MEMORANDUM

From: <u>Technical Director</u>, Naval Facilities Engineering and Expeditionary Warfare Center

To: (b) (6), Navy Petroleum Office

Subj: RED HILL FUEL FACILITY PIPELINE FAILURE FULL SYSTEM INTEGRITY REPORT

Encl: (1) Contractor's Root Cause Analysis dtd 07 September 2021

- 1. In support of the Navy Petroleum Office investigation of the pipeline failure at the Red Hill Fuel Facility on 06 May 2021, Naval Facilities Engineering and Expeditionary Warfare Center (NAVFAC EXWC) deployed a team of civilian and contractor subject matter experts to: objectively assess the event; provide recommendations to assist in returning the facility to full operability; and determine the cause of the failure.
- 2. NAVFAC's technical authority personnel with warranting and subject matter expertise over POL infrastructure have reviewed the Root Cause Analysis (enclosure), and concur with the findings.
- 3. NAVFAC EXWC's next deliverable is the Recommended Repair List. This deliverable will provide corrective recommendations to the JP-5 system and is scheduled for delivery on 14 September 2021.
- 4. If you have any questions on this report or following actions, my point of contact for this effort is (b) (6) (b) (6).





ROOT CAUSE ANALYSIS OF THE JP-5 PIPELINE DAMAGE

ASSESS TANK 20 PIPING FOR RETURN TO SERVICE AT RED HILL BULK FUEL STORAGE FACILITY

JOINT BASE PEARL HARBOR-HICKAM (JBPHH), HONOLULU, HI

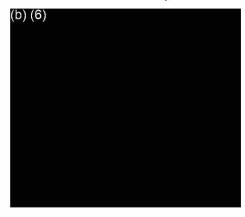
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September 7, 2021

ACRONYM DEFINITION

AFHE Automated Fuel Handling Equipment

ASME American Society of Mechanical Engineers
ASTM American Society for Testing and Materials

bbl Barrel(s)

DBB Double Block and Bleed

EXWC Engineering and Expeditionary Warfare Center

FLC Fleet Logistics Center

JBPHH Joint Base Pearl Harbor-Hickam

JP-5 Jet Fuel

lbf Pound Force

lbs Pounds

MOV Motor Operated Valve

NAVFAC Naval Facilities Engineering Command

NC Normally Closed

NFPA National Fire Protection Agency
NIWC Naval Information Warfare Center

NO Normally Open

PIT Pressure Indicating Transmitter

psi Pounds per Square Inch

psig Pounds Per Square Inch Gauge

RHTF Red Hill Tank Farm

SCADA Supervisory Control and Data Acquisition

UGPH Underground Pumphouse

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ASSESS TANK 20 PIPING FOR RETURN TO SERVICE AT RED HILL BULK FUEL STORAGE FACILITY

I. EXECUTIVE SUMMARY

Brockenbrough was contracted under NAVFAC EXWC Contract No. N39430-20-D-2242, Delivery Order No. N3943021F4122, to determine the root cause of the piping failure at Red Hill Tank Farm (RHTF) that occurred on May 6, 2021, at approximately 18:00 hours. See Appendix 'A' for a basic flow schematic of the system at the time.

Based upon collected field data and discussions with various facility personnel during site visits in June and July of 2021, it has been determined that the JP-5 piping system suffered a significant transient surge pressure at the noted date and time. This surge pressure was primarily caused by disregarding the proper valve sequencing dictated in the specific operations orders.

When all of the valves between a tank's closed skin valve at the RHTF and Surge Tank (b) (3) (A) are open except the butterfly valves (b) (3) (A), the closed butterfly valves leak. This allows the (b) (3) (A) column of JP-5 to sag as it tries to reach equilibrium with the atmospheric pressure on Surge Tank . The resulting void, technically a vacuum, created in the piping at upper portions of the RHTF will collapse rapidly if subjected to a high pressure source.

The following is what appears to have happened on May 6th. Towards the end of Evolution 3, the valve lineup below Tank 20 was set as described above for a period of over five minutes creating a vacuum with a volume of 23 bbl. Operations then moved to Evolution 4. As Tank 12 was being prepared for use in Evolution 4, the valve lineup was again set to allow for another five minutes of sag creating an additional 16 bbl of vacuum. When Tank 12's skin valve was opened, the inrush from the head in Tank 12 collapsed the 39 bbl of vacuum. This created a calculated transient surge pressure of approximately 350 psig in only milliseconds, or almost instantaneously, near Tanks 18 and 20. This energy displaced the (5) (3) (A) JP-5 mainline piping near Tank 20 at least 16 inches laterally and separated the Dresser couplings at Tanks 18 and 20.

It should be noted that while the incorrect sequencing of the valves was the primary, or root, cause, there were several other contributing factors in addition to the leaking butterfly valves. The AFHE system did not trigger an out-of-balance alarm or low pressure alarm prior to the event, and the use of Dresser couplings in sections of unrestrained pipe profoundly affected the amount of damage.

II. FINDINGS AND OBSERVATIONS

On May 6, 2021, the JP-5 piping system at the RHTF experienced a significant event that caused two Dresser couplings to completely separate and the piping to move enough to damage surrounding features in the area of Tanks 17, 18, 19, and 20. The event occurred during normal operations, and the operators had no explanation for the cause.

The facility had just completed Evolution 3 that involved moving JP-5 from Tank 12 to Tank 20. See Appendix 'B' for the DFSP Pearl Harbor Specific Operations Order (Evolution 3). Due to the piping and tank arrangement and varying vertical depths of product in the tanks at RHTF, product movements between tanks are often a multi-step process and may require the use of the pumps and surge tanks at the UGPH. In the case of Evolution 3, the final step involved pumping JP-5 from Surge Tank to Tank 20.

As Evolution 3 was being completed, the next movement, Evolution 4, was beginning. This evolution was to move product from Tank 12 to Tank 9. See Appendix 'B' for the DFSP Pearl Harbor Specific Operations Order (Evolution 4). This operation also required the use of the UGPH, and the first step was to gravity feed from Tank 12 to Surge Tank

At this point there was not anything amiss to the operations personnel as they began opening the last valve in the lineup between Tank 12 and Surge Tank 2. However, the event occurred as soon as the product started to flow out of Tank 12. A loud bang was heard by the operator who was in the lower piping tunnel near Tank 18 at the time. When the operator went to investigate, fuel was seen on the floor of the tunnel coming down from Tanks 17 through 20. The evolution was quickly stopped, and the system was secured.

It should be noted that the RHTF has been undergoing tank maintenance for several years. This includes changes to or temporary removals of the piping systems at the tank laterals. At the time of the event, the JP-5 piping systems at Tanks 18, 19, and 20 contained Dresser couplings, and the piping at Tanks 17, 18, and 19 was not connected to the tank. Blind flanges had been installed at the ends of any active piping, but no other arrangements had been made to restrain the system.

The primary physical damage clearly points to a large surge pressure created within the piping system. The damage included:

- 1. The unrestrained (b) (3) (A) piping at Tank 18 separated at the Dresser coupling and fell to the floor. See Photo 1. There did not appear to be any collateral damage.
- 2. The unrestrained (b) (3) (A) piping at Tank 19 moved longitudinally towards Tank 19 and began to separate at the Dresser coupling until it ran into a pipe support preventing it from completely coming apart. The pipe support and some adjacent conduits were bent, but there did not appear to be any additional collateral damage.
- 3. The (b)(3)(A) piping at Tank 20 completely separated at the Dresser coupling. See Photo 2. The only obvious collateral damage was to the tunnel's ceiling system directly above the Dresser coupling. The panels were mechanically damaged by the pressurized liquid.
- 4. The end of the (b) (3) (A) JP-5 mainline piping moved approximately 16 inches laterally towards Tank 19 creating a large indentation in adjacent ductwork and bending the adjacent conduit. See Photo 3.

Since the event, JP-5 Tanks 11, 12, and 20 and their associated piping systems have been secured. JP-5 Tanks 13, 14, 17, 18, and 19 are out of service for unrelated reasons. The remainder of RHTF and UGPH are still in operation but at a limited capacity until the cause is determined and damage is repaired.

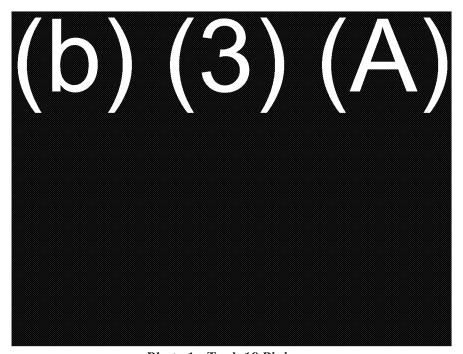


Photo 1 - Tank 18 Piping
This is the section of piping including the Dresser coupling seen at the far end that separated and fell to the floor.

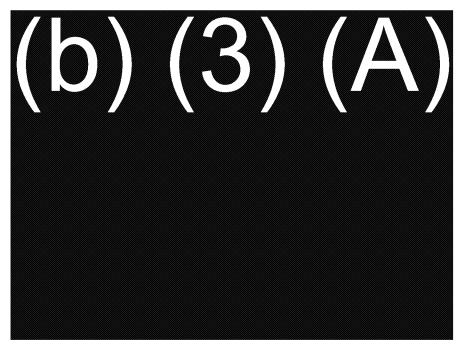


Photo 2 - Tank 20 PipingThe piping separated at Tank 20's Dresser coupling.

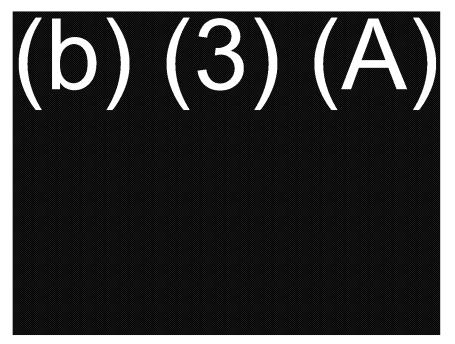


Photo 3 - Mainline Piping

The end of the (b) (3) (A) mainline piping between Tanks 19 and 20 moved approximately 16 inches laterally (to the right) as seen here by the collateral damage to the ductwork.

III. BACKGROUND

Distribution Piping System

There are three fuel products in the distribution piping systems at RHTF: JP-5, F-24, and F-76. The systems connect the RHTF with the UGPH via the lower tunnel that runs approximately (b) (3) (A) between the two facilities. At the RHTF, the JP-5's (b) (3) (A) mainline pipe runs the entire length of the lower tunnel in the tank farm from Tank 1 to Tank 20 (approximately (b) (3) (A)). The JP-5 pipeline then connects with each JP-5 tank via laterals (also referred to as the cross-tunnel piping) using a combination of (b) (3) (A) and (b) (3) (A) piping.

Within the JP-5 piping system there are numerous valves at both the RHTF and the UGPH. Some of these valves are only for maintenance or emergency purposes, and therefore, they stay open most of the time. These valves are referred to as normally open (NO) valves. The valves that are used to control the flow of JP-5 during each movement of fuel during an evolution are only opened when necessary. These valves are referred to as normally closed (NC) valves.

Each evolution has a specific operations order in which the NC valves are to be opened. The order is very important to control when and where the fuel and its associated pressure, either by pump or static pressure, is applied. The RHTF is very unique in its geographical footprint, elevation changes, physical size, and the volume of fuel within its tanks and piping systems. For this reason, any potential upset in a valve lineup that would not create significant issues at a normal bulk storage fuel facility are multiplied several magnitudes greater at RHTF.

Column Separation

The phenomenon of column separation and vacuum in piping systems and the damaging pressure surges created by it are well documented in scientific and engineering literature. The physics behind the creation of a vacuum in a pipeline vary depending on the situation. Due to the significant elevation change from the RHTF to the UGPH ((10)(3)(4)), there is always the potential for a large void or vacuum to be created in the piping system if the valves are not opened in the proper sequence. When the system is then exposed to pressure by opening a valve, the void collapses very rapidly creating a significant surge pressure in milliseconds. It is well known that the energy created this way can damage the pipe and any weaker components in the system.

Vacuum is normally measured as a pressure, however in this report the term also represents the void in the piping created by the column separation. All of the gauging at RHTF is measured in barrels, so the amount of vacuum created is also measured in barrels for simplicity.

IV. ANALYSIS

Physical Damage Assessment

A stress analysis of the mainline and cross-tunnel piping at Tanks 19 and 20 was performed based on measured movements indicated by the collateral damage. The purpose was to determine what forces and pressures the piping experienced during the event.

Pipe stress analysis utilizes analytical methods to determine how a piping system responds to the combination of pipe material, process pressures and temperatures, fluid weight, support methodology, and various potential loading conditions as required per ASME B31.3.

Caesar II software was used to analyze the piping system using 3D beam elements. The piping was modeled in accordance with available drawings and physical data taken during the two site visits. After the model was created, the load cases were defined in accordance with the relevant piping code, ASME B31.3. The software then determined the loads on supports and equipment connections, piping displacements, and pipe stresses for the various load cases defined.

The piping had a lateral displacement in the 'X' direction of approximately 16 inches measured at the blind flange at the end of the (b) (3) (A) mainline piping. The piping system at Tanks 19 & 20 were analyzed to determine the approximate forces that resulted in the measured deflection. All piping in the model is (b) (3) (A) . The piping was determined to be (b) (3) (A) based on the wall thickness determined by the pipe pedigree report dated 2019 and the data taken during the two site visits (see Figure 3 for piping material input). To determine the approximate force, the piping was modeled in the condition just after the surge event with the Dresser coupling separated and no connection between the lateral and Tank 20. A force was applied at the location of the blind flange on the lateral for Tank 19 (see Figure 4), and the resultant displacement was investigated.

The model was operated in an iterative process until a displacement at the blind flange (location where displacement was measured in field) was approximately 16-inch (see Figure 1 - Caesar II Model). This force was found to be approximately 78,000 lbf which equates to a pressure of 320 psi on the blind flange adjacent to Tank 19. As seen in Figure 2, the stress concentration was found to be most intense at (b) (3) (A) (in the Figure, the color gradient gray/yellow/red indicates increasing stress, with red being the highest stress concentration observed). Refer to Appendix 'D' for the analysis' full output.



Figure 1 - Caesar II Model

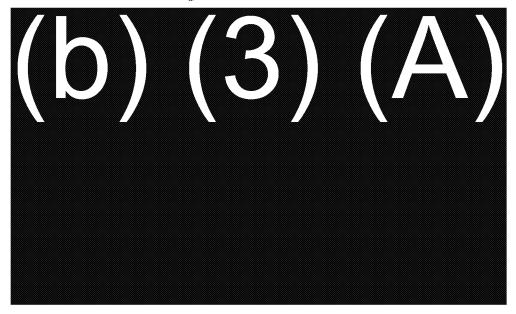


Figure 2 - Caesar Model Showing Stress Intensification at Tees/Joints

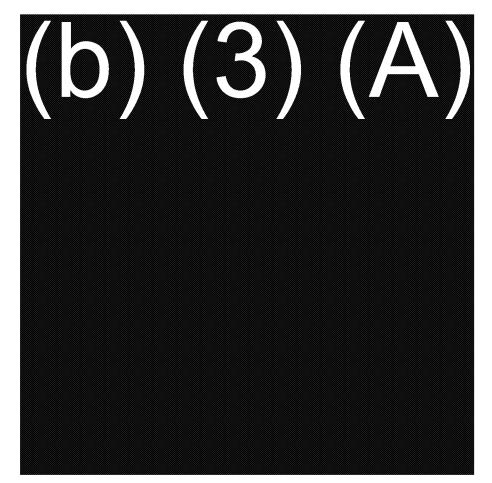


Figure 3 - Basic Inputs for Caesar Model

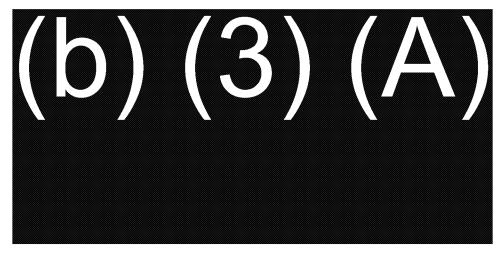


Figure 4 - Force Input at Blind Flange Adjacent to Tank 19

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Hydraulic and Surge Analysis

The sequence of events on May 6th were hydraulically modelled to determine if the estimated surge matches the measured pipe movement and its associated stress. The hydraulic and surge analysis was conducted independent of the stress analysis.

Introduction

In order to model the surge characteristics from the JP-5 piping located near Tanks 19 and 20, a computer simulation was performed using the KY PIPE 2008: SURGE v. 8.014 computer software program.

The system was modeled using the following steps:

- 1. First, the system was modeled using a number of pipe segments connected by components and piping junctions between the two tanks. Head losses were calculated using the Hazen Williams equation. The system was then modeled at steady state conditions.
- 2. Once the steady state conditions were successfully modeled, the next step consisted of modifying the state of one or more components in the system. The modifications to the steady state conditions produces transients throughout the system that can be modeled as a series of waves that travel through the system at the speed of sound. These waves are affected by friction attenuation, junctions, and component state changes.
- 3. For steady state conditions, the computer program records the pressures and flowrates in every pipe and node throughout the system. For surge analysis, it records the pressures and flowrates for all user defined nodes and updates the data at a specified time increment for a specified node.
- 4. The last step consisted of formatting and generating the System Report. This report printout consisted of two sections; the first detailed the steady state conditions throughout the system, the second detailed the simulation results. A table was also included showing the maximum and minimum heads (or pressures) encountered over the simulation at every node in the system.

Description of the System

The attached simplified flow schematic, Figure 5, shows the system that was modeled in KY PIPE for computer simulations. It consists of Tank 12 transferring fuel via gravity to Surge Tank. The valves at Tank 12 open and close at the times indicated, and the resulting pressure surges are calculated.

The tank, pipe segment and components used to build the model are shown below.

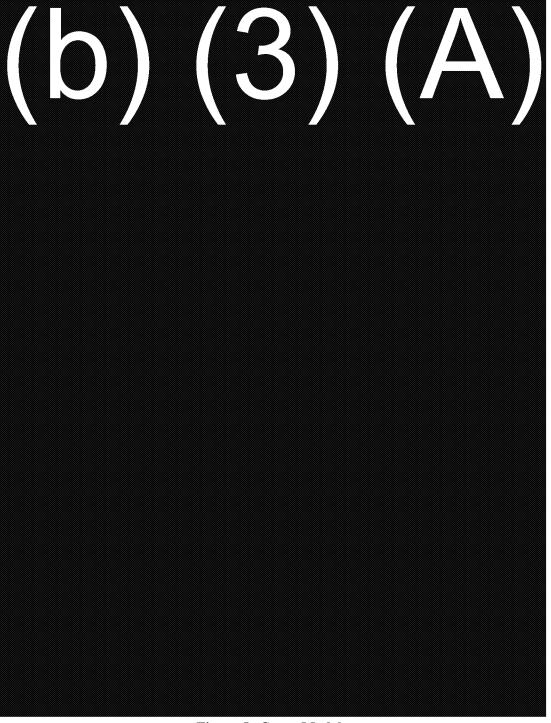
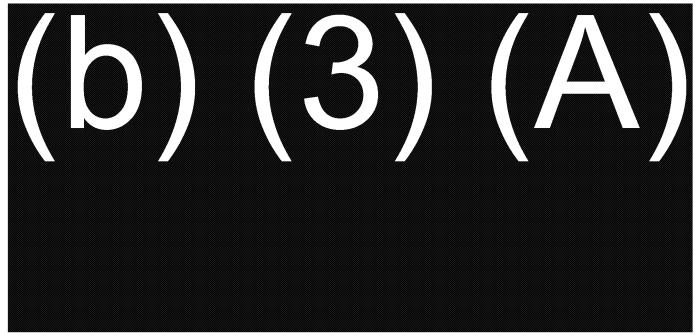


Figure 5 - Surge Model

Description of System Components

- 1. Product: Jet Fuel (JP-5), Specific Gravity: 0.84, Kinematic Viscosity: 1.5 X 10-5 ft. 2/sec.
- 2. Piping: (b) (3) (A)
- 3. Pumps: The scenario modeled in this situation is one in which fuel is transferred using gravity only from Tank 12 to Surge Tank. As a result, no pumps have been modeled in this system.
- 4. Valves: Valves included in this system include butterfly valves, ball valves and double block and bleed valve. The ball valve (b) (3) (A) at Tank 12 opens first, the double block and bleed valve (b) (3) (A) at Tank 12 then opens. Next the same ball valve starts to close and then the double block and bleed valve begins to close. Finally, the ball valve fully closes, followed by the complete closure of the double block and bleed valve. Butterfly valves (b) (3) (A) and are modeled as being slightly open for the first 100 seconds of the calculation to simulate leakage past the valves. All other valves are modeled to be fully open. This includes the gate valve (b) (3) (A) and the double block and bleed valve (b) (3) (A) at Surge Tank Valve operation times were taken from Automated Fuel Handling Equipment (AFHE) records at the site. The first operation (the opening of the ball valve) is shown to occur at time = 200 seconds to allow adequate time for the steady state condition to develop. Finally, double block and bleed valves do not open linearly. A majority of the opening time is spent lifting the plug, rather than turning the plug to allow flow through the valve. As a result, the double block and bleed valve is shown opening or closing during the last 14 seconds of its operating time.

Valve operation is summarized below in Table 1. Actual times are taken from reports generated by the AFHE system.



Discussion of Results

The opening of the valves at Tank 12 causes a surge in pressure in the piping system. At the (b) (3) (A) mainline piping between Tank 19 and Tank 20, represented by junction J-6, the maximum pressure surge is seen to be 357 psig as indicated in the nodes results shown in Figure 6, and as shown on the graph in Figure 7. The pressure is seen at t = 335, which is approximately 11 seconds after the double block and bleed valve begins to open. Prior to that, the system pressure in that area falls to -14.4 psig, which indicates that a vacuum (referred to in the calculation output as cavitation) has occurred. Refer to Appendix 'E' for the analysis' full output.

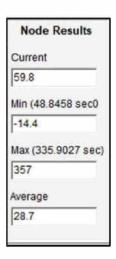
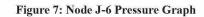


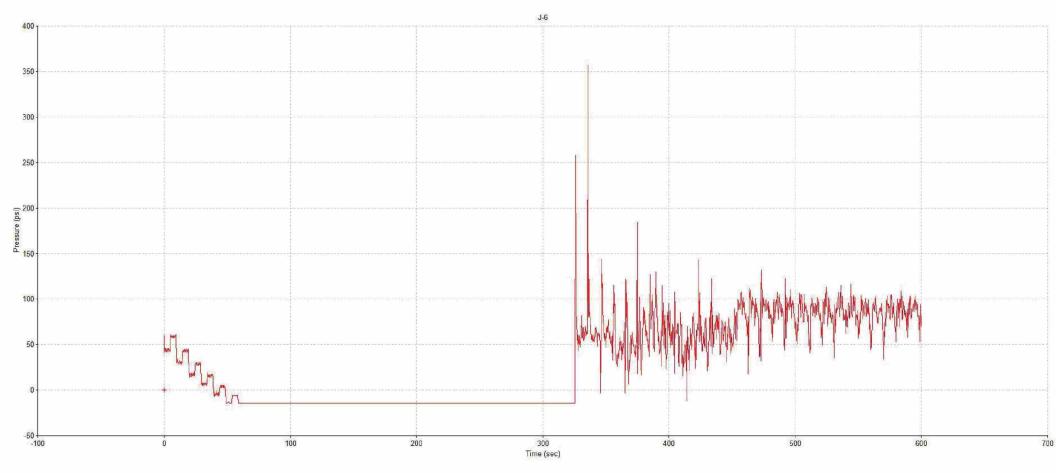
Figure 6 - Node J-6 Pressure Results

Note that this simulation models the system in its current condition and does not consider the failure in the piping system. It is beyond the capability of the surge software to model a rupture in the piping. Everything after the pressure surge, which would have caused the piping failure, indicates pressures that would have been obtained absent the piping failure. The intent of this calculation was to determine the level of the pressure surge that would be responsible for the damage, which was calculated to be 357 psig.

It should also be noted that the software indicated pressure surges elsewhere in the system, including in . In reviewing the data from the pressure indicating transmitter, the area of (b) (3) (A) (b) (3) (A) which is in the vicinity of the two butterfly valves (on the Tank 20 side), it was found that the AFHE system captured pressure readings from this transmitter only sporadically, with several seconds between pressure readings. At times, the interval between pressure readings was up to 10 seconds. As the pressure surge would have been very short lived (milliseconds), it is likely that the pressure rise occurred during one of these long intervals between pressure readings and was not read by (b) (3) (A) Although these pressure surges were seen in the system, damage was not incurred at these locations since the piping in these areas had been adequately restrained.

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Valve Analysis

Only four valves were actuated during the timeframe of the event. They are:

(b) (3) (A) - (b) (3) (A) DBB valve at Tank 12.
 (b) (3) (A) - (b) (3) (A) ball valve at Tank 12.
 (b) (3) (A) - (b) (3) (A) ball valve in the (b) (3) (A) Duter Loop section of the UGPH.
 (b) (3) (A) - (b) (3) (A) gate valve in the (b) (3) (A) branch line in the UGPH that leads to Surge Tank (a).

The AFHE system had trouble opening (b) (3) (A) for over 30 minutes leading up to the event, and (b) (3) (A) had both torque limit and stall alarms just four minutes before the event. We suspect that these problems are not related to the valve or its actuator but are due to the pressure differentials across the valves at the time.

The two valves in the UGPH did not have any issues on May 6, 2021 and operated normally without any alarms.

To confirm that all four valves are operating normally, each one was operated numerous times under noload conditions during the field investigation trip of July 2021. All four valves performed properly. See the results in Appendix 'F'. The valves generally do take longer to open/close than what is stamped on the nameplates, but they did not overload based on the measured amperages.

The testing also found that it takes the AFHE system from three to five seconds to sense movement in a valve, and the DBB valve's plug only rotates during the last 14 seconds when going from 0% to 100% open.

There is no indication that an equipment failure on any of these valves occurred at the time of the event.

AFHE Data Analysis (Sequence of Events)

The recorded data from the AFHE control system was the primary source of data to establish the sequence of events between 17:15:00 and 18:30:00 on May 6, 2021. See Figure 8. This image is an actual snapshot from the AFHE system. Using the system's event log, alarm log, data logging and charting features, a single chronological order of every event, alarm, and data point during the time frame can be determined. See Appendix 'G' for the printed data. This information, along with numerous discussions with FLC operations, FLC maintenance, NIWC, and ENGlobal personnel, has been used to develop the following general sequence shown in Table 2. The AFHE control system does monitor and record every data point that it measures. However, it does not measure/record it at a high enough frequency to detect an event that lasts for only milliseconds (such as a transient surge pressure).

It should be noted that the event occurred during the transition between the last step of Evolution 3 and the first step of Evolution 4. Evolution 3 involved completely filling Tank 20 from Tank 12 in steps using Surge Tank. Evolution 4 involved transferring JP-5 from Tank 12 to Tank 9 in steps using Surge Tank. Most of the valve lineup was already set from Evolution 3 prior to beginning Evolution 4, and only four valves were actuated during the time frame in question. The general sequence below only addresses the equipment and instrumentation readings that were involved with the event, and we have not included the unrelated events and alarms that occurred.

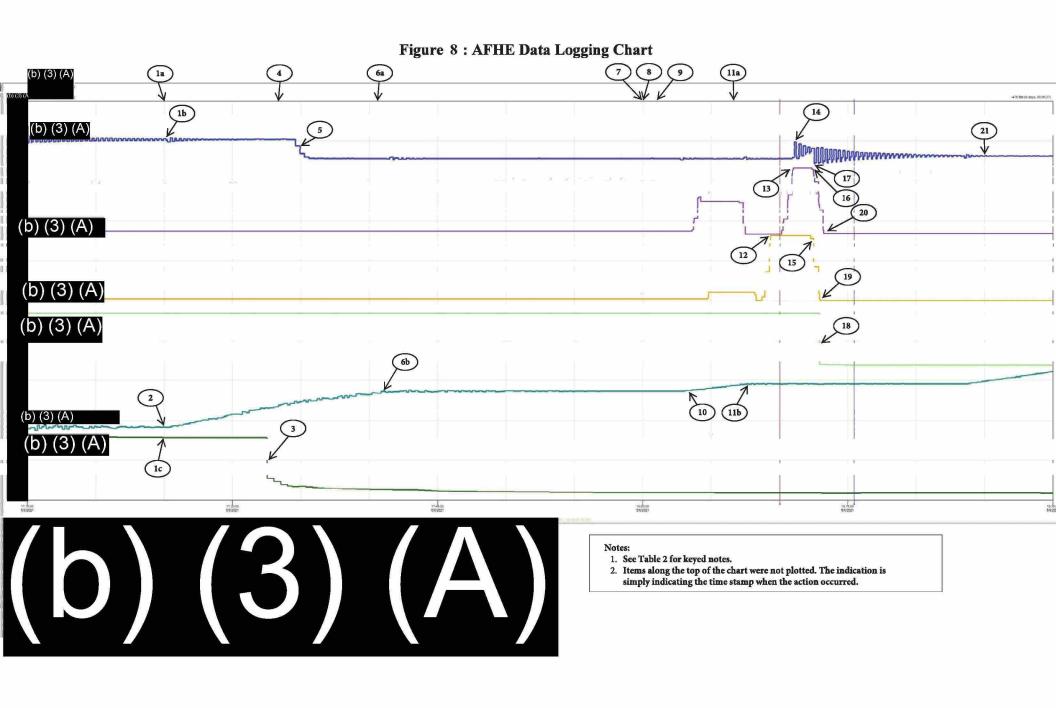


		TABLE 2	- Sequence of Eve	nts
Time Stamp (interval)	Figure 8 Keyed Notes	Equipment Item	Action/Reading	Commentary
17:24:58	1a	(b) (3) (A)	Valve is set to open	Once this gate valve in the branch line to Surge Tank is opened, all valves between Tank 20 and Surge Tank are now open except for the two butterfly valves (b) (3) (A) in the UGPH.
	1b	(b) (3) (A)	(b) (3) (A)	This pressure represents the full height of Tank 20 on the system between the RHTF and the UGPH. This represents the pressure on the closed butterfly valves that are leaking.
	1c	Tank 20	(b) (3) (A)	Tank 20's gross volume is steady at this time and does not start to show the expected decrease in volume for approximately 7.5 minutes. It is believed that the tank is losing volume at this time, and the delayed response is due to the tank gauging's precision and the AFHE polling frequency.
17:25:14 (00:16)	2	Surge Tank	(b) (3) (A)	Surge Tank net volume almost immediately starts to show an increase in volume. This appears to indicate that one or both butterfly valves are leaking. The butterfly valves could not be tested for leakage during the field investigation of July 2021, but FLC will be conducting a test to verify.
17:32:33 (07:19)	3	Tank 20	(b) (3) (A)	The AFHE system finally sees the drop in Tank 20's volume that has most likely been occurring since 17:24:58. It loses 44 bbl during this one reading. It finally settles out at (b) (3) (A) around 17:45:03 with a total loss of 58 bbl.
17:33:28 (00:55)	4	(b) (3) (A)	Valves set to close	The ball valve at Tank 20 (F) begins closing first with the DBB valve (E) starting to close about 1 minute later. Both the tank skin and ball valves are fully closed at 17:35:57.
17:35:41 (02:13)	5	(b) (3) (A)	31 psig	While Tank 20's skin and ball valves are closing the pressure in the UGPH drops 94 psi over a period of 82 seconds. This is expected as the 79.3 psi of head from Tank 20 has been removed from the system by the closing of Tank 20's skin and ball valve. An additional 14.7 psi is lost due to the vacuum created by the leaking butterfly valve(s). The pressure essentially remains at this level until the event at 18:11:07.
17:41:38 (05:57)	6a	(b) (3) (A)	Valve 0% open	Once this valve is closed, the flow to Surge Tank stops as would be expected. Surge Tank svolume has settled at
	6b	Surge Tank	(b) (3) (A)	this point with a total gain of 81 bbl over 16 minutes. Therefore, a vacuum of approximately 23 bbl (Tank 20's loss of 58 bbl minus Surge Tank

		TABLE 2	- Sequence of Eve	nts
Time Stamp (interval)	Figure 8 Keyed Notes	Equipment Item	Action/Reading	Commentary
				bbl) has formed in the piping at RHTF. AFHE does check for an out-of-balance between tanks during a transfer, but the tolerance is too high to catch this small amount.
18:00:21 (18:43)	7	Evolution 3	Complete	
18:00:52 (00:31)	8	Evolution 4	Start	
18:02:31 (01:39)	9	(b) (3) (A)	Valve is set to open	Once this gate valve in the branch line to Surge Tank is opened, all valves between RHTF and Surge Tank are now open except for the two butterfly valves in the UGPH.
18:03:06 (00:35)	10	Surge Tank	(b) (3) (A)	Within 35 seconds of opening (b) (A) Surge Tank starts gaining volume due the leaking butterfly valve(s).
18:07:31 (04:25)	11a	(b) (3) (A)	Valve is 0% open	Once this ball valve in the outer loop header is closed, the flow to Surge Tank stops as would be expected.
	11b	Surge Tank	(b) (3) (A)	Surge Tank 's volume has settled at this point with a total gain of 16 bbl over 4.5 minutes. The vacuum in the piping at RHTF has now grown to approximately 39 bbl. As noted above, AFHE does check for an out-of-balance between tanks during a transfer, but the tolerance is too high to catch this small amount.
18:09:21 (01:50)	12	(b) (3) (A)	100% open	Tank 12's ball valve is fully open.
18:11:01 (01:40)	13	(b) (3) (A)	100% open	Tank 12's DBB valve is fully open. It should be noted that field testing indicated that while it takes seconds for the motor actuator to completely open the valve, the plug goes from open over the last seconds. It is impossible to determine the exact moment of the surge, but it most likely occurred between when the valve started opening at 18:10:02 and when the plug first started to rotate at 18:10:46. There is also some lag or latency between when the valve actuator starts and the AFHE system detects the valve moving. Field testing indicated the lag to be about seconds.
18:11:07 (00:06)	14	(b) (3) (A)	110 psig	Once Tank 12's skin and ball valves are open, the pressure at the UGPH immediately goes from 30 psig to 110 psig in 22 seconds indicating a transient surge pressure in the system. This is approximately when the 39 bbl of vacuum collapses as the head of Tank

		TABLE 2	- Sequence of Eve	ents
Time Stamp (interval)	Figure 8 Keyed Notes	Equipment Item	Action/Reading	Commentary
				12 is introduced to the system. The transient surge pressure then causes the unrestrained piping to move which separates the Dresser coupling fittings.
18:12:18 (01:11)	15	(b) (3) (A)	Valve set to close	Tank 12's ball valve starts closing.
18:12:24 (00:06)	16	(b) (3) (A)	Valve set to close	Tank 12's DBB valve starts closing.
18:12:33 (00:09)	17	(b) (3) (A)	6 psig	As the valves start closing, the waveform changes and the system reaches its lowest point during the attenuation. This waveform, while not the same magnitude as the model, does mimic the model's shape.
18:12:56 (00:23)	18	Tank 12	(b) (3) (A)	Tank 12's net volume finally drops 473 bbl over 50 seconds. It is believed that the tank is losing volume before this time, and as noted above, the delayed response is due to the tank gauging's precision and the AFHE polling frequency.
18:12:57 (00:01)	19	(b) (3) (A)	0% open	Tank 12's ball valve is fully closed.
18:13:15 (00:18)	20	(b) (3) (A)	0% open	Tank 12's DBB valve is fully closed.
18:25:00 (11:45)	21	(b) (3) (A)	43 psig	The pressure has now settled, and it now shows the expected pressure of the head from the piping between UGPH and the ruptured pipe at Tank 18.

V. CONCLUSION

Root Cause

Our assessment of the data determined that the root cause of the event was procedural error. If the personnel had closed all of the normally closed valves at the end of Evolution 3 as prescribed by the operations order and then opened the valves in the prescribed order for Evolution 4, the system would have not experienced the damaging surge. This omission allowed either one or both of the closed butterfly valves in the lineup to leak, causing the column of fuel to sag into Surge Tank. This led to a vacuum in the main piping at the top of RHTF that rapidly collapsed when Tank 12 was opened for Evolution 4.

Supporting Evidence

At the end of Evolution 3, the valves in the lineup between Tank 20 and Surge Tank were open except for the two butterfly valves for approximately 10 minutes. The AFHE data indicates Surge Tank increasing in volume during this time, and it also shows a corresponding drop in Tank 20's volume of approximately the same amount. Therefore, the butterfly valve(s) must have been leaking due to the head from the column of JP-5 from the open Tank 20 (approximately (b) (3) (A)). Tank 20's skin and ball valves were then closed, but Surge Tank continued to gain volume while none of the RHTF tanks lost any volume and the pressure in the pipeline quickly sagged. This indicates continued leakage around the butterfly valve(s) and the creation of a vacuum. The pocket of vacuum did not stop growing until approximately five minutes later when (b) (3) (A) was closed. The presence of this vacuum pocket is corroborated by the expected and immediate drop in pressure at (b) (3) (A) from approximately 120 psig to 30 psig.

Approximately 25 minutes later at the official start of Evolution 4 (Tank 12 to Surge Tank was re-opened. This made all of the valves in the lineup between RHTF and Surge Tank with the exception of the two butterfly valves, open for approximately five additional minutes. The AFHE data indicates a second increase in Surge Tank volume during this time without the expected decrease in volume by one of the Red Hill tanks. Therefore, the butterfly valve(s) must have been leaking again as the column of JP-5 trapped below all of the tanks' closed skin valves sagged a little more trying to reach its natural state of equilibrium with Surge Tank.

The large pocket of perfect vacuum was probably created at the highest points in the JP-5 piping (the area of Tanks 17 – 20) while the column of JP-5 sagged through the leaking butterfly valve(s). It is estimated that the pocket was almost 39 bbl (the amount that Surge Tank gained after (b) (3) (A) closed). When the last remaining closed valve in the lineup for Tank 12 was finally opened to start Evolution 4, the quick opening nature of the double block and bleed valve (b) (3) (A) allowed a rapid inflow of JP-5 to collapse the pocket of vacuum. The resulting pressure wave from the collapse of the vacuum pocket is what displaced the unrestrained piping and separated the Dresser couplings creating all of the collateral damage.

Contributing Factors

The contributary causes of the piping failure at the RHTF include:

1. The butterfly valves were used for shut-off service during both evolutions, but butterfly valves are not appropriate for bubble-tight shut-off service. Therefore, the leaking butterfly valves contributed to the event.

- 2. AFHE's out-of-balance alarm during Evolutions 3 and 4 was set to (b) (3) (A) Evolution 3 involved an extra 23 bbl flowing into Surge Tank (without the corresponding decrease in Tank 12 or Tank 20's volume), and Evolution 4 involved an additional 16 bbl into Surge Tank . The lack of an out-of-balance alarm prior to the event was a contributing factor.
- 3. AFHE's low pressure alarm for (b) (3) (A) was set to -9 psig. When the tank skin and ball valves at Tank 20 were closed at the end of Evolution 3, (b) (3) (A) indicated a pressure drop from 125 psig down to 31 psig. This rapid drop alone was an indicator of a significant problem, and the 31 psig reading was clearly outside of the usual norm for Evolution 3. The lack of a low pressure alarm for (b) (3) (A) prior to the event was another contributing factor.
- 4. The use of Dresser couplings in sections of unrestrained piping was a contributing factor in this case. The physical damage seen at Tanks 17 20 would not have occurred if the piping systems had been fully installed and inherently restrained by connection to the tanks.

AFHE Data Discrepancies

The pressure at (b) (3) (A) dropped rapidly after the skin and ball valves at Tank 20 were closed as would be expected if the butterfly valve(s) were leaking. However, the pressure only sagged to 31 psig, while physics would say that the column of JP-5 should drop to about 40 feet above the level of Surge Tank (14.7 psig). Our assumption is that while the butterfly valve(s) leak when there is 120 psi on the system, they don't appear to leak when only seeing 31 psig.

A vacuum was being created during the periods that Surge Tank was gaining volume without a corresponding loss from the RHTF. In both instances of this, (b) (3) (A) did not see an appreciable drop in pressure. This is because the pipeline at RHTF is only sloped only change the pressure a modest 1 psi.

It should be noted that Tank 20's data indicates a single, immediate drop of about 40 bbl followed by another drop of 20 bbl over 2.5 minutes. It appears the rapid drop is not accurate, and it was most likely a steady decrease over the 10-minute timeframe between (b) (3) (A)' opening and closing. The misleading rapid drop is simply a function of the gauging system's precision along with the SCADA system's polling speed. These tanks are unique in the world, and the gauging system is a one-of-its-kind with limited precision under extremely rare conditions such as this anomaly. During normal operations, this does not present any problems as the volumes are large enough and occur over a much longer period that are easily measured by the system in real time.

(b) (3) (A) shows a maximum pressure of 110 psig at the time of the event and a minimum pressure of 6 psig afterwards while it attenuated the surge over a period of almost 15 minutes. During this time, the interval between SCADA readings was up to 20 seconds. Our model shows the same waveform of the attenuation but with much higher and lower pressures. This is because the model is calculating the pressure every millisecond. We believe the time interval between SCADA readings essentially failed to capture the spikes seen in the model.

Modelling Corroboration

The physical damage that was created during the event left enough evidence to verify the above conclusion. The ^[b] JP-5 mainline pipeline moved laterally 16 inches away from Tank 20 as measured from the large dent in the adjacent ductwork. As noted in Section IV, Physical Damage Assessment, our pipe stress analysis determined that a force of approximately 78,000 lbs was required to move the pipe the 16 inches. The 78,000 lbs of force is equivalent to a pressure of ^[b] applied to the interior of an ^[b] pipe, and in Section IV, Hydraulic and Surge Analysis, our surge analysis predicted

a transient surge pressure of approximately 357 psi created in milliseconds in the piping between Tanks 19 and 20. Therefore, it is reasonable to conclude that the surge pressure's energy created by the collapsing vacuum pocket was powerful enough to move the pipe, separate the Dresser coupling, and create the damage to the adjacent ductwork.

Considering that this analysis ignores any thrust from the fuel leaving the piping at Tank 20's separated Dresser coupling, the pipe should have moved even more. However, a pipe support on the section of pipe going to Tank 19 prevented it. The support has obvious damage from where the pipe's flange hit the support stopping the pipe's trajectory and preventing the Dresser coupling at Tank 19 from separating.

Disclaimer

Report is based on information known as of the date of the report and subject to revision should new information become available.

VI. APPENDICES

APPENDIX 'A' - Master Operational Schematic, Pearl Harbor AFHE



APPENDIX 'B' - DFSP Pearl Harbor Specific Operations Order

i. Evolution 3

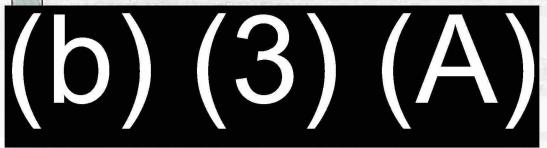
DFSP Pearl Harbor Specific Operations Order



1	Date	05/06/2	1 Time	~TBD	Location Various	STK	, tl	r fuel from JP5 hen to RH 20 fo ss Testing		
2	Operation Control Cont									
	Set pr 20.	Set procedure to transfer fuel from RH 12 to STK . Once filled, transfer fuel to RH tank 20.								
3	Refer	ences			13.000					
4	 DoD 4140.25-M, DoD Management of Bulk Petroleum Products, Natural Gas, and Coal 33 CFR Part 154, Facilities Transferring Oil or Hazardous Materials in Bulk 29 CFR §1910.38, Occupational Safety and Health Standards MIL-STD 3004-1: DoD Standard Practice Quality Assurance for Bulk Fuels, Lubricants, and Related Products UFC 3-460-03 Operation and Maintenance: Maintenance of Petroleum Fuel systems Operations, Maintenance, Environmental, and Safety Plan (OMES) Personnel Assignments WG-11 Control Operator WG-09/WG-08 Pump Operator 									
5	• 0			o monitor	the source	ank as r		red by Papa. Volume/Qty	~TBD bbl.	
			STK	Та	nk 20					
8	Com	municatio	ons Plan							
Handheld radios on channel 5-a										
9	9 Tools and Materials									
	Hard Hat if in the Red Hill Tunnel Complex Portable radios									
10		Preliminary								
	100000		o its High			. Transfe	er fu	iel from RH 12 1	to STK ; then fi	
11	Ope	rational F	Procedure							
	FILL SURGE TANK									

1

- Source tank is RH 12.
- Receipt tank is Surge Tank #
- Conwol operator will make preparations to transfer JPS fuel from Red Hill tank 10 to . He will notify the Red Hill rover that fuel transfer is about to start.
- Control operator will line up the piping and valve systems as follows:



FILL RH 20

- Issue tank is STK
- Receipt tank is RH 20. Hi(b) (3) (A) imit is

 Use JPS transfer numes Use JPS transfer pumps
- Control operator will make preparations to transfer JP-S fuel from STK Papa will notify both the Red Hill and the Kuahua rovers when fuel transfer is about
- Control Operator will line up the piping and valve systems as follows:

The pump suction is from the inside line and will discharge to the outside line, then to RH 20:



- Control operator and the rovers will verify that all other valves remain closed.
- Once the control operator opens up the skin valve of the source and destination tanks, both rovers will verify that the valves are open.
- Fill RH 20 up to its high operating limit and STOP pumping. DO NOT EXCEED THE HIGH OPERATING LIMIT

DFSP Pearl Harbor Specific Operations Order

- Once the transfer is complete, close all valves and return the piping system to its normal configuration.
- Once the transfer is complete, close all valves and proceed to the next tank.

12 | Quality Plan

1. None

13 Emergency Response Plan

- a. Stop all transfer operations and close all valves.
- b. Notify the chain of command of the emergency and respond to the emergency with clean up material and containers and drip pans as required by the emergency.
- c. If needed, make alignment preparations to pump the fuel back to the source tank.

14 Safety Plan

- a. Maintain communication between the control room operator and all involved parties.
- b. Do not lose focus or become complacent.
- c. Do not be impatient. Think all steps through.
- d. Accidents happen without warning. Be aware of your surroundings. Do not become distracted.
- e. Be aware of strange sounds or smells.
- f. Remain calm in an emergency.
- g. The worker must be able to react quickly and properly in a safe mode.
- h. Contact Control Room Operator by radio to secure the operation. Slowly close valves, taking at least 15 seconds to shut the valve completely. Inform the Fuel Supervisors of the situation.
- i. Anyone has the authority and responsibility to call a halt to an operation if they believe an unsafe condition exists.

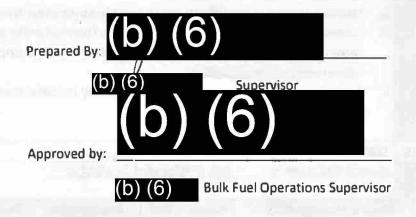
15 ORM

Overall RAC code of: RAC 3 Mitigated to a RAC 4

Hazard Threat/effect	Assess	RAC	Risk Control Action	Re-assess	Residual	Supervision
eak at pipe flanges.	0, 1	3	Area manned and monitored by, qualified operators	O, II	4	YES
Overfill the tank.	C, III	4	Area manned and monitored, qualified operators, Certified AFHE overfill protection	D, ##	5	YES

DFSP Pearl Harbor Specific Operations Order

		PROBABILITY						
Risk Assessment Matrix		Frequency of Occurrence Over Time						
		A Likely	B Probable	C May	D Unlikely			
1	Loss of Mission Capability, Unit Readiness or Asset; Death	1	1	2	- 3			
81	Significantly Degraded Mission Capability or Unit Readiness; Severe Injury or Damage	1	2	3	4			
III	Degraded Mission Capability or Unit Readiness; Minor Injury or Damage	2	3	4	5			
IV	Little or No Impact to Mission Capability or Unit Readiness; Minimal Injury or Damage.	3	4	5	5			



ii. Evolution 4

DFSP Pearl Harbor Specific Operations Order COPY





	Date	05/06/21	Time	~TBD	Vario	us ST	K [™] , 1	er fuel from JP5 then to RH 09 fo ess Testing					
2	Opera	ation	d vuole.										
	Set pr 09	ocedure to	transfer	fuel from	RH 121	to STK . Or	nce f	illed, transfer fu	iel to RH tank				
3	References												
		oD 4140.25- oal	·M, DoD	Managen	nent of I	Bulk Petrole	eum	Products, Natur	ral Gas, and				
								s Materials in B	ulk				
						and Health							
	ar	nd Related F	Products						els, Lubricants,				
								ce of Petroleun Plan (OMES)	n Fuel systems				
4	Perso	nnel Assigi	monte										
	• W	/G-11 Contr	ol Opera										
5	• W • W • O	/G-11 Contr /G-09/WG-0 ne Kuahua ne Red Hill	ol Opera 08 Pump rover to Rover to	Operator check pip monitor	eline du the sour	STK [®] , RH	-	cess ired by Papa. Volume/Qty	~TBD bbl.				
	• W • W • O	/G-11 Contr /G-09/WG-0 ne Kuahua ne Red Hill	ol Opera 08 Pump rover to Rover to	Operato check pip monitor	eline du the sour	rce tank as	requ	ired by Papa.	~TBD bbl.				
	• W • W • O • O	/G-11 Contr /G-09/WG-0 ne Kuahua ne Red Hill	ol Opera 08 Pump rover to Rover to H 12, FK	Operator check pip monitor	eline du the sour	STK, RH	requ	ired by Papa.	~TBD bbl.				
5	W O O Issue	/G-11 Contr /G-09/WG-0 ne Kuahua ne Red Hill Tank RI	rol Opera 08 Pump rover to Rover to H 12, K	Operator check pip monitor 6 Re Ta	eline du the sour	STK, RH	requ	ired by Papa.	~TBD bbl.				
5	• W • O • O Issue	/G-11 Contr /G-09/WG-0 ne Kuahua ne Red Hill Tank RI ST	rol Opera 08 Pump rover to Rover to H 12, K K S Plan on chan	Operator check pip monitor 6 Re Ta	eline du the sour	STK, RH	requ	ired by Papa.	~TBD bbl.				
5	• W • O • O Issue Comi	/G-11 Contr /G-09/WG-0 ne Kuahua ne Red Hill Tank RI ST munication	rol Opera 08 Pump rover to Rover to H 12, FK S Plan on chan rials	Operator check pip monitor 6 Re Ta	ceipt	STK, RH	requ	ired by Papa.	~TBD bbl.				
5 8	Comi	/G-11 Contr /G-09/WG-0 ne Kuahua ne Red Hill Tank RI Tank SI munication held radios	rol Opera 08 Pump rover to Rover to H 12, FK S Plan on chan rials	Operator check pip monitor 6 Re Ta	ceipt	STK, RH	requ	ired by Papa.	~TBD bbl.				
5 8	Comil Hand	/G-11 Contr /G-09/WG-0 ne Kuahua ne Red Hill Tank RI ST munication lheld radios s and Mater ard Hat if in ortable rad	rol Opera D8 Pump rover to Rover to H 12, FK S Plan on chan rials on the Rections	Operator check pip monitor 6 Re Ta nel 5-a Hill Tuni	ceipt nk nel Com	STK, RH 09	7	ired by Papa.					
5	Comil Hand Tools Hand Tools Preli	/G-11 Contr /G-09/WG-0 ne Kuahua ne Red Hill Tank RI ST munication held radios and Mater ard Hat if ir ortable rad	rol Opera 08 Pump rover to Rover to 112, rk s Plan on chan rials n the Rec ios r is for Ta	Operator check pip monitor 6 Re Ta nel 5-a Hill Tuni	ceipt nk nel Com	STK, RH 09	7	Volume/Qty					

1

- Source tank is RH 12.
- Receipt tank is Surge Tank #
- Control operator will make preparations to transfer JP5 fuel from Red Hill tank 10 to STK. He will notify the Red Hill rover that fuel transfer is about to start.
- Control operator will line up the piping and valve systems as follows:

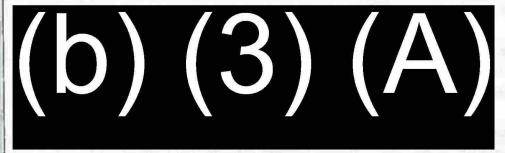


FILL RH 09

- Issue tank is STK
- Receipt tank is RH 09. High operating limit is (b) (3) (A)
- Use JP5 transfer pumps (b) (3) (A) as applicable
- Control operator will make preparations to transfer JP-5 fuel from STK to RH 09.
 Papa will notify both the Red Hill and the Kuahua rovers when fuel transfer is about to start.
- Control Operator will line up the piping and valve systems as follows:



 The pump suction is from the inside line and will discharge to the outside line, then to RH 20:



- Control operator and the rovers will verify that all other valves remain closed.
- Once the control operator opens up the skin valve of the source and destination tanks, both rovers will verify that the valves are open.
- Fill RH 09 up to its high operating limit and STOP pumping. DO NOT EXCEED THE HIGH OPERATING LIMIT

DFSP Pearl Harbor Specific Operations Order

- Once the transfer is complete, close all valves and return the piping system to its normal configuration.
- Once the transfer is complete, close all valves and proceed to the next tank.

12 Quality Plan

1. None

13 | Emergency Response Plan

- a. Stop all transfer operations and close all valves.
- b. Notify the chain of command of the emergency and respond to the emergency with clean up material and containers and drip pans as required by the emergency.
- c. If needed, make alignment preparations to pump the fuel back to the source tank.

14 Safety Plan

- a. Maintain communication between the control room operator and all involved parties.
- b. Do not lose focus or become complacent.
- c. Do not be impatient. Think all steps through.
- d. Accidents happen without warning. Be aware of your surroundings. Do not become distracted.
- e. Be aware of strange sounds or smells.
- f. Remain calm in an emergency.
- g. The worker must be able to react quickly and properly in a safe mode.
- h. Contact Control Room Operator by radio to secure the operation. Slowly close valves, taking at least 15 seconds to shut the valve completely. Inform the Fuel Supervisors of the situation.
- i. Anyone has the authority and responsibility to call a halt to an operation if they believe an unsafe condition exists.

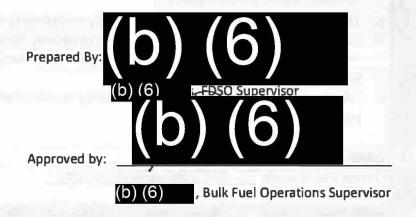
15 ORM

Overall RAC code of: RAC 3 Mitigated to a RAC 4

Hazard Threat/effect	Assess	RAC	Risk Control Action	Re-assess	Residual	Supervision
Leak at pipe flanges.	D, 1	3	Area manned and monitored by, qualified operators	D, II	4	YES
Overfill the tank.	C, III	4	Area manned and monitored, qualified operators, Certified AFHE overfill protection	D, III	5	YES

DFSP Pearl Harbor Specific Operations Order

		PROBABILITY						
	Risk Assessment Matrix	Frequency of Occurrence Over Time						
		A Likely	B Probable	C May	D Unlikely			
1.	Loss of Mission Capability, Unit Readiness or Asset; Death	1	1	2				
11	Significantly Degraded Mission Capability or Unit Readiness; Severe Injury or Damage	1	2	3	4			
m	Degraded Mission Capability or Unit Readiness; Minor injury or Damage	2	3	4	5			
IV	Little or No Impact to Mission Capability or Unit Readiness; Minimal Injury or Damage.	3	4	5	5			



APPENDIX 'C' - Government Furnished Information Listing

Government Furnished Information Listing

- 1. DFSP Pearl Harbor Specific Operations Order (Evolution 3); May 6, 2021.
- 2. DFSP Pearl Harbor Specific Operations Order (Evolution 4); May 6, 2021.
- 3. Pipe Stress Analysis Red Hill Lower Tunnel Piping, Tanks 1 to 16; April 2004; Draft; Weston Solutions.
- 4. Hydraulic Analysis and Dynamic Transient Surge Evaluation; September 2010; Final Report; Enterprise Engineering, Inc.
- 5. AFHE Data Alarm Logs, Event Logs, and Data Export.
- 6. Red Hill Skin Valve Piping Analytical Review of Piping Configuration; 23 June 1999; Thermal Engineering Corporation.
- 7. Red Hill Skin Valve Piping Addendum to the Analytical Review of Piping Configuration; 12 November 1999; Thermal Engineering Corporation.
- 8. Inspection and Repair of Red Hill Pipelines Technical Note; March, 8 2019; Enterprise Engineering, Inc.
- 9. Inspection and Repair of Red Hill Pipelines Pipe Pedigree Report; April 2019; Enterprise Engineering, Inc.

APPENDIX 'D' - Stress Analysis Output

CAESAR II Ver.12.00.00.4000, (Build 200403) Date: AUG 5, 2021 Time: 7:49

Job Name: 21-032 STRESS ANALYSIS

DISPLACEMENTS REPORT: Nodal Movements

CASE 1 (OPE) W+T1+P1+F1

Node	DX in.	DY in.	DZ in.	RX deg.	RY deg.	RZ deg.
10	-0.0000	0.0000	-0.0000	0.0000	0.0000	0.0000
20	-1.4350	0.0876	-0.0208	0.1365	2.2677	0.2376
30	-6.7537	0.3917	-0.0521	0.1838	3.5432	0.5940
40	-7.0843	0.4018	0.0409	0.1838	3.5432	0.5609
50	-13.6800	0.7082	-0.0886	0.1518	3.5432	0.5940
60	-15.5970	0.7898	-0.0987	0.1509	3.5432	0.5940
70	-15.9913	0.8066	-0.1008	0.1509	3.5432	0.5940
90	-7.1672	0.4046	0.0666	0.1838	3.5432	0.5108
100	-7.1148	1.7493	-9.8899	0.1838	3.5432	0.4666
110	-7.1096	1.8796	-10.8793	0.1838	3.5432	0.4665
300	-7.2539	-0.0000	10.4559	0.1838	3.5432	-0.0138
310	-7.3582	-0.0413	22.9478	0.1838	3.5432	0.0133
320	-7.3659	-0.0444	23.8136	0.1838	3.5432	0.0118
330	-7.3802	-0.0485	25.2978	0.1838	3.5432	0.0094
340	-33.3802	-0.0412	25.6688	0.1838	3.5432	-0.1306
350	-33.3909	-0.0000	26.7820	0.1838	3.5432	-0.1301
360	-33.4088	0.0676	28.6372	0.1838	3.5432	-0.1289
370	-33.4107	0.0794	28.9619	0.1838	3.5432	-0.1289
400	-7.1050	1.9935	-11.7451	0.1838	3.5432	0.4665

CAESAR II Ver.12.00.00.4000, (Build 200403) Date: AUG 16, 2021 Time: 15:0

Job:: 21-032 STRESS ANALYSIS

RESTRAINTS REPORT: Loads On Restraints

CASE 1 (OPE) W+T1+P1+F1

Node	FX lb.	FY lb.	FZ lb.	MX ft.lb.	MY ft.lb.	MZ ft.lb.	Restraint Type/Tag
10	-78000	4930	-0	63852.5	1039999.6	67469.7	TYPE=Rigid ANC;
20	0	0	0	0.0	0.0	0.0	TYPE=Rigid +Y;
50	0	0	0	0.0	0.0	0.0	TYPE=Rigid +Y;
100	0	0	0	0.0	0.0	0.0	TYPE=Rigid +Y;
110	0	0	0	0.0	0.0	0.0	TYPE=Rigid +Y;
300	0	-15213	0	0.0	0.0	0.0	TYPE=Rigid +Y;
350	0	-964	0	0.0	0.0	0.0	TYPE=Rigid +Y;

CAESAR II Ver.12.00.00.4000, (Build 200403) Date: AUG 16, 2021 Time: 15:0

Job:: 21-032 STRESS ANALYSIS

GLOBAL ELEMENT FORCES REPORT: Forces on Elements

CASE 1 (OPE) W+T1+P1+F1

Node	FX lb.	FY lb.	FZ lb.	MX ft.lb.	MY ft.lb.	MZ ft.lb.	Element Name
10	78000	-4930	0	-63852.5	- 1039999.6	-67469.7	
20	-78000	5652	-0	35634.9	623999.8	67469.7	
			_				
20	78000	-5652	0	-35634.9	-623999.8	-67469.7	
30	-78000	6736	-0	-13915.9	-0.0	67469.7	
30	78000	-8703	0	0.0	0.0	-67469.7	
40	-78000	9030	-0	-0.0	-0.0	-121030.2	
30	0	1967	0	13915.9	-0.0	0.0	
50	-0	-703	-0	-1457.1	0.0	-0.0	
50	0	703	0	1457.1	-0.0	0.0	
60	-0	-353	-0	-93.7	0.0	-0.0	
			_				
60	0	353	0	93.7	-0.0	0.0	
70	-0	0	-0	-0.0	0.0	0.0	FLANGE_FLG_300
40	78000	-9030	0	0.0	0.0	121030.2	
90	-78000	9120	-0	0.0	-0.0	-173030.2	
90	0	2120	0	-0.0	-0.0	16602.7	
100	-0	-303	-0	0.0	0.0	-347.4	
100	0	303	0	-0.0	-0.0	347.4	
110	-0	-122	-0	0.0	0.0	-64.0	
90	78000	-11241	0	-0.0	0.0	156427.5	
300	-78000	13137	-0	0.0	-0.0	14215.1	
200	70000	0070	2		0.0	4 4047 4	
300	78000	2076	0	-0.0	0.0	-14215.1	
310	-78000	204	-0	0.0	-0.0	-1536.6	
310	78000	-204	0	-0.0	0.0	1536.6	
320	-78000	327	-0	0.0	-0.0	-1219.5	
320	78000	-327	0	-0.0	0.0	1219.5	
330	-78000	480	-0	0.0	-0.0	-413.3	
330	78000	-480	0	-0.0	0.0	413.3	
340	-78000	500	-0	0.0	-0.0	-168.3	
340	78000	-500	0	-0.0	0.0	168.3	
350	-78000	615	-0	0.0	-0.0	668.4	

CAESAR II Ver.12.00.00.4000, (Build 200403) Date: AUG 16, 2021 Time: 15:0

Job:: 21-032 STRESS ANALYSIS

GLOBAL ELEMENT FORCES REPORT: Forces on Elements

CASE 1 (OPE) W+T1+P1+F1

Node	FX lb.	FY lb.	FZ lb.	MX ft.lb.	MY ft.lb.	MZ ft.lb.	Element Name
350	78000	349	0	-0.0	0.0	-668.4	
360	-78000	-158	-0	0.0	-0.0	34.5	
360	78000	158	-0	-0.0	0.0	-34.5	
370	-78000	-0	0	0.0	-0.0	0.0	FLANGE_FLG_300
110	0	122	0	-0.0	-0.0	64.0	
400	0	0	0	0.0	-0.0	0.0	

CAESAR II Ver.12.00.00.4000, (Build 200403) Date: AUG 16, 2021 Time: 15:0 Job:: 21-032 STRESS ANALYSIS

B31.3 STRESSES REPORT: Stresses on Elements

CASE 1 (OPE) W+T1+P1+F1

Piping Code (1 of 1): B31.3 -2018, Aug 30, 2019

The SLP column shows the longitudinal pressure stress.

Highest Stresses: (lb./sq.in.)

F/A	7945.0	@Node	320
Bending	204924.1	@Node	10
Torsion	6634.7	@Node	10
SIF/Index In-Plane	1.0	@Node	10
SIF/Index Out-Plane	1.0	@Node	10
SIF/Index Torsion	1.0	@Node	10
SIF/Index Axial	1.0	@Node	10

Node	SLP lb./sq.in.	F/A lb./sq.in.	Bending lb./sq.in.	Torsion lb./sq.in.	SIF/Index In-Plane	SIF/Index Out- Plane	SIF/index Torsion	SIF/Index Axial	Code lb./sq.in.
10		0.0	204924.1	6634.7	1.000	1.000	1.000	1.000	205353.2
20		0.0	122923.3	-6634.7	1.000	1.000	1.000	1.000	123637.4
20		0.0	122923.3	6634.7	1.000	1.000	1.000	1.000	123637.4
30		0.0	2736.9	-6634.7	1.000	1.000	1.000	1.000	13548.7
30		624.3	13269.4	0.0	1.000	1.000	1.000	1.000	13893.7
40		647.7	23803.3	-0.0	1.000	1.000	1.000	1.000	24451.0
30		0.0	2736.9	-0.0	1.000	1.000	1.000	1.000	2736.9
50		0.0	286.6	0.0	1.000	1.000	1.000	1.000	286.6
50		0.0	286.6	-0.0	1.000	1.000	1.000	1.000	286.6
60		0.0	18.4	0.0	1.000	1.000	1.000	1.000	18.4
60									
70									
40		647.7	23803.3	0.0	1.000	1.000	1.000	1.000	24451.0
90		654.2	34030.2	-0.0	1.000	1.000	1.000	1.000	34684.4

CAESAR II Ver.12.00.00.4000, (Build 200403) Date: AUG 16, 2021 Time: 15:0 Job:: 21-032 STRESS ANALYSIS

B31.3 STRESSES REPORT: Stresses on Elements CASE 1 (OPE) W+T1+P1+F1

Node	SLP lb./sq.in.	F/A lb./sq.in.	Bending lb./sq.in.	Torsion lb./sq.in.	SIF/Index In-Plane	SIF/Index Out- Plane	SIF/Index Torsion	SIF/Index Axial	Code lb./sq.in.
90		-0.0	3265.3	-0.0	1.000	1.000	1.000	1.000	3265.3
100		-0.0	68.3	0.0	1.000	1.000	1.000	1.000	68.3
100		-0.0	68.3	-0.0	1.000	1.000	1.000	1.000	68.3
110		-0.0	12.6	0.0	1.000	1.000	1.000	1.000	12.6
		-0.0	12.0	0.0	1.000	1.000	1.000	1.000	122,0
90		5595.1	30764.9	0.0	1.000	1.000	1.000	1.000	36360.0
300		5595.1	2795.7	-0.0	1.000	1.000	1.000	1.000	8390.8
300		5595.1	2795.7	0.0	1.000	1.000	1.000	1.000	8390.8
310		5595.1	302.2	-0.0	1.000	1.000	1.000	1.000	5897.3
310		5595.1	302.2	0.0	1.000	1.000	1.000	1.000	5897.3
320		7945.0	486.4	-0.0	1.000	1.000	1.000	1.000	8431.4
320		7945.0	486.4	0.0	1.000	1.000	1.000	1.000	8431.4
330		7945.0	164.8	-0.0	1.000	1.000	1.000	1.000	8109.8
330									
340									
340		7945.0	67.1	0.0	1.000	1.000	1.000	1.000	8012.1
350		7945.0	266.5	-0.0	1.000	1.000	1.000	1.000	8211.6
		70.4° 0			4 000	4 000	4 000	4.000	
350		7945.0	266.5	0.0	1.000	1.000	1.000	1.000	8211.6
360		7945.0	13.8	-0.0	1.000	1.000	1.000	1.000	7958.8
360									
370									
			40.0		4 000	4 000	4 000	4 000	400
110 400		-0.0	12.6	-0.0	1.000	1.000	1.000	1.000	12.6
400		0.0	0.0	0.0	1.000	1.000	1.000	1.000	0.0

BWS043528 B-411

APPENDIX 'E' - Surge Analysis Output

```
* * * * * * * * * * * * * * SURGE * * * * * * * * * * * * * *
 Transient Flow Modeling Software
  CopyRighted by KYPIPE LLC (www.kypipe.com)
 Version: 8.014 01/11/2016
* Company: AustinBroc Serial #: 592067
 Interface: Classic
* Licensed for Pipe2008
INPUT: g:\21 jobs\21-032 assess tank 20 piping - red hill\calcs\m\21-032 surge
analysis\21-032 s.DAT
OUTPUT: g:\21 jobs\21-032 assess tank 20 piping - red hill\calcs\m\21-032 surge
analysis\21-032 s.OUT
RUN DATE = 08/05/21
RUN TIME =
           22:29:53
*****
                   SYSTEM DATA
****************
THE FOLLOWING DEFAULT OVERRIDES HAVE BEEN DEFINED:
    Liquid Specific Gravity = 0.839999974
          Cavitation Head = 7.76000023E-02
     Time Increment Factor = 1
     Flow Conversion Factor = 448.859985
     Head Conversion Factor = 1.00000000
# of Increments for Cavity collapse: 1
   CV Setting for Inertial effects: 0.00000000E+00
Pressure Sensitive Demands at Junction Nodes.
Exit Head = 0.00000000E+00
Total Simulation Time = 600.0 sec
Time Increment = 0.00280 sec
ENGLISH UNITS ARE SPECIFIED:
FLOW in Gallons/Minute & HEAD in feet
 Dynamic Friction Option Selected.
 Pipe resistance changes with flowrate.
NUMBERS OF SPECIFIC ELEMENTS:
 Line Segments = 19 Components
 Junctions = 13 Bypass Lines = 0
 Side Orifices = 0 Relief Valves = 0
 Check Valves = 0 Variable Inputs =
```

LINE SEGMENT DATA

POSITION OF	END NODES	TRAVEL INCREMENTS	C/GA	INITIAL FLOWRATE	SEGMENT RESISTANCE	WAVE SPEED
Tank 12 O-AV-1 O-AV-2 J-1 J-3 J-2 O-AV-3 J-4b J-4c J-4e O-AV-5 J-4f J-4g J-1 O-AV-4 I-AV-6 J-4 J-5 J-3	I-AV-1 I-AV-2 J-3 J-2 J-1 I-AV-3 J-4b J-4c J-4e I-AV-5 J-4f J-4g I-AV-4 J-4 Tank 2 J-5 O-AV-6 J-4c J-6	1 1 3 1 1716 1 2 1 1 1 15 4 1 1 1 1 1 2			3) (A)

Total Number of Time Increments: 3549

(Limit is: 400,000)

Component Data

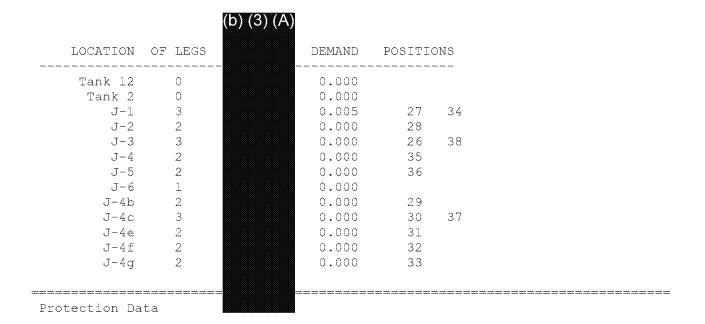
COMPONENT DATA

COMPONENT CHARACTERISTICS AND INITIAL CONDITIONS:

POS.	POS.	СН	ARACTERIS	STICS	INITIAL	HEAD	HEAD
#1	#2	(А)	(B)	(C)	FLOW	#1	#2
I-AV-1 I-AV-2 I-AV-3 I-AV-5 I-AV-4 I-AV-6	O-AV-1 O-AV-2 O-AV-3 O-AV-5 O-AV-4 O-AV-6	0.00 0.00 0.00 0.00 0.00 0.00	0.00 -0 0.00 -0 0.00 -0	0.346E-01 0.123E-01 0.903E+03 0.123E-01 0.123E-01 0.365E+05	(b)	(3)	(A)

Junction Data

JUNCTION NUMBER INITIAL INITIAL CONNECTING



Variable Input Data

INPUT # 1:

A VARIABLE AREA VALVE IS SPECIFIED AT POSITION #: I-AV-1 REFERENCE VALUE FOR VALVE RESISTANCE (R=1) = 0.03458

TIME		RATIO	INPUT	DATA:
	T	IME	RATI	0
	0.	.000	0.000	00
32	24	.000	0.000	00
33	88	.000	1.000	00
45	58.	.000	1.000	0.0
47	72.	.000	0.000	0.0

Following initial value is calculated for this variable input:

... This should agree with initial value previously defined (in parentheses)

Initial valve resistance = 0.00 (0.0346)

INPUT # 2:

REFERENCE VALUE FOR VALVE RESISTANCE (R=1) = 0.01233 A BALL VALVE IS AT POSITION I-AV-2

TIME	RATIO
0.0000	0.0000
200.0000 203.8000	0.0000 0.0430
207.6000 211.4000	0.1136 0.2031
215.2000	0.3062
222.8000	0.5371
230.4000	0.7773
234.2000 238.0000	0.8924 1.0000

```
415.0000 1.0000

418.9000 0.8924

422.8000 0.7773

426.7000 0.6578

430.6000 0.5371

434.5000 0.4188

438.4000 0.3062

442.3000 0.2031

446.2000 0.1136

450.1000 0.0430

454.0000 0.0000
```

Following initial value is calculated for this variable input:

... This should agree with initial value previously defined (in parentheses) Initial value resistance = 0.00 (0.0123)

INPUT # 3:

REFERENCE VALUE FOR VALVE RESISTANCE (R=1) = 0.03417 A BUTTERFLY VALVE IS AT POSITION I-AV-3

TIME	RATIO
0.0000	0.0031
100.0000	0.0031
100.1000	0.0025
100.2000	0.0020
100.3000	0.0015
100.4000	0.0011
100.5000	0.0008
100.6000	0.0005
100.7000	0.0003
100.8000	0.0001
100.9000	0.0000
101.0000	0.0000

Following initial value is calculated for this variable input:

... This should agree with initial value previously defined (in parentheses)
Initial value resistance = 0.00 (903.3859)

INPUT # 4:

REFERENCE VALUE FOR VALVE RESISTANCE (R=1) = 1.38097 A BUTTERFLY VALVE IS AT POSITION I-AV-6

TIME	RATIO
0.0000 100.0000 100.1000 100.2000 100.3000 100.4000 100.5000 100.6000 100.7000 100.8000 100.9000	0.0031 0.0031 0.0025 0.0020 0.0015 0.0011 0.0008 0.0005 0.0003 0.0001
101.0000	0.0000

Following initial value is calculated for this variable input:

... This should agree with initial value previously defined (in parentheses)
Initial value resistance = 0.00 (36507.4766)

Initial Conditions

**** SUMMARY OF INITIAL CONDITIONS FOR LINE SEGMENTS ****

END POSITION DESIGNATIONS: J - JUNCTION, C - COMPONENT, S - SDO
* - THIS DENOTES AN UNDESIGNATED END POSITION (UNACCEPTABLE) - CORRECT DATA

FLOW ---- END POSITIONS -------- HEAD ----HEAD ELEVATION #1 #1 to #2 #2 LOSS DIFFERENCE Tank 12 J I-AV-1 C I-AV-2 C 0-AV-1 C O-AV-2 C J-3 J J-1 J J-2 J J-3 J J-1 J J-2 J I-AV-3 C O-AV-3 C J-4b J J-4b J J-4c J J-4c J J-4e J I-AV-5 C J-4e J O-AV-5 C J-4f J J-4f J J-4g J J-4g J I-AV-4 C J-1 J J-4 J

Tabulated Results

O-AV-4 C

J-4 J

J-5 J

J-3 J

I-AV-6 C

****** FLOWRATE AND PRESSURE RESULTS *****

Tank 2 J

O-AV-6 C

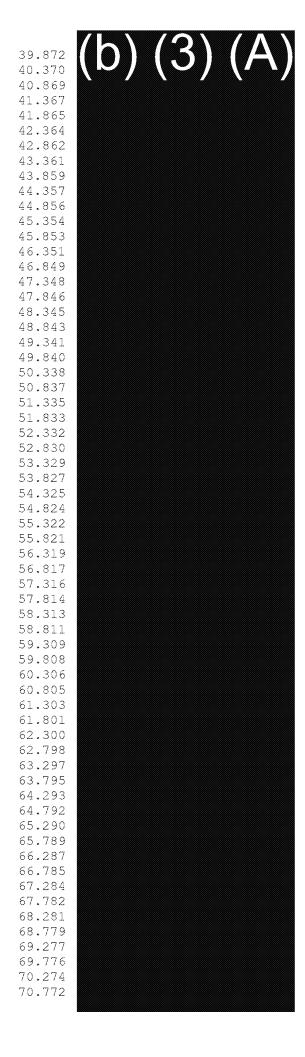
J-5 J

J-4c J J-6 J

TIME Head at Head at Head at J-6 J-3 J-1

0.498 0.997 1.495 1.994 2.492 2.990 3.489 3.987 4.486 4.984 5.482 5.981 6.479 6.978 7.476 7.974

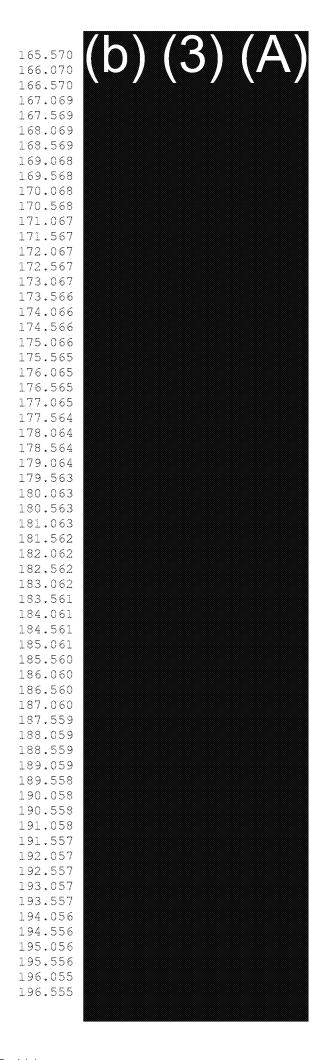
8.473 8.473 9.470 9.968 10.466 10.965 11.463 11.962 12.460 12.958 13.457 13.955 14.450 15.450 15.450 15.494 17.942 18.441 18.939 19.438 19.933 21.431 22.928 23.425 23.923 24.920 25.418 25.418 27.412 27.910 28.907 29.904 30.931 31.897 32.396	(b)	(3)	(A)
30.402 30.901 31.399 31.897			



71.271	(b)	3		(eta	$m{\langle}$
72.268 72.766 73.264		`	,	`	,
73.763 74.261 74.760					
75.258 75.756					
76.255 76.753 77.252					
77.750 78.248 78.747					
79.245 79.744					
80.242					
81.239 81.737 82.236					
82.734 83.232 83.731					
84.229 84.728					
85.226 85.724 86.223					
86.721 87.220 87.718					
88.216 88.715					
89.213 89.712 90.210					
90.708 91.207					
91.705 92.204 92.702					
93.200 93.699 94.197					
94.696 95.194					
95.692 96.191 96.689					
97.188 97.686 98.184					
98.683 99.181					
99.680 100.178 100.676					
101.175 101.673 102.172					
/ Mad					

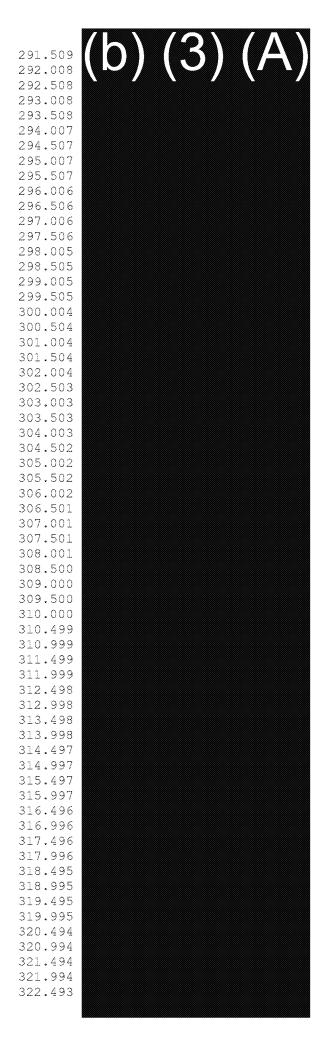
102.670 103.168 103.667 104.165 104.664 105.162	(b)	(3)	(A)
106.159 106.657 107.156 107.654 108.152 108.651 109.149 109.648			
110.146 110.644 111.143 111.641 112.140 112.638 113.136			
113.635 114.133 114.632 115.130 115.628 116.127 116.625 117.123			
117.622 118.120 118.619 119.117 119.615 120.114 120.612			
121.111 121.609 122.107 122.606 123.104 123.603 124.101 124.599			
125.098 125.596 126.095 126.593 127.091 127.590 128.088 128.588			
129.088 129.588 130.088 130.587 131.087 131.587 132.087			
132.586 133.086 133.586			

134.086 134.585	(b)	(3)	(A)
135.085 135.585 136.085			
136.584 137.084 137.584 138.084			
138.583 139.083 139.583			
140.083 140.582 141.082			
141.582 142.082 142.581			
143.081 143.581 144.081			
144.580 145.080 145.580 146.080			
146.579 147.079 147.579			
148.079 148.578 149.078			
149.578 150.078 150.577			
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154.576 155.075 155.575			
156.075 156.575 157.074 157.574			
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164.571 165.070			



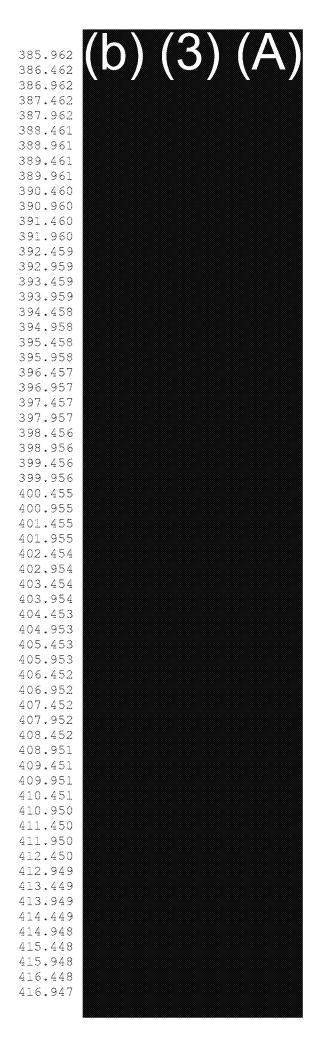
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206.050 206.550 207.050 207.550 208.049 208.549 209.049 210.048 210.548 211.048 211.548 212.047 212.547 213.047 213.547 214.046 214.546 215.046			
215.546 216.046 216.545 217.045 217.545 218.045 218.544 219.544 220.044 220.543 221.043 221.543 222.043 222.542 223.042 223.542			
224.042 224.541 225.041 225.541 226.041 226.540 227.040 227.540 228.040			

228.539 229.039 229.539 230.039	(b)	(3)	(A)
230.538 231.038 231.538 232.038 232.537 233.037			
233.537 234.037 234.536 235.036 235.536 236.036			
236.536 237.035 237.535 238.035 238.535			
239.034 239.534 240.034 240.534 241.033 241.533			
242.033 242.533 243.032 243.532 244.032 244.532			
245.031 245.531 246.031 246.531 247.030			
247.530 248.030 248.530 249.029 249.529 250.029			
250.529 251.028 251.528 252.028 252.528 253.027			
253.527 254.027 254.527 255.026 255.526			
256.026 256.526 257.025 257.525 258.025 258.525			
259.025 259.524			



322.993 323.493 323.993 324.493 324.992 325.492 325.992 326.492 327.491 327.991 327.991 328.491 328.990 329.490 329.490 330.490 330.989 331.489 331.989 331.489 332.489 332.489 332.488 333.488 334.488	(b)	(3)	(A)
335.987 336.487 336.986 337.486 337.986 338.486 338.985 339.485 340.485 340.984 341.484 341.984 342.484 342.983 343.483 344.483 344.983 344.483 344.983 345.482 345.982			
346.482 346.982 347.481 347.981 348.481 349.480 350.480 350.480 351.479 351.979 352.479 352.979 353.478 353.978			

354.478 354.978 355.477 355.977 356.477 356.977 357.476 357.976 358.476 359.475 369.475 360.475 360.975 361.474 361.974 361.974 362.474 362.974 363.473 363.473 364.473 365.473 365.473 365.473 365.473 365.473 365.473 367.472 367.472 367.971 368.471	(b)	(3)	(A)
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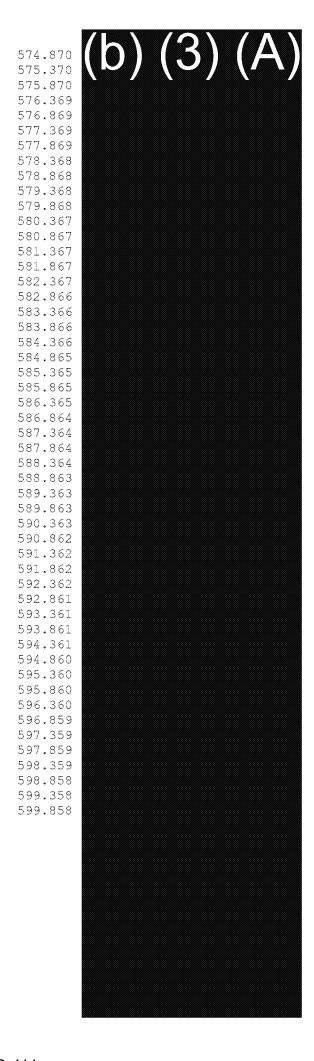
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425.943 426.443 426.942 427.442 427.942 428.442 428.941 429.441 429.941			
430.441 430.941 431.440 431.940 432.440 432.940 433.439 433.939 434.439			
434.939 435.438 435.938 436.438 436.938 437.437 437.937 438.437 438.937			
439.436 439.936 440.436 440.936 441.435 441.935 442.435 442.935 443.434			
443.934 444.934 445.433 445.933 446.433 446.933 447.432 447.932 448.432			

448.932 449.431 449.931	(b)	(3)	(A)
450.431 450.931 451.431 451.930 452.430 452.930			
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462.425 462.925 463.425 463.924 464.424 464.924			
465.424 465.923 466.423 466.923 467.423 467.922			
468.422 468.922 469.422 469.921 470.421 470.921			
471.421 471.921 472.420 472.920 473.420 473.920			
474.419 474.919 475.419 475.919 476.418			
476.918 477.418 477.918 478.417 478.917 479.417			
479.917			

480.416 480.916 481.416 481.916 482.415	(b)	(3)	(A)
482.915 483.415 483.915 484.414 484.914			
485.414 485.914 486.413 486.913 487.413 487.913			
488.412 488.912 489.412 489.912 490.411 490.911			
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496.908 497.408 497.908 498.408 498.907 499.407			
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505.404 505.904 506.404 506.903 507.403 507.903			
508.403 508.902 509.402 509.902 510.402			
510.901 511.401			

511.901 512.401 512.900 513.400 513.900 514.400 514.899 515.399 515.899 516.399	(b)	(3)	(A)
516.898 517.398 517.898 518.398 518.898 519.397 519.897 520.397 520.897 521.396 521.896 522.396			
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533.390 533.890 534.890 535.389 535.889 536.389 536.889 537.388 537.888 538.388 538.388			
538.888 539.388 539.887 540.387 540.887 541.387 541.886 542.386 542.886			

543.885 544.885 544.885 544.885 545.385 545.385 546.385 546.3883 547.883 549.3882 550.882 551.881 552.3881 5552.3881 5552.3881 5552.3881 5552.3881 5552.3881 5553.880 555.376 566.377 561.377 562.376 563.377 564.875 566.377 566.377 566.377 566.377 566.377 567.377 566.377 566.377 567.377 566.377 567.377 566.377 567.377 566.377 567.377 567.377 568.377 569.377 561.377 561.377 562.376 563.377 563.377 564.877 565.377 566.377 567.377 567.377 567.377 567.377 567.377 567.377 567.377 567.377 577.377
(b)
(3)



Max/Min Summary

SUMMARY OF MAXIMUM AND MINIMUM HEADS:

Position no.	MaxHead ft	MinHead ft	Time Reverse Gra	MaxPressure ad. psi	MinPressure psi	MaxTime (sec)	MinTime (sec)
Tank 12	/b\ /s	$\Lambda \Lambda \Lambda$	0.000	62.157	62.157	0.00280	0.00280
Tank 2		3) (A)	0.000	2.661	2.661	0.00280	0.00280
I-AV-1	(/ (-	/ (/	0.022	232.151	-5.724	326.19394	385.45432
I-AV-2			441.806	227.335	-14.391	326.19113	5.31718
I-AV-3			0.414	394.635	-14.391	331.02866	340.70370
0-AV-4			0.011	6.645	-3.551	0.21840	0.07280
0-AV-5			0.980	13.207	-7.255	0.30240	0.44520
0-AV-6			1.039	464.738	-14.391	331.02304	331.16342
J-1			0.272	378.752	-14.391	331.02304	340.72336
J-2			0.305	387.197	-14.391	331.02585	340.70651
J-3			281.926	214.030	-14.391	335.84653	58.53375
J-4			0.532	442.151	-14.391	331.02585	340.69809
J-5			0.258	18.566	-6.096	0.28000	0.12320
J-6			284.007	356.952	-14.391	335.90268	48.84579
J-4b			1.064	15.134	-9.175	0.28560	0.14000
J-4c			1.002	13.739	-8.376	0.27440	0.12880
J-4e			1.014	12.826	-7.437	0.27720	0.45080
J-4f			0.980	13.578	-7.375	0.29960	0.44520
J-4g			0.454	9.642	-7.223	0.98840	0.07840
O-AV-1			0.022	213.474	-14.391	326.19394	5.31998
0-AV-2			441.806	227.156	-14.391	326.19113	48.95499
0-AV-3			0.414	15.325	-9.940	0.28280	0.13440
I-AV-5			0.980	13.208	-7.254	0.30240	0.44520
I-AV-4			0.011	6.645	-3.549	0.21840	0.07280
I-AV-6			1.039	15.229	-10.171	0.28280	0.12040

Max/Min Line Pressures

SUMMARY OF MAX/MIN LINE PRESSURES:

START NODE	END NODE	MAX PRESS.	MIN PRE: psi	SS.
		J.		*** *** ***
Tank 12	I-AV-1	232.15	-5.72	
0-AV-1	I-AV-2	227.34	-14.39	Cavitation
0-AV-2	J-3	227.16	-14.39	Cavitation
J-1	J-2	387.20	-14.39	Cavitation
J-3	J-1	378.75	-14.39	Cavitation
J-2	I-AV-3	394.63	-14.39	Cavitation
0-AV-3	J-4b	15.33	-9.94	
J-4b	J-4c	15.13	-9.17	
J-4c	J-4e	13.74	-8.38	
J-4e	I-AV-5	13.21	-7.44	
O-AV-5	J-4f	13.58	-7.38	
J-4f	J-4g	13.58	-7.38	
J-4g	I-AV-4	9.64	-7.22	
J-1	J - 4	442.15	-14.39	Cavitation
O-AV-4	Tank 2	6.64	-3.55	
I-AV-6	J-5	18.57	-10.17	
J-4	0-AV-6	464.74	-14.39	Cavitation
J-5	J-4c	18.57	-8.38	
J-3	J-6	356.95	-14.39	Cavitation

Highest Surge Pressure in the Network: 464.74 psi at Node: O-AV-6

Lowest Surge Pressure in the Network: -14.39 psi at Node: I-AV-2

**** END OF THIS SIMULATION ****

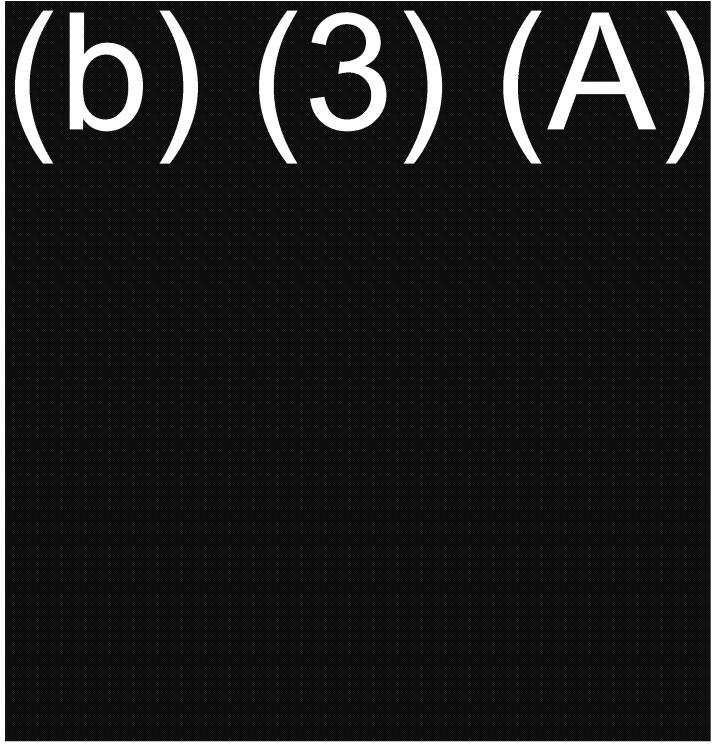
END RUN AT TIME 22:32:51

APPENDIX 'F' - Valve Testing Results

Valve Testing Results

7/12/2021 & 7/13/2021

Nameplate Data:



33

APPENDIX 'G' - AFHE Data

B-411 BWS043558

34

i. Event Log

Eventid GroupName TagName	i a ania a Nia da	Everations E.	and State - Franch Dalacity	Francis (ml. co. Fr	and in it is a left of a	Malica Chain a	Origination Tare FrankSterra	etorName O	ana an Nisa da	Comment
C2772 1 977 1997 1997 277 1977 1977 1977	PH-VS-APP02		entstate eventments 999	eventivatue ev	enternit cinitating	valuestring	5/7/2021 2:24:59 5/6/2021 17:24:59		peratorNode H-WS-HMI01	Valve Position set to Open
527782 (D) (3) (A)	PH-VS-APP02		999	0	0		5/7/2021 3:33:28 5/6/2021 17:33:28		I-WS-HMI01	Valve Position set to Close
527783	PH-VS-APP01		999	0	0		5/7/2021 3:34:19 5/6/2021 17:34:19		I-WS-HMIOL	Audible Alarm Reset
527784	PH-VS-APP01		999	0	C		5/7/2021 3:34:21 5/6/2021 17:34:21		4-WS-HMI01	Audible Alarm Reset
527785	PH-VS-APP02		999	0	C		5/7/2021 3:34:40 5/6/2021 17:34:40	888888888888888888	4-WS-HMI01.	Valve Position set to Close
527786	PH-VS-APPO1		999	0	0		5/7/2021 3:35:41 5/6/2021 17:35:41		I-WS-HMI01	Alarm Acknowledged All Tank-RH-20 From Alarm Detail
527787	PH-VS-APP01	OPR	999	0	0		5/7/2021 3:35:47 5/6/2021 17:35:48	PI	H-WS-HMI01	Audible Alarm Reset
527788	PH-VS-APP01	OPR	999	0	0		5/7/2021 3:35:50 5/6/2021 17:35:50	PI	H-WS-HMI01	Audible Alarm Reset
527789	PH-VS-APP02	OPR	999	0	0		5/7/2021 3:36:12 5/6/2021 17:36:12	PI	I-WS-HMI01	Valve Percent Open Set To: 50%
527790	PH-VS-APP02	OPR	999	0	0		5/7/2021 3:36:55 5/6/2021 17:36:55	Pi	H-WS-HMI01	Valve Percent Open Set To: 50%
527791	PH-VS-APP02	OPR	999	G	0		5/7/2021 3:37:45 5/6/2021 17:37:45	Pl	4-WS-HMI01	Valve Percent Open Set To: 50%
527792	PH-VS-APP02	OPR	999	0	0		5/7/2021 3:37:54 5/6/2021 17:37:54	PI	4-WS-HMI01	Valve Percent Open Set To: 50%
527793	PH-VS-APP01		999	0	0		5/7/2021 3:38:53 5/6/2021 17:38:53		H-WS-HMI01	Evolution Product Type: JPS
527794	PH-VS-APP01		999	0	Ci		5/7/2021 3:38:57 5/6/2021 17:38:57		H-WS-HMI01	Evolution Type: Transfer
527795	PH-VS-APP01		999	9	0		5/7/2021 3:38:58 5/6/2021 17:38:58		I-WS-HMIOL	Product Filter Selected
527796	PH-VS-APP01		999	0	0		5/7/2021 3:39:06 5/6/2021 17:39:06	000000000000000000000000000000000000000	4-WS-HMI01	Audible Alarm Reset
527797	PH-VS-APP01		999	0	0		5/7/2021 3:39:18 5/6/2021 17:39:18	200000000000000000000	4-WS-HMI01	Evolution Client: JP-5 TRANSFER
527798	PH-VS-APP01		999	0	0		5/7/2021 3:39:31 5/6/2021 17:39:31		4-WS-HMI01	Evolution Document Number: NWO
527799	PH-VS-APP01		999	0	0		5/7/2021 3:39:38 5/6/2021 17:39:38		H-WS-HMI01	Evolution 4 Tank RH 12 Selected as Source
527800 537801	PH-VS-APP01		999	0	•		5/7/2021 3:39:43 5/6/2021 17:39:43		H-WS-HMI01	Evolution 4 Tank_STK Selected as Intermediate
527801	PH-VS-APP01		999	0	0		5/7/2021 3:39:50 5/6/2021 17:39:50		1-WS-HMI01	Evolution 4 Tank_RH_09 Selected as Destination
527802 527803	PH-VS-APP02 PH-VS-APP02		999 999	0 0	0		5/7/2021 3:40:34 5/6/2021 17:40:34 5/7/2021 3:41:54 5/6/2021 17:41:54		4-WS-HMI01 4-WS-HMI02	Valve Position set to Close Alarm Acknowledged Ali MOV-01128 From Alarm Detai
527804	PH-VS-APPO1		999	0	0		5/7/20213:41:54 5/6/202117:41:54 5/7/20213:42:02 5/6/202117:42:02		4-WS-HMI02	Audibie Alarm Reset
527805	PH-VS-APPO1		999	0	0		5/7/2021 4:00:21 5/6/2021 17:42:02		1-WS-HMI01	Complete Evolution
527806	PH-VS-APPO1		999	0	0		5/7/2021 4:00:21 5/6/2021 18:00:21	000000000000000000000000000000000000000	1-WS-HMI01	Start Evolution
527807	PH-VS-APP01		999	0	0		5/7/2021 4:00:59 5/6/2021 18:00:59		I-WS-HMIOL	Log Data Was Selected
527808	PH-VS-APP02		999	0	0		5/7/2021 4:02:31 5/6/2021 18:02:31		1-WS-HMI01	Valve Position set to Open
527809	PH-VS-APP02		999	0	0		5/7/2021 4:03:13 5/6/2021 18:03:13		4-WS-HMI02	Alarm Acknowledged All MOV-0112B From Alarm Detail
527810	PH-VS-APP02		999	n	n		5/7/2021 4:03:30 5/6/2021 18:03:30	88800088888888888	1-WS-HMI02	Valve Position set to Open
527811	PH-VS-APP02		999	0	o.		5/7/2021 4:04:01 5/6/2021 18:04:01	8888888888888888888	I-WS-HMI02	Valve Position set to Stop
527812	PH-VS-APP02		999	0	0		5/7/2021 4:04:40 5/6/2021 18:04:40		I-WS-HMI02	Valve Percent Open Set To: 50%
527813	PH-VS-APP02		999	0	0		5/7/2021 4:05:52 5/6/2021 18:05:52		I-WS-HMI02	Valve Percent Open Set To: 50%
527814	PH-VS-APP02		999	0	C		5/7/2021 4:06:24 5/6/2021 18:06:24	000000000000000000000000000000000000000	4-WS-HMI01	Valve Position set to Close
527815	PH-VS-APP02	OPR	999	0	0		5/7/2021 4:06:38 5/6/2021 18:06:38	PI	4-WS-HMI02	Valve Position set to Open
527816	PH-VS-APP02	OPR	999	0	0		5/7/2021 4:06:58 5/6/2021 18:06:58	PI	4-WS-HMI02	Valve Position set to Close
527817	PH-VS-APP02	OPR	999	0	0		5/7/2021 4:07:20 5/6/2021 18:07:20	Pl	H-WS-HMI02	Valve Percent Open Set To: 50%
527818	PH-VS-APP02	OPR	999	0	0		5/7/2021 4:07:35 5/6/2021 18:07:35	P	H-WS-HMI02	Valve Position set to Stop
527819	PH-VS-APP02	OPR	999	0	0		5/7/2021 4:07:46 5/6/2021 18:07:46	PI	I-WS-HMI02	Alarm Acknowledged Ali(b) (3) (A) From Alarm Detail
527820	PH-VS-APP02	OPR	999	G	G		5/7/2021 4:07:47 5/6/2021 18:07:47	PI	4-WS-HMI02	Alarm Acknowledged All(b) (3) (A) From Alarm Detail
527821	PH-VS-APP02	OPR	999	0	G		5/7/2021 4:07:54 5/6/2021 18:07:54	bi	4-WS-HMI02	Valve Position set to Open
527822	PH-VS-APP02	OPR	999	0	0		5/7/2021 4:08:05 5/6/2021 18:08:05	PI	4-WS-HMI02	Valve Position set to Close
527823	PH-VS-APP02		999	0	0		5/7/2021 4:08:25 5/6/2021 18:08:25		H-WS-HMI02	Alarm Acknowledged Ali(b) (3) (A) From Alarm Detail
527824	PH-VS-APP02		999	0	Ci .		5/7/2021 4:08:26 5/6/2021 18:08:26		H-WS-HMI02	Alarm Acknowledged All(b) (3) (A) From Alarm Detail
527825	PH-VS-APP02		999	0	0		5/7/2021 4:08:37 5/6/2021 18:08:37		I-WS-HMI02	Valve Position set to Open
527826	PH-VS-APP02		999	0	0		5/7/2021 4:10:02 5/6/2021 18:10:02		4-WS-HMI02	Valve Position set to Open
527827	PH-VS-APP02		999	0	0		5/7/2021 4:12:11 5/6/2021 18:12:11		4-WS-HMI02	Valve Position set to Close
527828	PH-VS-APP02		999	0	0		5/7/2021 4:12:17 5/6/2021 18:12:17	***************************************	4-WS-HMI02	Valve Position set to Close
527829	PH-VS-APP01		999	0	0		5/7/2021 4:13:09 5/6/2021 18:13:09		H-WS-HMI01	Audibie Alarm Reset
527830 527831	PH-VS-APPO1		999	0	-		5/7/2021 4:13:28 5/6/2021 18:13:28		H-WS-HMI01	Evolution Product Type: None
527831 527832	PH-VS-APP01 PH-VS-APP01		999 999	0	0		5/7/2021 4:13:31 5/6/2021 18:13:31 5/7/2021 4:13:32 5/6/2021 18:13:32		4-WS-HMI01 4-WS-HMI01	Evolution Type: Transfer Product Filter Selected
527833	PH-VS-APP01 PH-VS-APP01		999	0	G G		5/7/2021 4:13:32 5/6/2021 18:13:32 5/7/2021 4:13:49 5/6/2021 18:13:49		4-WS-HMI01	Evolution Client: JP-5 TRANSFER
527834	PH-VS-APPO1		999	0	0		5/7/2021 4:13:54 5/6/2021 18:13:54		4-WS-HMI01	Evolution Document Number: NWO
527835	PH-VS-APPO1		999	0	0		5/7/2021 4:13:55 5/6/2021 18:13:55		I-WS-HMI01	Evolution P-Code: N/A
527836	PH-VS-APP01		999	0	O O		5/7/2021 4:14:04 5/6/2021 18:14:04	000000000000000000000000000000000000000	I-WS-HMI01	Evolution 5 Tank_RH_20 Selected as Source
527837	PH-VS-APP01		999	0	Ö		5/7/2021 4:14:15 5/6/2021 18:14:15		I-WS-HMI01	Evolution 5 Tank STK Selected as Destination
527838	PH-VS-APP01		999	0	0		5/7/2021 4:16:35 5/6/2021 18:16:35		1-WS-HMI01	Set Pump To Off
527839	PH-VS-APP01		999	0	ß		5/7/2021 4:17:54 5/6/2021 18:17:54		4-WS-HMI01	Complete Evolution
527840	PH-VS-APP01		999	0	0		5/7/2021 4:18:41 5/6/2021 18:18:41		1-WS-HMI01	Start Evolution
527841	PH-VS-APP01		999	0	0		5/7/2021 4:18:45 5/6/2021 18:18:45		I-WS-HMI01	Log Data Was Selected
527842	PH-VS-APP02		999	0	0		5/7/2021 4:19:47 5/6/2021 18:19:47	200000000000000000000000000000000000000	H-WS-HMI02	Valve Position set to Close
527843	PH-VS-APP02	OPR	999	0	0		5/7/2021 4:19:59 5/6/2021 18:19:59	PI	I-WS-HMI02	Valve Position set to Close
527844	PH-VS-APP02	OPR	999	0	0		5/7/2021 4:20:07 5/6/2021 18:20:07	Pł	4-WS-HMI02	Valve Position set to Close
527845	PH-VS-APP02	OPR	999	0	0		5/7/2021 4:20:13 5/6/2021 18:20:13	Pł	4-WS-HMI02	Valve Position set to Close
527846	PH-VS-APP02	OPR	999	0	0		5/7/2021 4:23:13 5/6/2021 18:23:13	PI	1-WS-HMI01	Valve Position set to Open
527847	PH-VS-APP02	OPR	999	0	0		5/7/2021 4:23:58 5/6/2021 18:23:58	Pł	H-WS-HMI01	Valve Position set to Close
527848	PH-VS-APP02	OPR	999	0	0		5/7/2021 4:24:07 5/6/2021 18:24:07	bt	I-WS-HMI01	Valve Position set to Close

ii. Alarm Log

Alarmid GroupName	TagName	TagType	LoggingNode	Priority AlarmType	LimitString	ValueString	OriginationTime EventStamp	ACKTime Nori	malTime UnAckDuration	OperatorName	OperatorNode	AlarmTransition	AlarmState	Comment	AlarmDetailld
16366567 PD06 Valves		s	PH-VS-APP02	500 DSC	TRUE	TRUE	5/7/2021 3:25:11 5/6/2021 17:25:11	25:16.9	25:16.8 000 00:00:06.006	NULL	NULL	NULL	NULL	NULL	6742936
16366568 PD06 Valves		S	PH-VS-APP02	500 DSC	TRUE	TRUE	5/7/2021 3:26:04 5/6/2021 17:26:04	26:11.8	26:11.8 000 00:00:07.992	NULL	NULL	NULL	NULL	NULL	6742939
16366569 PD21 Valves		s	PH-VS-APP02	500 DSC	TRUE	TRUE	5/7/2021 3:33:39 5/6/2021 17:33:39		33:47.0 000 00:00:08.008		NULL	NULL.	NULL	NULL	6742943
16366570 PD21 Tanks		s	PH-VS-APPOL	1 DSC	TRUE	TRUE	5/7/2021 3:34:13 5/6/2021 17:34:13		35:26.3 NULL	DefaultUser	PH-WS-HMI01	NULL.	NULL	NULL	6742946
16366571 PD21 Valves		s	PH-VS-APP02	500 DSC	TRUE	TRUE	5/7/2021 3:34:36 5/6/2021 17:34:36		34:42.0 000 00:00:06.021	NULL	NULL	NULL	NULL	NULL	6742947
16366572 PD21 Valves		s	PH-VS-APP02	500 DSC	TRUE	TRUE	5/7/2021 3:35:08 5/6/2021 17:35:08		35:16.9 000 00:00:08.969		NUII.	NULL	NULL.	NULL	6742950
16366573 PD21 Valves		S	PH-VS-APP02	500 DSC	TRUE	TRUE	5/7/2021 3:35:57 5/6/2021 17:35:57		36:01.9 000 00:00:04.958	NULL	NULL	NULL	NULL	NULL	6742957
16366574 PD02 Valves		S	PH-VS-APP02	1 DSC	Alarm	Alarm	5/7/2021 3:39:01 5/6/2021 17:39:01		03:29.3 000 00:02:52.697	DefaultUser	PH-WS-HMI02	NULL	NULL	NULL	6742960
16366575 PD06 Valves		s	PH-VS-APP02	500 DSC	TRUE	TRUE	5/7/2021 3:40:45 5/6/2021 17:40:45	40:51.7	40:51.7 000 00:00:06.997		NULL	NULL.	NULL	NULL	6742963
16366576 PD06 Valves		s	PH-VS-APP02	500 DSC	TRUE	TRUE	5/7/2021 3:41:38 5/6/2021 17:41:38		41:46.7 000 00:00:08.999		NULL	NULL	NULL	NULL	6742964
16366577 PD06 Valves		s	PH-VS-APP02	500 DSC	TRUE	TRUE	5/7/2021 4:02:42 5/6/2021 18:02:42		02:51.4 000 00:00:08.997	NULL	NULL	NULL	NULL	NULL	6742971
16366578 PD06 Valves		S	PH-VS-APP02	500 DSC	TRUE	TRUE	5/7/2021 4:03:34 5/6/2021 18:03:34		03:41.4 000 00:00:06.999	NULI	NULL.	NULL	NULL.	NULL	6742975
16366579 PD02 Valves		S	PH-VS-APP02	500 DSC	TRUE	TRUE	5/7/2021 4:03:37 5/6/2021 18:03:37		03:46.3 000 00:00:09.004		NULL	NULL	NULL	NULL	6742976
16366580 PD02 Valves		S	PH-VS-APP02	500 DSC	TRUE	TRUE	5/7/2021 4:04:11 5/6/2021 18:04:11		04:16.3 000 00:00:05.006		NULL	NULL	NULL	NULL	6742981
16366581 PD02 Valves		Š	PH-VS-APP02	500 DSC	TRUE	TRUE	5/7/2021 4:04:14 5/6/2021 18:04:14		04:21.3 000 00:00:07.000		NULL	NULL.	NULL	NULL	6742982
16366582 PD02 Valves		S	PH-VS-APP02	500 DSC	TRUE	TRUE	5/7/2021 4:04:48 5/6/2021 18:04:48		04:56.3 000 00:00:07.996		NULL	NULL	NULL	NULL	6742987
16366583 PD02 Valves		Š	PH-VS-APP02	250 DSC	Alarm	Alarm	5/7/2021 4:04:52 5/6/2021 18:04:52		08:11.3 000 00:02:53.709		PH-WS-HMI02	NULL	NULL	NULL	6742988
16366584 PD02 Valves		S	PH-VS-APP02	250 DSC	Alarm	Alarm	5/7/2021 4:04:57 5/6/2021 18:04:57		08:11.3 000 00:02:48.717		PH-WS-HMI02	NULL	NULL.	NULL.	6742991
16366585 PD02 Valves		Š	PH-VS-APP02	500 DSC	TRUE	TRUE	5/7/2021 4:04:59 5/6/2021 18:04:59		05:06.3 000 00:00:06.999		NULL	NULL	NULL	NULL	6742992
16366586 PD22 Valves		S	PH-VS-APP02	500 DSC	TRUE	TRUE	5/7/2021 4:06:36 5/6/2021 18:06:36		06:41.6 000 00:00:06.005		NULL	NULL	NULL	NULL	6742995
16366587 PD02 Valves		Š	PH-VS-APP02	500 DSC	TRUE	TRUE	5/7/2021 4:07:06 5/6/2021 18:07:06		07:11.3 000 00:00:04.996		NULL	NULL	NULL	NULL	6743000
16366588 PD22 Valves		S	PH-VS-APP02	500 DSC	TRUE	TRUE	5/7/2021 4:07:30 5/6/2021 18:07:31		07:36.6 000 00:00:05.999		NULL	NULL	NULL	NULL	6743003
16366589 PD02 Valves		· ·	PH-VS-APP02	500 DSC	TRUE	TRUE	5/7/2021 4:07:31 5/6/2021 18:07:31		07:36.3 000 00:00:05.003		NULL	NULL	NULL	NULL	6743004
16366590 PD02 Valves		c	PH-VS-APP02	500 DSC	TRUE	TRUE	5/7/2021 4:08:13 5/6/2021 18:08:13		08:21.3 000 00:00:08.006		NULL.	NULL	NULL	NULL.	6743013
16366591 PD02_Valves		c	PH-VS-APP02	500 DSC	TRUE	TRUE	5/7/2021 4:08:19 5/6/2021 18:08:19		08:26.3 000 00:00:05.712		PH-WS-HMI02	NULL	NULL	NULL	6743014
16366592 PD02 Valves		S	PH-VS-APP02	500 DSC	TRUE	TRUE	5/7/2021 4:08:44 5/6/2021 18:08:44		08:51.3 000 00:00:06.996		NULL	NULL	NULL	NULL	6743019
16366593 PD02_Valves			PH-VS-APP02	500 DSC	TRUE	TRUE	5/7/2021 4:09:26 5/6/2021 18:09:26		09:31.3 000 00:00:04.993		NULL	NULL	NULL	NULL	6743022
16366594 PD02_Valves			PH-VS-APP02	500 DSC	TRUE	TRUE	5/7/2021 4:10:12 5/6/2021 18:10:12		10:21.3 000 00:00:09.004		NULL	NULL NULL	NULL	NULL	6743025
16366595 PD02_Valves			PH-VS-APP02	500 DSC	TRUE	TRUE	5/7/2021 4:11:04 5/6/2021 18:11:04		11:11.3 000 00:00:06.998		NULL	NULL	NULL	NULL	6743028
16366596 PD02_Valves			PH-VS-APP02	500 DSC	TRUE	TRUE	5/7/2021 4:12:18 5/6/2021 18:12:18		12:26.2 000 00:00:07.999		NULL.	NULL	NULL	NULL.	6743031
16366597 PD02_Valves		S	PH-VS-APP02	500 DSC	TRUE	TRUE	5/7/20214:12:18 5/6/202118:12:24		12:31.2 000 00:00:07.003		NULL	NULL	NULL.	NULL	6743032
16366598 Evolution			PH-VS-APPO1	1 DSC	TRUE	TRUE	5/7/2021 4:12:58 5/6/2021 18:12:58		17:57.8 NULL	DefaultUser	NULL	NULL	NULL	NULL	6743032
16366599 PD02 Valves		5	PH-VS-APP02	500 DSC	TRUE	TRUE	5/7/2021 4:13:00 5/6/2021 18:13:00		13:06.2 000 00:00:05.995		NULL	NULL.	NULL	NULL	6743040
16366600 PD02_Valves			PH-VS-APP02	500 DSC	TRUE	TRUE	5/7/2021 4:13:19 5/6/2021 18:13:19		13:26.2 000 00:00:06.998		NULL	NULL NULL	NULL	NO.D.I	6743043
16366601 PD22 Pumps		S	PH-VS-APP01	500 DSC	TRUE	TRUE			16:27.7 NULL	NULL	NULL	NULL	NULL	(b) (3) (A) Status: Off, LOR: Remote	6743048
16366602 PD18 Pumps		5	PH-VS-APPOI	500 DSC	TRUE	TRUE	5/7/2021 4:16:27 5/6/2021 18:16:27 5/7/2021 4:16:40 5/6/2021 18:16:40		16:40.6 NULL	NULL.	NULL	NULL	NULL	(b) (3) (A) status: Off-Cooling 19 sec. I,OR: Remote	6743050
		S												the state of the s	
16366603 PD22_Valves 16366604 PD22 Valves		5	PH-VS-APP02	500 DSC	TRUE	TRUE	5/7/2021 4:19:55 5/6/2021 18:19:55		20:01.5 000 00:00:05.979		NULL	NULL	NULL	NULL	6743054 6743057
		S	PH-VS-APP02	500 DSC	TRUE		5/7/2021 4:20:02 5/6/2021 18:20:02		20:11.5 000 00:00:09.004		NULL	NULL	NULL	NULL	
16366605 PD22_Valves		3	PH-VS-APP02	500 DSC	TRUE	TRUE	5/7/2021 4:20:10 5/6/2021 18:20:10		20:16.5 000 00:00:05.995		NULL	NULL.	NULL	NULL	6743058
16366606 PD22_Valves		5	PH-VS-APP02	500 DSC	TRUE	TRUE	5/7/2021 4:20:29 5/6/2021 18:20:29		20:36.5 000 00:00:06.983		NULL	NULL	NULL	NULL	6743063
16366607 PD22_Valves		S	PH-VS-APP02	500 DSC	TRUE	TRUE	5/7/2021 4:23:25 5/6/2021 18:23:25		23:31.5 000 00:00:06.021		NULL	NULL	NULL	NULL	6743066
16366608 PD08_Valves		5	PH-VS-APP02	500 DSC	TRUE	TRUE	5/7/2021 4:24:09 5/6/2021 18:24:09		24:16.2 000 00:00:06.977		NUU.	NULL	NULL.	NULL	6743069
16366609 PD09_Valves		S	PH-VS-APP02	500 DSC	TRUE	TRUE	5/7/2021 4:24:16 5/6/2021 18:24:16		24:21.3 000 00:00:05.034		NULL	NULL	NULL.	NULL	6743072
16366610 PD22_Valves		5	PH-VS-APP02	500 DSC	TRUE	TRUE	5/7/2021 4:24:19 5/6/2021 18:24:19		24:26.4 000 00:00:07.008		NULL	NULL	NULL	(b) (B) (A) Network Channel A Failed	6743073
16366613 PD11_Valves		S	PH-VS-APP02	250 DSC	Alarm	Alarm	5/7/2021 4:24:58 5/6/2021 18:24:58		25:48.3 NULL	NULL	NULL	NULL.	NULL		6743084
16366611 PD08_Valves		5	PH-VS-APP02	500 DSC	TRUE	TRUE	5/7/2021 4:25:07 5/6/2021 18:25:07		25:16.2 000 00:00:09.002		NULL	NULL	NULL	NULL	6743078
16366612 PD09_Valves		S	PH-VS-APP02	500 DSC	TRUE	TRUE	5/7/2021 4:25:09 5/6/2021 18:25:09	25:16.3	25:16.3 000 00:00:07.009	NOLL	NULL	NULL	NULL	NULL	6743079

iii. Data Export

ime Tag Name	Server	Value Qualit
5/6/2021 17:15:00 / 6 \ / 6 \ / 6	PH-VS-SQL	4 Good
$_{5/6/2021}^{5/6/2021}_{17:15:00}$ (b) (3) (A	PH-VS-SQL	2 Good
5/6/2021 17:15:00	PH-VS-SQL	107 Good
5/6/2021 17:15:00	PH-VS-SQL	213092 Good
5/6/2021 17:15:00	PH-VS-SQL	272297 Good
5/6/2021 17:15:00	PH-VS-SQL	1233 Good
5/6/2021 17:15:03	PH-VS-SQL	213092 Good
5/6/2021 17:15:03	PH-VS-SQL	1231 Good
5/6/2021 17:15:08	PH-VS-SQL	137 Good
5/6/2021 17:15:14	PH-VS-SQL	1233 Good
5/6/2021 17:15:19	PH-VS-SQL	106 Good
5/6/2021 17:15:20	PH-VS-SQL	110 Good
5/6/2021 17:15:27	PH-VS-SQL	136 Good
5/6/2021 17:15:33	PH-VS-SQL	213092 Good
5/6/2021 17:15:33	PH-VS-SQL	1227 Good
5/6/2021 17:15:38	PH-VS-SQL	107 Good
5/6/2021 17:15:39	PH-VS-SQL	109 Good
5/6/2021 17:15:40	PH-VS-SQL	112 Good
5/6/2021 17:15:43	PH-VS-SQL	1239 Good
5/6/2021 17:15:44	PH-VS-SQL	272297 Good
5/6/2021 17:15:48	PH-VS-SQL	135 Good
5/6/2021 17:15:53	PH-VS-SQL	213092 Good
5/6/2021 17:15:53	PH-VS-SQL	1232 Good
5/6/2021 17:15:57	PH-VS-SQL	108 Good
5/6/2021 17:15:58	PH-VS-SQL	108 Good
5/6/2021 17:15:59	PH-VS-SQL	110 Good
5/6/2021 17:16:03	PH-VS-SQL	1235 Good
5/6/2021 17:16:07	PH-VS-SQL	135 Good
5/5/2021 17:16:14	PH-VS-SQL	1238 Good
5/6/2021 17:16:17	PH-VS-SQL	109 Good
5/6/2021 17:16:18	PH-VS-SQL	109 Good
5/5/2021 17:16:19	PH-VS-SQL	111 Good
5/6/2021 17:16:23	PH-VS-SQL	213092 Good
5/6/2021 17:16:23	PH-VS-SQL	1231 Good
5/6/2021 17:16:27	PH-VS-SQL	134 Good
5/6/2021 17:16:33	PH-VS-SQL	1234 Good
5/6/2021 17:16:36	PH-VS-SQL	109 Good
5/6/2021 17:16:38	PH-VS-SQL	110 Good
5/6/2021 17:16:39	PH-VS-SQL	112 Good
5/6/2021 17:16:35	PH-VS-SQL	1233 Good
5/6/2021 17:16:46	PH-VS-SQL	133 Good
5/6/2021 17:16:46 5/6/2021 17:16:53	PH-VS-SQL	1236 Good
5/6/2021 17:16:56 5/6/2021 17:16:56	PH-VS-SQL	1236 G000 110 Good
5/6/2021 17:16:56 5/6/2021 17:16:57	PH-VS-SQL	110 Good
	PH-VS-SQL PH-VS-SQL	110 Good 111 Good
5/6/2021 17:16:58 5/5/2021 17:47:62	PH-VS-SQL PH-VS-SQL	
5/6/2021 17:17:03	PH-V5-SQL	1239 Good

(b) (3) (A)		
5/6/2021 17:17:06	PH-VS-SQL	133 Good
5/6/2021 17:17:14	PH-VS-SQL	1235 Good
5/6/2021 17:17:16	PH-VS-SQL	110 Good
5/6/2021 17:17:17	PH-VS-SQL	111 Good
5/6/2021 17:17:18	PH-VS-SQL	113 Good
5/6/2021 17:17:23	PH-VS-SQL	1236 Good
5/6/2021 17:17:26	PH-VS-SQL	132 Good
5/6/2021 17:17:33	PH-VS-SQL	1230 Good
5/6/2021 17:17:37	PH-VS-SQL	111 Good
5/6/2021 17:17:38	PH-VS-SQL	113 Good
5/6/2021 17:17:44	PH-VS-SQL	1237 Good
5/6/2021 17:17:45	PH-VS-SQL	132 Good
5/6/2021 17:17:53	PH-VS-SQL	1230 Good
5/6/2021 17:17:55	PH-VS-SQL	111 Good
5/6/2021 17:17:56	PH-VS-SQL	112 Good
5/6/2021 17:17:57	PH-VS-SQL	112 Good
5/6/2021 17:18:03	PH-VS-SQL	1236 Good
5/6/2021 17:18:05	PH-VS-SQL	131 Good
5/6/2021 17:18:13	PH-VS-SQL	213092 Good
5/6/2021 17:18:15	PH-VS-SQL	112 Good
5/6/2021 17:18:16	PH-VS-SQL	112 Good
5/6/2021 17:18:17	PH-VS-SQL	114 Good
5/6/2021 17:18:23	PH-VS-SQL	1239 Good
5/6/2021 17:18:24	PH-VS-SQL	272297 Good
5/6/2021 17:18:25	PH-VS-SQL	131 Good
5/6/2021 17:18:33	PH-VS-SQL	1235 Good
5/6/2021 17:18:34	PH-VS-SQL	112 Good
5/6/2021 17:18:35	PH-VS-SQL	113 Good
5/6/2021 17:18:36	PH-VS-SQL	113 Good
5/6/2021 17:18:43	PH-VS-SQL	1235 Good
5/6/2021 17:18:45	PH-VS-SQL	130 Good
5/6/2021 17:18:54	PH-VS-SQL	272297 Good
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5/6/2021 17:19:03	PH-VS-SQL	1232 Good
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5/6/2021 17:19:16	PH-VS-SQL	115 Good
5/6/2021 17:19:25	PH-VS-SQL	129 Good
5/6/2021 17:19:33	PH-VS-SQL	1235 Good
5/6/2021 17:19:34	PH-VS-SQL	114 Good
5/6/2021 17:19:35	PH-VS-SQL	114 Good
5/6/2021 17:19:43	PH-VS-SQL	1233 Good
5/6/2021 17:19:44	PH-VS-SQL	272297 Good
P	age 2	

(b) (3) (A)	
5/6/2021 17:19:45	PH-VS-SQL	129 Good
5/6/2021 17:19:53	PH-VS-SQL	114 Good
5/6/2021 17:19:53	PH-VS-SQL	1236 Good
5/6/2021 17:19:54	PH-VS-SQL	114 Good
5/6/2021 17:19:55	PH-VS-SQL	115 Good
5/6/2021 17:20:03	PH-VS-SQL	129 Good
5/6/2021 17:20:03	PH-VS-SQL	1235 Good
5/6/2021 17:20:12	PH-VS-SQL	115 Good
5/6/2021 17:20:14	PH-VS-SQL	1234 Good
5/6/2021 17:20:14	PH-VS-SQL	272297 Good
5/6/2021 17:20:14	PH-VS-SQL	115 Good
5/6/2021 17:20:15	PH-VS-SQL	116 Good
5/6/2021 17:20:23	PH-VS-SQL	128 Good
5/6/2021 17:20:23	PH-VS-SQL	1237 Good
5/6/2021 17:20:33	PH-VS-SQL	115 Good
5/6/2021 17:20:33	PH-VS-SQL	1236 Good
5/6/2021 17:20:34	PH-VS-SQL	115 Good
5/6/2021 17:20:42	PH-VS-SQL	128 Good
5/6/2021 17:20:43	PH-VS-SQL	272297 Good
5/6/2021 17:20:53	PH-VS-SQL	115 Good
5/6/2021 17:20:53	PH-VS-SQL	1234 Good
5/6/2021 17:20:54	PH-VS-SQL	116 Good
5/6/2021 17:21:02	PH-VS-SQL	128 Good
5/6/2021 17:21:03	PH-VS-SQL	1233 Good
5/6/2021 17:21:03	PH-VS-SQL	272297 Good
5/6/2021 17:21:12	PH-VS-SQL	115 Good
5/6/2021 17:21:13	PH-VS-SQL	115 Good
5/6/2021 17:21:14	PH-VS-SQL	1232 Good
5/6/2021 17:21:22	PH-VS-SQL	127 Good
5/6/2021 17:21:32	PH-VS-SQL	116 Good
5/6/2021 17:21:33	PH-VS-SQL	116 Good
5/6/2021 17:21:33	PH-VS-SQL	1234 Good
5/6/2021 17:21:33	PH-VS-SQL	272297 Good
5/6/2021 17:21:41	PH-VS-SQL	127 Good
5/6/2021 17:21:44	PH-VS-SQL	1236 Good
5/6/2021 17:21:52	PH-VS-SQL	116 Good
5/6/2021 17:21:53	PH-VS-SQL	116 Good
5/6/2021 17:21:53	PH-VS-SQL	1235 Good
5/6/2021 17:22:01	PH-VS-SQL	126 Good
5/6/2021 17:22:03	PH-VS-SQL	1235 Good
5/6/2021 17:22:03	PH-VS-SQL	272297 Good
5/6/2021 17:22:11	PH-VS-SQL	116 Good
5/6/2021 17:22:12	PH-VS-SQL	116 Good
5/6/2021 17:22:13	PH-VS-SQL	1234 Good
5/6/2021 17:22:22	PH-VS-SQL	126 Good
5/6/2021 17:22:23	PH-VS-SQL PH-VS-SQL	1233 Good
5/6/2021 17:22:31	PH-V5-SQL	116 Good

(b) (3) (<i>i</i>		
5/6/2021 17:22:32	PH-VS-SQL	117 Ga
5/6/2021 17:22:33	PH-VS-SQL	1235 G
5/6/2021 17:22:33	PH-VS-SQL	272297 G
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5/6/2021 17:22:44	PH-VS-SQL	1233 G
5/6/2021 17:22:51	PH-VS-SQL	1255 GC
5/6/2021 17:22:52	PH-VS-SQL	117 G
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5/6/2021 17:22:35	PH-VS-SQL	1254 G
5/6/2021 17:23:03	PH-VS-SQL	1235 G
5/6/2021 17:23:10	PH-VS-SQL	118 G
5/6/2021 17:23:10	PH-VS-SQL	117 G
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	PH-VS-SQL PH-VS-SQL	272297 G
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5/6/2021 17:23:30	PH-VS-SQL	117 Go
5/6/2021 17:23:31 5/6/2021 17:23:33	PH-VS-SQL PH-VS-SQL	1234 G
5/6/2021 17:23:33	PH-VS-SQL PH-VS-SQL	1254 G
	PH-VS-SQL PH-VS-SQL	213092 G
5/6/2021 17:23:44	PH-VS-SQL PH-VS-SQL	1234 G
5/6/2021 17:23:44	PH-VS-SQL PH-VS-SQL	1234 G
5/6/2021 17:23:50		
5/6/2021 17:23:51	PH-VS-SQL	117 Go
5/6/2021 17:23:53	PH-VS-SQL	1234 Go 272297 Go
5/6/2021 17:23:53	PH-VS-SQL	
5/6/2021 17:23:58	PH-VS-SQL	125 Gd
5/6/2021 17:24:03	PH-VS-SQL	1234 Go
5/6/2021 17:24:09	PH-VS-SQL	117 G
5/6/2021 17:24:10	PH-VS-SQL	117 G
5/6/2021 17:24:14	PH-VS-SQL	1234 G
5/6/2021 17:24:19	PH-VS-SQL	125 G
5/6/2021 17:24:23	PH-VS-SQL	1234 G
5/6/2021 17:24:24	PH-VS-SQL	272297 G
5/6/2021 17:24:29	PH-VS-SQL	118 G
5/6/2021 17:24:30	PH-VS-SQL	118 G
5/6/2021 17:24:33	PH-VS-SQL	1235 G
5/6/2021 17:24:38	PH-VS-SQL	125 G
5/6/2021 17:24:43	PH-VS-SQL	1234 G
5/6/2021 17:24:48	PH-VS-SQL	119 G
5/6/2021 17:24:49	PH-VS-SQL	118 G
5/6/2021 17:24:53	PH-VS-SQL	1234 G
5/6/2021 17:24:53	PH-VS-SQL	272297 G
5/6/2021 17:24:58	PH-VS-SQL	125 G
5/6/2021 17:25:03	PH-VS-SQL	1234 G
5/6/2021 17:25:08	PH-VS-SQL	118 G
5/6/2021 17:25:09	PH-VS-SQL	118 G
5/6/2021 17:25:14	PH-VS-SQL	1234 G

(b) (3)		
5/6/2021 17:25:14	PH-VS-SQL	110 Goo
5/6/2021 17:25:23	PH-VS-SQL	1235 Goo
5/6/2021 17:25:28	PH-VS-SQL	131 Goo
5/6/2021 17:25:29	PH-VS-SQL	130 Goo
5/6/2021 17:25:33	PH-VS-SQL	1237 Goo
5/6/2021 17:25:37	PH-VS-SQL	112 Goo
5/6/2021 17:25:43	PH-VS-SQL	1237 Goo
5/6/2021 17:25:47	PH-VS-SQL	128 Goo
5/6/2021 17:25:48	PH-VS-SQL	127 Goo
5/6/2021 17:25:53	PH-VS-SQL	1237 Goo
5/6/2021 17:25:54	PH-VS-SQL	115 Goo
5/6/2021 17:26:03	PH-VS-SQL	1239 Goo
5/6/2021 17:26:07	PH-VS-SQL	127 Goo
5/6/2021 17:26:08	PH-VS-SQL	126 Goo
5/6/2021 17:26:14	PH-VS-SQL	272297 Goo
5/6/2021 17:26:15	PH-VS-SQL	116 Goo
5/6/2021 17:26:23	PH-VS-SQL	1241 Goo
5/6/2021 17:26:27	PH-VS-SQL	125 Goo
5/6/2021 17:26:28	PH-VS-SQL	124 Goo
5/6/2021 17:26:33	PH-VS-SQL	1242 Goo
5/6/2021 17:26:36	PH-VS-SQL	117 Goo
5/6/2021 17:26:43	PH-VS-SQL	1243 Goo
5/6/2021 17:26:44	PH-VS-SQL	125 Goo
5/6/2021 17:26:46	PH-VS-SQL	124 Goo
5/6/2021 17:26:47	PH-VS-SQL	123 Goo
5/6/2021 17:26:53	PH-VS-SQL	213092 Goo
5/6/2021 17:26:53	PH-VS-SQL	1244 Goo
5/6/2021 17:26:54	PH-VS-SQL	117 Goo
5/6/2021 17:27:03	PH-VS-SQL	1245 Goo
5/6/2021 17:27:04	PH-VS-SQL	272297 Goo
5/6/2021 17:27:04	PH-VS-SQL	124 Goo
5/6/2021 17:27:06	PH-VS-SQL	123 Goo
5/6/2021 17:27:07	PH-VS-SQL	123 Goo
5/6/2021 17:27:13	PH-VS-SQL	213092 Goo
5/6/2021 17:27:13	PH-VS-SQL	1246 Goo
5/6/2021 17:27:14	PH-VS-SQL	118 Goo
5/6/2021 17:27:20	PH-VS-SQL	123 Goo
5/6/2021 17:27:23	PH-VS-SQL	1247 Goo
5/6/2021 17:27:25	PH-VS-SQL	122 Goo
5/6/2021 17:27:26	PH-VS-SQL	122 Goo
5/6/2021 17:27:30	PH-VS-SQL	119 Goo
5/6/2021 17:27:43	PH-VS-SQL	1250 Goo
5/6/2021 17:27:44	PH-VS-SQL	123 Goo
5/6/2021 17:27:45	PH-VS-SQL	122 Goo
5/6/2021 17:27:46	PH-VS-SQL	122 Goo
5/6/2021 17:27:53	PH-VS-SQL	1251 Goo
5/6/2021 17:27:54	PH-VS-SQL	119 Goo

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	(b) (3) (<i>A</i>		
5/6/2021 17:28:02	() (-) (-)	PH-VS-SQL	123 God
5/6/2021 17:28:03		PH-VS-SQL	1250 God
5/6/2021 17:28:05		PH-VS-SQL	1230 Got
· · ·		PH-VS-SQL	121 God
5/6/2021 17:28:06 5/6/2021 17:28:13		PH-VS-SQL	
· · · .		888888888	120 God
5/6/2021 17:28:14		PH-VS-SQL	213092 God
5/6/2021 17:28:14		PH-VS-SQL	1254 Go
5/6/2021 17:28:22		PH-VS-SQL	122 Go
5/6/2021 17:28:23		PH-VS-SQL	1253 Go
5/6/2021 17:28:24		PH-VS-SQL	122 Go
5/6/2021 17:28:25		PH-VS-SQL	121 Go
5/6/2021 17:28:32		PH-VS-SQL	120 Go
5/6/2021 17:28:33		PH-VS-SQL	1255 Go
5/6/2021 17:28:39		PH-VS-SQL	122 Go
5/6/2021 17:28:43		PH-VS-SQL	1254 Go
5/6/2021 17:28:44		PH-VS-SQL	121 Go
5/6/2021 17:28:45		PH-VS-SQL	121 Go
5/6/2021 17:28:50		PH-VS-SQL	120 Go
5/6/2021 17:28:53		PH-VS-SQL	1256 Go
5/6/2021 17:28:58		PH-VS-SQL	122 Go
5/6/2021 17:29:03		PH-VS-SQL	213092 Go
5/6/2021 17:29:03		PH-VS-SQL	1256 Go
5/6/2021 17:29:04		PH-VS-SQL	122 Go
5/6/2021 17:29:05		PH-VS-SQL	121 Go
5/6/2021 17:29:10		PH-VS-SQL	120 Go
5/6/2021 17:29:13		PH-VS-SQL	1258 Go
5/6/2021 17:29:22		PH-VS-SQL	122 Go
5/6/2021 17:29:23		PH-VS-SQL	121 Go
5/6/2021 17:29:23		PH-VS-SQL	1259 Go
5/6/2021 17:29:24		PH-VS-SQL	121 Go
5/6/2021 17:29:29		PH-VS-SQL	120 Go
5/6/2021 17:29:33		PH-VS-SQL	1261 Go
5/6/2021 17:29:41		PH-VS-SQL	122 Go
5/6/2021 17:29:43		PH-VS-SQL	122 Go
5/6/2021 17:29:43		PH-VS-SQL	1262 Go
5/6/2021 17:29:44		PH-VS-SQL	121 Go
5/6/2021 17:29:47		PH-VS-SQL	120 Go
5/6/2021 17:29:53		PH-VS-SQL	1264 Go
5/6/2021 17:29:54		PH-VS-SQL	272297 Go
5/6/2021 17:29:57		PH-VS-SQL	122 Go
5/6/2021 17:30:03		PH-VS-SQL	121 Go
5/6/2021 17:30:03		PH-VS-SQL	1264 Go
5/6/2021 17:30:04		PH-VS-SQL	121 Go
5/6/2021 17:30:08		PH-VS-SQL	120 Go
5/6/2021 17:30:13		PH-VS-SQL	213092 Go
5/6/2021 17:30:19		PH-VS-SQL	122 Go
5/6/2021 17:30:22		PH-VS-SQL	122 Go

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5/6/2021 17:30:23	PH-VS-SQL	1264 Goo
5/6/2021 17:30:23	PH-VS-SQL	272297 Goo
5/6/2021 17:30:27	PH-VS-SQL	120 Goo
5/6/2021 17:30:33	PH-VS-SQL	1264 Goo
5/6/2021 17:30:38	PH-VS-SQL	122 Goo
5/6/2021 17:30:42	PH-VS-SQL	121 Goo-
5/6/2021 17:30:43	PH-VS-SQL	121 Goo
5/6/2021 17:30:43	PH-VS-SQL	213092 Goo
5/6/2021 17:30:43	PH-VS-SQL	1270 Goo-
5/6/2021 17:30:52	PH-VS-SQL	120 Good
5/6/2021 17:30:53	PH-VS-SQL	1269 Good
5/6/2021 17:30:55	PH-VS-SQL	122 Good
5/6/2021 17:31:01	PH-VS-SQL	121 Goo
5/6/2021 17:31:02	PH-VS-SQL	121 Good
5/6/2021 17:31:03	PH-VS-SQL	1268 Good
5/6/2021 17:31:10	PH-VS-SQL	121 Goo
5/6/2021 17:31:13	PH-VS-SQL	213092 Good
5/6/2021 17:31:14	PH-VS-SQL	1273 Good
5/6/2021 17:31:14	PH-VS-SQL	272297 Good
5/6/2021 17:31:17	PH-VS-SQL	122 Good
5/6/2021 17:31:21	PH-VS-SQL	121 Good
5/6/2021 17:31:22	PH-VS-SQL	121 Goo
5/6/2021 17:31:23	PH-VS-SQL	1273 Goo-
5/6/2021 17:31:27	PH-VS-SQL	121 Good
5/6/2021 17:31:33	PH-VS-SQL	213092 Good
5/6/2021 17:31:33	PH-VS-SQL	1274 Good
5/6/2021 17:31:35	PH-VS-SQL	122 Good
5/6/2021 17:31:40	PH-VS-SQL	121 Goo
5/6/2021 17:31:42	PH-VS-SQL	121 Good
5/6/2021 17:31:43	PH-VS-SQL	122 Good
5/6/2021 17:31:43	PH-VS-SQL	1274 Goo
5/6/2021 17:31:44	PH-VS-SQL	272297 Good
5/6/2021 17:31:53	PH-VS-SQL	1275 Goo
5/6/2021 17:32:00	PH-VS-SQL	121 Good
5/6/2021 17:32:01	PH-VS-SQL	121 Good
5/6/2021 17:32:03	PH-VS-SQL	1278 Good
5/6/2021 17:32:07	PH-VS-SQL	122 Good
5/6/2021 17:32:14	PH-VS-SQL	1277 Goo
5/6/2021 17:32:14	PH-VS-SQL	272297 Goo
5/6/2021 17:32:18	PH-VS-SQL	121 Goo
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Į.	b) (3) (A)	
5/6/2021 17:32:33	PH-VS-SQL 272253	Go
5/6/2021 17:32:40	PH-VS-SQL 121	Go
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5/6/2021 17:32:43	PH-VS-SQL 1279	Go
5/6/2021 17:32:53	PH-VS-SQL 122	Go
5/6/2021 17:32:53	PH-VS-SQL 1278	Go
5/6/2021 17:32:54	PH-VS-SQL 120	Go
5/6/2021 17:32:59	PH-VS-SQL 121	Go
5/6/2021 17:33:00	PH-VS-SQL 121	Go
5/6/2021 17:33:03	PH-VS-SQL 1281	Go
5/6/2021 17:33:04	PH-VS-SQL 272250	Go
5/6/2021 17:33:12	PH-VS-SQL 122	Go
5/6/2021 17:33:14	PH-VS-SQL 1282	Go
5/6/2021 17:33:17	PH-VS-SQL 121	Go
5/6/2021 17:33:19		Go
5/6/2021 17:33:21		Go
5/6/2021 17:33:23	PH-VS-SQL 1285	
5/6/2021 17:33:26		Go
5/6/2021 17:33:33		Go
5/6/2021 17:33:33	PH-VS-SQL 1286	
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5/6/2021 17:33:42		Go
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5/6/2021 17:34:24	PH-VS-SQL 272244	
5/6/2021 17:34:33	PH-VS-SQL 1294	
5/6/2021 17:34:37		Go
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5/6/2021 17:34:43	PH-VS-SQL 213092	
5/6/2021 17:34:43	PH-VS-SQL 1290	
5/6/2021 17:34:43	PH-VS-SQL 1292	
5/6/2021 17:34:54	PH-VS-SQL 272245	
5/6/2021 17:34:57	PH-VS-SQL 56	Go

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5/6/2021 17:34:58	PH-VS-SQL 55	Good
5/6/2021 17:35:03	PH-VS-SQL 1294	Good
5/6/2021 17:35:13	PH-VS-SQL 213092	
5/6/2021 17:35:14	PH-VS-SQL 1297	Good
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5/6/2021 17:35:53	PH-VS-SQL 272243	
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5/6/2021 17:36:03		Goo
5/6/2021 17:36:03		Goo
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5/6/2021 17:36:14	PH-VS-SQL 272243	
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5/6/2021 17:37:44	PH-VS-SQL	272242 Goo
5/6/2021 17:37:53	PH-VS-SQL	213092 Goo
5/6/2021 17:37:53	PH-VS-SQL	1306 Goo
5/6/2021 17:37:54	PH-VS-SQL	31 Goo
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5/6/2021 17:37:57	PH-VS-SQL	31 Goo
5/6/2021 17:38:03	PH-VS-SQL	1302 Goo
5/6/2021 17:38:03	PH-VS-SQL	272242 Goo
5/6/2021 17:38:06	PH-VS-SQL	31 Goo
5/6/2021 17:38:13	PH-VS-SQL	31 Goo
5/6/2021 17:38:14	PH-VS-SQL	1307 Goo
5/6/2021 17:38:14	PH-VS-SQL	31 Goo
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5/6/2021 17:38:33	PH-VS-SQL	31 Goo
5/6/2021 17:38:33	PH-VS-SQL	1306 Goo
5/6/2021 17:38:33	PH-VS-SQL	272242 Goo
5/6/2021 17:38:34	PH-VS-SQL	31 Goo
5/6/2021 17:38:36	PH-VS-SQL	30 Goo
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5/6/2021 17:38:57	PH-VS-SQL	30 Goo
5/6/2021 17:39:02	PH-VS-SQL	31 Goo
5/6/2021 17:39:03	PH-VS-SQL	1310 Goo
5/6/2021 17:39:04	PH-VS-SQL	272241 Goo
5/6/2021 17:39:12	PH-VS-SQL	30 Goo
5/6/2021 17:39:13	PH-VS-SQL	31 Goo
5/6/2021 17:39:14	PH-VS-SQL	1311 Goo
5/6/2021 17:39:18	PH-VS-SQL	31 Goo
5/6/2021 17:39:23	PH-VS-SQL	1310 Goo
5/6/2021 17:39:27	PH-VS-SQL	30 Goo
5/6/2021 17:39:32	PH-VS-SQL	30 Goo
5/6/2021 17:39:33	PH-VS-SQL	30 Goo
5/6/2021 17:39:33	PH-VS-SQL	1309 Goo
5/6/2021 17:39:34	PH-VS-SQL	272241 Goo
5/6/2021 17:39:43	PH-VS-SQL	1309 Goo
5/6/2021 17:39:47	PH-VS-SQL	31 Goo
5/6/2021 17:39:50	PH-VS-SQL	30 Goo
5/6/2021 17:39:52	PH-VS-SQL	30 Goo
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	(b) (3) (A)	
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5/6/2021 17:40:44	PH-VS-SQL 1312	Good
5/6/2021 17:40:50	PH-VS-SQL 30	Good
5/6/2021 17:40:51	PH-VS-SQL 30	Good
5/6/2021 17:40:53	PH-VS-SQL 1316	Good
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5/6/2021 17:41:11	PH-VS-SQL 30	Good
5/6/2021 17:41:14	PH-VS-SQL 1314	Good
5/6/2021 17:41:19	PH-VS-SQL 30	Good
5/6/2021 17:41:23	PH-VS-SQL 1315	Good
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5/6/2021 17:41:50	PH-VS-SQL 31	Good
5/6/2021 17:41:53	PH-VS-SQL 213092	Good
5/6/2021 17:41:54	PH-VS-SQL 33	Good
5/6/2021 17:42:09	PH-VS-SQL 29	Good
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5/6/2021 17:42:44	PH-VS-SQL	272241 Good
5/6/2021 17:42:48	PH-VS-SQL	31 Good
5/6/2021 17:42:49	PH-VS-SQL	31 Good
5/6/2021 17:42:53	PH-VS-SQL	213092 Good
5/6/2021 17:42:53	PH-VS-SQL	1319 Good
5/6/2021 17:42:59	PH-VS-SQL	29 Good
5/6/2021 17:43:03	PH-VS-SQL	1316 Good
5/6/2021 17:43:08	PH-VS-SQL	32 Good
5/6/2021 17:43:09	PH-VS-SQL	31 Good
5/6/2021 17:43:12	PH-VS-SQL	31 Good
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5/6/2021 17:43:14	PH-VS-SQL	272241 Good
5/6/2021 17:43:17	PH-VS-SQL	29 Good
5/6/2021 17:43:24	PH-VS-SQL	1318 Good
5/6/2021 17:43:27	PH-VS-SQL	30 Good
5/6/2021 17:43:28	PH-VS-SQL	30 Good
5/6/2021 17:43:33	PH-VS-SQL	1315 Good
5/6/2021 17:43:34	PH-VS-SQL	272240 Good
5/6/2021 17:43:37	PH-VS-SQL	31 Good
5/6/2021 17:43:43	PH-VS-SQL	1315 Good
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5/6/2021 17:44:53	PH-VS-SQL	213092 Goo
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5/6/2021 17:45:03	PH-VS-SQL	1317 Goo
5/6/2021 17:45:03	PH-VS-SQL	272239 Goo
5/6/2021 17:45:06	PH-VS-SQL	30 Goo
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5/6/2021 17:45:23	PH-VS-SQL	1318 Goo
5/6/2021 17:45:23	PH-VS-SQL	272239 Goo
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/6/2021 18:06:53	PH-VS-SQL	30	Good
/6/2021 18:06:56	PH-VS-SQL	1331	Good
/6/2021 18:06:56	PH-VS-SQL	272238	Good
/6/2021 18:07:00	PH-VS-SQL	30	Good
/6/2021 18:07:01	PH-VS-SQL	30	Good
/6/2021 18:07:03	PH-VS-SQL	48	Good
/6/2021 18:07:06	PH-VS-SQL	1332	Good
/6/2021 18:07:07	PH-VS-SQL	29	Good
/6/2021 18:07:17	PH-VS-SQL	272237	Good
/6/2021 18:07:20	PH-VS-SQL	16	Good
/6/2021 18:07:20	PH-VS-SQL	32	Good
/6/2021 18:07:21	PH-VS-SQL	33	Good
/6/2021 18:07:23	PH-VS-SQL	12	Good
/6/2021 18:07:26	PH-VS-SQL	1333	Good
/6/2021 18:07:26	PH-VS-SQL	272237	Good
/6/2021 18:07:26	PH-VS-SQL	37	Good
/6/2021 18:07:30	PH-VS-SQL	0	Good
/6/2021 18:07:36	PH-VS-SQL	1333	Good
, /6/2021 18:07:36	PH-VS-SQL	272237	Good
/6/2021 18:07:36	PH-VS-SQL	26	Good
/6/2021 18:07:39	PH-VS-SQL		Good

(D) (3) (A)		
5/6/2021 18:07:40	PH-VS-SQL	29	Good
5/6/2021 18:07:45	PH-VS-SQL	32	Good
5/6/2021 18:07:46	PH-VS-SQL	1333	Good
5/6/2021 18:07:46	PH-VS-SQL	272237	Good
5/6/2021 18:07:53	PH-VS-SQL	29	Good
5/6/2021 18:07:56	PH-VS-SQL	1334	Good
5/6/2021 18:07:56	PH-VS-SQL	272237	Good
5/6/2021 18:07:59	PH-VS-SQL	30	Good
5/6/2021 18:08:00	PH-VS-SQL	30	Good
5/6/2021 18:08:06	PH-VS-SQL	1333	Good
5/6/2021 18:08:06	PH-VS-SQL	29	Good
5/6/2021 18:08:06	PH-VS-SQL	272237	Good
5/6/2021 18:08:11	PH-VS-SQL	9	Good
5/6/2021 18:08:16	PH-VS-SQL	1334	Good
5/6/2021 18:08:16	PH-VS-SQL	31	Good
5/6/2021 18:08:18	PH-VS-SQL	0	Good
5/6/2021 18:08:19	PH-VS-SQL	30	Good
5/6/2021 18:08:20	PH-VS-SQL	30	Good
5/6/2021 18:08:25	PH-VS-SQL	29	Good
5/6/2021 18:08:26	PH-VS-SQL	213091	Good
5/6/2021 18:08:26	PH-VS-SQL	1333	
5/6/2021 18:08:33	PH-VS-SQL	30	Good
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5/6/2021 18:08:40	PH-VS-SQL		Good
5/6/2021 18:08:43	PH-VS-SQL		Good
5/6/2021 18:08:46	PH-VS-SQL	1334	
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5/6/2021 18:11:36	PH-VS-SQL 44	Goo
5/6/2021 18:11:45	PH-VS-SQL 91	Goo
5/6/2021 18:11:46	PH-VS-SQL 1334	Goo
5/6/2021 18:11:55	PH-VS-SQL 52	Goo
5/6/2021 18:11:56	PH-VS-SQL 1334	Goo
5/6/2021 18:11:56	PH-VS-SQL 60	Goo
5/6/2021 18:12:04	PH-VS-SQL 85	Goo
5/6/2021 18:12:06	PH-VS-SQL 213092	Goo
5/6/2021 18:12:06	PH-VS-SQL 1333	Goo
5/6/2021 18:12:13	PH-VS-SQL 54	Goo
5/6/2021 18:12:14	PH-VS-SQL 57	Goo
5/6/2021 18:12:15	PH-VS-SQL 63	Goo
5/6/2021 18:12:16	PH-VS-SQL 1334	Goo
5/6/2021 18:12:18	PH-VS-SQL 94	Goo
5/6/2021 18:12:21	PH-VS-SQL 80	Goo
5/6/2021 18:12:24	PH-VS-SQL 98	Goo
5/6/2021 18:12:26	PH-VS-SQL 1333	Goo
5/6/2021 18:12:31	PH-VS-SQL 87	Goo
5/6/2021 18:12:31	PH-VS-SQL 59	Goo
5/6/2021 18:12:33	PH-VS-SQL 6	Goo
5/6/2021 18:12:34	PH-VS-SQL 7	Goo
5/6/2021 18:12:35	PH-VS-SQL 79	Goo
5/6/2021 18:12:35	PH-VS-SQL 51	Goo
5/6/2021 18:12:35	PH-VS-SQL 12	Goo
5/6/2021 18:12:36	PH-VS-SQL 213092	Goo
5/6/2021 18:12:36	PH-VS-SQL 1333	Goo
5/6/2021 18:12:42	PH-VS-SQL 82	Goo
5/6/2021 18:12:46	PH-VS-SQL 1333	Goo
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5/6/2021 18:12:56	PH-VS-SQL 1333	Goo
5/6/2021 18:12:57		Goo
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5/6/2021 18:13:02		Goo
5/6/2021 18:13:06	PH-VS-SQL 1333	
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	(b) (3) (A)	
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5/6/2021 18:13:26	PH-VS-SQL 212619	Go
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5/6/2021 18:13:26	PH-VS-SQL 272237	Go
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5/6/2021 18:13:33	PH-VS-SQL 19	Go
5/6/2021 18:13:34	PH-VS-SQL 27	Go
5/6/2021 18:13:36	PH-VS-SQL 1334	Go
5/6/2021 18:13:41	PH-VS-SQL 74	Go
5/6/2021 18:13:46	PH-VS-SQL 1333	Go
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5/6/2021 18:13:56	PH-VS-SQL 212621	
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5/6/2021 18:15:27	PH-VS-SQL 24	Go

	b) (3) (A)	
5/6/2021 18:15:31	PH-VS-SQL 36	Good
5/6/2021 18:15:32	PH-VS-SQL 42	Good
5/6/2021 18:15:36	PH-VS-SQL 1333	Good
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5/6/2021 18:15:46	PH-VS-SQL 212616	Good
5/6/2021 18:15:46	PH-VS-SQL 1333	Good
5/6/2021 18:15:47	PH-VS-SQL 25	Good
5/6/2021 18:15:50	PH-VS-SQL 34	Good
5/6/2021 18:15:51	PH-VS-SQL 39	Good
5/6/2021 18:15:56	PH-VS-SQL 1334	Goo
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5/6/2021 18:15:57	PH-VS-SQL 60	Good
5/6/2021 18:16:06	PH-VS-SQL 212616	Good
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5/6/2021 18:16:06	PH-VS-SQL 27	Good
5/6/2021 18:16:10	PH-VS-SQL 38	Good
5/6/2021 18:16:11	PH-VS-SQL 42	Good
5/6/2021 18:16:16	PH-VS-SQL 59	Good
5/6/2021 18:16:17	PH-VS-SQL 1333	Goo
5/6/2021 18:16:17	PH-VS-SQL 272237	Good
5/6/2021 18:16:26	PH-VS-SQL 1333	Good
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5/6/2021 18:16:29	PH-VS-SQL 36	Goo
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5/6/2021 18:16:56	PH-VS-SQL 272237	Goo
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(b) (3)		
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5/6/2021 18:19:57	PH-VS-SQL	212616 God
5/6/2021 18:19:57	PH-VS-SQL	1333 God
5/6/2021 18:20:00	PH-VS-SQL	37 God
5/6/2021 18:20:05	PH-VS-SQL	43 God
5/6/2021 18:20:06	PH-VS-SQL	45 God
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5/6/2021 18:20:07	PH-VS-SQL	1333 God
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5/6/2021 18:20:17	PH-VS-SQL	212616 God
5/6/2021 18:20:19	PH-VS-SQL	37 God
5/6/2021 18:20:25	PH-VS-SQL	44 God
5/6/2021 18:20:26	PH-VS-SQL	46 God
5/6/2021 18:20:27	PH-VS-SQL	1334 God
5/6/2021 18:20:28	PH-VS-SQL	49 Go
5/6/2021 18:20:37	PH-VS-SQL	212616 God
5/6/2021 18:20:39	PH-VS-SQL	38 God
5/6/2021 18:20:45	PH-VS-SQL	45 God
5/6/2021 18:20:46	PH-VS-SQL	46 God
5/6/2021 18:20:49	PH-VS-SQL	49 God
5/6/2021 18:20:57	PH-VS-SQL	212616 God
5/6/2021 18:20:57	PH-VS-SQL	1333 God
5/6/2021 18:20:58	PH-VS-SQL	38 God
5/6/2021 18:21:04	PH-VS-SQL	44 Go
5/6/2021 18:21:05	PH-VS-SQL	45 God
5/6/2021 18:21:07	PH-VS-SQL	1333 God
5/6/2021 18:21:09	PH-VS-SQL	48 God
5/6/2021 18:21:17	PH-VS-SQL	212616 God
5/6/2021 18:21:17	PH-VS-SQL	1333 God
5/6/2021 18:21:18	PH-VS-SQL	39 Go
5/6/2021 18:21:24	PH-VS-SQL	45 God
5/6/2021 18:21:25	PH-VS-SQL	46 God
5/6/2021 18:21:27	PH-VS-SQL	1333 God
5/6/2021 18:21:28	PH-VS-SQL	48 God
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5/6/2021 18:21:47	PH-VS-SQL	1333 God
5/6/2021 18:21:47	PH-VS-SQL	272237 God
5/6/2021 18:21:48	PH-VS-SQL	47 God
5/6/2021 18:21:57	PH-VS-SQL	1334 God
5/6/2021 18:21:58	PH-VS-SQL	39 Go
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5/5/2021 18:22:04	PH-VS-SQL	46 God

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5/6/2021 18:22:07	PH-VS-SQL	212616 Go
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5/6/2021 18:22:17	PH-VS-SQL	1333 Gc
5/6/2021 18:22:17	PH-VS-SQL	40 Gc
5/6/2021 18:22:23	PH-VS-SQL	45 Gc
5/6/2021 18:22:24	PH-VS-SQL	45 Gc
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VII. REFERENCES AND CRITERIA

The following primary references and criteria documents have been utilized in the overall facility inspection and evaluation:

ASME B31.3	Process Piping, 2016 Edition
ASTM A53	Standard Specification for Pipe, Steel, Black and Hot-Dipped, Zinc-Coated, Welded and Seamless
NFPA 30	Flammable and Combustible Liquids Code
NFPA 750	Standard on Water Mist Fire Protection Systems
MIL-HDBK-1022	Petroleum Fuel Facilities (superseded by UFC 3-460-01 - Design: Petroleum Fuel Facilities)