for the Chevron Refinery between 2008 and 2010. Relative to the 5-year mean value of 4,561,312 MMBTU, the variations are relatively small compared to those shown in Table A-1 for the FCC Furnace. In addition, since the FCC's MMBtu energy use is only a few percent of Chevron Refinery's total energy use for fuel burning, and the energy use from burning fuel appears to contribute only about half of the total GHG emissions for the facility, without additional explanation and quantification, it is not clear that FCC operations are representative of your facility's annual GHG emissions.

Table A-2. Total Fuel Burning Heat Content

	2006 (MMBTU)	2007 (MMBTU)	2008 (MMBTU)	2009 (MMBTU)	2010 (MMBTU)
All	4,649,600	4,968,139	4,392,463	4,490,778	4,305,579
% of 5-year mean <sup>a</sup>	101.9%	108.9%	96.3%	98.5%	94.4%

a: Percentage of the average 4,561,312 MMBtu energy use between 2006 and 2010.

The GHGERP identified the "major plant turnaround" of the FCC unit as the reason for the assertion that calendar year 2010 was not representative of normal operations. However, the GHGERP does not include the supporting data, analysis,

and results needed to assess this claim. The CAB's evaluation of energy use by your facility does not appear to validate the claim either. The CAB, therefore, requests additional information to document FCC unit operation as the means to evaluate the relative suitability of calendar years 2006 through 2010 as an appropriate representation of baseline GHG emissions. For the purpose of establishing trend information, the CAB requests similar information for calendar years 2011 through 2014.

- b) Statement#1 indicates that the "major plant turnaround" of the FCC unit during 2010 resulted in annual CO<sub>2</sub>e emission levels that were not representative of "normal operations". It is unclear to what extent this shutdown resulted in annual refining activity failing to meet planned levels, and thus annual CO<sub>2</sub>e emissions that would not be representative of "normal operations." It is also unclear to what extent the annual impact of the "major plant turnaround" was mitigated by production before and after the shutdown. As such, the CAB requests a discussion of pre and post shutdown mitigation efforts, and the estimated net impact that this shutdown had on annual Refinery operations for 2010 versus that for 2006, 2007, 2008, and 2009.
- c) Statement#1 indicates that an analysis of Refinery operations for the years 2006 – 2010 was performed. While the GHGERP only addresses operations associated with the FCC unit, it is unclear if the analysis identified other factors useful for the assessment of whether calendar year 2010 is representative of normal operations. It is unclear if the analysis considered differences between planned and actual annual production in the assessment of "normal operations." The CAB requests additional information, if available, from the analysis to evaluate the relative suitability of calendar years 2006 through 2010 as representative of baseline GHG emissions. Please include discussions of associated mitigation efforts, and the estimated net impact of any other factors on annual refining activity for 2010 versus that for 2006, 2007, 2008, and 2009. For the purpose of establishing trend information, the CAB requests similar information for calendar years 2011 through 2014.
- d) Statement#2 presents the annual GHG emissions for the facility in 2009, but the GHGERP does not include the supporting documentation needed to confirm your results. Table 1 in your GHGERP includes 2010 GHG emissions for the facility, and this value appears to match the facility total reported in the EPA Facility Level Information on GHGs Tool (FLIGHT) at: <http://qhadata.epa.gov/ghgp/main.do>. However, it is unclear if the annual GHG emissions for calendar years 2009 and 2010 were calculated in a consistent manner. For example, the 2010 value has not been corrected to reflect the current greenhouse gas global warming potentials (GWPs) for methane (CH<sub>4</sub>) and nitrous oxide (N<sub>2</sub>O). To assist in the evaluation of the relative suitability of emission years 2006 – 2010 for establishment of baseline GHG emissions, the CAB requests that you provide the refinery's annual GHG emissions with supporting information and spreadsheet calculations for calendar years 2006, 2007, 2008, 2009, and 2010. Please ensure that the information provided for the annual GHG emission inventories has sufficient detail to enable validation of the calculations. The CAB requests that any inconsistencies in year to year GHG calculation methods be discussed and their impact quantified.
- e) To assist in the evaluation of operating trends, annual GHG emissions information for calendar years 2011 through 2014 is also needed. For the 2011 through 2014 GHG inventories, the CAB requests that you provide confirmation that the EPA

GHG Reporting Program CO<sub>2</sub>e information available at EPA's FLIGHT website (<http://ghgdata.epa.gov/ghgp/main.do>) are accurate, and consistent with the 2006 – 2010 annual GHG emissions discussed previously. The CAB requests that any causes of inaccuracy or inconsistency (e.g., data quality, data source, calculation methods) be discussed and their impact quantified. The CAB requests the submission of updated data and calculations if revisions are needed to ensure accuracy or consistency. Note that the CAB used updated GWPs from the EPA Emission Factor Hub website (<http://www.epa.gov/climateleadership/center-corporate-climate-leadership-ghg-emission-factors-hub>) to correct for the change in GWPs that occurred during the reporting periods. As can be seen in the Table A-3 below, these corrections are insignificant in magnitude.

Table A-3. EPA FLIGHT Annual GHG emissions for Chevron Refinery with GWP Corrections

	GHG Summary Report: <a href="http://ghgdata.epa.gov/ghgp/main.do">http://ghgdata.epa.gov/ghgp/main.do</a>	Chevron Refinery	2010	2011	2012	2013	2014
	CO <sub>2</sub> equivalent emissions from facility subparts C-II, SS, and TT	Metric Tons	529,650.8	560,055.7	568,094.9	462,620.6	536,124.3
	CO <sub>2</sub> equivalent emissions from supplier subparts LL-QQ	Metric Tons	0.0	0.0	0.0	0.0	0.0
	Biogenic CO <sub>2</sub> emissions from facility subparts C-II, SS, and TT	Metric Tons	0.0	0.0	0.0	0.0	0.0
	Reported Total (no GWP corrections)	Metric Tons	529,650.8	560,055.7	568,094.9	462,620.6	536,124.3
	Calculated Total (April 2014 GWP)	Metric Tons	529,748.0	560,159.2	568,194.4	462,620.6	536,124.3
	Difference (Reported - Calculated)	Metric Tons	-97.2	-103.5	-99.5	0.0	0.0
	% Difference	%	-0.01835%	-0.01848%	-0.01752%	-0.00001%	-0.00001%

- f) This initial CAB review examined fuel burning data from annual emissions inventory submissions for calendar years 2006 – 2014. Seven fuels with possible erroneous heat content information were identified. They are summarized below in Table A-4 and documented in more detail in the file "Chev-Ref-2009-review-9.xlsx" located on the enclosed CD. Please see Sheets "2-Review Comments" and "3- ProcessesHeatCO2." The CAB requests confirmation and explanation, or correction of these values.

Table A-4. Fuels with Possible Erroneous Heat Content Information

Emission Year	Fuel Type	Fuel Material Code	SCC	Fuel Heat Content (Annual Ave.)	Fuel Heat Content Unit Numerator	Fuel Heat Content Unit Denominator	Review Comments:
2013	Refinery Gas	553	30600106	1.129	E6BTU	E6FT3S	The "Fuel Heat Content Unit Denominator" changed from "E3BTU" to "E6BTU" after 2012. It is unclear if the "Throughput" values are consistent with "E6BTU". See Sheet "3- ProcessesHeatCO2" for CAB fuel burning related GHG emissions estimates.
2013	Liquid Petroleum Gas (LPG)	178	30600107	91.5	E6BTU	E6BTU	The "Fuel Heat Content Unit Denominator" appears to be incorrect. For this case a corrected value of E3GAL seems plausible. It is unclear if the "Throughput" value and units are consistent with this heat content unit.
2013	Refinery Gas	553	20200701	1.129	E6BTU	E6FT3S	The "Fuel Heat Content Unit Denominator" changed from "E3BTU" to "E6BTU" after 2012. It is unclear if the "Throughput" values are consistent with "E6BTU".
2013	Refinery Gas	553	20200701	111.022	E6BTU	E6FT3S	It appears that the "Fuel Heat Content" for Refinery Gas and Gasoline have been swapped. A corrected value of 1.129 E6BTU/E6FT3S seems plausible. Also the "Fuel Heat Content Unit Denominator" changed from "E3BTU" to "E6BTU" after 2012. It is unclear if the "Throughput" values are consistent with "E6BTU".
2013	Gasoline	127	20201701	1.129	E6BTU	E3GAL	It appears that the "Fuel Heat Content" for Refinery Gas and Gasoline have been swapped. A corrected value of 111.022 E6BTU/E3GAL seems plausible.
2014	Refinery Gas	553	30600106	1.057	E6BTU	E6FT3S	The "Fuel Heat Content Unit Denominator" changed from "E3BTU" to "E6BTU" after 2012. It is unclear if the "Throughput" values are consistent with "E6BTU".
2014	Refinery Gas	553	20200701	1.057	E6BTU	E6FT3S	The "Fuel Heat Content Unit Denominator" changed from "E3BTU" to "E6BTU" after 2012. It is unclear if the "Throughput" values are consistent with "E6BTU".

For your written response to our request for additional information, the CAB also requests that you provide emissions inventory data and supporting calculations in an excel spreadsheet format to enable us to verify your results. Please email the requested information to [CAB.Emissions@doh.hawaii.gov](mailto:CAB.Emissions@doh.hawaii.gov). Also mail a hardcopy of the requested information to:

Clean Air Branch  
Hawaii Department of Health  
919 Ala Moana Boulevard, Room 203  
Honolulu, Hawaii 96814

**Attachment III**  
**Chevron letter with Preliminary Recommendation**  
**Dated June 30, 2016**



Kristi Mitchum  
HES Manager

Chevron Products Company  
Hawaii Refinery  
91-480 Malakole Street  
Kapolei HI 96707-1807  
Tel 808-682-3145  
Fax 808-682-2324  
Kristi.Mitchum@chevron.com

June 30, 2016

**CERTIFIED MAIL No. 7015 0640 0003 9266 0915  
RETURN RECEIPT REQUESTED**

Mr. Nolan Hirai  
Manager, Clean Air Branch  
Environmental Management Division  
919 Ala Moana Boulevard  
Honolulu, Hawaii 96814

**Chevron Hawaii Refinery  
GHG Emission Reduction Plan – Additional Information Request**

Dear Mr. Hirai:

Per your May 27, 2016 request, we are providing a preliminary recommendation for a revised set of information regarding our GHG Emissions Reduction Plan (GHGERP). The recommendations below address the remaining items, originally requested in the Department of Health, Clean Air Branch (CAB) letters dated February 10, 2016 and April 20, 2016. We appreciate your staff's efforts to help clarify the questions concerning the refinery's GHGERP, submitted June 30, 2015.

As indicated in the table below, the refinery has addressed the requested information in items 1, 2 (b), 2(c), 2(e), and 2(f). We plan to provide the information described for items 2(a) and 2(d) below.

Referenced Line Item # for Requested Additional Information (April 20, 2016 CAB letter2)	Status	Preliminary Plan
1	Complete. No further action.	
2a	In progress	Provide dates and supporting process information identifying process unit shutdown periods. Provide utilization-related data supporting the determination that 2010 is not representative of normal source operation. Some or all of this information may be Confidential Business Information (CBI) and will be submitted per DOH's CBI protocol, provided to the refinery by email, June 9, 2016
2b	Complete. No further action.	
2c	Complete. No further action.	

Manager, Clean Air Branch

June 30, 2016

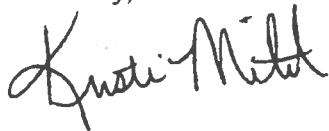
Page 3

2d	In progress	Provide input process data and parameters used in the estimation of 2009 and 2010 GHG emissions, consistent with the GHG MRR reporting.
2e	Complete. No further action.	
2f	Complete. No further action.	

We believe the preliminary recommendation above is consistent with the discussions with your staff. Due to the extensive data collection, we may request additional time to complete collection of the information, as noted in your May 27, 2016 letter.

If you should have questions or require further information, please contact Kristi Mitchum at (808) 682-3145.

Sincerely,



Enclosures

Manager, Clean Air Branch  
June 30, 2016  
Page 3

bcc: Kristi Mitchum

Records File: A-3-0-0-16

Electronic File:

\KAPHIN\DATA1.KAPHI.CHEVRONTEXACO.NET\SHARE\Envr\GHG\Emission Reduction Plan\2016 DOH Request for Additional Information\Correspondence\Jun 30 2016 Preliminary Plan for GHG Additional Information Request.docx

Sch 6/30/16

AS 6/30/16

legal review: Susan Owen 6/30/16

Discussed early draft w/ KM. 6/29/16

**Attachment IV**  
**CD with Chevron Hawaii Refinery GHG Emissions**

**Attachment V**  
**Chevron Hawaii Refinery GHG emissions**

This is a sheet for calculating direct GHG emissions in the Hawaii Refinery.

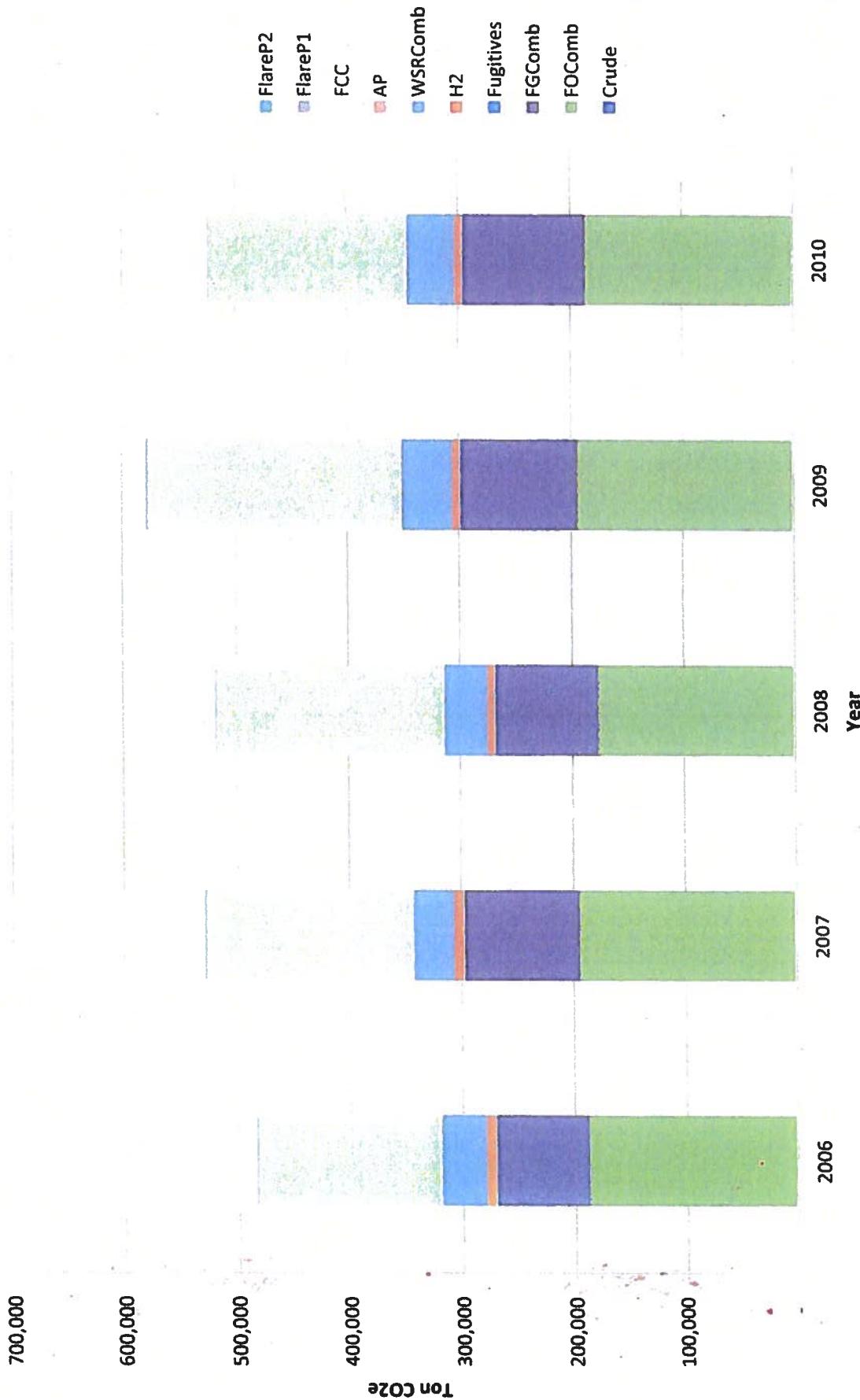
Process Units	Tab
FCC Unit (Regenerator) (Plant 53)	FCC
Fuel Oil Combustion	FO Comb
Fuel Gas Combustion	FG Comb
WSR Combustion (Cogens)	WSR Comb
Flare P1 Sweet	Flare P1
Flare P2 Sour	Flare P2
Acid Plant (Unit 62)	AP
Crude Tank	Crude
Diesel Engine	Diesel Eng
Fugitives	Fugitives
Hydrogen Manufacturing (Unit 57)	H2 Manufac

Color Code
Description
Inputs
Intermediate Expressions
Final Expression (Emission Rate)
Not Used

Attachment V

GHG Calculations 2006-2010.xlsx  
GHG Breakdown

# Hawaii Refinery CO<sub>2</sub>e Emissions



Year	Crude	FCC	FO Comb	FG Comb	Fugitives	Flare P1	Flare P2	H2	AP	WSR Comb	TOTAL (ton CO2e)
2006	46	162,976	186,569	82,136	363	1,044	118	8,993	584	39,700	482,530
2007	46	184,301	193,906	102,017	363	1,053	93	9,354	577	35,745	527,454
2008	42	203,649	175,891	91,098	363	424	99	6,908	486	38,457	517,418
2009	45	226,349	193,346	103,990	363	1,017	117	7,247	485	44,986	577,945
2010	37	177,838	186,197	108,645	363	-	8	7,035	475	42,529	523,117

Demonstration Workbook Calculated Emissions			
Year	Fuel Combustion	FCC	Remaining Sources
2006	308,406	162,976	11,148
			482,530
			536,124
			10%
2007	331,667	184,301	11,486
			527,454
			569,048
			7%
2008	305,447	203,649	8,321
			517,418
			522,593
			1%
2009	342,322	226,349	9,274
			577,945
			581,734
			1%
2010	337,371	177,838	7,907
			523,117
			529,651
			1%

Demonstration Workbook Calculated Emissions			
Year	Fuel Combustion	FCC	Remaining Sources
2006	308,406	162,976	11,148
			482,530
			536,124
			10%
2007	331,667	184,301	11,486
			527,454
			569,048
			7%
2008	305,447	203,649	8,321
			517,418
			522,593
			1%
2009	342,322	226,349	9,274
			577,945
			581,734
			1%
2010	337,371	177,838	7,907
			523,117
			529,651
			1%

Notes on GHG emission calculations for historical years:

GWP potentials in Default Const tab are the current factors, effective 2014, for consistency with the MRR reporting.

Input data averaging periods are different from EPA's NT methodology. Different averaging periods of data such as heating value can cause differences in calculation results.

Some emission factors have changed from the earlier years in this historical data set (e.g. FO combustion). This spreadsheet uses the current EFs for consistency with MRR reporting.

Some sources have been added to the historical years for consistency with the current MRR inventory (AP and Crude).

GHG emissions for internal combustion engines (ICE) have been added to the 2015 and later years inventory to account for newly permitted sources.

Actual Emissions	% Diff
536,124	10%

Attachment V  
 GHG Calculations 2006-2010.xlsx  
 Default Const

Type of Value	Parameter Name	Variable Name	Unit	Variable Value
Global Constant	F to R	STPConv	dimensionless	459.671
Global Constant	MolVolConvEPA, StdCond	StdMolVolEPA	scf/mol	0.8495
Global Constant	Operating Hours in a Month	OperatingHoursMonth	hr	732
Global Constant	kg to tonne	ConvTonneKG	dimensionless	0.001
Global Constant	mmbbl to bbl	ConvBblMmbbl	dimensionless	1000000
Global Constant	tonne to lb	ConvlbTonne	dimensionless	2204.62
Global Constant	kg to lb	ConvLbKg	dimensionless	2.20462
Global Constant	bbl to gal	ConvGalBbl	dimensionless	42
Global Constant	mbtu to mmbtu	ConvMmbtuMbtu	dimensionless	0.001
Global Constant	mscf to scf	ConvScfmScf	dimensionless	1000
Global Constant	g to lb	ConvLbG	dimensionless	0.00220462
Global Constant	btu to mmbtu	ConvMmbtuBtu	dimensionless	0.000001
Global Constant	Minute to Hour	ConvHrMin	dimensionless	0.016666667
Global Constant	Operating Hours in a 30d Month	OperatingHoursMonth	hr	720
Global Constant	Operating Hours in a 31d Month	OperatingHoursMonth	hr	744
Global Constant	Operating Hours in a 28d Month	OperatingHoursMonth	hr	672
Global Constant	Operating Hours in a 29d Month	OperatingHoursMonth	hr	696
Global Constant	Methane GWP 2014 updated value	MGWP	dimensionless	25
Global Constant	Nitrous Oxide GWP 2014 updated value	NGWP	dimensionless	298
Global Constant	Methane GWP old value	oMGWP	dimensionless	21
Global Constant	Nitrous Oxide GWP old value	oNGWP	dimensionless	301

Entity - Proc Unit ID	Material Name	Type of Value	Parameter Name	Variable Name	Unit	Variable Value
Crude Tank	Methane	Global Emission Factor	Deft Emiss Factor, Storage Tanks, EPA Y	EF	tmo/1000000 bbl	0.1
Diesel Engine	Carbon Dioxide Carbon Dioxide Methane Methane Nitrogen Oxide (N2O) Nitrogen Oxide (N2O)	Global Emission Factor Global Emission Factor Global Emission Factor Global Emission Factor Global Emission Factor Global Emission Factor	Comb, Distillate Fuel Oil No. 2, EPA Default HHV, Distillate Fuel Oil No. 2, EPA Comb, Distillate Fuel Oil No. 2, EPA Default HHV, Distillate Fuel Oil No. 2, EPA Comb, Distillate Fuel Oil No. 2, EPA Default HHV, Distillate Fuel Oil No. 2, EPA	EF EF EF EF EF EF	kg/mmbtu mmmbtu/gal kg/mmbtu mmmbtu/gal kg/mmbtu mmmbtu/gal	73.96 0.138 0.003 0.138 0.0006 0.138
FCC Unit (Regenerator) [Plant 53]	Methane Methane Nitrogen Oxide (N2O) Nitrogen Oxide (N2O)	Global Emission Factor Global Emission Factor Global Emission Factor Global Emission Factor	Comb, Petroleum Coke, EPA Comb, Petroleum Products, EPA Comb, Petroleum Coke, EPA Comb, Petroleum Products, EPA	EF_CO2 EF_CH4 EF_CO2 EF_N2O	kg/mmbtu kg/mmbtu kg/mmbtu kg/mmbtu	102.41 0.003 102.41 0.0006
Fuel Oil Combustion	Carbon Dioxide Methane Nitrogen Oxide (N2O)	Global Emission Factor Global Emission Factor Global Emission Factor	Comb, Distillate Fuel Oil No. 6, EPA Comb, Distillate Fuel Oil No. 6, EPA Comb, Distillate Fuel Oil No. 6, EPA	EF EF EF	kg/mmbtu kg/mmbtu kg/mmbtu	75.1 0.003 102.41
Fugitives						
Fuel Gas Combustion	Methane	Global Emission Factor, 2014, 2015	Comb, Natural Gas, Pipeline, EPA	EF	kg/mmbtu	0.0001
	Nitrogen Oxide (N2O)	Global Emission Factor, 2014, 2015	Comb, Natural Gas, Pipeline, EPA	EF	kg/mmbtu	0.0001
	Methane	Global Emission Factor, 2013 and earlier	Comb, Fuel Gas, EPA	EF	kg/mmbtu	0.003
	Nitrogen Oxide (N2O)	Global Emission Factor, 2013 and earlier	Comb, Fuel Gas, EPA	EF	kg/mmbtu	0.0006
Flare P1 Sweet	Carbon Dioxide Methane Methane Nitrogen Oxide (N2O) Nitrogen Oxide (N2O) Methane	Global Emission Factor Global Emission Factor Global Emission Factor Global Emission Factor Global Emission Factor Global Emission Factor	Flr, Refinery Default, EPA Comb, Petroleum Products, EPA Flr, Refinery Default, EPA Comb, Petroleum Products, EPA Flr, Refinery Default, EPA Default weight fraction of carbon in methane in f_Ch4	EF_CO2 EF_CH4 EF_CO2 EF_N2O EF_CO2 dimensionless	kg/mmbtu kg/mmbtu kg/mmbtu kg/mmbtu kg/mmbtu dimensionless	60 0.003 60 0.0006 60 0.4
Flare P2 Sour	Carbon Dioxide Methane Methane Nitrogen Oxide (N2O) Nitrogen Oxide (N2O) Methane	Global Emission Factor Global Emission Factor Global Emission Factor Global Emission Factor Global Emission Factor Global Emission Factor	Flr, Refinery Default, EPA Comb, Petroleum Products, EPA Flr, Refinery Default, EPA Comb, Petroleum Products, EPA Flr, Refinery Default, EPA Default weight fraction of carbon in methane in f_Ch4	EF_CO2 EF_CH4 EF_CO2 EF_N2O EF_CO2 dimensionless	kg/mmbtu kg/mmbtu kg/mmbtu kg/mmbtu kg/mmbtu dimensionless	60 0.003 60 0.0006 60 0.4
Hydrogen Manufacturing (Unit 57)						
Acid Plant [Unit 62]						
WSR Combustion (Cogens)	Carbon Dioxide Methane Nitrogen Oxide (N2O)	Global Emission Factor Global Emission Factor Global Emission Factor	Comb, Naphtha (<401 deg F), EPA Comb, Naphtha (<401 deg F), EPA Comb, Naphtha (<401 deg F), EPA	EF EF EF	kg/mmbtu kg/mmbtu kg/mmbtu	68.02 0.003 0.0006

Attachment V  
GHG Calculations 2006-2010.xlsx

Crude

Month	Year	Process Unit	Emission Scenario	GHG Species	Crude Received	Units	Species Emission Rate Expression	Emission Rate	Species	Units	Converted Rate	Units	MT/Month	CO2e	Comments
Jan	2010	Crude Receiving Tanks	Venting	Methane	1492000	bbl	CrudeReceived * EF / ConvBblMmbbl *	328.929304	Ib/month	0.1492	MT/month	3.73			
Feb	2010	Crude Receiving Tanks	Venting	Methane	440079	bbl	CrudeReceived * EF / ConvBblMmbbl *	97.0206965	Ib/month	0.044079	MT/month	1.1001975			
Mar	2010	Crude Receiving Tanks	Venting	Methane	430569	bbl	CrudeReceived * EF / ConvBblMmbbl *	94.92410288	Ib/month	0.0430569	MT/month	1.0764225			
Apr	2010	Crude Receiving Tanks	Venting	Methane	1050333	bbl	CrudeReceived * EF / ConvBblMmbbl *	231.5585138	Ib/month	0.1050333	MT/month	2.6258325			
May	2010	Crude Receiving Tanks	Venting	Methane	1731924	bbl	CrudeReceived * EF / ConvBblMmbbl *	381.8234289	Ib/month	0.1731924	MT/month	4.32981			
Jun	2010	Crude Receiving Tanks	Venting	Methane	1491503	bbl	CrudeReceived * EF / ConvBblMmbbl *	328.8197344	Ib/month	0.1491503	MT/month	3.7287575			
Jul	2010	Crude Receiving Tanks	Venting	Methane	1386339	bbl	CrudeReceived * EF / ConvBblMmbbl *	305.6350686	Ib/month	0.1386339	MT/month	3.4658475			
Aug	2010	Crude Receiving Tanks	Venting	Methane	1323702	bbl	CrudeReceived * EF / ConvBblMmbbl *	291.8259903	Ib/month	0.1323702	MT/month	3.309255			
Sep	2010	Crude Receiving Tanks	Venting	Methane	1320190	bbl	CrudeReceived * EF / ConvBblMmbbl *	291.0517278	Ib/month	0.132019	MT/month	3.300475			
Oct	2010	Crude Receiving Tanks	Venting	Methane	1762869	bbl	CrudeReceived * EF / ConvBblMmbbl *	386.5466255	Ib/month	0.1762869	MT/month	4.4071725			
Nov	2010	Crude Receiving Tanks	Venting	Methane	1310805	bbl	CrudeReceived * EF / ConvBblMmbbl *	288.9826919	Ib/month	0.1310805	MT/month	3.2770125			
Dec	2010	Crude Receiving Tanks	Venting	Methane	1104842	bbl	CrudeReceived * EF / ConvBblMmbbl *	243.575677	Ib/month	0.1104842	MT/month	2.762105			
Jan	2009	Crude Receiving Tanks	Venting	Methane	1559299	bbl	CrudeReceived * EF / ConvBblMmbbl *	343.761761	Ib/month	0.1559299	MT/month	3.8982475			
Feb	2009	Crude Receiving Tanks	Venting	Methane	1427805	bbl	CrudeReceived * EF / ConvBblMmbbl *	314.7767459	Ib/month	0.1427805	MT/month	3.5695125			
Mar	2009	Crude Receiving Tanks	Venting	Methane	1594532	bbl	CrudeReceived * EF / ConvBblMmbbl *	351.5337138	Ib/month	0.1594532	MT/month	3.98633			
Apr	2009	Crude Receiving Tanks	Venting	Methane	1506419	bbl	CrudeReceived * EF / ConvBblMmbbl *	332.1081456	Ib/month	0.1506419	MT/month	3.7660475			
May	2009	Crude Receiving Tanks	Venting	Methane	1623472.49	bbl	CrudeReceived * EF / ConvBblMmbbl *	357.9139921	Ib/month	0.162347249	MT/month	4.058881225			
Jun	2009	Crude Receiving Tanks	Venting	Methane	1331272	bbl	CrudeReceived * EF / ConvBblMmbbl *	293.498877	Ib/month	0.1331272	MT/month	3.32818			
Jul	2009	Crude Receiving Tanks	Venting	Methane	1529534	bbl	CrudeReceived * EF / ConvBblMmbbl *	337.2041247	Ib/month	0.1529534	MT/month	3.823835			
Aug	2009	Crude Receiving Tanks	Venting	Methane	1506679	bbl	CrudeReceived * EF / ConvBblMmbbl *	332.1634657	Ib/month	0.1506679	MT/month	3.7666975			
Sep	2009	Crude Receiving Tanks	Venting	Methane	1436862	bbl	CrudeReceived * EF / ConvBblMmbbl *	316.7734702	Ib/month	0.1436862	MT/month	3.592155			
Oct	2009	Crude Receiving Tanks	Venting	Methane	1490289	bbl	CrudeReceived * EF / ConvBblMmbbl *	328.5520935	Ib/month	0.1490289	MT/month	3.7257225			
Nov	2009	Crude Receiving Tanks	Venting	Methane	1406602	bbl	CrudeReceived * EF / ConvBblMmbbl *	310.1022901	Ib/month	0.1406602	MT/month	3.516505			
Dec	2009	Crude Receiving Tanks	Venting	Methane	1472692.53	bbl	CrudeReceived * EF / ConvBblMmbbl *	324.6727405	Ib/month	0.147269253	MT/month	3.681731325			
Jan	2008	Crude Receiving Tanks	Venting	Methane	1.397.466	bbl	CrudeReceived * EF / ConvBblMmbbl *	308.0881483	Ib/month	0.1397466	MT/month	3.493665			
Feb	2008	Crude Receiving Tanks	Venting	Methane	1.384.529	bbl	CrudeReceived * EF / ConvBblMmbbl *	305.2360324	Ib/month	0.1384529	MT/month	3.4613225			
Mar	2008	Crude Receiving Tanks	Venting	Methane	1.486.376	bbl	CrudeReceived * EF / ConvBblMmbbl *	327.6884257	Ib/month	0.1486376	MT/month	3.71594			

## Attachment V

## GHG Calculations 2006-2010.xlsx

								Crude
Apr	2008	Crude Receiving Tanks	Venting	Methane	269.218	bbl	CrudeReceived * EF / ConvBblMmbbl *	59.35233872
May	2008	Crude Receiving Tanks	Venting	Methane	1,291.791	bbl	ConvLbTonne	Ib/month
							CrudeReceived * EF / ConvBblMmbbl *	0.0269218
							ConvLbTonne	MT/month
Jun	2008	Crude Receiving Tanks	Venting	Methane	1,623.674	bbl	CrudeReceived * EF / ConvBblMmbbl *	284.7908274
Jul	2008	Crude Receiving Tanks	Venting	Methane	1,627.361	bbl	ConvLbTonne	Ib/month
							CrudeReceived * EF / ConvBblMmbbl *	0.1291791
							ConvLbTonne	MT/month
Aug	2008	Crude Receiving Tanks	Venting	Methane	1,611.706	bbl	CrudeReceived * EF / ConvBblMmbbl *	357.9584174
Sep	2008	Crude Receiving Tanks	Venting	Methane	1,550.789	bbl	ConvLbTonne	Ib/month
							CrudeReceived * EF / ConvBblMmbbl *	0.1623674
							ConvLbTonne	MT/month
Oct	2008	Crude Receiving Tanks	Venting	Methane	1,557.031	bbl	CrudeReceived * EF / ConvBblMmbbl *	358.7712608
Nov	2008	Crude Receiving Tanks	Venting	Methane	1,509.513	bbl	ConvLbTonne	Ib/month
							CrudeReceived * EF / ConvBblMmbbl *	0.1611706
							ConvLbTonne	MT/month
Dec	2008	Crude Receiving Tanks	Venting	Methane	1,356.291	bbl	CrudeReceived * EF / ConvBblMmbbl *	343.2661683
Jan	2007	Crude Receiving Tanks	Venting	Methane	1466545	bbl	ConvLbTonne	Ib/month
Feb	2007	Crude Receiving Tanks	Venting	Methane	1339636	bbl	CrudeReceived * EF / ConvBblMmbbl *	332.7903101
Mar	2007	Crude Receiving Tanks	Venting	Methane	1693629	bbl	ConvLbTonne	Ib/month
							CrudeReceived * EF / ConvBblMmbbl *	0.1550789
							ConvLbTonne	MT/month
Apr	2007	Crude Receiving Tanks	Venting	Methane	1578161	bbl	CrudeReceived * EF / ConvBblMmbbl *	373.3808366
May	2007	Crude Receiving Tanks	Venting	Methane	1600416	bbl	ConvLbTonne	Ib/month
							CrudeReceived * EF / ConvBblMmbbl *	0.1636229
							ConvLbTonne	MT/month
Jun	2007	Crude Receiving Tanks	Venting	Methane	1527688	bbl	CrudeReceived * EF / ConvBblMmbbl *	323.3174438
Jul	2007	Crude Receiving Tanks	Venting	Methane	1602345	bbl	ConvLbTonne	Ib/month
							CrudeReceived * EF / ConvBblMmbbl *	0.1339636
							ConvLbTonne	MT/month
Aug	2007	Crude Receiving Tanks	Venting	Methane	1618201	bbl	CrudeReceived * EF / ConvBblMmbbl *	347.9245304
Sep	2007	Crude Receiving Tanks	Venting	Methane	1509742	bbl	ConvLbTonne	Ib/month
Oct	2007	Crude Receiving Tanks	Venting	Methane	1558936	bbl	CrudeReceived * EF / ConvBblMmbbl *	352.8309122
							ConvLbTonne	Ib/month
Nov	2007	Crude Receiving Tanks	Venting	Methane	1522028	bbl	CrudeReceived * EF / ConvBblMmbbl *	336.7917519
Dec	2007	Crude Receiving Tanks	Venting	Methane	1487195	bbl	ConvLbTonne	Ib/month
							CrudeReceived * EF / ConvBblMmbbl *	0.1578161
							ConvLbTonne	MT/month
Jan	2006	Crude Receiving Tanks	Venting	Methane	1591074	bbl	CrudeReceived * EF / ConvBblMmbbl *	352.7518289
Feb	2006	Crude Receiving Tanks	Venting	Methane	1303237	bbl	ConvLbTonne	Ib/month
Mar	2006	Crude Receiving Tanks	Venting	Methane	1615911	bbl	CrudeReceived * EF / ConvBblMmbbl *	332.8407408
							ConvLbTonne	Ib/month
Apr	2006	Crude Receiving Tanks	Venting	Methane	1616167	bbl	CrudeReceived * EF / ConvBblMmbbl *	335.5493369
May	2006	Crude Receiving Tanks	Venting	Methane	1647856	bbl	ConvLbTonne	Ib/month
							CrudeReceived * EF / ConvBblMmbbl *	0.1509742
							ConvLbTonne	MT/month
Jun	2006	Crude Receiving Tanks	Venting	Methane	1614604	bbl	CrudeReceived * EF / ConvBblMmbbl *	356.7713562
							ConvLbTonne	Ib/month
							CrudeReceived * EF / ConvBblMmbbl *	0.1591074
							ConvLbTonne	MT/month
Jul	2006	Crude Receiving Tanks	Venting	Methane	1549070	bbl	ConvLbTonne	Ib/month
Aug	2006	Crude Receiving Tanks	Venting	Methane	1620232	bbl	CrudeReceived * EF / ConvBblMmbbl *	357.1958572
							ConvLbTonne	Ib/month
Sep	2006	Crude Receiving Tanks	Venting	Methane	1514354	bbl	CrudeReceived * EF / ConvBblMmbbl *	333.8575115
							ConvLbTonne	Ib/month

Attachment V  
GHG Calculations 2006-2010.xlsx

Crude							
Oct	2006	Crude Receiving Tanks	Venting	Methane	1052789	bbl	CrudeReceived * EF / ConvBblMmbbl *
						ConvLbTonne	
Nov	2006	Crude Receiving Tanks	Venting	Methane	1574147	bbl	CrudeReceived * EF / ConvBblMmbbl *
						ConvLbTonne	
Dec	2006	Crude Receiving Tanks	Venting	Methane	1660198	bbl	CrudeReceived * EF / ConvBblMmbbl *
						ConvLbTonne	







Month	Year	Process Unit	Emission Scenario	GHG Species	Inlet Air Flow Rate [FlowRateAir]	Units	Enriched O <sub>2</sub> Flow Rate [FlowRateO2Enrich]	Units	Species Emission Rate Expression	Species Emission Rate	Units	Converted Rate	Units	Mt/Month CO <sub>2</sub> e	Comments
Jan	2007	FCC Unit- Plant 53	Coke Combustion	Carbon Dioxide	10952980	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_CH4 / EF_CO2	1094.111536	Ibs/month	1894.138709	Mt/month	15641.38708	
Jan	2007	FCC Unit- Plant 53	Coke Combustion	Methane	10952980	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_CH4 / EF_CO2	0.489261235	Ibs/month	0.489261235	Mt/month	12.40703	
Jan	2007	FCC Unit- Plant 53	Coke Combustion	Nitrogen Oxide	10952980	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_N2O / EF_CO2	218.0223072	Ibs/month	0.089256247	Mt/month	29.57638	
Feb	2007	FCC Unit- Plant 53	Coke Combustion	Carbon Dioxide	7325280	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_CH4 / EF_CO2	249.782048	Ibs/month	11330.389018	Mt/month		
Feb	2007	FCC Unit- Plant 53	Coke Combustion	Methane	7325280	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_CH4 / EF_CO2	731.416165	Ibs/month	0.33192511	Mt/month	8.28762	
Feb	2007	FCC Unit- Plant 53	Coke Combustion	Nitrogen Oxide	7325280	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_N2O / EF_CO2	146.3482363	Ibs/month	0.068382522	Mt/month	19.78199	
Mar	2007	FCC Unit- Plant 53	Coke Combustion	Carbon Dioxide	9062880	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_CH4 / EF_CO2	30904420.6	Ibs/month	14018.02815	Mt/month		
Mar	2007	FCC Unit- Plant 53	Coke Combustion	Methane	9062880	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_CH4 / EF_CO2	905.3145435	Ibs/month	0.410844258	Mt/month	10.26811	
Mar	2007	FCC Unit- Plant 53	Coke Combustion	Nitrogen Oxide	9062880	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_N2O / EF_CO2	0.08212852	Ibs/month	0.08212852	Mt/month	24.47440	
Apr	2007	FCC Unit- Plant 53	Coke Combustion	Carbon Dioxide	10133860	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_CH4 / EF_CO2	34725348.8	Ibs/month	15751.62559	Mt/month		
Apr	2007	FCC Unit- Plant 53	Coke Combustion	Methane	10133860	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_CH4 / EF_CO2	1017.214157	Ibs/month	0.461428344	Mt/month	11.53571	
Apr	2007	FCC Unit- Plant 53	Coke Combustion	Nitrogen Oxide	10133860	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_N2O / EF_CO2	203.4548314	Ibs/month	0.092253669	Mt/month	27.50113	
May	2007	FCC Unit- Plant 53	Coke Combustion	Carbon Dioxide	93052830	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_CH4 / EF_CO2	32428844.8	Ibs/month	14708.49816	Mt/month		
May	2007	FCC Unit- Plant 53	Coke Combustion	Methane	93052830	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_CH4 / EF_CO2	948.9059551	Ibs/month	0.438970865	Mt/month	10.77177	
May	2007	FCC Unit- Plant 53	Coke Combustion	Nitrogen Oxide	93052830	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_N2O / EF_CO2	169.881319	Ibs/month	0.088174779	Mt/month	25.67981	
Jun	2007	FCC Unit- Plant 53	Coke Combustion	Carbon Dioxide	92628000	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_CH4 / EF_CO2	3165.1620	Ibs/month	14356.055040	Mt/month		
Jun	2007	FCC Unit- Plant 53	Coke Combustion	Carbon Dioxide	92628000	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_CH4 / EF_CO2	32428844.8	Ibs/month	14708.49816	Mt/month	10.51452	
Jun	2007	FCC Unit- Plant 53	Coke Combustion	Methane	92628000	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_CH4 / EF_CO2	948.9059551	Ibs/month	0.438970865	Mt/month	10.77177	
Jul	2007	FCC Unit- Plant 53	Coke Combustion	Nitrogen Oxide	92628000	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_N2O / EF_CO2	17366.43249	Ibs/month	17366.43249	Mt/month		
Jul	2007	FCC Unit- Plant 53	Coke Combustion	Carbon Dioxide	11227860	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_CH4 / EF_CO2	1121.562019	Ibs/month	0.508725279	Mt/month	12.71831	
Jul	2007	FCC Unit- Plant 53	Coke Combustion	Methane	11227860	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_CH4 / EF_CO2	1121.562019	Ibs/month	0.508725279	Mt/month	12.71831	
Aug	2007	FCC Unit- Plant 53	Coke Combustion	Nitrogen Oxide	92628000	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_N2O / EF_CO2	224.3124039	Ibs/month	0.01746516	Mt/month	39.32046	
Aug	2007	FCC Unit- Plant 53	Coke Combustion	Carbon Dioxide	10268640	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_CH4 / EF_CO2	32727054.4	Ibs/month	18905.47893	Mt/month		
Aug	2007	FCC Unit- Plant 53	Coke Combustion	Methane	10268640	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_CH4 / EF_CO2	1091.810011	Ibs/month	0.482327279	Mt/month	12.38093	
Aug	2007	FCC Unit- Plant 53	Coke Combustion	Nitrogen Oxide	10268640	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_N2O / EF_CO2	17366.43249	Ibs/month	17366.43249	Mt/month		
Sep	2007	FCC Unit- Plant 53	Coke Combustion	Carbon Dioxide	10864640	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_CH4 / EF_CO2	3618.18222.4	Ibs/month	16402.74823	Mt/month		
Sep	2007	FCC Unit- Plant 53	Coke Combustion	Methane	10864640	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_CH4 / EF_CO2	1058.324941	Ibs/month	0.48052282	Mt/month	12.01256	
Sep	2007	FCC Unit- Plant 53	Coke Combustion	Nitrogen Oxide	10864640	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_N2O / EF_CO2	2118.36520021	Ibs/month	0.098947556	Mt/month	28.63784	
Oct	2007	FCC Unit- Plant 53	Coke Combustion	Carbon Dioxide	11227860	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_CH4 / EF_CO2	36198185.2	Ibs/month	16418.33749	Mt/month		
Oct	2007	FCC Unit- Plant 53	Coke Combustion	Methane	11227860	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_CH4 / EF_CO2	1060.3316558	Ibs/month	0.480659613	Mt/month	12.02398	
Oct	2007	FCC Unit- Plant 53	Coke Combustion	Nitrogen Oxide	11227860	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_N2O / EF_CO2	212.06833716	Ibs/month	0.098191803	Mt/month	26.66516	
Nov	2007	FCC Unit- Plant 53	Coke Combustion	Carbon Dioxide	9748880	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_CH4 / EF_CO2	33238860.8	Ibs/month	15076.00439	Mt/month		
Nov	2007	FCC Unit- Plant 53	Coke Combustion	Methane	9748880	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_CH4 / EF_CO2	973.6410741	Ibs/month	0.441636868	Mt/month	11.04062	
Nov	2007	FCC Unit- Plant 53	Coke Combustion	Nitrogen Oxide	9748880	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_N2O / EF_CO2	2170754.32	Ibs/month	0.088327338	Mt/month	28.32155	
Dec	2007	FCC Unit- Plant 53	Coke Combustion	Carbon Dioxide	9419280	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_CH4 / EF_CO2	32119744.8	Ibs/month	14569.28849	Mt/month		
Dec	2007	FCC Unit- Plant 53	Coke Combustion	Methane	9419280	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_CH4 / EF_CO2	840.3162821	Ibs/month	0.428725245	Mt/month	10.86922	
Dec	2007	FCC Unit- Plant 53	Coke Combustion	Nitrogen Oxide	9419280	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_N2O / EF_CO2	+	Ibs/month	+	Mt/month	28.45865	
Jan	2008	FCC Unit- Plant 53	Coke Combustion	Carbon Dioxide	9310731846	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_CH4 / EF_CO2	31748585.6	Ibs/month	14401.39144	Mt/month		
Jan	2008	FCC Unit- Plant 53	Coke Combustion	Methane	9310731846	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_CH4 / EF_CO2	830.073108	Ibs/month	0.421674565	Mt/month	10.54686	
Jan	2008	FCC Unit- Plant 53	Coke Combustion	Nitrogen Oxide	9310731846	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_N2O / EF_CO2	127.1814528	Ibs/month	0.07688605	Mt/month	17.19120	
Feb	2008	FCC Unit- Plant 53	Coke Combustion	Carbon Dioxide	6385910358	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_CH4 / EF_CO2	11940858.48	Ibs/month	5419.55914	Mt/month		
Feb	2008	FCC Unit- Plant 53	Coke Combustion	Methane	6385910358	Ibs	0.93	Ibs	CokeBurned * CarbonContent * 44/12 * EF_CH4 / EF_CO2	350.068843	Ibs/month	0.158706843	Mt/month	3.986902	

Mar	2006	FCC Unit- Plant 53	Coke Combustion	Nitrogen Oxide	3503332394	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_N2O / 70/00137759	lb/month	0.031752128	MT/month
Apr	2006	FCC Unit- Plant 53	Coke Combustion	Carbon Dioxide	8164240.557	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	27840600.3	lb/month
Apr	2006	FCC Unit- Plant 53	Coke Combustion	Methane	8164240.557	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	0.565063592	lb/month
Apr	2006	FCC Unit- Plant 53	Coke Combustion	Nitrogen Oxide	8164240.557	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_N2O	815.547233	lb/month
May	2006	FCC Unit- Plant 53	Coke Combustion	Carbon Dioxide	8952108.813	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	165.108247	lb/month
May	2006	FCC Unit- Plant 53	Coke Combustion	Methane	8952108.813	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	30529651.05	lb/month
May	2006	FCC Unit- Plant 53	Coke Combustion	Nitrogen Oxide	8952108.813	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	13846.89061	lb/month
Jun	2006	FCC Unit- Plant 53	Coke Combustion	Carbon Dioxide	8919019.998	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_N2O	84.249229	lb/month
Jun	2006	FCC Unit- Plant 53	Coke Combustion	Methane	8919019.998	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	0.05625152	lb/month
Jun	2006	FCC Unit- Plant 53	Coke Combustion	Nitrogen Oxide	8919019.998	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	0.0812503	lb/month
Jul	2006	FCC Unit- Plant 53	Coke Combustion	Carbon Dioxide	1018566.28	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	30413857.85	lb/month
Jul	2006	FCC Unit- Plant 53	Coke Combustion	Methane	1018566.28	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	635.8072846	lb/month
Jul	2006	FCC Unit- Plant 53	Coke Combustion	Nitrogen Oxide	1018566.28	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	70/00137759	lb/month
Aug	2006	FCC Unit- Plant 53	Coke Combustion	Carbon Dioxide	3804346.838	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	274040860.3	lb/month
Aug	2006	FCC Unit- Plant 53	Coke Combustion	Methane	3804346.838	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	1017.76228	lb/month
Aug	2006	FCC Unit- Plant 53	Coke Combustion	Nitrogen Oxide	3804346.838	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	303.562452	lb/month
Sep	2006	FCC Unit- Plant 53	Coke Combustion	Carbon Dioxide	7983865.613	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	32750822.71	lb/month
Sep	2006	FCC Unit- Plant 53	Coke Combustion	Methane	7983865.613	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	14855.440986	lb/month
Sep	2006	FCC Unit- Plant 53	Coke Combustion	Nitrogen Oxide	7983865.613	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	12628.65395	lb/month
Oct	2006	FCC Unit- Plant 53	Coke Combustion	Carbon Dioxide	11170007.68	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	0.461849745	lb/month
Oct	2006	FCC Unit- Plant 53	Coke Combustion	Methane	11170007.68	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	0.09232949	lb/month
Oct	2006	FCC Unit- Plant 53	Coke Combustion	Nitrogen Oxide	11170007.68	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	14855.740986	lb/month
Nov	2006	FCC Unit- Plant 53	Coke Combustion	Carbon Dioxide	11170007.68	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	0.355174829	lb/month
Nov	2006	FCC Unit- Plant 53	Coke Combustion	Methane	11170007.68	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	10.87046	lb/month
Nov	2006	FCC Unit- Plant 53	Coke Combustion	Nitrogen Oxide	11170007.68	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	25.83663	lb/month
Dec	2006	FCC Unit- Plant 53	Coke Combustion	Carbon Dioxide	11175015.55	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	17277.22972	lb/month
Dec	2006	FCC Unit- Plant 53	Coke Combustion	Methane	11175015.55	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	53681194.14	lb/month
Dec	2006	FCC Unit- Plant 53	Coke Combustion	Nitrogen Oxide	11175015.55	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	30.16412	lb/month
Jan	2007	FCC Unit- Plant 53	Coke Combustion	Carbon Dioxide	11240984.84	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	12318.12364	lb/month
Jan	2007	FCC Unit- Plant 53	Coke Combustion	Methane	11240984.84	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	0.36804729	lb/month
Jan	2007	FCC Unit- Plant 53	Coke Combustion	Nitrogen Oxide	11240984.84	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	0.072169456	lb/month
Feb	2007	FCC Unit- Plant 53	Coke Combustion	Carbon Dioxide	11240984.84	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	27156781.74	lb/month
Feb	2007	FCC Unit- Plant 53	Coke Combustion	Methane	11240984.84	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	768.5311514	lb/month
Feb	2007	FCC Unit- Plant 53	Coke Combustion	Nitrogen Oxide	11240984.84	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	1115.8030982	lb/month
Mar	2007	FCC Unit- Plant 53	Coke Combustion	Carbon Dioxide	11240984.84	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	223.1601984	lb/month
Mar	2007	FCC Unit- Plant 53	Coke Combustion	Methane	11240984.84	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	0.01022383	lb/month
Mar	2007	FCC Unit- Plant 53	Coke Combustion	Nitrogen Oxide	11240984.84	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	17387.01393	lb/month
Apr	2007	FCC Unit- Plant 53	Coke Combustion	Carbon Dioxide	11240984.84	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	12.73339	lb/month
Apr	2007	FCC Unit- Plant 53	Coke Combustion	Methane	11240984.84	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	0.059335434	lb/month
Apr	2007	FCC Unit- Plant 53	Coke Combustion	Nitrogen Oxide	11240984.84	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	0.101687087	lb/month
May	2007	FCC Unit- Plant 53	Coke Combustion	Carbon Dioxide	11240984.84	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	40077783.03	lb/month
May	2007	FCC Unit- Plant 53	Coke Combustion	Methane	11240984.84	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	18178.98821	lb/month
May	2007	FCC Unit- Plant 53	Coke Combustion	Nitrogen Oxide	11240984.84	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	0.532535833	lb/month
Jun	2007	FCC Unit- Plant 53	Coke Combustion	Carbon Dioxide	11240984.84	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	13.31340	lb/month
Jun	2007	FCC Unit- Plant 53	Coke Combustion	Methane	11240984.84	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	0.108507167	lb/month
Jun	2007	FCC Unit- Plant 53	Coke Combustion	Nitrogen Oxide	11240984.84	Ibs	0.93	Ib/C/lb coke	CokeBurned * CarbonContent * 44/12 * EF_Co2	31.73914	lb/month

Month	Year	Process Unit	Emission Scenario	GHG Species	Fuel Use (Liquid Volume) [FuelUsage]	Units	Heat Content (Liquids) HHV	Units	Species Emission Rate Calculation	Emission Rate	Units	Converted Rate	Units	MT/month CO <sub>2</sub> e	Comments
Jan	2010	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	31340	lbh	6327	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * ConvMmbtuBbl	32828971.56	lb/month	14891.44232	lb/month	14891.44232	
Jan	2010	Fuel Oil Combustion Sources	Stationary Comb	Methane	31340	lbh	6327	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * ConvMmbtuBbl	1311.45282	lb/month	5344654.54	lb/month	14.8716135	
Jan	2010	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	31340	lbh	6327	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * ConvMmbtuBbl	262.2800524	lb/month	0.116872908	lb/month	35.4532658	
Feb	2010	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	33916	lbh	6331	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * ConvMmbtuBbl	35522989.07	lb/month	16126.58784	lb/month	16126.58784	
Feb	2010	Fuel Oil Combustion Sources	Stationary Comb	Methane	33918	lbh	6331	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * ConvMmbtuBbl	1420.228288	lb/month	0.644204574	lb/month	16.1051135	
Feb	2010	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	33918	lbh	6331	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * ConvMmbtuBbl	284.04552576	lb/month	0.128840915	lb/month	38.35459261	
Mar	2010	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	33340	lbh	6318	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * ConvMmbtuBbl	34875375.68	lb/month	15819.22321	lb/month	15819.22321	
Mar	2010	Fuel Oil Combustion Sources	Stationary Comb	Methane	33340	lbh	6318	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * ConvMmbtuBbl	1393.157482	lb/month	0.6312836	lb/month	15.798159	
Mar	2010	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	33340	lbh	6318	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * ConvMmbtuBbl	276.631984	lb/month	0.126385272	lb/month	37.66261106	
Apr	2010	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	30450	lbh	6345	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * ConvMmbtuBbl	31988911.51	lb/month	14514.47937	lb/month	14514.47937	
Apr	2010	Fuel Oil Combustion Sources	Stationary Comb	Methane	30450	lbh	6345	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * ConvMmbtuBbl	1278.252124	lb/month	0.5790561	lb/month	14.4951525	
Apr	2010	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	30450	lbh	6345	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * ConvMmbtuBbl	255.6304246	lb/month	0.11586122	lb/month	34.55644356	
May	2010	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	31282	lbh	6351	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * ConvMmbtuBbl	32863516.49	lb/month	14920.28585	lb/month	14920.28585	
May	2010	Fuel Oil Combustion Sources	Stationary Comb	Methane	31282	lbh	6351	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * ConvMmbtuBbl	1313.886575	lb/month	0.586015946	lb/month	14.9003865	
May	2010	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	31282	lbh	6351	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * ConvMmbtuBbl	282.797735	lb/month	0.119203169	lb/month	35.52285338	
Jun	2010	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	33876	lbh	6320	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * ConvMmbtuBbl	3544727.28	lb/month	16078.63353	lb/month	16078.63353	
Jun	2010	Fuel Oil Combustion Sources	Stationary Comb	Methane	33876	lbh	6320	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * ConvMmbtuBbl	1416.0030887	lb/month	642288986	lb/month	16.057224	
Jun	2010	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	33876	lbh	6320	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * ConvMmbtuBbl	283.2006174	lb/month	0.128457782	lb/month	36.28042202	
Jul	2010	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	32359	lbh	6309	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * ConvMmbtuBbl	33800860.57	lb/month	15331.88512	lb/month	15331.88512	
Jul	2010	Fuel Oil Combustion Sources	Stationary Comb	Methane	32359	lbh	6309	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * ConvMmbtuBbl	1350.236904	lb/month	0.612258793	lb/month	15.31146583	
Jul	2010	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	32359	lbh	6309	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * ConvMmbtuBbl	270.0477808	lb/month	0.122491759	lb/month	36.50254406	
Aug	2010	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	32822	lbh	6373	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * ConvMmbtuBbl	36151831.92	lb/month	16398.21462	lb/month	16398.21462	
Aug	2010	Fuel Oil Combustion Sources	Stationary Comb	Methane	32822	lbh	6373	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * ConvMmbtuBbl	1444.147747	lb/month	0.655051778	lb/month	16.3763745	
Aug	2010	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	32822	lbh	6373	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * ConvMmbtuBbl	268.828493	lb/month	0.131011036	lb/month	39.04128861	
Sep	2010	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	28624	lbh	6331	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * ConvMmbtuBbl	31052008.22	lb/month	11084.97075	lb/month	11084.97075	
Sep	2010	Fuel Oil Combustion Sources	Stationary Comb	Methane	28624	lbh	6331	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * ConvMmbtuBbl	1240.657405	lb/month	0.562846532	lb/month	14.0662158	
Sep	2010	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	28624	lbh	6331	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * ConvMmbtuBbl	288.0852854	lb/month	0.112528726	lb/month	33.53335347	
Oct	2010	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	33425	lbh	6363	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * ConvMmbtuBbl	33213323.71	lb/month	15972.51395	lb/month	15972.51395	
Oct	2010	Fuel Oil Combustion Sources	Stationary Comb	Methane	33425	lbh	6363	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * ConvMmbtuBbl	1355.04721	lb/month	0.538049385	lb/month	15.9512453	
Oct	2010	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	33425	lbh	6363	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * ConvMmbtuBbl	281.331481	lb/month	0.127609565	lb/month	38.02776557	
Nov	2010	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	32314	lbh	6359	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * ConvMmbtuBbl	34021461.82	lb/month	15431.96282	lb/month	15431.96282	
Nov	2010	Fuel Oil Combustion Sources	Stationary Comb	Methane	32314	lbh	6359	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * ConvMmbtuBbl	1616454778	lb/month	0.616454778	lb/month	15.4113445	
Nov	2010	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	32314	lbh	6359	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * ConvMmbtuBbl	271.809442	lb/month	0.12329036	lb/month	36.70855301	
Dec	2010	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	33567	lbh	6347	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * ConvMmbtuBbl	33273999.7	lb/month	15000.93615	lb/month	16000.93615	
Dec	2010	Fuel Oil Combustion Sources	Stationary Comb	Methane	33567	lbh	6347	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * ConvMmbtuBbl	1409.081213	lb/month	0.639149247	lb/month	15.97873118	

Dec	2010	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	33567	bbl	6347	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	281.8162426	lb/month	0.127282949	MT/month	38.0932512
Jan	2009	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	36719	bbl	6314	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	383.8556588	lb/month	17411.46583	MT/month	17411.46583
Jan	2009	Fuel Oil Combustion Sources	Stationary Comb	Methane	36719	bbl	6314	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	ConvMmbtu/bbl	lb/month	17895531288	MT/month	17.3826245
Jan	2009	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	36719	bbl	6314	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	153.38221	lb/month	0.13510626	MT/month	41.45566536
Feb	2009	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	33395	bbl	6287	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	308.676442	lb/month	15767.57281	MT/month	15767.57281
Feb	2009	Fuel Oil Combustion Sources	Stationary Comb	Methane	33395	bbl	6287	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	34761506.37	lb/month	629863095	MT/month	15.4657738
Feb	2009	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	33395	bbl	6287	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	1348.608776	lb/month	ConvMmbtu/bbl	ConvMmbtu/bbl	
Mar	2009	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	37900	bbl	6328	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	277.77217553	lb/month	0.125972819	MT/month	37.5384046
Mar	2009	Fuel Oil Combustion Sources	Stationary Comb	Methane	37900	bbl	6328	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	397.06123.18	lb/month	18011.32312	MT/month	18011.32312
Apr	2009	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	37900	bbl	6328	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	1586.20998	lb/month	0.7194936	MT/month	17.98734
Apr	2009	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	33723	bbl	6282	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	317.2419961	lb/month	0.1438972	MT/month	42.8818186
May	2009	Fuel Oil Combustion Sources	Stationary Comb	Methane	33723	bbl	6292	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	1493.362851	lb/month	6.83855348	MT/month	15.9138337
May	2009	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	37900	bbl	6328	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	286.6725303	lb/month	0.12731107	MT/month	37.9386974
Jun	2009	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	35290	bbl	6324	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	369562024.55	lb/month	16760.3644	MT/month	16760.3644
Jun	2009	Fuel Oil Combustion Sources	Stationary Comb	Methane	35290	bbl	6324	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	1476.041327	lb/month	0.6692188	MT/month	16.36047
Jul	2009	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	33723	bbl	6282	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	295.2082654	lb/month	0.133904376	MT/month	39.90350405
Aug	2009	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	31427	bbl	6303	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	327.96229.18	lb/month	14876.13701	MT/month	14876.13701
Aug	2009	Fuel Oil Combustion Sources	Stationary Comb	Methane	31427	bbl	6303	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	1310.102384	lb/month	0.594253143	MT/month	14.85632858
Sep	2009	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	31427	bbl	6303	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	262.0204724	lb/month	0.118950629	MT/month	35.4748732
Sep	2009	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	35350	bbl	6308	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	36919412.61	lb/month	16746.38378	MT/month	16746.38378
Sep	2009	Fuel Oil Combustion Sources	Stationary Comb	Methane	35350	bbl	6308	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	1474.810091	lb/month	6686834	MT/month	16.724085
Sep	2009	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	35350	bbl	6308	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	294.9620182	lb/month	0.13379268	MT/month	39.87021864
Sep	2009	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	33960	bbl	6345	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	35875739.82	lb/month	16162.26262	MT/month	16162.26262
Sep	2009	Fuel Oil Combustion Sources	Stationary Comb	Methane	33960	bbl	6345	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	1125.12942	lb/month	6.6462866	MT/month	16.1607715
Sep	2009	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	33960	bbl	6345	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	285.025884	lb/month	0.12928572	MT/month	38.5271456
Sep	2009	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	34521	bbl	6313	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	36082185.68	lb/month	16356.62358	MT/month	16356.62358
Sep	2009	Fuel Oil Combustion Sources	Stationary Comb	Methane	34521	bbl	6313	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	1441.9885606	lb/month	0.653793219	MT/month	16.34483048
Sep	2009	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	34521	bbl	6313	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	288.273213	lb/month	0.130756544	MT/month	34.95627595
Oct	2009	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	38044	bbl	6299	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	396.76327.04	lb/month	17986.90062	MT/month	17986.90062
Oct	2009	Fuel Oil Combustion Sources	Stationary Comb	Methane	38044	bbl	6299	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	1584.939828	lb/month	0.718917458	MT/month	17.9723367
Oct	2009	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	38044	bbl	6299	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	316.9879657	lb/month	0.143783494	MT/month	42.84748109
Nov	2009	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	27119	bbl	6342	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	284.75646.23	lb/month	12916.35122	MT/month	12916.35122
Nov	2009	Fuel Oil Combustion Sources	Stationary Comb	Methane	27119	bbl	6342	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	1137.50917	lb/month	0.1515665094	MT/month	12.89915235
Nov	2009	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	27119	bbl	6342	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	227.501834	lb/month	0.103193219	MT/month	30.7515792
Dec	2009	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	28856	bbl	6333	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	302.558542.42	lb/month	13724.1531	MT/month	13724.1531
Dec	2009	Fuel Oil Combustion Sources	Stationary Comb	Methane	28856	bbl	6333	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	1208.550163	lb/month	0.54823544	MT/month	13.7058786
Dec	2009	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	28856	bbl	6333	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	241.7303036	lb/month	0.108647029	MT/month	32.67481458

Jan	2008	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	34582	bbl	6312	mbtu/bbl	FuelUsage <sup>HHV</sup> /EF * ConvLbKg *	36140218.72	lb/month	16392.94696	MT/month	16392.94696
Jan	2008	Fuel Oil Combustion Sources	Stationary Comb	Methane	34582	bbl	6312	mbtu/bbl	FuelUsage <sup>HHV</sup> /EF * ConvLbKg *	1443.6836337	lb/month	0.654844752	MT/month	16.3711183
Jan	2008	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	34582	bbl	6312	mbtu/bbl	FuelUsage <sup>HHV</sup> /EF * ConvLbKg *	288.7357674	lb/month	0.3086885	MT/month	39.02874722
Feb	2008	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	32201	bbl	6312	mbtu/bbl	FuelUsage <sup>HHV</sup> /EF * ConvLbKg *	3365.9394.04	lb/month	15264.217667	MT/month	15264.217667
Feb	2008	Fuel Oil Combustion Sources	Stationary Comb	Methane	32201	bbl	6312	mbtu/bbl	FuelUsage <sup>HHV</sup> /EF * ConvLbKg *	1344.284882	lb/month	0.609781.136	MT/month	15.2439534
Feb	2008	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	32201	bbl	6312	mbtu/bbl	FuelUsage <sup>HHV</sup> /EF * ConvLbKg *	268.85639944	lb/month	0.21951627	MT/month	36.34.545491
Mar	2008	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	32628	bbl	6312	mbtu/bbl	FuelUsage <sup>HHV</sup> /EF * ConvLbKg *	34098174.09	lb/month	15468.58699	MT/month	15468.58699
Mar	2008	Fuel Oil Combustion Sources	Stationary Comb	Methane	32628	bbl	6312	mbtu/bbl	FuelUsage <sup>HHV</sup> /EF * ConvLbKg *	1362.110816	lb/month	0.617843808	MT/month	15.4465052
Mar	2008	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	32628	bbl	6312	mbtu/bbl	FuelUsage <sup>HHV</sup> /EF * ConvLbKg *	272.4221632	lb/month	0.123568762	MT/month	36.4224096
Apr	2008	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	8430	bbl	6312	mbtu/bbl	FuelUsage <sup>HHV</sup> /EF * ConvLbKg *	88019844.539	lb/month	3986.083016	MT/month	3986.083016
Apr	2008	Fuel Oil Combustion Sources	Stationary Comb	Methane	8430	bbl	6312	mbtu/bbl	FuelUsage <sup>HHV</sup> /EF * ConvLbKg *	351.9245488	lb/month	0.15563048	MT/month	3.9807762
Apr	2008	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	8430	bbl	6312	mbtu/bbl	FuelUsage <sup>HHV</sup> /EF * ConvLbKg *	70.38490976	lb/month	0.031926096	MT/month	9.513975608
May	2008	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	28750	bbl	6312	mbtu/bbl	FuelUsage <sup>HHV</sup> /EF * ConvLbKg *	30045436.59	lb/month	3623.397	MT/month	3623.397
May	2008	Fuel Oil Combustion Sources	Stationary Comb	Methane	28750	bbl	6312	mbtu/bbl	FuelUsage <sup>HHV</sup> /EF * ConvLbKg *	1200.217174	lb/month	0.54441	MT/month	13.61025
May	2008	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	28750	bbl	6312	mbtu/bbl	FuelUsage <sup>HHV</sup> /EF * ConvLbKg *	240.0433448	lb/month	0.108842	MT/month	32.448535
Jun	2008	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	33223	bbl	6312	mbtu/bbl	FuelUsage <sup>HHV</sup> /EF * ConvLbKg *	347195884	lb/month	15748.73856	MT/month	15748.73856
Jun	2008	Fuel Oil Combustion Sources	Stationary Comb	Methane	33223	bbl	6312	mbtu/bbl	FuelUsage <sup>HHV</sup> /EF * ConvLbKg *	1346.5950093	lb/month	0.629110728	MT/month	15.2777882
Jun	2008	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	33223	bbl	6312	mbtu/bbl	FuelUsage <sup>HHV</sup> /EF * ConvLbKg *	292.2184409	lb/month	0.125822146	MT/month	31.74949939
Jul	2008	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	34999	bbl	6312	mbtu/bbl	FuelUsage <sup>HHV</sup> /EF * ConvLbKg *	36576008.19	lb/month	16590.617197	MT/month	16590.617197
Jul	2008	Fuel Oil Combustion Sources	Stationary Comb	Methane	34999	bbl	6312	mbtu/bbl	FuelUsage <sup>HHV</sup> /EF * ConvLbKg *	1481.092205	lb/month	0.662741084	MT/month	16.5652566
Jul	2008	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	34999	bbl	6312	mbtu/bbl	FuelUsage <sup>HHV</sup> /EF * ConvLbKg *	27.6180358	lb/month	0.132548213	MT/month	39.489335741
Aug	2008	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	32891	bbl	6312	mbtu/bbl	FuelUsage <sup>HHV</sup> /EF * ConvLbKg *	34373024.52	lb/month	15591.3602	MT/month	15591.3602
Aug	2008	Fuel Oil Combustion Sources	Stationary Comb	Methane	32891	bbl	6312	mbtu/bbl	FuelUsage <sup>HHV</sup> /EF * ConvLbKg *	1373.090194	lb/month	0.622823976	MT/month	15.5705394
Aug	2008	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	32891	bbl	6312	mbtu/bbl	FuelUsage <sup>HHV</sup> /EF * ConvLbKg *	281.7483725	lb/month	0.127799064	MT/month	3.08412107
Sep	2008	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	33745	bbl	6312	mbtu/bbl	FuelUsage <sup>HHV</sup> /EF * ConvLbKg *	35265504.62	lb/month	15986.18284	MT/month	15986.18284
Sep	2008	Fuel Oil Combustion Sources	Stationary Comb	Methane	33745	bbl	6312	mbtu/bbl	FuelUsage <sup>HHV</sup> /EF * ConvLbKg *	1408.741862	lb/month	0.63899532	MT/month	15.974843
Sep	2008	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	33745	bbl	6312	mbtu/bbl	FuelUsage <sup>HHV</sup> /EF * ConvLbKg *	281.7483725	lb/month	0.127799064	MT/month	3.08412107
Oct	2008	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	33550	bbl	6312	mbtu/bbl	FuelUsage <sup>HHV</sup> /EF * ConvLbKg *	35667718.18	lb/month	15933.74676	MT/month	15933.74676
Oct	2008	Fuel Oil Combustion Sources	Stationary Comb	Methane	33550	bbl	6312	mbtu/bbl	FuelUsage <sup>HHV</sup> /EF * ConvLbKg *	1400.601259	lb/month	0.6353028	MT/month	15.88257
Oct	2008	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	33550	bbl	6312	mbtu/bbl	FuelUsage <sup>HHV</sup> /EF * ConvLbKg *	280.1202518	lb/month	0.1210656	MT/month	37.8640688
Nov	2008	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	31964	bbl	6312	mbtu/bbl	FuelUsage <sup>HHV</sup> /EF * ConvLbKg *	33404255.14	lb/month	15151.93328	MT/month	15151.93328
Nov	2008	Fuel Oil Combustion Sources	Stationary Comb	Methane	31964	bbl	6312	mbtu/bbl	FuelUsage <sup>HHV</sup> /EF * ConvLbKg *	1334.391018	lb/month	0.605270304	MT/month	15.1317576
Nov	2008	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	31964	bbl	6312	mbtu/bbl	FuelUsage <sup>HHV</sup> /EF * ConvLbKg *	266.8782035	lb/month	0.121054061	MT/month	36.0711012
Dec	2008	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	32841	bbl	6312	mbtu/bbl	FuelUsage <sup>HHV</sup> /EF * ConvLbKg *	34320771.59	lb/month	15567.65864	MT/month	15567.65864
Dec	2008	Fuel Oil Combustion Sources	Stationary Comb	Methane	32841	bbl	6312	mbtu/bbl	FuelUsage <sup>HHV</sup> /EF * ConvLbKg *	1371.002885	lb/month	0.621877176	MT/month	15.5468294
Dec	2008	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	32841	bbl	6312	mbtu/bbl	FuelUsage <sup>HHV</sup> /EF * ConvLbKg *	274.2005572	lb/month	0.124375435	MT/month	37.06387969
Jan	2007	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	31350	bbl	6312	mbtu/bbl	FuelUsage <sup>HHV</sup> /EF * ConvLbKg *	32773039.71	lb/month	14865.61843	MT/month	14865.61843

Attachment V  
GHG Calculations 2006-2010.xlsx  
FO\_Comb

Jan	2007	Fuel Oil Combustion Sources	Stationary Comb	Methane	31360	bbl	6312	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	1309.17602	lb/month	0.59383296	MT/month	14.845824
Jan	2007	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	31360	bbl	6312	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	261.8352041	lb/month	0.13765592	MT/month	35.924442
Feb	2007	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	28116	bbl	6312	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	29382869.4	lb/month	13327.86122	MT/month	
Feb	2007	Fuel Oil Combustion Sources	Stationary Comb	Methane	28116	bbl	6312	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	1173.749776	lb/month	0.33404576	MT/month	13.316144
Feb	2007	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	28116	bbl	6312	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	234.7499553	lb/month	0.06460915	MT/month	31.73131273
Mar	2007	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	36763	bbl	6312	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	384.19491.67	lb/month	7426.80301	MT/month	17426.80301
Mar	2007	Fuel Oil Combustion Sources	Stationary Comb	Methane	36763	bbl	6312	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	1524.733356	lb/month	0.696144168	MT/month	17.4026042
Mar	2007	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	36763	bbl	6312	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	308.9466711	lb/month	0.33228834	MT/month	41.98192411
Apr	2007	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	34034	bbl	6312	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	35567526.58	lb/month	16133.77865	MT/month	16133.77865
Apr	2007	Fuel Oil Combustion Sources	Stationary Comb	Methane	34034	bbl	6312	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	1420.8066854	lb/month	0.644467824	MT/month	16.1116856
Apr	2007	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	34034	bbl	6312	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	284.1613308	lb/month	0.120893565	MT/month	38.1020231
May	2007	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	38036	bbl	6312	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	39749851.35	lb/month	18030.25072	MT/month	18030.25072
May	2007	Fuel Oil Combustion Sources	Stationary Comb	Methane	38036	bbl	6312	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	1567.376805	lb/month	0.729249696	MT/month	18.0826224
May	2007	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	38036	bbl	6312	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	317.575377	lb/month	0.144049539	MT/month	42.92585188
Jun	2007	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	38318	bbl	6312	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	40044557.89	lb/month	18163.92752	MT/month	18163.92752
Jun	2007	Fuel Oil Combustion Sources	Stationary Comb	Methane	38318	bbl	6312	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	1589.84345	lb/month	0.72559648	MT/month	18.139712
Jun	2007	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	38316	bbl	6312	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	319.92989	lb/month	0.14511793	MT/month	43.2451302
Jul	2007	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	34045	bbl	6312	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	35579022.22	lb/month	16138.3522	MT/month	16138.3522
Jul	2007	Fuel Oil Combustion Sources	Stationary Comb	Methane	34045	bbl	6312	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	1421.265868	lb/month	0.64467612	MT/month	16.116903
Jul	2007	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	34045	bbl	6312	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	284.2531735	lb/month	0.120893524	MT/month	38.12286975
Aug	2007	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	34395	bbl	6312	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	35844792.75	lb/month	16304.30312	MT/month	16304.30312
Aug	2007	Fuel Oil Combustion Sources	Stationary Comb	Methane	34395	bbl	6312	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	1435.87207	lb/month	0.65130372	MT/month	16.282563
Aug	2007	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	34395	bbl	6312	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	287.1754414	lb/month	0.130289744	MT/month	38.81770171
Sep	2007	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	31273	bbl	6312	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	32682119.6	lb/month	14824.37772	MT/month	14824.37772
Sep	2007	Fuel Oil Combustion Sources	Stationary Comb	Methane	31273	bbl	6312	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	1305.544059	lb/month	0.52165528	MT/month	14.80463382
Sep	2007	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	31273	bbl	6312	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	261.1086117	lb/month	0.118437106	MT/month	35.29425747
Oct	2007	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	35140	bbl	6312	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	36723361.46	lb/month	16657.45637	MT/month	16657.45637
Oct	2007	Fuel Oil Combustion Sources	Stationary Comb	Methane	35140	bbl	6312	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	1486.978487	lb/month	16654.41104	MT/month	16.332276
Oct	2007	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	35140	bbl	6312	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	293.3955974	lb/month	0.130982208	MT/month	39.65649798
Nov	2007	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	32072	bbl	6312	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	335171721.48	lb/month	15203.12865	MT/month	15203.12865
Nov	2007	Fuel Oil Combustion Sources	Stationary Comb	Methane	32072	bbl	6312	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	1338.89966	lb/month	0.607315392	MT/month	15.122848
Nov	2007	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	32072	bbl	6312	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	267.779319	lb/month	0.121463078	MT/month	36.19595736
Dec	2007	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	34128	bbl	6312	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	35657672.09	lb/month	16177.73679	MT/month	16177.73679
Dec	2007	Fuel Oil Combustion Sources	Stationary Comb	Methane	34128	bbl	6312	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	1124.730842	lb/month	0.646247808	MT/month	16.1561952
Dec	2007	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	34128	bbl	6312	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	244.9461685	lb/month	0.129245562	MT/month	36.51638396
Jan	2008	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	35662	bbl	6312	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	37268482.08	lb/month	16904.90065	MT/month	16904.90065
Jan	2008	Fuel Oil Combustion Sources	Stationary Comb	Methane	35662	bbl	6312	mbtu/bbl	FuelUsage*HRV*EF * ConvLbKg *	1488.770256	lb/month	0.675295632	MT/month	16.8223938

FO Comb

Jan	2006	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	35662	bbi	6312	mbtu/bbl	FuelUsage*HV*EF * ConvLbkg * 297.754/0512	lb/month	0.13569/126	Mt/month	40.247/61967
Feb	2006	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	26270	bbi	6312	mbtu/bbl	FuelUsage*HV*EF * ConvLbkg * 27453691.11	lb/month	12452.79562	Mt/month	12452.79562
Feb	2006	Fuel Oil Combustion Sources	Stationary Comb	Methane	26270	bbi	6312	mbtu/bbl	FuelUsage*HV*EF * ConvLbkg * ConvMmbtuBbl	lb/month	1497448/72	Mt/month	12.382/18
Feb	2006	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	26270	bbi	6312	mbtu/bbl	FuelUsage*HV*EF * ConvLbkg * 1096.685397	lb/month	0.099489744	Mt/month	28.647/94371
Mar	2006	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	35910	bbi	6312	mbtu/bbl	FuelUsage*HV*EF * ConvLbkg * 218.337/0784	lb/month	37536477.1	lb/month	17028.25264
Mar	2006	Fuel Oil Combustion Sources	Stationary Comb	Methane	35918	bbi	6312	mbtu/bbl	FuelUsage*HV*EF * ConvLbkg * 1499.457407	lb/month	680143248	lb/month	17.0035512
Mar	2006	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	35918	bbi	6312	mbtu/bbl	FuelUsage*HV*EF * ConvLbkg * 289.8914815	lb/month	0.13802865	lb/month	40.5385758
Apr	2006	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	34843	bbi	6312	mbtu/bbl	FuelUsage*HV*EF * ConvLbkg * 364.12979/03	lb/month	16516.6691	lb/month	16516.6691
Apr	2006	Fuel Oil Combustion Sources	Stationary Comb	Methane	34843	bbi	6312	mbtu/bbl	FuelUsage*HV*EF * ConvLbkg * 1454.579722	lb/month	0.659787048	lb/month	15.496762
May	2006	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	34843	bbi	6312	mbtu/bbl	FuelUsage*HV*EF * ConvLbkg * 290.9159444	lb/month	0.13195741	lb/month	39.3233866
May	2006	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	35450	bbi	6312	mbtu/bbl	FuelUsage*HV*EF * ConvLbkg * 37047.739/84	lb/month	16804.40604	lb/month	16804.40604
May	2006	Fuel Oil Combustion Sources	Stationary Comb	Methane	35450	bbi	6312	mbtu/bbl	FuelUsage*HV*EF * ConvLbkg * 1479.719959	lb/month	16772812	lb/month	16.78203
May	2006	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	35450	bbi	6312	mbtu/bbl	FuelUsage*HV*EF * ConvLbkg * 295.98339918	lb/month	0.13425624	lb/month	40.00835952
Jun	2006	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	31973	bbi	6312	mbtu/bbl	FuelUsage*HV*EF * ConvLbkg * 334.13660/67	lb/month	15156.19956	lb/month	15156.19956
Jun	2006	Fuel Oil Combustion Sources	Stationary Comb	Methane	31973	bbi	6312	mbtu/bbl	FuelUsage*HV*EF * ConvLbkg * 1334.765738	lb/month	0.605440728	lb/month	15.1360182
Jun	2006	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	31973	bbi	6312	mbtu/bbl	FuelUsage*HV*EF * ConvLbkg * 266.9533476	lb/month	0.121088148	lb/month	36.08428759
Jul	2006	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	32727	bbi	6312	mbtu/bbl	FuelUsage*HV*EF * ConvLbkg * 34201.654/9	lb/month	15513.61908	lb/month	15513.61908
Jul	2006	Fuel Oil Combustion Sources	Stationary Comb	Methane	32727	bbi	6312	mbtu/bbl	FuelUsage*HV*EF * ConvLbkg * 1386.243738	lb/month	0.619178472	lb/month	15.4929618
Jul	2006	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	32727	bbi	6312	mbtu/bbl	FuelUsage*HV*EF * ConvLbkg * 273.2487475	lb/month	0.123943694	lb/month	36.93522993
Aug	2006	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	35127	bbi	6312	mbtu/bbl	FuelUsage*HV*EF * ConvLbkg * 367.09775/7	lb/month	16651.29396	lb/month	16651.29396
Aug	2006	Fuel Oil Combustion Sources	Stationary Comb	Methane	35127	bbi	6312	mbtu/bbl	FuelUsage*HV*EF * ConvLbkg * 1466.43578	lb/month	0.665164872	lb/month	16.629718
Aug	2006	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	35127	bbi	6312	mbtu/bbl	FuelUsage*HV*EF * ConvLbkg * 233.287156	lb/month	0.133032974	lb/month	39.6432637
Sep	2006	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	32895	bbi	6312	mbtu/bbl	FuelUsage*HV*EF * ConvLbkg * 34377204/76	lb/month	15593.25632	lb/month	15593.25632
Sep	2006	Fuel Oil Combustion Sources	Stationary Comb	Methane	32895	bbi	6312	mbtu/bbl	FuelUsage*HV*EF * ConvLbkg * 1373.257181	lb/month	0.62259972	lb/month	15.572493
Sep	2006	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	32895	bbi	6312	mbtu/bbl	FuelUsage*HV*EF * ConvLbkg * 274.6514361	lb/month	0.124579844	lb/month	37.12482331
Oct	2006	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	25757	bbi	6312	mbtu/bbl	FuelUsage*HV*EF * ConvLbkg * 269.17576/01	lb/month	12209.62162	lb/month	12209.62162
Oct	2006	Fuel Oil Combustion Sources	Stationary Comb	Methane	25757	bbi	6312	mbtu/bbl	FuelUsage*HV*EF * ConvLbkg * 107.5.269348	lb/month	0.487734552	lb/month	12.1933638
Oct	2006	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	25757	bbi	6312	mbtu/bbl	FuelUsage*HV*EF * ConvLbkg * 215.0536956	lb/month	0.097544891	lb/month	25.0583793
Nov	2006	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	33146	bbi	6312	mbtu/bbl	FuelUsage*HV*EF * ConvLbkg * 346.39514/48	lb/month	15712.23816	lb/month	15712.23816
Nov	2006	Fuel Oil Combustion Sources	Stationary Comb	Methane	33146	bbi	6312	mbtu/bbl	FuelUsage*HV*EF * ConvLbkg * 1383.735598	lb/month	0.627552656	lb/month	15.6913164
Nov	2006	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	33146	bbi	6312	mbtu/bbl	FuelUsage*HV*EF * ConvLbkg * 276.7471197	lb/month	0.125530531	lb/month	37.4080983
Dec	2006	Fuel Oil Combustion Sources	Stationary Comb	Carbon Dioxide	32487	bbi	6312	mbtu/bbl	FuelUsage*HV*EF * ConvLbkg * 339.5020/82	lb/month	15399.85159	lb/month	15399.85159
Dec	2006	Fuel Oil Combustion Sources	Stationary Comb	Methane	32487	bbi	6312	mbtu/bbl	FuelUsage*HV*EF * ConvLbkg * 1356.224534	lb/month	0.615173832	lb/month	15.3793458
Dec	2006	Fuel Oil Combustion Sources	Stationary Comb	Nitrogen Oxide	32487	bbi	6312	mbtu/bbl	FuelUsage*HV*EF * ConvLbkg * 271.2449067	lb/month	0.123034766	lb/month	36.66438309



































Month	Year	Process Unit	Emission Scenario	GHG Species	Freshstock Volume [Fecofloc<1]	Units	Carbon Content [CarbonContent]	Units	Molecular Weight [MW]	Units	Freshstock Volume at Standard Conditions [STP] [m³]	Feedstock Volume at STP [Fecofloc<1]	Units	Emission Rate Expression [f(FecoflocCalc)]	Units	Emission Rate Expression	Units	Conversion Rate	Units	MT/month	CO2e	Comments
Jan	2010	Urt 51 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	4028.530228	m³/d	0.708	kg/d	28.33	kg/m³	4028.530228 * CarbonContent	4028.530228	kg/month	441.72 * FecoflocCalc * CarbonContent	kg/month	587.028458	kg/month	452.250026	kg/month	452.250026		
Feb	2010	Urt 51 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	5709.205444	m³/d	0.708	kg/d	28.24	kg/m³	5709.205444 * (0.8 * STPComv) / (0.8 * STPComv)	5709.205444	kg/month	441.72 * FecoflocCalc * CarbonContent	kg/month	587.028458	kg/month	581.721428	kg/month	581.721428		
Mar	2010	Urt 51 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	5347.380091	m³/d	0.708	kg/d	28.54	kg/m³	5347.380091 * (0.8 * STPComv) / (0.8 * STPComv)	5347.380091	kg/month	441.72 * FecoflocCalc * CarbonContent	kg/month	587.028458	kg/month	581.017934	kg/month	581.017934		
Apr	2010	Urt 51 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	7700.19174	m³/d	0.708	kg/d	27.08	kg/m³	7700.19174 * (0.8 * STPComv) / (0.8 * STPComv)	7700.19174	kg/month	441.72 * FecoflocCalc * CarbonContent	kg/month	781.168516	kg/month	772.485009	kg/month	772.485009		
May	2010	Urt 51 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	8114.524072	m³/d	0.708	kg/d	28.76	kg/m³	8114.524072 * (0.8 * STPComv) / (0.8 * STPComv)	8114.524072	kg/month	441.72 * FecoflocCalc * CarbonContent	kg/month	824.030803	kg/month	846.778312	kg/month	846.778312		
Jun	2010	Urt 51 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	9105.35409	m³/d	0.708	kg/d	27.51	kg/m³	9105.35409 * (0.8 * STPComv) / (0.8 * STPComv)	9105.35409	kg/month	441.72 * FecoflocCalc * CarbonContent	kg/month	902.309794	kg/month	911.128757	kg/month	911.128757		
Jul	2010	Urt 51 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	3003.620712	m³/d	0.708	kg/d	28.00	kg/m³	3003.620712 * (0.8 * STPComv) / (0.8 * STPComv)	3003.620712	kg/month	441.72 * FecoflocCalc * CarbonContent	kg/month	311.683079	kg/month	311.683079	kg/month	311.683079		
Aug	2010	Urt 51 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	5023.013865	m³/d	0.708	kg/d	28.91	kg/m³	5023.013865 * (0.8 * STPComv) / (0.8 * STPComv)	5023.013865	kg/month	441.72 * FecoflocCalc * CarbonContent	kg/month	581.194948	kg/month	580.295257	kg/month	580.295257		
Sep	2010	Urt 51 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	6012.950504	m³/d	0.708	kg/d	28.76	kg/m³	6012.950504 * (0.8 * STPComv) / (0.8 * STPComv)	6012.950504	kg/month	441.72 * FecoflocCalc * CarbonContent	kg/month	602.309794	kg/month	602.305715	kg/month	602.305715		
Oct	2010	Urt 51 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	4793.028531	m³/d	0.708	kg/d	28.00	kg/m³	4793.028531 * (0.8 * STPComv) / (0.8 * STPComv)	4793.028531	kg/month	441.72 * FecoflocCalc * CarbonContent	kg/month	5085.918877	kg/month	5084.971507	kg/month	5084.971507		
Nov	2010	Urt 51 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	5253.122072	m³/d	0.708	kg/d	28.50	kg/m³	5253.122072 * (0.8 * STPComv) / (0.8 * STPComv)	5253.122072	kg/month	441.72 * FecoflocCalc * CarbonContent	kg/month	511.429763	kg/month	510.478124	kg/month	510.478124		
Dec	2010	Urt 51 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	5501.854267	m³/d	0.708	kg/d	27.34	kg/m³	5501.854267 * (0.8 * STPComv) / (0.8 * STPComv)	5501.854267	kg/month	441.72 * FecoflocCalc * CarbonContent	kg/month	510.203574	kg/month	513.487357	kg/month	513.487357		
Jan	2009	Urt 51 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	5950.684111	m³/d	0.801	kg/d	28.00	kg/m³	5950.684111 * (0.8 * STPComv) / (0.8 * STPComv)	5950.684111	kg/month	441.72 * FecoflocCalc * CarbonContent	kg/month	5055.918877	kg/month	5054.971507	kg/month	5054.971507		
Feb	2009	Urt 51 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	5053.646567	m³/d	0.801	kg/d	28.50	kg/m³	5053.646567 * (0.8 * STPComv) / (0.8 * STPComv)	5053.646567	kg/month	441.72 * FecoflocCalc * CarbonContent	kg/month	511.429763	kg/month	510.478124	kg/month	510.478124		
Mar	2009	Urt 51 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	4793.473046	m³/d	0.801	kg/d	28.00	kg/m³	4793.473046 * (0.8 * STPComv) / (0.8 * STPComv)	4793.473046	kg/month	441.72 * FecoflocCalc * CarbonContent	kg/month	5085.918877	kg/month	5084.971507	kg/month	5084.971507		
Apr	2009	Urt 51 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	5950.684111	m³/d	0.801	kg/d	27.28	kg/m³	5950.684111 * (0.8 * STPComv) / (0.8 * STPComv)	5950.684111	kg/month	441.72 * FecoflocCalc * CarbonContent	kg/month	5055.918877	kg/month	5054.971507	kg/month	5054.971507		
May	2009	Urt 51 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	5053.646567	m³/d	0.801	kg/d	28.00	kg/m³	5053.646567 * (0.8 * STPComv) / (0.8 * STPComv)	5053.646567	kg/month	441.72 * FecoflocCalc * CarbonContent	kg/month	511.429763	kg/month	510.478124	kg/month	510.478124		
Jun	2009	Urt 51 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	4793.473046	m³/d	0.801	kg/d	28.00	kg/m³	4793.473046 * (0.8 * STPComv) / (0.8 * STPComv)	4793.473046	kg/month	441.72 * FecoflocCalc * CarbonContent	kg/month	5085.918877	kg/month	5084.971507	kg/month	5084.971507		
Jul	2009	Urt 51 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	5950.684111	m³/d	0.801	kg/d	27.34	kg/m³	5950.684111 * (0.8 * STPComv) / (0.8 * STPComv)	5950.684111	kg/month	441.72 * FecoflocCalc * CarbonContent	kg/month	5085.918877	kg/month	5084.971507	kg/month	5084.971507		
Aug	2009	Urt 51 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	5053.646567	m³/d	0.801	kg/d	28.00	kg/m³	5053.646567 * (0.8 * STPComv) / (0.8 * STPComv)	5053.646567	kg/month	441.72 * FecoflocCalc * CarbonContent	kg/month	511.429763	kg/month	510.478124	kg/month	510.478124		
Sep	2009	Urt 51 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	4793.473046	m³/d	0.801	kg/d	28.00	kg/m³	4793.473046 * (0.8 * STPComv) / (0.8 * STPComv)	4793.473046	kg/month	441.72 * FecoflocCalc * CarbonContent	kg/month	5085.918877	kg/month	5084.971507	kg/month	5084.971507		
Oct	2009	Urt 51 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	5950.684111	m³/d	0.801	kg/d	27.28	kg/m³	5950.684111 * (0.8 * STPComv) / (0.8 * STPComv)	5950.684111	kg/month	441.72 * FecoflocCalc * CarbonContent	kg/month	5055.918877	kg/month	5054.971507	kg/month	5054.971507		
Nov	2009	Urt 51 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	5053.646567	m³/d	0.801	kg/d	28.00	kg/m³	5053.646567 * (0.8 * STPComv) / (0.8 * STPComv)	5053.646567	kg/month	441.72 * FecoflocCalc * CarbonContent	kg/month	511.429763	kg/month	510.478124	kg/month	510.478124		
Dec	2009	Urt 51 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	4793.473046	m³/d	0.801	kg/d	28.00	kg/m³	4793.473046 * (0.8 * STPComv) / (0.8 * STPComv)	4793.473046	kg/month	441.72 * FecoflocCalc * CarbonContent	kg/month	5085.918877	kg/month	5084.971507	kg/month	5084.971507		
Jan	2008	Urt 51 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	5053.646567	m³/d	0.719	kg/d	28.76	kg/m³	5053.646567 * (0.8 * STPComv) / (0.8 * STPComv)	5053.646567	kg/month	441.72 * FecoflocCalc * CarbonContent	kg/month	511.429763	kg/month	510.478124	kg/month	510.478124		
Feb	2008	Urt 51 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	6007.900018	m³/d	0.719	kg/d	28.00	kg/m³	6007.900018 * (0.8 * STPComv) / (0.8 * STPComv)	6007.900018	kg/month	441.72 * FecoflocCalc * CarbonContent	kg/month	602.308008	kg/month	601.265062	kg/month	601.265062		
Mar	2008	Urt 51 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	5621.497164	m³/d	0.719	kg/d	28.00	kg/m³	5621.497164 * (0.8 * STPComv) / (0.8 * STPComv)	5621.497164	kg/month	441.72 * FecoflocCalc * CarbonContent	kg/month	563.720522	kg/month	562.020322	kg/month	562.020322		
Apr	2008	Urt 51 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	5621.497164	m³/d	0.719	kg/d	28.00	kg/m³	5621.497164 * (0.8 * STPComv) / (0.8 * STPComv)	5621.497164	kg/month	441.72 * FecoflocCalc * CarbonContent	kg/month	563.720522	kg/month	562.020322	kg/month	562.020322		
May	2008	Urt 51 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	5621.497164	m³/d	0.719	kg/d	28.00	kg/m³	5621.497164 * (0.8 * STPComv) / (0.8 * STPComv)	5621.497164	kg/month	441.72 * FecoflocCalc * CarbonContent	kg/month	563.720522	kg/month	562.020322	kg/month	562.020322		
Jun	2008	Urt 51 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	5621.497164	m³/d	0.719	kg/d	28.00	kg/m³	5621.497164 * (0.8 * STPComv) / (0.8 * STPComv)	5621.497164	kg/month	441.72 * FecoflocCalc * CarbonContent	kg/month	563.720522	kg/month	562.020322	kg/month	562.020322		
Jul	2008	Urt 51 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	5621.497164	m³/d	0.719	kg/d	28.00	kg/m³	5621.497164 * (0.8 * STPComv) / (0.8 * STPComv)	5621.497164	kg/month	441.72 * FecoflocCalc * CarbonContent	kg/month	563.720522	kg/month	562.020322	kg/month	562.020322		
Aug	2008	Urt 51 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	5621.497164	m³/d	0.719	kg/d	28.00	kg/m³	5621.497164 * (0.8 * STPComv) / (0.8 * STPComv)	5621.497164	kg/month	441.72 * FecoflocCalc * CarbonContent	kg/month	563.720522	kg/month	562.020322	kg/month	562.020322		

Sep	2008	Unit 57 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	7611 4440097	mod	0.719	Br/B	10 15842881	Br-B-mol	Fuelback * (B8 * STPCavr) / 7728 617351	mod	44.172 * Feedstock/Cole * CarbonContent * (MW * Fuel * StabMol/MEPa) * Com/LDG	1073553 488	Br/month	459 51320781
Oct	2008	Unit 57 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	6320 474053	mod	0.719	Br/B	10 15842881	Br-B-mol	Fuelback * (B8 * STPCavr) / 8448 5650001	mod	44.172 * Feedstock/Cole * CarbonContent * (MW * Fuel * StabMol/MEPa) * Com/LDG	1107422 688	Br/month	502 3180793
Nov	2008	Unit 57 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	9700 4485	mod	0.719	Br/B	10 15842881	Br-B-mol	Fuelback * (B8 * STPCavr) / 8841 164112	mod	44.172 * Feedstock/Cole * CarbonContent * (MW * Fuel * StabMol/MEPa) * Com/LDG	1303070 201	Br/month	591 0565038
Dec	2008	Unit 57 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	5604 485004	mod	0.719	Br/B	10 15842881	Br-B-mol	Fuelback * (B8 * STPCavr) / 10107 70757	mod	44.172 * Feedstock/Cole * CarbonContent * (MW * Fuel * StabMol/MEPa) * Com/LDG	1324900 424	Br/month	600 8654378
Jan	2009	Unit 57 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	1347 42070	mod	0.719	Br/B	10 15842881	Br-B-mol	Fuelback * (B8 * STPCavr) / 13885 06208	mod	44.172 * Feedstock/Cole * CarbonContent * (MW * Fuel * StabMol/MEPa) * Com/LDG	1785123 058	Br/month	614 2550222
Feb	2009	Unit 57 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	10245 81055	mod	0.719	Br/B	10 15842881	Br-B-mol	Fuelback * (B8 * STPCavr) / 10402 646835	mod	44.172 * Feedstock/Cole * CarbonContent * (MW * Fuel * StabMol/MEPa) * Com/LDG	1303091 686	Br/month	618 5606868
Mar	2009	Unit 57 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	13277 5386	mod	0.719	Br/B	10 15842881	Br-B-mol	Fuelback * (B8 * STPCavr) / 13786 55403	mod	44.172 * Feedstock/Cole * CarbonContent * (MW * Fuel * StabMol/MEPa) * Com/LDG	1807117 107	Br/month	619 0656062
Apr	2009	Unit 57 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	13458 07723	mod	0.719	Br/B	10 15842881	Br-B-mol	Fuelback * (B8 * STPCavr) / 13885 25465	mod	44.172 * Feedstock/Cole * CarbonContent * (MW * Fuel * StabMol/MEPa) * Com/LDG	1791217 531	Br/month	612 4535713
May	2009	Unit 57 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	14703 68854	mod	0.719	Br/B	10 15842881	Br-B-mol	Fuelback * (B8 * STPCavr) / 14830 02204	mod	44.172 * Feedstock/Cole * CarbonContent * (MW * Fuel * StabMol/MEPa) * Com/LDG	1857000 871	Br/month	617 6817188
Jun	2009	Unit 57 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	1251 36023	mod	0.719	Br/B	10 15842881	Br-B-mol	Fuelback * (B8 * STPCavr) / 17298 40359	mod	44.172 * Feedstock/Cole * CarbonContent * (MW * Fuel * StabMol/MEPa) * Com/LDG	1888678 751	Br/month	756 9006494
Jul	2009	Unit 57 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	13300 13194	mod	0.719	Br/B	10 15842881	Br-B-mol	Fuelback * (B8 * STPCavr) / 1504 8789	mod	44.172 * Feedstock/Cole * CarbonContent * (MW * Fuel * StabMol/MEPa) * Com/LDG	1770195 029	Br/month	302 5481656
Aug	2009	Unit 57 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	13286 57442	mod	0.719	Br/B	10 15842881	Br-B-mol	Fuelback * (B8 * STPCavr) / 1561 26869	mod	44.172 * Feedstock/Cole * CarbonContent * (MW * Fuel * StabMol/MEPa) * Com/LDG	1788722 137	Br/month	602 7351258
Sep	2009	Unit 57 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	12515 55109	mod	0.719	Br/B	10 15842881	Br-B-mol	Fuelback * (B8 * STPCavr) / 17076 421893	mod	44.172 * Feedstock/Cole * CarbonContent * (MW * Fuel * StabMol/MEPa) * Com/LDG	1865770 581	Br/month	755 5851057
Oct	2009	Unit 57 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	13465 88713	mod	0.719	Br/B	10 15842881	Br-B-mol	Fuelback * (B8 * STPCavr) / 18803 5662	mod	44.172 * Feedstock/Cole * CarbonContent * (MW * Fuel * StabMol/MEPa) * Com/LDG	1748402 229	Br/month	814 165552
Nov	2009	Unit 57 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	871 1590121	mod	0.719	Br/B	10 15842881	Br-B-mol	Fuelback * (B8 * STPCavr) / 9719 304122	mod	44.172 * Feedstock/Cole * CarbonContent * (MW * Fuel * StabMol/MEPa) * Com/LDG	1727389 188	Br/month	577 874616
Dec	2009	Unit 57 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	14703 55752	mod	0.719	Br/B	10 15842881	Br-B-mol	Fuelback * (B8 * STPCavr) / 14890 83297	mod	44.172 * Feedstock/Cole * CarbonContent * (MW * Fuel * StabMol/MEPa) * Com/LDG	1944971 66	Br/month	851 287303
Jan	2010	Unit 57 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	13139 685222	mod	0.719	Br/B	10 15842881	Br-B-mol	Fuelback * (B8 * STPCavr) / 1341 95816	mod	44.172 * Feedstock/Cole * CarbonContent * (MW * Fuel * StabMol/MEPa) * Com/LDG	1748830 386	Br/month	763 2618043
Feb	2010	Unit 57 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	9044 891955	mod	0.719	Br/B	10 15842881	Br-B-mol	Fuelback * (B8 * STPCavr) / 9184 233775	mod	44.172 * Feedstock/Cole * CarbonContent * (MW * Fuel * StabMol/MEPa) * Com/LDG	1703553 112	Br/month	546 6863358
Mar	2010	Unit 57 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	68793 8407076	mod	0.719	Br/B	10 15842881	Br-B-mol	Fuelback * (B8 * STPCavr) / 9117 1971	mod	44.172 * Feedstock/Cole * CarbonContent * (MW * Fuel * StabMol/MEPa) * Com/LDG	1195002 131	Br/month	542 0711098
Apr	2010	Unit 57 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	13172 73713	mod	0.719	Br/B	10 15842881	Br-B-mol	Fuelback * (B8 * STPCavr) / 13314 95334	mod	44.172 * Feedstock/Cole * CarbonContent * (MW * Fuel * StabMol/MEPa) * Com/LDG	1745253 335	Br/month	781 6345338
May	2010	Unit 57 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	14287 80573	mod	0.719	Br/B	10 15842881	Br-B-mol	Fuelback * (B8 * STPCavr) / 14507 55766	mod	44.172 * Feedstock/Cole * CarbonContent * (MW * Fuel * StabMol/MEPa) * Com/LDG	1701627 683	Br/month	882 5649149
Jun	2010	Unit 57 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	13635 59014	mod	0.719	Br/B	10 15842881	Br-B-mol	Fuelback * (B8 * STPCavr) / 14651 8524	mod	44.172 * Feedstock/Cole * CarbonContent * (MW * Fuel * StabMol/MEPa) * Com/LDG	1841683 111	Br/month	835 4560475
Jul	2010	Unit 57 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	14359 41271	mod	0.719	Br/B	10 15842881	Br-B-mol	Fuelback * (B8 * STPCavr) / 14640 48881	mod	44.172 * Feedstock/Cole * CarbonContent * (MW * Fuel * StabMol/MEPa) * Com/LDG	1911181 764	Br/month	888 6864957
Aug	2010	Unit 57 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	12628 25425	mod	0.719	Br/B	10 15842881	Br-B-mol	Fuelback * (B8 * STPCavr) / 15222 88214	mod	44.172 * Feedstock/Cole * CarbonContent * (MW * Fuel * StabMol/MEPa) * Com/LDG	1807771 984	Br/month	782 3861988
Sep	2010	Unit 57 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	12688 69048	mod	0.719	Br/B	10 15842881	Br-B-mol	Fuelback * (B8 * STPCavr) / 15168 303737	mod	44.172 * Feedstock/Cole * CarbonContent * (MW * Fuel * StabMol/MEPa) * Com/LDG	172516 273	Br/month	782 318242
Oct	2010	Unit 57 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	7865 40279	mod	0.719	Br/B	10 15842881	Br-B-mol	Fuelback * (B8 * STPCavr) / 8016 041513	mod	44.172 * Feedstock/Cole * CarbonContent * (MW * Fuel * StabMol/MEPa) * Com/LDG	1020690 894	Br/month	478 7212826
Nov	2010	Unit 57 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	14105 33769	mod	0.719	Br/B	10 15842881	Br-B-mol	Fuelback * (B8 * STPCavr) / 14603 71202	mod	44.172 * Feedstock/Cole * CarbonContent * (MW * Fuel * StabMol/MEPa) * Com/LDG	1868013 095	Br/month	856 3883453
Dec	2010	Unit 57 - Hydrogen Manufacturing	Hydrogen Plant	Carbon Dioxide	14024 67682	mod	0.719	Br/B	10 15842881	Br-B-mol	Fuelback * (B8 * STPCavr) / 14748 272025	mod	44.172 * Feedstock/Cole * CarbonContent * (MW * Fuel * StabMol/MEPa) * Com/LDG	193177 955	Br/month	876 8751239





Attachment V  
GHG Calculations 2006-2010.xlsx  
W/SR Comb

Month	Year	Process Unit	Emission Scenario	GHG Species	Fuel Use (Liquid Volume) [FuelUsage]	Units	Heat Content (Liquid - HHV [HHV])	Units	Species Emission Rate Expression	Units	Converted Rate	Units	MT/month	CO2t	Comments
Jan	2010	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	12708	bbl	4986	mbtu/bbl	FuelUsage*HHV*EF*ConvLdg *ConvMmbtu/Mbtu	9501657.985	lb/month	4339.88926	MT/month	4339.88926	
Jan	2010	WSR Combustion Sources	Stationary Comb	Methane	12708	bbl	4986	mbtu/bbl	FuelUsage*HHV*EF*ConvLdg *ConvMmbtu/Mbtu	419.0679793	lb/month	0.190086264	MT/month	47521566	
Jan	2010	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	12708	bbl	4986	mbtu/bbl	FuelUsage*HHV*EF*ConvLdg *ConvMmbtu/Mbtu	83.8155567	lb/month	0.038617253	MT/month	11.32914133	
Feb	2010	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	9082	bbl	4958	mbtu/bbl	FuelUsage*HHV*EF*ConvLdg *ConvMmbtu/Mbtu	6752403.566	lb/month	3062.842379	MT/month	3062.842379	
Feb	2010	WSR Combustion Sources	Stationary Comb	Methane	9082	bbl	4958	mbtu/bbl	FuelUsage*HHV*EF*ConvLdg *ConvMmbtu/Mbtu	297.8125564	lb/month	0.135085688	MT/month	33771417	
Feb	2010	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	9082	bbl	4958	mbtu/bbl	FuelUsage*HHV*EF*ConvLdg *ConvMmbtu/Mbtu	59.56251308	lb/month	0.027017134	MT/month	8051105613	
Mar	2010	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	10228	bbl	4994	mbtu/bbl	FuelUsage*HHV*EF*ConvLdg *ConvMmbtu/Mbtu	7659652.39	lb/month	3474.365549	MT/month	3474.365549	
Mar	2010	WSR Combustion Sources	Stationary Comb	Methane	10228	bbl	4994	mbtu/bbl	FuelUsage*HHV*EF*ConvLdg *ConvMmbtu/Mbtu	337.826521	lb/month	0.153235856	MT/month	38308974	
Mar	2010	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	10228	bbl	4994	mbtu/bbl	FuelUsage*HHV*EF*ConvLdg *ConvMmbtu/Mbtu	67.56538421	lb/month	0.030647179	MT/month	9132853462	
Apr	2010	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	10552	bbl	4874	mbtu/bbl	FuelUsage*HHV*EF*ConvLdg *ConvMmbtu/Mbtu	7712420.102	lb/month	3498.299073	MT/month	3498.299073	
Apr	2010	WSR Combustion Sources	Stationary Comb	Methane	10552	bbl	4874	mbtu/bbl	FuelUsage*HHV*EF*ConvLdg *ConvMmbtu/Mbtu	340.1537288	lb/month	0.154291344	MT/month	38372836	
Apr	2010	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	10552	bbl	4874	mbtu/bbl	FuelUsage*HHV*EF*ConvLdg *ConvMmbtu/Mbtu	66.03075656	lb/month	0.030552539	MT/month	9195764102	
May	2010	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	9211	bbl	5033	mbtu/bbl	FuelUsage*HHV*EF*ConvLdg *ConvMmbtu/Mbtu	6951909.075	lb/month	3153.336653	MT/month	3153.336653	
May	2010	WSR Combustion Sources	Stationary Comb	Methane	9211	bbl	5033	mbtu/bbl	FuelUsage*HHV*EF*ConvLdg *ConvMmbtu/Mbtu	306.611691	lb/month	0.139076889	MT/month	3476522225	
May	2010	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	9211	bbl	5033	mbtu/bbl	FuelUsage*HHV*EF*ConvLdg *ConvMmbtu/Mbtu	61.32233821	lb/month	0.02715378	MT/month	8288982564	
Jun	2010	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	9865	bbl	4969	mbtu/bbl	FuelUsage*HHV*EF*ConvLdg *ConvMmbtu/Mbtu	7350831.317	lb/month	3334.284964	MT/month	3334.284964	
Jun	2010	WSR Combustion Sources	Stationary Comb	Methane	9865	bbl	4969	mbtu/bbl	FuelUsage*HHV*EF*ConvLdg *ConvMmbtu/Mbtu	324.206269	lb/month	0.14705755	MT/month	3676430276	
Jun	2010	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	9865	bbl	4969	mbtu/bbl	FuelUsage*HHV*EF*ConvLdg *ConvMmbtu/Mbtu	64.84120538	lb/month	0.029411511	MT/month	8764630276	
Jul	2010	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	8677	bbl	5025	mbtu/bbl	FuelUsage*HHV*EF*ConvLdg *ConvMmbtu/Mbtu	57.67540554	lb/month	2565.802699	MT/month	2565.802699	
Jul	2010	WSR Combustion Sources	Stationary Comb	Methane	8677	bbl	5025	mbtu/bbl	FuelUsage*HHV*EF*ConvLdg *ConvMmbtu/Mbtu	288.3770277	lb/month	0.130805775	MT/month	3227044375	
Jul	2010	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	8677	bbl	5025	mbtu/bbl	FuelUsage*HHV*EF*ConvLdg *ConvMmbtu/Mbtu	6273561.329	lb/month	2845.552277	MT/month	2845.552277	
Aug	2010	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	8307	bbl	5036	mbtu/bbl	FuelUsage*HHV*EF*ConvLdg *ConvMmbtu/Mbtu	276.6845632	lb/month	0.125502156	MT/month	31375539	
Aug	2010	WSR Combustion Sources	Stationary Comb	Methane	8307	bbl	5036	mbtu/bbl	FuelUsage*HHV*EF*ConvLdg *ConvMmbtu/Mbtu	55.33691263	lb/month	0.02510431	MT/month	7479528496	
Sep	2010	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	8307	bbl	5036	mbtu/bbl	FuelUsage*HHV*EF*ConvLdg *ConvMmbtu/Mbtu	8491058.533	lb/month	3851.483944	MT/month	3851.483944	

Sep	2010	WSR Combustion Sources	Stationary Comb	Methane	11208	b61	5052	mbtub61	FuelUsage*HHV*EF * ConvLbkg * ConvMbtubuMbu	374.4953778	lb/month	0.169868448	MT/month	4.2467112
Sep	2010	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	11208	b61	5052	mbtub61	FuelUsage*HHV*EF * ConvLbkg * ConvMbtubuMbu	74.89807557	lb/month	0.03397369	MT/month	10.1241596
Oct	2010	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	11766	b61	5010	mbtub61	FuelUsage*HHV*EF * ConvLbkg * ConvMbtubuMbu	83356588.077	lb/month	4009.619833	MT/month	4009.619833
Oct	2010	WSR Combustion Sources	Stationary Comb	Methane	11766	b61	5010	mbtub61	FuelUsage*HHV*EF * ConvLbkg * ConvMbtubuMbu	369.8715706	lb/month	0.17684298	MT/month	4.4210745
Oct	2010	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	11766	b61	5010	mbtub61	FuelUsage*HHV*EF * ConvLbkg * ConvMbtubuMbu	77.97431411	lb/month	0.035365956	MT/month	10.53984161
Nov	2010	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	9426	b61	5056	mbtub61	FuelUsage*HHV*EF * ConvLbkg * ConvMbtubuMbu	71465688.799	lb/month	3241.687365	MT/month	3241.687365
Nov	2010	WSR Combustion Sources	Stationary Comb	Methane	9426	b61	5056	mbtub61	FuelUsage*HHV*EF * ConvLbkg * ConvMbtubuMbu	315.2023875	lb/month	0.142973568	MT/month	3.5743392
Nov	2010	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	9426	b61	5056	mbtub61	FuelUsage*HHV*EF * ConvLbkg * ConvMbtubuMbu	63.0404775	lb/month	0.028594744	MT/month	8.521224653
Dec	2010	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	13454	b61	5052	mbtub61	FuelUsage*HHV*EF * ConvLbkg * ConvMbtubuMbu	10192603.63	lb/month	4623.282736	MT/month	4623.282736
Dec	2010	WSR Combustion Sources	Stationary Comb	Methane	13454	b61	5052	mbtub61	FuelUsage*HHV*EF * ConvLbkg * ConvMbtubuMbu	449.5414716	lb/month	0.203908824	MT/month	5.0977206
Dec	2010	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	13454	b61	5052	mbtub61	FuelUsage*HHV*EF * ConvLbkg * ConvMbtubuMbu	88.90829431	lb/month	0.040787665	MT/month	12.15296591
Jan	2009	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	16661	b61	4974	mbtub61	FuelUsage*HHV*EF * ConvLbkg * ConvMbtubuMbu	12427312.4	lb/month	5636.940788	MT/month	5636.940788
Jan	2009	WSR Combustion Sources	Stationary Comb	Methane	16661	b61	4974	mbtub61	FuelUsage*HHV*EF * ConvLbkg * ConvMbtubuMbu	548.1025757	lb/month	0.248615442	MT/month	6.21538605
Jan	2009	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	16661	b61	4974	mbtub61	FuelUsage*HHV*EF * ConvLbkg * ConvMbtubuMbu	109.62505151	lb/month	0.049723088	MT/month	14.81748034
Feb	2009	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	17224	b61	4912	mbtub61	FuelUsage*HHV*EF * ConvLbkg * ConvMbtubuMbu	9004136.495	lb/month	4084.21247	MT/month	4084.21247
Feb	2009	WSR Combustion Sources	Stationary Comb	Methane	17224	b61	4912	mbtub61	FuelUsage*HHV*EF * ConvLbkg * ConvMbtubuMbu	397.1245146	lb/month	0.180132864	MT/month	5033216
Feb	2009	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	17224	b61	4912	mbtub61	FuelUsage*HHV*EF * ConvLbkg * ConvMbtubuMbu	79.42490293	lb/month	0.036026573	MT/month	10.73991869
Mar	2009	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	18987	b61	5008	mbtub61	FuelUsage*HHV*EF * ConvLbkg * ConvMbtubuMbu	8934539.071	lb/month	4052.6454572	MT/month	4052.6454572
Mar	2009	WSR Combustion Sources	Stationary Comb	Methane	18987	b61	5008	mbtub61	FuelUsage*HHV*EF * ConvLbkg * ConvMbtubuMbu	394.0549428	lb/month	0.178740528	MT/month	4.4685132
Mar	2009	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	18987	b61	5008	mbtub61	FuelUsage*HHV*EF * ConvLbkg * ConvMbtubuMbu	78.81098857	lb/month	0.035748106	MT/month	10.65233547
Apr	2009	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	11312	b61	5006	mbtub61	FuelUsage*HHV*EF * ConvLbkg * ConvMbtubuMbu	8491816.722	lb/month	3851.827853	MT/month	3851.827853
Apr	2009	WSR Combustion Sources	Stationary Comb	Methane	11312	b61	5006	mbtub61	FuelUsage*HHV*EF * ConvLbkg * ConvMbtubuMbu	65590971.108	lb/month	2889.617761	MT/month	2889.617761
May	2009	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	11312	b61	5045	mbtub61	FuelUsage*HHV*EF * ConvLbkg * ConvMbtubuMbu	74.9057635	lb/month	0.033976723	MT/month	10.12506351
May	2009	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	8712	b61	5045	mbtub61	FuelUsage*HHV*EF * ConvLbkg * ConvMbtubuMbu	280.6926393	lb/month	0.13185612	MT/month	3.295403
May	2009	WSR Combustion Sources	Stationary Comb	Methane	8712	b61	5045	mbtub61	FuelUsage*HHV*EF * ConvLbkg * ConvMbtubuMbu	58.13652785	lb/month	0.02637124	MT/month	7.958624752

Jun	2009	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	5204	bbl	5046	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * Conv/Mmbtu/Mbtu	6564568.7	bbl/month	3159.07698
Jun	2009	WSR Combustion Sources	Stationary Comb	Methane	5204	bbl	5046	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * Conv/Mmbtu/Mbtu	307.1700397	bbl/month	0.139330162
Jun	2009	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	5204	bbl	5046	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * Conv/Mmbtu/Mbtu	61.43400794	bbl/month	0.02786503
Jul	2009	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	5502	bbl	5018	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * Conv/Mmbtu/Mbtu	4892693.3	bbl/month	2219.29399
Jul	2009	WSR Combustion Sources	Stationary Comb	Methane	5502	bbl	5018	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * Conv/Mmbtu/Mbtu	215.79052483	bbl/month	0.097881108
Jul	2009	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	5502	bbl	5018	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * Conv/Mmbtu/Mbtu	43.15812866	bbl/month	0.019576222
Aug	2009	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	6333	bbl	5063	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * Conv/Mmbtu/Mbtu	4800258.256	bbl/month	2180.991852
Aug	2009	WSR Combustion Sources	Stationary Comb	Methane	6333	bbl	5063	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * Conv/Mmbtu/Mbtu	212.0686581	bbl/month	0.086191937
Sep	2009	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	6333	bbl	5063	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * Conv/Mmbtu/Mbtu	42.4133363	bbl/month	0.01923337
Sep	2009	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	10866	bbl	5009	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * Conv/Mmbtu/Mbtu	8161886.87	bbl/month	3702.17548
Sep	2009	WSR Combustion Sources	Stationary Comb	Methane	10866	bbl	5009	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * Conv/Mmbtu/Mbtu	359.978096	bbl/month	0.016328342
Sep	2009	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	10866	bbl	5009	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * Conv/Mmbtu/Mbtu	71.99556192	bbl/month	0.032656576
Oct	2009	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	10849	bbl	4992	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * Conv/Mmbtu/Mbtu	8121470.225	bbl/month	3683.841308
Oct	2009	WSR Combustion Sources	Stationary Comb	Methane	10849	bbl	4992	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * Conv/Mmbtu/Mbtu	358.1948056	bbl/month	0.162474524
Oct	2009	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	10849	bbl	4992	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * Conv/Mmbtu/Mbtu	71.63896111	bbl/month	0.032494925
Nov	2009	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	11055	bbl	5034	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * Conv/Mmbtu/Mbtu	8345307.21	bbl/month	3785.372177
Nov	2009	WSR Combustion Sources	Stationary Comb	Methane	11055	bbl	5034	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * Conv/Mmbtu/Mbtu	358.0670631	bbl/month	0.16695261
Nov	2009	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	11055	bbl	5034	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * Conv/Mmbtu/Mbtu	73.61341261	bbl/month	0.033390522
Dec	2009	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	16053	bbl	5012	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * Conv/Mmbtu/Mbtu	12065265.49	bbl/month	5472.728401
Dec	2009	WSR Combustion Sources	Stationary Comb	Methane	16053	bbl	5012	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * Conv/Mmbtu/Mbtu	532.1355404	bbl/month	0.24137598
Dec	2009	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	16053	bbl	5012	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * Conv/Mmbtu/Mbtu	106.4271081	bbl/month	0.048274582
Jan	2008	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	9132	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * Conv/Mmbtu/Mbtu	7059353.713	bbl/month	3202.072789
Jan	2008	WSR Combustion Sources	Stationary Comb	Methane	9132	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * Conv/Mmbtu/Mbtu	311.3565019	bbl/month	0.1412638
Jan	2008	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	9132	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * Conv/Mmbtu/Mbtu	62.27070038	bbl/month	0.028245276
Feb	2008	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	6326	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * Conv/Mmbtu/Mbtu	5284465.832	bbl/month	2398.996232
Feb	2008	WSR Combustion Sources	Stationary Comb	Methane	6326	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF * ConvLbKg * Conv/Mmbtu/Mbtu	233.0656496	bbl/month	0.0571874

Feb	2008	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	6836	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*		46,613,929.72	lb/month	0,021,143,748	MT/month	6,300,835,904	
Mar	2008	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	10206	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	ConvLbkg	Conv/Mbtu/MMbtu					
Mar	2008	WSR Combustion Sources	Stationary Comb	Methane	10206	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	ConvLbkg	Conv/Mbtu/MMbtu	78,855,93,078	lb/month	357,8,653,479	MT/month	3,578,653,479
Mar	2008	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	10206	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	ConvLbkg	Conv/Mbtu/MMbtu	347,967,939	lb/month	0,157,835,779	MT/month	3,945,894,75
Apr	2008	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	9546	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	ConvLbkg	Conv/Mbtu/MMbtu	69,593,587,87	lb/month	0,031,567,158	MT/month	9,407,013,084
Apr	2008	WSR Combustion Sources	Stationary Comb	Methane	9546	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	ConvLbkg	Conv/Mbtu/MMbtu	737,9390,116	lb/month	3347,239,033	MT/month	3347,239,033
Apr	2008	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	9546	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	ConvLbkg	Conv/Mbtu/MMbtu	325,465,6035	lb/month	0,147,628,889	MT/month	3,690,722,25
May	2008	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	9889	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	ConvLbkg	Conv/Mbtu/MMbtu	65,093,120,69	lb/month	0,029,525,778	MT/month	8,798,68,844
May	2008	WSR Combustion Sources	Stationary Comb	Methane	9889	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	ConvLbkg	Conv/Mbtu/MMbtu	77,218,44,529	lb/month	3502,573,926	MT/month	3502,573,926
Jun	2008	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	9889	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	ConvLbkg	Conv/Mbtu/MMbtu	340,563,4441	lb/month	0,154,47,685	MT/month	3,861,997,125
Jun	2008	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	9889	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	ConvLbkg	Conv/Mbtu/MMbtu	68,113,88,881	lb/month	0,030,889,5977	MT/month	9,207,001,146
Jun	2008	WSR Combustion Sources	Stationary Comb	Methane	9889	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	ConvLbkg	Conv/Mbtu/MMbtu	451,3750,145	lb/month	2047,405,651	MT/month	2047,405,651
Jul	2008	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	9889	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	ConvLbkg	Conv/Mbtu/MMbtu	199,077,483,86	lb/month	0,050,930,135	MT/month	2,257,503,375
Jul	2008	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	9889	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	ConvLbkg	Conv/Mbtu/MMbtu	39,815,496,72	lb/month	0,018,650,027	MT/month	5,381,885,046
Jul	2008	WSR Combustion Sources	Stationary Comb	Methane	10414	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	ConvLbkg	Conv/Mbtu/MMbtu	80,503,84,315	lb/month	3651,597,243	MT/month	3651,597,243
Jul	2008	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	10414	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	ConvLbkg	Conv/Mbtu/MMbtu	55,095,846	lb/month	0,161,025,1	MT/month	4,026,317,275
Jul	2008	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	10414	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	ConvLbkg	Conv/Mbtu/MMbtu	71,011,916,92	lb/month	0,032,210,602	MT/month	9,588,729,596
Aug	2008	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	8243	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	ConvLbkg	Conv/Mbtu/MMbtu	63,721,25,783	lb/month	2890,351,073	MT/month	2890,351,073
Aug	2008	WSR Combustion Sources	Stationary Comb	Methane	8243	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	ConvLbkg	Conv/Mbtu/MMbtu	281,040,537,3	lb/month	0,127,477,995	MT/month	3,188,949,875
Sep	2008	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	8599	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	ConvLbkg	Conv/Mbtu/MMbtu	56,208,107,47	lb/month	0,025,495,599	MT/month	7,597,688,502
Sep	2008	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	8599	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	ConvLbkg	Conv/Mbtu/MMbtu	58,635,3219	lb/month	0,026,596,707	MT/month	7,925,188,66
Sep	2008	WSR Combustion Sources	Stationary Comb	Methane	8599	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	ConvLbkg	Conv/Mbtu/MMbtu	46,846,540,286	lb/month	3015,180,017	MT/month	3015,180,017
Oct	2008	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	8599	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	ConvLbkg	Conv/Mbtu/MMbtu	233,718,169	lb/month	0,132,835,5	MT/month	3,324,883,375
Oct	2008	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	6073	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	ConvLbkg	Conv/Mbtu/MMbtu	207,055,845	lb/month	0,093,918,945	MT/month	2,347,973,625
Oct	2008	WSR Combustion Sources	Stationary Comb	Methane	6073	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	ConvLbkg	Conv/Mbtu/MMbtu	41,411,169	lb/month	0,018,783,789	MT/month	5,597,569,122
Nov	2008	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	6073	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	ConvLbkg	Conv/Mbtu/MMbtu	737,011,3,699	lb/month	3343,031,315	MT/month	3343,031,315

Attachment V  
GHG Calculations 2006-2010.xlsx  
WSR Comb

Nov	2008	WSR Combustion Sources	Stationary Comb	Methane	9534	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*		325 0564701	lb/month	0.147443331	MT/month	3 68608275
Nov	2008	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	9534	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/MBtu/MBtu	65 01128402	lb/month	0.02948662	MT/month	8 787621276
Dec	2008	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	14858	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lb/g * Conv/MBtu/MBtu	1148570 93	lb/month	5209 85518	MT/month	5209 85518
Dec	2008	WSR Combustion Sources	Stationary Comb	Methane	14858	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lb/g * Conv/MBtu/MBtu	506 5753128	lb/month	0.22977897	MT/month	5 74447425
Dec	2008	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	14858	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/MBtu/MBtu	101 3150626	lb/month	0.045855784	MT/month	1 3 69482865
Jan	2007	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	10128	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/MBtu/MBtu	7623296 364	lb/month	3551 313317	MT/month	3551 313317
Jan	2007	WSR Combustion Sources	Stationary Comb	Methane	10128	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/MBtu/MBtu	345 3065724	lb/month	0 15682952	MT/month	3 915738
Jan	2007	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	10128	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/MBtu/MBtu	69 06171448	lb/month	0 0313235904	MT/month	9 335119382
Feb	2007	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	10879	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lb/g * Conv/MBtu/MBtu	8409845 493	lb/month	3814 642935	MT/month	3814 642935
Mar	2007	WSR Combustion Sources	Stationary Comb	Methane	10879	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/MBtu/MBtu	370 9135031	lb/month	0 168243735	MT/month	4 206093375
Feb	2007	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	8456	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lb/g * Conv/MBtu/MBtu	72 18270061	lb/month	0 033648747	MT/month	1 0 02732681
Mar	2007	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	8456	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/MBtu/MBtu	6535762 194	lb/month	2965 030804	MT/month	2965 030804
Mar	2007	WSR Combustion Sources	Stationary Comb	Methane	8456	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lb/g * Conv/MBtu/MBtu	298 3026548	lb/month	0 13077204	MT/month	3 269301
Mar	2007	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	8456	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/MBtu/MBtu	57 66053096	lb/month	0 026154408	MT/month	7 79401584
Apr	2007	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	11514	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/MBtu/MBtu	8900722 585	lb/month	4037 304653	MT/month	4037 304653
Apr	2007	WSR Combustion Sources	Stationary Comb	Methane	11514	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lb/g * Conv/MBtu/MBtu	352 5634177	lb/month	0 17860401	MT/month	4 45160025
Apr	2007	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	11514	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lb/g * Conv/MBtu/MBtu	78 51269555	lb/month	0 035612802	MT/month	10 512615
May	2007	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	12031	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lb/g * Conv/MBtu/MBtu	9360381 572	lb/month	4218 587136	MT/month	4218 587136
May	2007	WSR Combustion Sources	Stationary Comb	Methane	12031	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lb/g * Conv/MBtu/MBtu	410 1963075	lb/month	0 186059415	MT/month	4 651485375
May	2007	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	12031	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/MBtu/MBtu	6636503 682	lb/month	0 03721883	MT/month	11 08914113
Jun	2007	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	8585	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lb/g * Conv/MBtu/MBtu	292 7008387	lb/month	0 132767025	MT/month	3 31917525
Jun	2007	WSR Combustion Sources	Stationary Comb	Methane	8585	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lb/g * Conv/MBtu/MBtu	58 54016773	lb/month	0 026553405	MT/month	7 91291469
Jul	2007	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	8585	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/MBtu/MBtu	4967521 568	lb/month	2253 232561	MT/month	2253 232561
Jul	2007	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	6426	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lb/g * Conv/MBtu/MBtu	219 0909248	lb/month	0 0937809	MT/month	2 48445225
Jul	2007	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	6426	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lb/g * Conv/MBtu/MBtu	43 81818496	lb/month	0 019875618	MT/month	5 922934164

Attachment V  
GHG Calculations 2006-2010.xlsx  
WSR Comb

Aug	2007	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	7260	b61	5155	mbtu/bbl	FuelUsage*HHV*EF*		5617232 584	lb/month	2545 668906	MT/month	2545 668906	
Aug	2007	WSR Combustion Sources	Stationary Comb	Methane	7260	b61	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Mbtu/Mbtu		0 1122759	lb/month	0 1122759	MT/month	0 1122759
Aug	2007	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	7260	b61	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lbkg * Conv/Mbtu/Mbtu	247 5255947	lb/month	0 0224518	MT/month	2 8068975	
Sep	2007	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	5617	b61	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lbkg * Conv/Mbtu/Mbtu	49 20513893	lb/month	0 0224518	MT/month	6 69164354	
Sep	2007	WSR Combustion Sources	Stationary Comb	Methane	5617	b61	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lbkg * Conv/Mbtu/Mbtu	5115171 213	lb/month	2320 205393	MT/month	2320 205393	
Sep	2007	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	5617	b61	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lbkg * Conv/Mbtu/Mbtu	225 6029564	lb/month	0 102231905	MT/month	2 558297625	
Sep	2007	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	5617	b61	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lbkg * Conv/Mbtu/Mbtu	45 12059288	lb/month	0 020465381	MT/month	6 098981538	
Oct	2007	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	5984	b61	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lbkg * Conv/Mbtu/Mbtu	5283414 285	lb/month	2441 878548	MT/month	2441 878548	
Oct	2007	WSR Combustion Sources	Stationary Comb	Methane	5984	b61	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lbkg * Conv/Mbtu/Mbtu	237 433738	lb/month	0 10759826	MT/month	2 6824565	
Oct	2007	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	5984	b61	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lbkg * Conv/Mbtu/Mbtu	47 4465759	lb/month	0 021539562	MT/month	6 410816256	
Nov	2007	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	7110	b61	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lbkg * Conv/Mbtu/Mbtu	5496277 365	lb/month	2493 072441	MT/month	2 6824565	
Nov	2007	WSR Combustion Sources	Stationary Comb	Methane	7110	b61	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lbkg * Conv/Mbtu/Mbtu	242 4115274	lb/month	0 10955615	MT/month	2 74890375	
Nov	2007	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	7110	b61	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lbkg * Conv/Mbtu/Mbtu	48 48230548	lb/month	0 021199123	MT/month	6 55338654	
Dec	2007	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	5591	b61	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lbkg * Conv/Mbtu/Mbtu	4322037 517	lb/month	1960 445572	MT/month	1 960 445572	
Dec	2007	WSR Combustion Sources	Stationary Comb	Methane	5591	b61	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lbkg * Conv/Mbtu/Mbtu	190 6220504	lb/month	0 086464815	MT/month	2 161620375	
Dec	2007	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	5591	b61	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lbkg * Conv/Mbtu/Mbtu	38 12441209	lb/month	0 017292833	MT/month	5 153302974	
Jan	2006	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	12213	b61	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lbkg * Conv/Mbtu/Mbtu	9827591 3	lb/month	457 72573	MT/month	457 72573	
Jan	2006	WSR Combustion Sources	Stationary Comb	Methane	12713	b61	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lbkg * Conv/Mbtu/Mbtu	433 4427212	lb/month	0 186606545	MT/month	4 915163625	
Jan	2006	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	12713	b61	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lbkg * Conv/Mbtu/Mbtu	86 68854425	lb/month	0 039321309	MT/month	1 117175008	
Feb	2006	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	14358	b61	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lbkg * Conv/Mbtu/Mbtu	11089233 53	lb/month	5034 53393	MT/month	5034 53393	
Feb	2006	WSR Combustion Sources	Stationary Comb	Methane	14358	b61	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lbkg * Conv/Mbtu/Mbtu	97 90561774	lb/month	0 04400524	MT/month	0 04400524	
Mar	2006	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	17053	b61	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lbkg * Conv/Mbtu/Mbtu	13182562 29	lb/month	5979 516784	MT/month	5979 516784	
Mar	2006	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	17053	b61	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lbkg * Conv/Mbtu/Mbtu	581 4126269	lb/month	0 263724645	MT/month	6 593116725	
Mar	2006	WSR Combustion Sources	Stationary Comb	Methane	17053	b61	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lbkg * Conv/Mbtu/Mbtu	116 2825254	lb/month	0 052744929	MT/month	1 5 17198884	
Apr	2006	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	17053	b61	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lbkg * Conv/Mbtu/Mbtu	28686334 056	lb/month	3749 777311	MT/month	3749 777311	
Apr	2006	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	1694	b61	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lbkg * Conv/Mbtu/Mbtu	354 6080301	lb/month	0 1653821	MT/month	4 13456775	

Attachment V  
GHG Calculations 2005c-2010.xlsx  
WSR Comb

Apr	2006	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	10694	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Mmbtu/Mbtu	72 92120602	lb/month	0.033076542	Mt/month	9.856805516
May	2006	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	5997	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lb/G * Conv/Mmbtu/Mbtu	4635889 642	lb/month	2102 806671	Mt/month	2102 806671
May	2006	WSR Combustion Sources	Stationary Comb	Methane	5997	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lb/G * Conv/Mmbtu/Mbtu	204 4844065	lb/month	0.092743605	Mt/month	2 318590125
May	2006	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	5997	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lb/G * Conv/Mmbtu/Mbtu	40 89288129	lb/month	0.018548721	Mt/month	5.527518858
Jun	2006	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	6636	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lb/G * Conv/Mmbtu/Mbtu	5129858 874	lb/month	2326 867612	Mt/month	2326 867612
Jun	2006	WSR Combustion Sources	Stationary Comb	Methane	6636	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lb/G * Conv/Mmbtu/Mbtu	226 2507589	lb/month	0 10262574	Mt/month	5.5656435
Jun	2006	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	6636	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lb/G * Conv/Mmbtu/Mbtu	45 25015178	lb/month	0 020525148	Mt/month	6.116494104
Jul	2006	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	6739	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lb/G * Conv/Mmbtu/Mbtu	5209491 457	lb/month	2362 983851	Mt/month	2362 983851
Jul	2006	WSR Combustion Sources	Stationary Comb	Methane	6739	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lb/G * Conv/Mmbtu/Mbtu	229 7624871	lb/month	0 04219535	Mt/month	2605465875
Jul	2006	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	6739	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lb/G * Conv/Mmbtu/Mbtu	45 95249742	lb/month	0 020843727	Mt/month	6.211430646
Aug	2006	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	6956	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lb/G * Conv/Mmbtu/Mbtu	5377230 907	lb/month	2439 073404	Mt/month	2439 073404
Aug	2006	WSR Combustion Sources	Stationary Comb	Methane	6956	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lb/G * Conv/Mmbtu/Mbtu	237 1609824	lb/month	0 10757454	Mt/month	2 6893635
Aug	2006	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	6956	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lb/G * Conv/Mmbtu/Mbtu	47 43219647	lb/month	0 02151498	Mt/month	6.411442584
Sep	2006	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	7047	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lb/G * Conv/Mmbtu/Mbtu	5447576 173	lb/month	2470 981926	Mt/month	2470 981926
Sep	2006	WSR Combustion Sources	Stationary Comb	Methane	7047	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lb/G * Conv/Mmbtu/Mbtu	240 2635772	lb/month	0 10898185	Mt/month	2 724546375
Sep	2006	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	7047	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lb/G * Conv/Mmbtu/Mbtu	48 05221543	lb/month	0 02196371	Mt/month	6.495516558
Oct	2006	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	6864	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lb/G * Conv/Mmbtu/Mbtu	6713034 126	lb/month	3044 98468	Mt/month	3044 98468
Oct	2006	WSR Combustion Sources	Stationary Comb	Methane	6864	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lb/G * Conv/Mmbtu/Mbtu	296 076189	lb/month	0.13429806	Mt/month	3.3574515
Oct	2006	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	6864	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lb/G * Conv/Mmbtu/Mbtu	59 1523781	lb/month	0 026858612	Mt/month	8.004164376
Nov	2006	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	7108	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lb/G * Conv/Mmbtu/Mbtu	5494731 295	lb/month	2492 37115	Mt/month	2492 37115
Nov	2006	WSR Combustion Sources	Stationary Comb	Methane	7108	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lb/G * Conv/Mmbtu/Mbtu	242 3433385	lb/month	0 10982522	Mt/month	2 7481305
Nov	2006	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	7108	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lb/G * Conv/Mmbtu/Mbtu	48 4686577	lb/month	0 02198504	Mt/month	6.551543112
Dec	2006	WSR Combustion Sources	Stationary Comb	Carbon Dioxide	8814	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lb/G * Conv/Mmbtu/Mbtu	68113528 649	lb/month	3090 566283	Mt/month	3090 566283
Dec	2006	WSR Combustion Sources	Stationary Comb	Methane	8814	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lb/G * Conv/Mmbtu/Mbtu	300 5084673	lb/month	0 13630851	Mt/month	3 40771275
Dec	2006	WSR Combustion Sources	Stationary Comb	Nitrogen Oxide	8814	bbl	5155	mbtu/bbl	FuelUsage*HHV*EF*	Conv/Lb/G * Conv/Mmbtu/Mbtu	60 10169346	lb/month	0 027261702	Mt/month	8 123987196



## **Appendix B**

**August 31, 2018 IES Response to  
DOH Email dated July 24, 2018**

**From:** Chung, Anna S.  
**To:** "McFall, Keith"  
**Cc:** Madsen, Michael A; Peak, Mark  
**Subject:** RE: [\*EXTERNAL\*] Status question: Monday email: IES GHG Reduction Plan Discussion  
**Date:** Friday, August 31, 2018 4:42:00 PM  
**Attachments:** [image002.png](#)  
[IES Response to DOH July 24 Email Request.docx](#)  
[Item 1 2016 Refinery eGGRT GHG Calc Workbook.xlsx](#)  
[Item 1 2017 Refinery eGGRT GHG Calc Summary.xlsx](#)  
[Item 2 2010 FCC CO2 Calculation Differences.xlsx](#)  
[Item 3 2009 FO FG WSR Calculation Difference.xlsx](#)

---

Hi Keith,

Please find attached our response to your emailed request on July 24, 2018 and supporting documentation. Let me know if you have any questions.

Thank you,



**Anna S. P. T. Chung**  
Environmental Engineer  
[achung@islandenergyservices.com](mailto:achung@islandenergyservices.com)

**IES Downstream, LLC**  
91-480 Malakole Street  
Kapolei, HI 96707  
Tel +1 808.682.2366  
Fax +1 808.682.2214

Official Licensee of the Texaco Brand in Hawai'i

---



**From:** McFall, Keith [mailto:[Keith.McFall@doh.hawaii.gov](mailto:Keith.McFall@doh.hawaii.gov)]  
**Sent:** Tuesday, August 28, 2018 1:51 PM  
**To:** Chung, Anna S. <[AChung@islandenergyservices.com](mailto:AChung@islandenergyservices.com)>  
**Cc:** Madsen, Michael A <[michael.madsen@doh.hawaii.gov](mailto:michael.madsen@doh.hawaii.gov)>; Peak, Mark <[MPeak@islandenergyservices.com](mailto:MPeak@islandenergyservices.com)>  
**Subject:** RE: [\*EXTERNAL\*] Status question: Monday email: IES GHG Reduction Plan Discussion

## IES Response to DOH Email Request on July 24, 2018

Prepared by Anna Chung  
August 31, 2018

### REQUEST:

*While it sounded like the GHGERP outlined the reasons for the emissions differences highlighted in the "IES-chev-ref-ref-SLEIS-2016-16.xlsx" file, we would like to have the detailed calculations to document the reasons.*

*We think this can be accomplished if we received:*

- 1) *annual emissions inventory calculations that follow the requirements of EPA's e-GGRT reporting for the 2016 and 2017 emissions years. These calculations would be consistent with the information already provided for the proposed 2006 – 2010 emission years.*
- 2) *calculations that document the difference between FCC CO<sub>2</sub> emission calculations for 2010 as reported to EPA and provided in the GHGERP supporting spreadsheet; I believe we talked about the ~3.5% difference in the meeting, and I may have forgotten the explanation for the difference, but I think it would be good to document this if the data is available.*
- 3) *calculations that compare the results of facility reporting requirements for EPA e-GGRT & CAB annual emissions for annual fuel throughputs, higher heating values (HHVs), and annual heats associated with fuel oil combustion, fuel gas combustion, and WSR combustion for the 2009 baseline year.*
- 4) *corrections for any errors in annual emissions reporting to CAB for 2006 – 2017 of fuel oil, fuel gas, or WSR combustion throughputs or HHVs; as I recall from the meeting, the 2010 fuel gas combustion throughputs reported to DOH were in error. These would be errors, not differences caused by conflicting e-GGRT and DOH annual emissions reporting requirements.*

### RESPONSE:

- 1) *annual emissions inventory calculations that follow the requirements of EPA's e-GGRT reporting for the 2016 and 2017 emissions years. These calculations would be consistent with the information already provided for the proposed 2006 – 2010 emission years.*

The following excel spreadsheets were used for inputting GHG data in eGGRT for RY2016 and RY 2017.

- 2016 Refinery eGGRT GHG Calc Workbook
- 2017 Refinery eGGRT GHG Calc Summary

2016 emission data were collected and calculations completed using formulas in the workbook "2016 Refinery eGGRT GHG Calc Workbook.xlsx". The data was then reentered into EPA's eGGRT website, calculations completed using the online IVT calculator and verified against the workbook calculations prior to submittal.

In 2017, IES worked with Sphera to configure Essential Suite, the GHG software program that Chevron used for calculating RY2015 and RY2016 GHG emissions, to complete the GHG calculations instead of

using the excel workbook. Emission reports were configured by Sphera to replicate the workbook tabs to facilitate data entry into eGGRT. The file “2017 Refinery eGGRT GHG Calc Summary.xlsx” gathers the various reports into one file with a summary sheet listing all the process units and their emissions. Included in the summary are comments comparing the Essential Suite and IVT calculations.

**2) *calculations that document the difference between FCC CO<sub>2</sub> emission calculations for 2010 as reported to EPA and provided in the GHGERP supporting spreadsheet;***

Three calculation methods documenting the 2010 CO<sub>2</sub>e emission results obtained by using different averaging periods of the same data are presented in the file “FCC 2010 CO<sub>2</sub> Calculation Differences.xlsx.” Method 1 presents the results from the GHGERP supporting spreadsheet, submitted to the DOH in 2016, which calculates the monthly CO<sub>2</sub>e and sums the emissions to get the annual CO<sub>2</sub>e emitted. Calculating the FCC’s CO<sub>2</sub>e monthly provides more accurate emissions results because it is more sensitive to operational data fluctuations (the FCC was shut down in December for ~12 days). As a result, calculation method 1 is 3.5% lower than what was reported to the EPA. Recalculating the 2010 FCC data using the GHG Emission Calculation Summary spreadsheet, method 3, which replicates the eGGRT IVT yields a result nearly equivalent to the eGGRT FLIGHT report result. The eGGRT IVT uses an average of the hourly data over the year (8760 data points) to calculate a single average for the annual CO<sub>2</sub>e. This smooths out the effects of outlier data, resulting in higher emissions. Method 2 shows that averaging the average monthly data, provided in 2016, also results in emissions much lower than IVT calculations. Method 4 recalculates annual emissions using data from the EPA Flight report and shows the difficulty of recalculating the same number as eGGRT.

**3) *calculations that compare the results of facility reporting requirements for EPA e-GGRT & CAB annual emissions for annual fuel throughputs, higher heating values (HHVs), and annual heats associated with fuel oil combustion, fuel gas combustion, and WSR combustion for the 2009 baseline year.***

The results of facility reporting requirements for EPA e-GGRT & CAB annual emissions for annual fuel throughputs, higher heating values (HHVs), and annual heats associated with fuel oil combustion, fuel gas combustion, and whole straight run (WSR) combustion for the 2009 baseline year differ from each other for several reasons. In 2009, CAB annual emission calculations were prepared by the refinery’s Environmental department to reflect air emissions from permitted refinery equipment. GHG reporting was managed at a corporate level and calculations were completed by the refinery’s process engineering department to reflect overall refinery GHG emissions. Two independent groups with different emissions reporting purposes contributed to the differences in data used for calculating air and GHG emissions.

A comparison of annual emissions and GHG reported results are on the attached spreadsheet “FO FG WSR Calculation Difference.xlsx”, tab “FO FG WSR Summary.” These calculations were compiled by DOH in a spreadsheet titled “IES-chev-ref-SLEIS-2016-15.xlsx” and summarizes the 2006-2010 GHG data submitted by Chevron in 2016 with annual emissions data submitted to CAB.

**Fuel Oil Combustion**

Fuel oil throughput data for 2009 annual emissions used pi tags that measure low sulfur fuel oil (LSFO) flow to each emission unit identified in the covered source permit (CSP). This meets DOH HAR 11-60.1-111 definition of "verifiable documentation". Fuel oil throughput data for 2009 EPA GHG emissions used tank drop to calculate daily fuel oil use from the LSFO tank that feeds the refinery. This meets the EPA 40 CFR 98.6 definition of "company record". As a result, two valid but, different methods were used for gathering fuel use. The difference in pi data and tank drop can be attributed to a delta between the meter readings and pi, which averages ~65 bpd more (6%). Calculating GHG emissions using fuel oil tank drop is more conservative and reflects a slightly higher fuel consumption resulting in greater CO<sub>2</sub>e emissions.

The 2009 fuel oil HHVs used in the both calculations come from lab StarLIMs data however, the averaging period used by each method is different causing a slight 0.06% difference in the number. Annual emissions use the average gross-BTU (higher heating value) of all the lab samples taken throughout the year while GHG emissions uses a weighted average gross-BTU (higher heating value) based on the monthly average HHV and fuel usage.

#### *Fuel Gas Combustion*

Fuel gas throughput data for 2009 annual emissions used the pi tags that measure fuel gas for each process unit identified in the CSP. 2009 EPA GHG emission calculations used the pi tag for the fuel gas mix drum which is upstream of the process units. This tag captures additional fuel gas use that was not used for combustion in an air-permitted combustion unit, for example, use of fuel gas for insignificant activities like furnace pilot flames. Thus, the GHG calculation has a 22.86% higher throughput.

The 2009 annual emission HHVs use the average HHV of all the lab StarLIMs samples taken throughout the year whereas, the GHG HHVs uses the default Natural Gas HHV per 40 CFR 98 Table C-1. This results in a 0.78% lower HHV used for GHG emissions.

#### *WSR Combustion*

Like fuel oil, 2009 WSR throughput data for annual emissions used pi tags that measure WSR flow to each emission unit identified in the CSP. WSR throughput data for 2009 EPA GHG emissions used tank drop to calculate daily WSR use from the WSR tank that feeds the refinery. The difference in pi data and tank drop can be attributed to a delta between the meter readings and pi, which averages ~4.5 bpd more (~1%).

The 2009 WSR HHVs used in the both calculations come from the lab StarLIMs data however, the annual emissions use the net-BTU (Lower Heating Value) and the EPA GHG emissions calculations use the gross-BTU (Higher Heating Value). Net-BTU is ~11 MMscfs lower than the gross-BTU. In addition to this, the averaging period used for the annual HHV is different. Annual emissions use the average HHV of all the lab samples taken throughout the year while GHG emissions uses a weighted average HHV based on the monthly average HHV and fuel usage. This results in a 6.7% higher HHV used for GHG emissions. Starting from RY2015, the annual emissions calculations use the gross-BTU value so, there should be no significant differences in the HHVs.

- 4) *corrections for any errors in annual emissions reporting to CAB for 2006 – 2017 of fuel oil, fuel gas, or WSR combustion throughputs or HHVs; as I recall from the meeting, the 2010 fuel gas combustion throughputs reported to DOH were in error. These would be errors, not differences caused by conflicting e-GGRT and DOH annual emissions reporting requirements.*

IES has not conducted a separate audit to validate the numbers that were submitted from 2006 through 2015 by the former owner, Chevron, however, upon review of past submittals from 2006 -2017, we can confirm that the reported fuel gas throughput in 2010 is overstated by a magnitude of 110% due to a unit conversion error for the crude furnace throughput. The crude furnace throughput was overstated by a factor of 1000 compared to 2009 throughput, as shown in Figure 2 below. No other errors for fuel oil, fuel gas, WSR throughput or HHV are suspected.

**Figure 1. 2010 Fuel Gas Throughput**

Emission Unit ID	Emission Unit Description (78 characters max.)	Fuel Type	Annual Process Thruput	CORRECTED-Annual Throughput	Process Thruput Units
F5103	01 crude furnace	RFG	1119.34	1.11934	E6FT3S
F5153	02 crude furnace	RFG	461.77	0.46177	E6FT3S
F5201	01 boiler	RFG	151.11	151.11	E6FT3S
F5202	02 boiler	RFG	171.58	171.58	E6FT3S
F5203	03 boiler	RFG	107.1	107.1	E6FT3S
F5300	FCC Furnace	RFG	58.404	58.404	E6FT3S
F5600	Hydrogenation	RFG	11.272	11.272	E6FT3S
F5700	H2 Manufac.	RFG	94.237	94.237	E6FT3S
F5930	Isom Furnace 01	RFG	51.158	51.158	E6FT3S
F5950	Isom Furnace 02	RFG	12.614	12.614	E6FT3S
F6003	Asphalt Furnace	RFG	0	0	E6FT3S
F6200	Acid Plant CC	RFG	43.322	43.322	E6FT3S
F6262	Acid Pt Furnace	RFG	40.455	40.455	E6FT3S
KC6701	01 cogen, combined cycle	RFG	146.92	146.92	E6FT3S
KS6701	01 cogen, simple cycle	RFG	20.03	20.03	E6FT3S
KC6702	02 cogen, combined cycle	RFG	220.6	220.6	E6FT3S
KS6702	02 cogen, simple cycle	RFG	35.91	35.91	E6FT3S
KC6703	03 cogen, combined cycle	RFG	273.76	273.76	E6FT3S
KS6703	03 cogen, simple cycle	RFG	0	0	E6FT3S
					3019.6
					1440

**Figure 2. 2009 Fuel Gas Throughput**

Emission Unit ID	Process ID No. (Fuel ID No.)	Emission Unit Description (78 characters max.)	Fuel Type	Fuel Material Code	Annual Process Thruput	Daily Process Thruput	Process Thruput Units
F5103	2	01 crude furnace	RFG	553	1.072	0.00	E6FT3S
F5153	2	02 crude furnace	RFG	553	0.442	0.00	E6FT3S
F5201	2	01 boiler	RFG	553	151.111	0.41	E6FT3S
F5202	2	02 boiler	RFG	553	134.985	0.37	E6FT3S
F5203	2	03 boiler	RFG	553	142.757	0.39	E6FT3S
F5300	2	FCC Furnace	RFG	553	57.816	0.16	E6FT3S
F5600	2	Hydrogenation	RFG	553	17.832	0.05	E6FT3S
F5700	2	H2 Manufac.	RFG	553	94.595	0.26	E6FT3S
F5930	2	Isom Furnace 01	RFG	553	35.434	0.10	E6FT3S
F5950	2	Isom Furnace 02	RFG	553	14.194	0.04	E6FT3S
F6003	2	Asphalt Furnace	RFG	553	0.000	0.00	E6FT3S
F6200	2	Acid Plant CC	RFG	553	40.847	0.11	E6FT3S
F6262	2	Acid Pt Furnace	RFG	553	41.863	0.11	E6FT3S
KC6701	2	01 cogen, combined cycle	RFG	553	230	0.63	E6FT3S
KS6701	2	01 cogen, simple cycle	RFG	553	0	0.00	E6FT3S
KC6702	2	02 cogen, combined cycle	RFG	553	230	0.63	E6FT3S
KS6702	2	02 cogen, simple cycle	RFG	553	0	0.00	E6FT3S
KC6703	2	03 cogen, combined cycle	RFG	553	212	0.58	E6FT3S
KS6703	2	03 cogen, simple cycle	RFG	553	18	0.05	E6FT3S
					1424		

**General Information:**

- This workbook was built to calculate Greenhouse Gas (GHG) emissions for Hawaii Refinery and to list and organize all of the data elements required for EPA reporting under the US EPA's Greenhouse Gas Reporting Program (GHGRP). The rule can be found here: [http://www.ecfr.gov/cgi-bin/retrieveECFR?gp=&SID=32e4ac22189c45a4f794cb8868e1e75&n=pt40.21.98&r=PART&t=y-HTML#se40.21.98\\_136](http://www.ecfr.gov/cgi-bin/retrieveECFR?gp=&SID=32e4ac22189c45a4f794cb8868e1e75&n=pt40.21.98&r=PART&t=y-HTML#se40.21.98_136)
- The **orange** tabs summarize the data for each Subpart and the **blue** tabs are calculation spreadsheets.
- The **blue** tabs are modified versions of the 'Optional Calculation Spreadsheets' provided by the EPA. Instructions and original copies of the EPA's 'Optional Calculation Spreadsheets' can be found here: <https://www.ccdsupport.com/confluence/display/help/Optional+Calculation+Spreadsheets+Instructions>

As noted on each tab, the calculation spreadsheets are locked to avoid inadvertent changes. If modifications need to be made, they can be unlocked using the password "GHG".

All emissions calculations are done using these EPA spreadsheets except for Subpart MM emissions because no EPA spreadsheet was available for Subpart MM.

Subpart C and Subpart MM use emission factors from Tables C-1, C-2, MM-1, and MM-2. For reference these are included in dark blue tabs at the end of this workbook.

**Instructions:**

- Enter activity data into **light green boxes** on the **blue** tabs. Type in the data or **paste** values. The emissions results should automatically appear once all activity data has been pasted.
- Enter non-emissions data into **data tables** on the **orange** tabs.

**Data Entry Notes:**

- The calculation spreadsheets assume all gas volumes are measured using 60F as standard temperature, so the spreadsheets use a Molar Conversion Volume of 836.6 scf/kg-mole in emissions calculations. However, the EPA requires that for Subpart P calculations are done using gas volume measured using 68F as standard temperature. The calculation spreadsheet converts the gas volume from 60F to 68F and uses a Molar Conversion Volume of 849.5 scf/kg-mole in emissions calculations. Therefore you should enter all gas volumes using 60F as standard temperature.
- If data is collected more frequently than the calculation spreadsheet requires, average data arithmetically (straight average). For example, daily HHVs should be averaged to a single monthly value using the following formula:

$$\bar{x} = \frac{1}{n} * \sum_{i=1}^n x_i$$

**GHG Reporting Year Summary: 2016**

Subpart	Process Unit	CO2 Equation	CH4 Equation	N2O Equation	Tier	CO2 Emissions (tonnes)	CH4 Emissions (tonnes)	N2O Emissions (tonnes)	2016		Total CO2e Emissions
									2015	Total CO2e	
C	GP - 4 Diesel Engines	C-2a and C2b	C-9a	C-9a	1	31,774,465.51	1,288.97	0.25779	31,886,513	1,018,577	
C	GP - 1 Fuel Oil Combustion Sources	C-2a and C2b	C-9a	C-9a	2	115,303,514.61	4,606.00	0.92120	115,693,182	155,004,802	
C	GP - 3 WSR Combustion Sources	C-2a and C2b	C-9a	C-9a	2	57,140,225.10	2,520.15	0.50403	57,353,430	52,761,570	
C	GP - 2 Mix Drum Fuel Gas	C-3	C-8	C-8	3	107,796,310.00	1,673.86	0.16739	107,888,037	122,710,386	
P	Unit 27 - Hydrogen Manufacturing	P-1	N/A	N/A		5,433,024.32			5,433,024	5,838,766	
Y	Sweet Flare	Y-3	Y-4	Y-5		23,935.52	0.07225	0.00024	25,813	0.0000	
Y	Sour Flare	Y-3	Y-4	Y-5		437,554.85	1,320.74	0.00438	471,877	35,244	
Y	FCC Unit - Plant 53	Y-6 and Y-7a	Y-9	Y-10		184,685,974.83	5,410.19	1,08204	185,143,677	182,740,232	
Y	Unit 62 - Acid Plant	Y-12	N/A	N/A		588,779.07			588,779	641,270	
Y	Equipment Leaks	N/A	Y-21	N/A					14,500.00	362,500	
Y	Storage Tanks	N/A	Y-22	N/A					1,64523	41,131	36,535
										TOTAL CO2e:	504,887,964
											521,149,883

**Subpart A - Facility Information**

Plant Code	Hawaii Refinery	None
Primary NAICS Code	324110	
Did you use BAN/M?	No	
Do you have a cogen unit?	No	
Total CO2e Emissions	504,887,96	521,149,883

**General Information:**

- This workbook is used to summarize the GHG emissions calculations from reports created in Essential Suite.
- All emissions calculations are done in Essential Suite.
- Subpart C and Subpart MM use emission factors from Tables C-1, C-2, MM-1, and MM-2. For reference these are included in dark blue tabs at the end of this workbook. These factors are built into the Essential Suite calculations.

**Instructions:**

- Enter data into EPA's Electronic Greenhouse Gas Tool (e-GGRT). All data for both the Webform sections and the Inputs Verifier Tool (IVT) sections will be found in this workbook.
- Copy/paste value the prior year emissions into a new column for comparision with current reporting year emissions.
- Copy/paste the Essential Suite Reports into this spreadsheet and verify links are working properly.

**Data Entry Notes:**

- The EPA calculation spreadsheets (and Essential Suite) assume all gas volumes are measured using 60F as standard temperature, so the spreadsheets use a Molar Conversion Volume of 836.6 scf/kg-mole in emissions calculations. However, the EPA requires that for Subpart P calculations are done using gas volume measured using 65F as standard temperature. The calculation spreadsheet (and Essential Suite report) converts the gas volume from 60F to 68F and uses a Molar Conversion Volume of 849.5 scf/kg-mole in emissions calculations. **Therefore you should enter all gas volumes using 60F as standard temperature in the calculation spreadsheet/Essential Suite but, enter the eGGRT IVT gas volumes using the 68F column.**
- If data is collected more frequently than the calculation spreadsheet requires, average data arithmetically (straight average). For example, daily HHVs should be averaged to a single monthly value using the following formula:  

$$\bar{A} = \frac{1}{n} * \sum_{i=1}^n x_i$$

**GHG Reporting Year Summary: 2017**

Subpart	Process Unit	2016			2017			
		CO2 Equation	CH4 Equation	N2O Equation	Tier	CO2 Emissions (tonnes)	CH4 Emissions (tonnes)	N2O emissions (tonnes)
C	GP - 4 Diesel Engines	C-2a and C2b	C-9a	C-9a	1	37,498.197	1,5210	0.3042
C	GP - 1 Fuel Oil Combustion Sources	C-2a and C2b	C-9a	C-9a	2	95,728.568	3,8240	0.7648
C	GP - 3 WSR Combustion Sources	C-2a and C2b	C-9a	C-9a	2	54,023.549	2,3827	0.4765
C	GP - 2 Mix Drum Fuel Gas	C-3	C-8	C-8	3	120,172.440	1,5278	0.1528
C	Catalytic Oxidizer	C-3	C-8	C-8	3	105,815	0.0042	0.0004
P	Unit 57 - Hydrogen Manufacturing	P-1	N/A	N/A		4,881.102		4,881.102
Y	Sweet Flare	Y-3	Y-4	Y-5		0.000	0.0000	0.0000
Y	Sour Flare	Y-3	Y-4	Y-5		130,335	0.3934	0.0013
Y	FCC Unit - Plant 53	Y-6 and Y-7-a	Y-9	Y-10		161,832.057	4,7413	0.9483
Y	Unit 62 - Acid Plant	Y-12	N/A	N/A		581,045		581,045
Y	Equipment Leaks	N/A	Y-21	N/A		14,5000		362,500
Y	Storage Tanks	N/A	Y-22	N/A		1,5506		38,765
						1,5506		41,131
								TOTAL CO2e: 504,887.964
								eGGRT IVT CO2e: 476,522.800

**Subpart A - Facility Information**

Plant Code	Hawaii Refinery
Primary NAICS Code	None
Did you use BAMM?	324110
Do you have a cogen unit?	No
Total CO2e Emissions	476,523.43

**Item 2. FCC CO<sub>2</sub> Calculation Differences**

YEAR	2010												
Process Unit	FCC Unit- Plant #3												
Method	Data Source	Flow Rate [Gas Volume] [FlowRateAlt]	Flow Rate O <sub>2</sub> Enriched [FlowRateCO2Enrich]	Concentration, Enriched (ppmv) - Oxygen [FlowRateAlt]	Concentration (ppmv) - Carbon Dioxide [MolPerC1CO2]	Concentration (ppmv) - Carbon Monoxide [MolPerC1CO]	Concentration (ppmv), Oxygen [MolPerC1O2]	Annual Tons CO <sub>2e</sub>	Annual Tons CH <sub>4</sub> e	Annual Tons NO <sub>x</sub>	Annual Tons CO <sub>2e</sub>	Difference	Data Input Methodology
1	Submitted 2016 Data												Calculated monthly emissions using the average monthly data. Sum monthly emissions to get annual emissions.
2	Average of 2016 Submitted Data												Calculated annual emission using average of the average monthly data.
3	GHG Calculation Spreadsheet												Calculated using the GHG Spreadsheet used for 2016 & 2017 emissions using annual average of hourly data
4	egGRT GHG Report Summary												Used data as summarized on GHG Summary Report to recalculate annual emissions.
5	egGRT Flight Report												From egGRT Flight Report.

**Item 3. FO FG WSR Calculation Difference**

**2009 FO FG WSR Summary**

		Throughput Unit		2009 Throughput		HHV		HHV Unit Num		HHV Unit Denom		Conversion factor to Throughput Unit		Throughput in HHV Unit Denom		Heat (MMBTU)	
<b>Fuel Oil</b>		<b>AEI</b>	BBL	381,694.0		150,262	E6BTU		E3GAL		0.0420			16,031.1		2,408,872	
		<b>GHG</b>	BBL	406,304.0		150,359	E6BTU		E3GAL		0.0420			17,064.8		2,565,841	
				6.06%	0.06%							6.06%	6.12%				
<b>Refinery Fuel Gas</b>		<b>AEI</b>	E6FT3S	1,423.8		1,036	E6BTU		E3FT3S		1,000.00			1,423,848.0		1,475,107	
		<b>GHG</b>	E6FT3S	1,845.8		1,028	E6BTU		E3FT3S		1,000.00			1,845,824.9		1,897,508	
				22.86%	-0.78%							22.86%	22.26%				
<b>Whole Straight Run</b>		<b>AEI</b>	BBL	129,991.0		111,143	E6BTU		E3GAL		0.0420			5,459.6		606,799	
		<b>GHG</b>	BBL	131,668.0		119,150	E6BTU		E3GAL		0.0420			5,530.1		658,905	
				1.27%	6.72%							1.27%	7.91%				

**GHG EMISSION REDUCTION PLAN REV 2**  
**IES DOWNSTREAM, LLC**  
**JANUARY 2021**



## **Appendix C**

### **CAB Letter dated July 22, 2019**



STATE OF HAWAII  
DEPARTMENT OF HEALTH  
P.O Box 3378  
HONOLULU, HAWAII 96801-3378

In reply please refer to  
File:

19-445E CAB  
File No. 0863

July 22, 2019

Mr. Jon Mauer  
President & CEO  
IES Downstream, LLC  
91-480 Makakole Street  
Kapolei, Hawaii 96707

Dear Mr. Mauer:

**SUBJECT: Greenhouse Gas (GHG) Emission Reduction Plan  
Covered Source Permit (CSP) No. 0863-01-C  
IES Downstream, LLC  
Kapolei Refinery  
Located At: 91-480 Makakole Street, Kapolei, Oahu**

The Department of Health, Clean Air Branch (CAB), has reviewed the IES Downstream, LLC (IES) Greenhouse Gas Emission Reduction Plan (GHGERP) dated December 14, 2018. The plan well documents and accurately projects the planned division of equipment ownership at the Kapolei Refinery. The plan also provides sufficient justification that calendar year 2010 is unrepresentative of normal operations for the baseline year, calendar year 2009 is a more suitable baseline year, and that the calendar year 2009 actual GHG emissions are the most recent representative emissions of normal operations.

The CAB identified minor concerns with respect to the documentation of GHG emissions estimates for calendar years 2006 – 2010 in Sections 2.1 and 2.2 of the GHGERP. The facility-wide emission estimates included in several of the tables did not match those calculated in Attachment V from Appendix B of the GHGERP. For example, in Table 1 of the GHGERP, the proposed 2009 baseline is 581,734 metric tons of CO<sub>2</sub>e while Attachment V presents a calculated value of 577,945 metric tons of CO<sub>2</sub>e. Based on the information currently available, the CAB has concluded that 577,945 metric tons of CO<sub>2</sub>e is the most accurate estimate for 2009 GHG emissions. While Attachment V also notes that the associated approximate 1% difference is due to the “Difference in Averaging Periods, GWP and EF Changes”, the CAB cannot concur with the larger 581,734 metric tons of CO<sub>2</sub>e value without additional justification.

The CAB also had questions related to calculations in Section 2.3 of the GHGERP that determine the baseline emission split between equipment that IES owns and the equipment that IES sold. The two spreadsheet files that Gail Godenzi of IES sent in a March 13, 2019 email and a follow-up email on March 25, 2019, provided the information needed to document the split in emissions. However, the CAB cannot concur with the proposed CO<sub>2</sub>e baseline emission level of 347,277 metric tons for the IES Terminal as it is associated with a total combined CO<sub>2</sub>e emissions level of 581,734 metric tons. As stated above, IES should provide additional information to justify use of the 581,734 metric ton value or alternatively propose a revised baseline emission split using the 2009 total combined baseline CO<sub>2</sub>e emissions level of 577,945 metric tons from Attachment V in Appendix B of the GHGERP.

Mr. Jon Mauer  
July 22, 2019  
Page 2

Section 3.0 of the GHGERP proposes a facility-wide GHG emissions cap for the IES Terminal of 291,713 metric tons per year. This value results from the application of a 16% reduction from the proposed IES Terminal CO<sub>2</sub>e baseline emissions level of 347,277 metric tons. The CAB cannot concur with the proposed facility-wide GHG emissions cap without the larger 581,734 metric tons of CO<sub>2</sub>e combined total being adequately justified. Alternatively, IES could also propose a revised facility-wide GHG emissions cap for the IES Terminal based on the 2009 total combined baseline CO<sub>2</sub>e emissions level of 577,945 metric tons from Attachment V in Appendix B of the GHGERP.

Sections 4.0 and 5.0 of the GHGERP presents a GHG Control Assessment, and Proposed Control Strategy, respectively, that are based on a facility-wide GHG emissions cap that is 16% less than the proposed IES Terminal baseline. The CAB cannot currently concur with the contents of these sections because of issues raised with respect to Sections 2.0 and 3.0 of the GHGERP. However, if the CAB had been able to concur with the facility-wide GHG emissions cap for the IES Terminal that represented a 16% reduction from an approved IES Terminal baseline, the contents of these sections would have met the requirements of the HAR.

Please note that CAB appreciates the consistent use of metric tons for quantifying emissions throughout the IES documentation. However, in future updates, please also include the corresponding values in short tons for the IES Terminal proposed baseline emission rate and facility-wide GHG emissions cap.

Based on the results of this review, it appears that relatively minor revisions to technical content in the GHGERP are needed. However, because of the business transactions that have occurred since submitting the GHGERP, a comprehensive revision to the GHGERP could require a significant amount of effort for marginal, if any, addition in clarity. Another option would be for IES to resubmit the GHGERP with an errata document, and the updated information. This would include the contents of the two spreadsheet files provided on March 13, 2019 and clarification in the March 25, 2019 email.

In accordance with HAR §11-60.1-204(e), the CAB requests that a revised GHG Emission Reduction Plan or errata document be provided by August 23, 2019.

If there are any questions regarding this matter, please contact Mr. Keith McFall of my staff at (808) 586-4200.

Sincerely,



MARIANNE ROSSIO, P.E.  
Manager, Clean Air Branch

KM:rkb



DAVID Y. IGE  
GOVERNOR OF HAWAII



FILE COPY

BRUCE S. ANDERSON, Ph.D.  
DIRECTOR OF HEALTH

Initials KH mri 7-22-21  
Mailed Out JUL 22 2019

STATE OF HAWAII  
DEPARTMENT OF HEALTH  
P.O. Box 3378  
HONOLULU, HAWAII 96801-3378

July 22, 2019

In reply, please refer to:  
File:

19-445E CAB  
File No. 0863

Mr. Jon Mauer  
President & CEO  
IES Downstream, LLC  
91-480 Makakole Street  
Kapolei, Hawaii 96707

Dear Mr. Mauer:

**SUBJECT:** Greenhouse Gas (GHG) Emission Reduction Plan  
Covered Source Permit (CSP) No. 0863-01-C  
IES Downstream, LLC  
Kapolei Refinery  
Located At: 91-480 Makakole Street, Kapolei, Oahu

The Department of Health, Clean Air Branch (CAB), has reviewed the IES Downstream, LLC (IES) Greenhouse Gas Emission Reduction Plan (GHGERP) dated December 14, 2018. The plan well documents and accurately projects the planned division of equipment ownership at the Kapolei Refinery. The plan also provides sufficient justification that calendar year 2010 is unrepresentative of normal operations for the baseline year, calendar year 2009 is a more suitable baseline year, and that the calendar year 2009 actual GHG emissions are the most recent representative emissions of normal operations.

The CAB identified minor concerns with respect to the documentation of GHG emissions estimates for calendar years 2006 – 2010 in Sections 2.1 and 2.2 of the GHGERP. The facility-wide emission estimates included in several of the tables did not match those calculated in Attachment V from Appendix B of the GHGERP. For example, in Table 1 of the GHGERP, the proposed 2009 baseline is 581,734 metric tons of CO<sub>2</sub>e while Attachment V presents a calculated value of 577,945 metric tons of CO<sub>2</sub>e. Based on the information currently available, the CAB has concluded that 577,945 metric tons of CO<sub>2</sub>e is the most accurate estimate for 2009 GHG emissions. While Attachment V also notes that the associated approximate 1% difference is due to the "Difference in Averaging Periods, GWP and EF Changes", the CAB cannot concur with the larger 581,734 metric tons of CO<sub>2</sub>e value without additional justification.

The CAB also had questions related to calculations in Section 2.3 of the GHGERP that determine the baseline emission split between equipment that IES owns and the equipment that IES sold. The two spreadsheet files that Gail Godenzi of IES sent in a March 13, 2019 email and a follow-up email on March 25, 2019, provided the information needed to document the split in emissions. However, the CAB cannot concur with the proposed CO<sub>2</sub>e baseline emission level of 347,277 metric tons for the IES Terminal as it is associated with a total combined CO<sub>2</sub>e emissions level of 581,734 metric tons. As stated above, IES should provide additional information to justify use of the 581,734 metric ton value or alternatively propose a revised baseline emission split using the 2009 total combined baseline CO<sub>2</sub>e emissions level of 577,945 metric tons from Attachment V in Appendix B of the GHGERP.

Mr. Jon Mauer  
July 22, 2019  
Page 2

Section 3.0 of the GHGERP proposes a facility-wide GHG emissions cap for the IES Terminal of 291,713 metric tons per year. This value results from the application of a 16% reduction from the proposed IES Terminal CO<sub>2</sub>e baseline emissions level of 347,277 metric tons. The CAB cannot concur with the proposed facility-wide GHG emissions cap without the larger 581,734 metric tons of CO<sub>2</sub>e combined total being adequately justified. Alternatively, IES could also propose a revised facility-wide GHG emissions cap for the IES Terminal based on the 2009 total combined baseline CO<sub>2</sub>e emissions level of 577,945 metric tons from Attachment V in Appendix B of the GHGERP.

Sections 4.0 and 5.0 of the GHGERP presents a GHG Control Assessment, and Proposed Control Strategy, respectively, that are based on a facility-wide GHG emissions cap that is 16% less than the proposed IES Terminal baseline. The CAB cannot currently concur with the contents of these sections because of issues raised with respect to Sections 2.0 and 3.0 of the GHGERP. However, if the CAB had been able to concur with the facility-wide GHG emissions cap for the IES Terminal that represented a 16% reduction from an approved IES Terminal baseline, the contents of these sections would have met the requirements of the HAR.

Please note that CAB appreciates the consistent use of metric tons for quantifying emissions throughout the IES documentation. However, in future updates, please also include the corresponding values in short tons for the IES Terminal proposed baseline emission rate and facility-wide GHG emissions cap.

Based on the results of this review, it appears that relatively minor revisions to technical content in the GHGERP are needed. However, because of the business transactions that have occurred since submitting the GHGERP, a comprehensive revision to the GHGERP could require a significant amount of effort for marginal, if any, addition in clarity. Another option would be for IES to resubmit the GHGERP with an errata document, and the updated information. This would include the contents of the two spreadsheet files provided on March 13, 2019 and clarification in the March 25, 2019 email.

In accordance with HAR §11-50.1-204(e), the CAB requests that a revised GHG Emission Reduction Plan or errata document be provided by August 23, 2019.

If there are any questions regarding this matter, please contact Mr. Keith McFall of my staff at (808) 586-4200.

Sincerely,

MARIANNE ROSSIO, P.E.  
Manager, Clean Air Branch

KM:rkb

Mr. Jon Mauer  
July 22, 2019  
Page 2

Section 3.0 of the GHGERP proposes a facility-wide GHG emissions cap for the IES Terminal of 291,713 metric tons per year. This value results from the application of a 16% reduction from the proposed IES Terminal CO<sub>2</sub>e baseline emissions level of 347,277 metric tons. The CAB cannot concur with the proposed facility-wide GHG emissions cap without the larger 581,734 metric tons of CO<sub>2</sub>e combined total being adequately justified. Alternatively, IES could also propose a revised facility-wide GHG emissions cap for the IES Terminal based on the 2009 total combined baseline CO<sub>2</sub>e emissions level of 577,945 metric tons from Attachment V in Appendix B of the GHGERP.

Sections 4.0 and 5.0 of the GHGERP presents a GHG Control Assessment, and Proposed Control Strategy, respectively, that are based on a facility-wide GHG emissions cap that is 16% less than the proposed IES Terminal baseline. The CAB cannot currently concur with the contents of these sections because of issues raised with respect to Sections 2.0 and 3.0 of the GHGERP. However, if the CAB had been able to concur with the facility-wide GHG emissions cap for the IES Terminal that represented a 16% reduction from an approved IES Terminal baseline, the contents of these sections would have met the requirements of the HAR.

Please note that CAB appreciates the consistent use of metric tons for quantifying emissions throughout the IES documentation. However, in future updates, please also include the corresponding values in short tons for the IES Terminal proposed baseline emission rate and facility-wide GHG emissions cap.

Based on the results of this review, it appears that relatively minor revisions to technical content in the GHGERP are needed. However, because of the business transactions that have occurred since submitting the GHGERP, a comprehensive revision to the GHGERP could require a significant amount of effort for marginal, if any, addition in clarity. Another option would be for IES to resubmit the GHGERP with an errata document, and the updated information. This would include the contents of the two spreadsheet files provided on March 13, 2019 and clarification in the March 25, 2019 email.

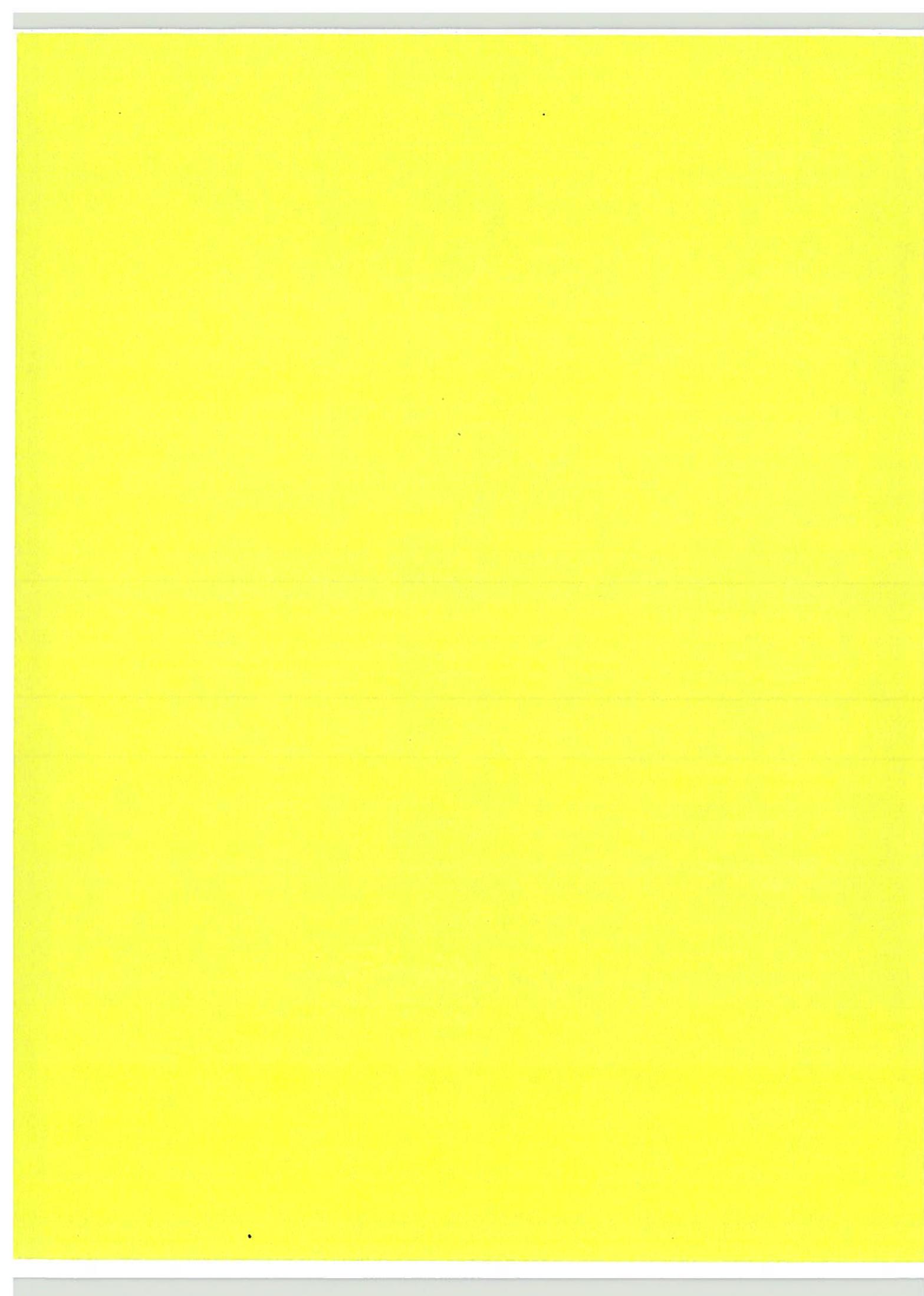
In accordance with HAR §11-60.1-204(e), the CAB requests that a revised GHG Emission Reduction Plan or errata document be provided by August 23, 2019.

If there are any questions regarding this matter, please contact Mr. Keith McFall of my staff at (808) 586-4200.

Sincerely,

  
MARIANNE ROSSIO, P.E.  
Manager, Clean Air Branch

KM:rkb



**GHG EMISSION REDUCTION PLAN REV 2**  
**IES DOWNSTREAM, LLC**  
**JANUARY 2021**



## **Appendix D**

**IES Email response sent March 25,  
2019**

**From:** McFall, Keith  
**To:** Godenzi, Gail  
**Subject:** RE: [\*EXTERNAL\*] follow-up to 2/7/2019 meeting-: Emailing - GHG Partnering Request.pdf  
**Date:** Monday, March 25, 2019 4:01:10 PM  
**Attachments:** image001.png  
image002.png  
image003.png

---

Hi Gail,

This answers the question very well.

Thank you,

Keith

Keith McFall, PE, PhD  
Environmental Engineer, Clean Air Branch  
Environmental Management Division  
Tel: (808) 586-4200

**From:** Godenzi, Gail <Gail.Godenzi@islandenergyservices.com>  
**Sent:** Monday, March 25, 2019 3:40 PM  
**To:** McFall, Keith <Keith.McFall@doh.hawaii.gov>  
**Subject:** RE: [\*EXTERNAL\*] follow-up to 2/7/2019 meeting-: Emailing - GHG Partnering Request.pdf

FCC Startup heater was never used in the 2009 baseline year

**From:** McFall, Keith <Keith.McFall@doh.hawaii.gov>  
**Sent:** Tuesday, March 19, 2019 2:29 PM  
**To:** Godenzi, Gail <Gail.Godenzi@islandenergyservices.com>  
**Cc:** Lum, Darin W C <darin.lum@doh.hawaii.gov>; Madsen, Michael A <michael.madsen@doh.hawaii.gov>  
**Subject:** RE: [\*EXTERNAL\*] follow-up to 2/7/2019 meeting-: Emailing - GHG Partnering Request.pdf

Hi Gail,

Thank you again for the information. It provides the information needed to document the emission split between the two owners.

I only have one minor follow-up, and you probably mentioned this in our conversations. It seems likely that these are presumed insignificant for the purposes of the split, but I would like clarification on emissions associated with the "FCC Startup Air Heater". They do not appear to be included in the "Fuel Gas to Refinery 2009 HDOH Request" file.

Thank you,

Keith

Keith McFall, PE, PhD  
Environmental Engineer, Clean Air Branch  
Environmental Management Division  
Tel: (808) 586-4200

**From:** McFall, Keith  
**Sent:** Wednesday, March 13, 2019 11:14 AM  
**To:** 'Godenzi, Gail' <Gail.Godenzi@islandenergyservices.com>  
**Cc:** Lum, Darin W C <darin.lum@doh.hawaii.gov>; Madsen, Michael A <michael.madsen@doh.hawaii.gov>  
**Subject:** RE: [\*EXTERNAL\*] follow-up to 2/7/2019 meeting-: Emailing - GHG Partnering Request.pdf

Hi Gail,

Thank you. I will review and get back to you ASAP.

Keith

Keith McFall, PE, PhD  
Environmental Engineer, Clean Air Branch  
Environmental Management Division  
Tel: (808) 586-4200

**From:** Godenzi, Gail <[Gail.Godenzi@islandenergyservices.com](mailto:Gail.Godenzi@islandenergyservices.com)>  
**Sent:** Wednesday, March 13, 2019 10:33 AM  
**To:** McFall, Keith <[Keith.McFall@doh.hawaii.gov](mailto:Keith.McFall@doh.hawaii.gov)>; Madsen, Michael A <[michael.madsen@doh.hawaii.gov](mailto:michael.madsen@doh.hawaii.gov)>  
**Cc:** Lum, Darin W C <[darin.lum@doh.hawaii.gov](mailto:darin.lum@doh.hawaii.gov)>  
**Subject:** RE: [\*EXTERNAL\*] follow-up to 2/7/2019 meeting:- Emailing - GHG Partnering Request.pdf

Keith, see attached spreadsheets for the calculations of the below requested emissions. Emission factors are included.

Let me know when you have some time and we can walk thru these calculations over the phone, or I can come to you and we can do it FTF.

LMK

Gail



**Gail Godenzi**  
Environmental and Process Engineer  
[gail.godenzi@islandenergyservices.com](mailto:gail.godenzi@islandenergyservices.com)

IES Downstream, LLC  
91-480 Malakole Street  
Kapolei, HI 96707  
Tel +1 808. 682.3113  
Mobile +1 808.352.7840

Official Licensee of the Texaco Brand in Hawai'i



---

**From:** McFall, Keith <[Keith.McFall@doh.hawaii.gov](mailto:Keith.McFall@doh.hawaii.gov)>  
**Sent:** Tuesday, March 12, 2019 1:51 PM  
**To:** Godenzi, Gail <[Gail.Godenzi@islandenergyservices.com](mailto:Gail.Godenzi@islandenergyservices.com)>; Madsen, Michael A <[michael.madsen@doh.hawaii.gov](mailto:michael.madsen@doh.hawaii.gov)>  
**Cc:** Lum, Darin W C <[darin.lum@doh.hawaii.gov](mailto:darin.lum@doh.hawaii.gov)>  
**Subject:** [\*EXTERNAL\*] follow-up to 2/7/2019 meeting:- Emailing - GHG Partnering Request.pdf

Hi Gail,

Thank you for the update and letter for reference.

As we discussed in our last telcon, a partnership with a 16% reduction from the combined baseline would remove the need for the information we requested on 2/7/2019 (attached). However, as I recall from our conversations and your 2/28/2019 email (also attached), there should not be a lot of effort needed on your part to respond to that request. I agreed that the emissions by individual unit by process were not needed, but that emissions from groups of units by process for each owner would be needed. So, in the four examples below (taken from the "2009 Baseline Info") sheet, we are requesting the calculation details associated with the

- A. 103,699 CO<sub>2</sub>e Metric Ton combined emissions associated with units F-5103 & F-5153 from Fuel Oil Combustions
- B. 89,647 CO<sub>2</sub>e Metric Ton combined emissions associated with units F-5201, F-5202, & F-5203 from Fuel Oil Combustion
- C. 76,598 CO<sub>2</sub>e Metric Ton combined emissions associated with units F-5103 through F-6704 from Fuel Gas Combustion
- D. 27,391 CO<sub>2</sub>e Metric Ton combined emissions associated with units F-5300 through F-5203 from Fuel Gas Combustion.

Sub-part	Emission Group for "IES 2009 Summary" & "Summary Data" (e.g., Crude, FCC, FO Comb, FG Comb, Flare P1, Flare P2, Fugitives, H2 Manufac, AP, WSR Comb)	Owner	Equipment	Equipment Desc.	Permit	Process / Fuel Info	CO2e Metric Ton	Supporting Calculation Reference
C	FO Comb	Eagle Ref.	F-5103	Crude Atm Furnace	CSP 0088-01-C	Fuel Oil Combustion	103,699	?
C	FO Comb	Eagle Ref.	F-5153	Crude VacFurnace	CSP 0088-01-C	Fuel Oil Combustion		?
C	FO Comb	IES Term.	F-5201	Boiler	Retired	Fuel Oil Combustion	89,647	?
C	FO Comb	IES Term.	F-5202	Boiler	Retired	Fuel Oil Combustion		?
C	FO Comb	IES Term.	F-5203	Boiler	Retired	Fuel Oil Combustion		?
C	FG Comb	Eagle Ref.	F-5103	Crude Atm Furnace	CSP 0088-01-C	Fuel Gas Combustion	76,598	?
C	FG Comb	Eagle Ref.	F-5153	Crude VacFurnace	CSP 0088-01-C	Fuel Gas Combustion		?
C	FG Comb	Eagle Ref.	F-5700	Hydrogen Furnace	CSP 0088-01-C	Fuel Gas Combustion		?
C	FG Comb	Eagle Ref.	F-5930	Isomerization Furnace	CSP 0088-01-C	Fuel Gas Combustion		?
C	FG Comb	Eagle Ref.	F-5950	Isomerization Furnace	CSP 0088-01-C	Fuel Gas Combustion		?
C	FG Comb	Eagle Ref.	F-5600	Hydrogenation Furnace	CSP 0088-01-C	Fuel Gas Combustion		?
C	FG Comb	Eagle Ref.	F-6200	Acid Plant Combustion Chamber	CSP 0088-01-C	Fuel Gas Combustion		?
C	FG Comb	Eagle Ref.	F-6260	Acid Plant Pre-heater	CSP 0088-01-C	Fuel Gas Combustion		?
C	FG Comb	Eagle Ref.	F-6701	Cogen	CSP 0088-01-C	Fuel Gas Combustion		?
C	FG Comb	Eagle Ref.	F-6702	Cogen	CSP 0088-01-C	Fuel Gas Combustion		?
C	FG Comb	Eagle Ref.	F-6703	Cogen	CSP 0088-01-C	Fuel Gas Combustion		?
C	FG Comb	Eagle Ref.	F-6704	Cogen	CSP 0088-02-C	Fuel Gas Combustion		?
C	FG Comb	IES Term.	F-5300	FCC Furnace	TBD	Fuel Gas Combustion	27,391	?
C	FG Comb	IES Term.	F-5310	FCC Startup Air Heater	TBD	Fuel Gas Combustion		?
C	FG Comb	IES Term.	F-5201	Boiler	Retired	Fuel Gas Combustion		?
C	FG Comb	IES Term.	F-5202	Boiler	Retired	Fuel Gas Combustion		?
C	FG Comb	IES Term.	F-5203	Boiler	Retired	Fuel Gas Combustion		?

Could you propose a delivery date for the information in the spreadsheet "IES-DS-GHGERP-Dec2018-1.xlsx" if indication of a tentative agreement between the two owners cannot be presented by that time?

Thank you,

Keith

Keith McFall, PE, PhD  
 Environmental Engineer, Clean Air Branch  
 Environmental Management Division  
 Tel: (808) 586-4200



## **GHGERP Change Log**

<b>Date</b>	<b>Description of Review/ Amendment</b>
06/2018	Start of Change Log
12/18/18	GHG plan submitted to HDOH with split between IES and Par
8/22/19	Revised 12/18/18 plan to IES only with Lower FCC Combustion based on HDOH request (Rev 1)
1/24/21	Revised 8/22/19 plan - Transferred Boilers 1/2/3 equipment ownership to Par, updated Sections 2,3,4,5, and added Section 6 regarding partnering (Rev 2).